

## Supplementary Information

# Benzene Adsorption: A Significant Inhibitor for the Hydrogen Oxidation Reaction in Alkaline Conditions

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## Methods

**Materials.** 0.1 M aqueous solutions of organic cations were prepared from TMAOH (25% in water, ACROS) and BTMAOH (40% in water, Sigma-Aldrich). 0.1 M NaOH solutions were made with NaOH pellets (99.99%, Alfa Aesar). 20 wt<sub>metal</sub>% Pt/C, Pt<sub>3</sub>Mo<sub>1</sub>/C, Pt<sub>1</sub>Ni<sub>1</sub>/C and Pt<sub>1</sub>Ru<sub>1</sub>/C were obtained from E-TEK. We used Pt<sub>3</sub>Mo<sub>1</sub> alloy catalyst instead of Pt<sub>1</sub>Mo<sub>1</sub> because the composition of Pt<sub>3</sub> to Mo<sub>1</sub> is known as most active for hydrogen oxidation.<sup>1</sup> The X-ray diffraction data indicates the bimetallic catalysts form an alloy structure (**Figure S3**). The catalyst inks were prepared by ultrasonically blending of 10 mg of the Pt or Pt alloy catalysts with 40  $\mu$ l of 5 wt% Nafion<sup>®</sup> suspension in alcohol (Solution Technology, Inc.) for 1 hour in 10 ml of de-ionized water (18.2 M $\Omega$  cm, Millipore) in an ice bath. Before RDE experiments, 20  $\mu$ l of the solution was deposited onto the 5.0 mm in diameter glassy carbon electrode, disk geometric area is 0.196 cm<sup>2</sup>, which was polished with 0.05  $\mu$ m alumina, resulting in a catalyst loading of 20  $\mu$ g<sub>metal</sub> cm<sup>-2</sup>.

**RDE measurement.** RDE measurements were performed using a CHI Electrochemical Station (Model 760D) in a standard three-electrode cell at a room temperature, 25  $\pm$  1  $^{\circ}$ C. A platinized Pt wire served as a counter electrode and a Hg/HgO (Radiometer Analytical Inc.) in 1.0 M KOH as a reference electrode for alkaline electrolytes and a Ag/AgCl (Bioanalytical Systems Inc.) in 3.0 M NaCl as a reference electrode for acidic electrolyte. All potentials initially measured vs. the Hg/HgO electrode (or Ag/AgCl electrode) were converted to a RHE scale by measuring HOR/HER currents on the Pt/C and the bimetallic catalysts in the same electrolyte, whereby the potential at zero current corresponds to 0.0 V vs. RHE. After the electrolytes were saturated with pure hydrogen, polarization plots were recorded between ca. - 0.1 and 1.2 V vs. RHE at a sweep rate of 5 mV s<sup>-1</sup> and rotation rate of 900 rpm. After the electrolytes were saturated with nitrogen, the cyclic voltammogram at 25  $^{\circ}$ C was recorded between 0.0 and 1.2 V vs. RHE at a scan rate of

20 mV s<sup>-1</sup> at 0 rpm. The RDE measurements were repeated 2-3 times independently to ensure the data reproducibility. Typical standard deviation is 5-10 % of the measured HOR current. The AC impedance was measured from 100 to 0.001 kHz with a voltage perturbation of 5 mV in the hydrogen saturated electrolytes at 0.1 V vs. RHE. We measured the impedance of the RDE in the organic cation solutions. **Figure S4** shows the impedance of Pt/C in 0.1 M TMAOH, BTMAOH, and NaOH. It was noted that the extrapolated high frequency resistance corresponding to the electrolyte resistance were similar, ca. 9.1, 7.5 and 8.2  $\Omega$ , for TMAOH, BTMAOH and NaOH, indicating that there is no significant pH effect on our experiments.

The HOR/HER charge transfer coefficient ( $\alpha$ ) and exchange current density ( $i_0$ ) for the catalysts were obtained by fitting the HOR/HER kinetic current densities to the Butler-Volmer equation. The exchange current density was normalized by geometric area of the electrode.

**Computational details.** The electronic structure calculations were performed using generalized gradient approximation (GGA) to density functional theory (DFT) with Perdew-Wang (PW91) exchange-correlation functional<sup>2,3</sup> and projector augmented-wave pseudopotentials<sup>4,5</sup> as implemented in Vienna Ab initio Software Package (VASP)<sup>6-9</sup>. Extended Pt(111), Pt<sub>3</sub>Mo<sub>1</sub>(111), Pt<sub>1</sub>Ni<sub>1</sub>(111), and Pt<sub>1</sub>Ru<sub>1</sub>(111) surfaces were modeled using super cells with the dimensions of 16.80  $\times$  16.80 Å, 16.91  $\times$  16.91 Å, 15.89  $\times$  15.89 Å and 16.48  $\times$  16.48 Å, respectively. These correspond to the unit cells of the size  $(3a\sqrt{2} \times 3b\sqrt{2})R\gamma$  where a, b, and  $\gamma$  are the cell parameters determined from the bulk calculations. In all the cases we modeled the system using three layers of metal atoms and a vacuum region of 20 Å. To simulate the effect of the bulk, the two top layers and the adsorbed species were allowed to relax until the convergence in energy was  $1 \times 10^{-5}$  eV while the bottom layers were held fixed. The electronic energies were calculated using 4 $\times$ 4 $\times$ 1 k-

point Monkhorst-Pack<sup>10</sup> mesh and Methfessel-Paxton smearing<sup>11</sup> of order 2 with a value of  $\sigma = 0.2$  to aid convergence. In all the cases, plane-wave basis cutoff was set to 400 eV. The change in the free energy during the adsorption was calculated as

$$\Delta rG = \Delta E_{\text{BTMA}} + \Delta \text{ZPE} + T\Delta S$$

where  $\Delta E_{\text{BTMA}}$ ,  $\Delta \text{ZPE}$ , and  $\Delta S$  are the change in the electronic energy, zero point energy, and entropy in the adsorption process. Adsorption energy was calculated using the following formula:

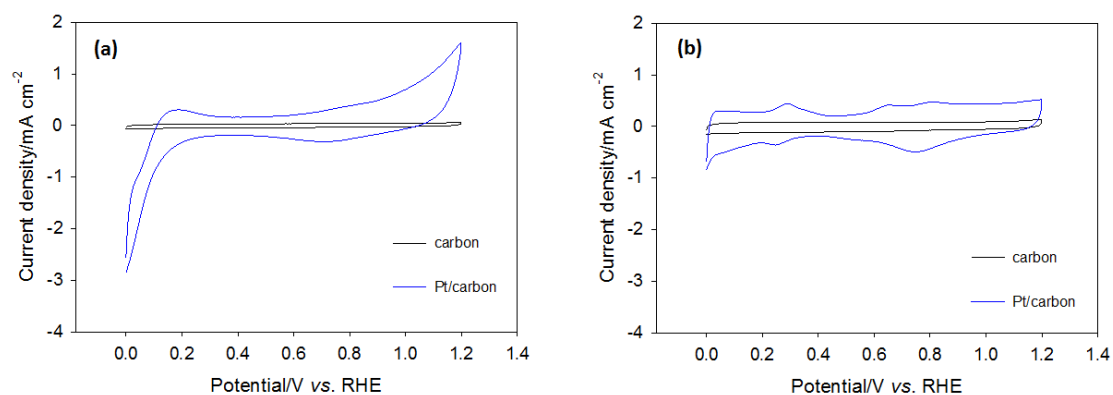
$$\Delta E_{\text{BTMA}} = E_{\text{surface+BTMA}} - [E_{\text{surface}} + E_{\text{BTMA}}]$$

where  $E_{\text{surface+BTMA}}$  is the energy of BTMA adsorbed on the Pt(111) or alloy surfaces,  $E_{\text{surface}}$  is the energy of the clean surface, and  $E_{\text{ad}}$  is the energy of BTMA in the gas phase. Zero point energies were calculated using the vibrational frequencies obtained from the normal mode analysis. Entropy of BTMA at  $T = 298$  K was calculated using B3LYP/6-31+G(d,p) level of theory and polarizable continuum model as implemented in Gaussian 09 quantum chemical package<sup>12</sup>. The calculations were carried out with the assumption that the change in the solvation of the large organic cations will not have a significant effect on the calculated free energies of adsorption. For the calculations of the local electric field effects on the adsorption energies of BTMA the binding energy was calculated as a function of applied electric field using

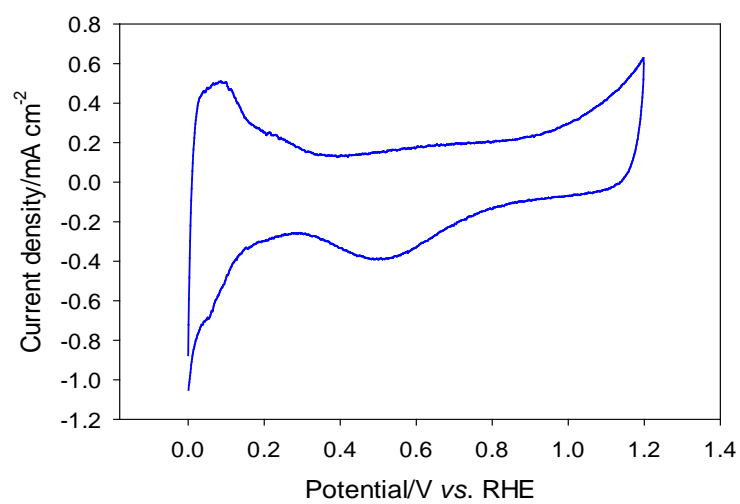
$$\Delta E_{\text{BTMA,field}} = E_{\text{surface+BTMA, field}} - [E_{\text{surface,field}} + E_{\text{BTMA}}]$$

where the same field is applied to the surface with and without adsorbed BTMA, but the isolated BTMA cation is in vacuum without a field.

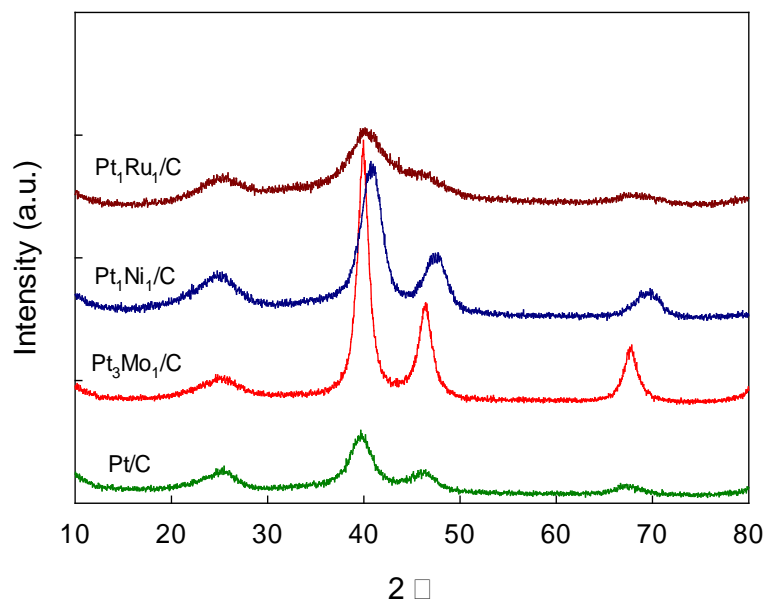
Charge transfer between the metal surfaces and BTMA in the orientation with the highest binding energy is obtained by analyzing the electronic charges calculated using Bader's analysis of charge densities.<sup>13-16</sup>



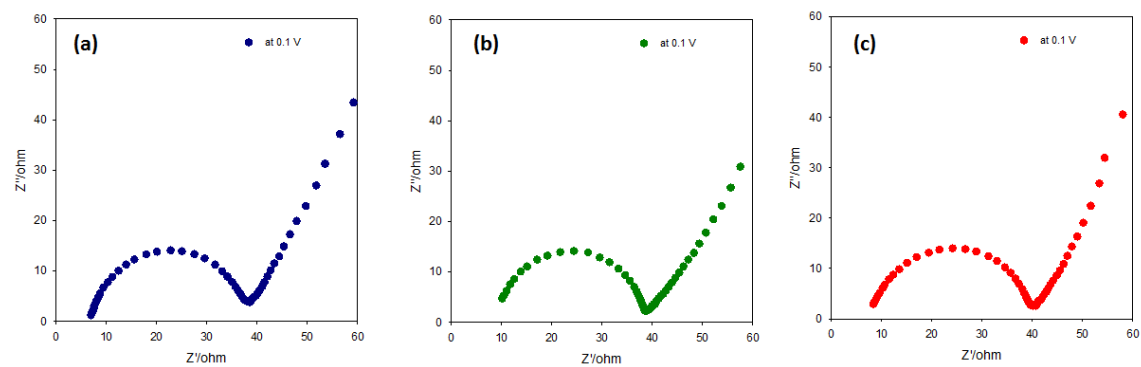
**Figure S1.** CV of carbon and Pt/C in 0.1 M (a) BTMAOH and (b) TMAOH solutions: the CVs were performed at 25 °C at a scan rate of  $20 \text{ mV s}^{-1}$  at 0 rpm.



**Figure S2.** CV of carbon-supported Pt<sub>1</sub>Ru<sub>1</sub>/C in 0.1 M NaOH; the CVs were performed at 25 °C at a scan rate of 20 mV s<sup>-1</sup> at 0 rpm.



**Figure S3.** XRD patterns of Pt/C, Pt<sub>3</sub>Mo<sub>1</sub>/C, Pt<sub>1</sub>Ni<sub>1</sub>/C, and Pt<sub>1</sub>Ru<sub>1</sub>/C. These XRD patterns show that all bimetallic catalysts are single phase alloys.



**Figure S4.** Impedance measured at 900 rpm at 0.1 V vs RHE with Pt/C catalyst in (a) BTMAOH, (b) TMAOH, and (c) NaOH.



**Table S1.** Adsorption energies for BTMA cation ( $\Delta E_{\text{BTMA}}$ ) in eV calculated using DFT with PW91 functional on Pt(111), Pt<sub>3</sub>Mo<sub>1</sub>(111), Pt<sub>1</sub>Ni<sub>1</sub>(111), and Pt<sub>1</sub>Ru<sub>1</sub>(111) surfaces.

orientation/ system	(1)	(2)	(3)	(4)
Pt	-2.30	-2.15	-1.52	-2.15
Pt <sub>3</sub> Mo <sub>1</sub>	-1.61	-1.67	-0.99	-1.71
Pt <sub>1</sub> Ni <sub>1</sub>	-1.45	-1.56	-0.47	-1.52
Pt <sub>1</sub> Ru <sub>1</sub>	-1.32	-1.42	-0.37	-1.39

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