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Table S1 Key variables for the design of moving bed heat exchanger and regenerator in baseline CFB cases

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Table S3 Process model validation of regeneration duty outputs and thermodynamic properties in an encapsulated solvent system

Notes: ^{a)} In FB configuration; ^{b)} At capsule permeability of 3260 barrer and capsule thickness of 10 μm ; ^{c)} Average value at the loading range and operating conditions used; ^{d)} at 60 °C

Table S1

Parameter	CFB No HI	CFB HI
Number of units of MBHE heater	0	8
Number of units of MBHE cooler	8	8
MBHE heater height (m)	n/a	9.9
MBHE heater length & width (m)	n/a	4.9
MBHE cooler height (m)	10.9	10.9
MBHE cooler length & width (m)	5.8	4.9
Overall heat transfer coefficient in the regenerator ($\text{W/m}^2\cdot\text{K}$)	304	
Recycled- CO_2 stream flowrate (% of stripped- CO_2 flowrate)	20	
Recycled- CO_2 stream superficial velocity (m/s)	0.1	
Tube diameter (m)	0.019	
Tube arrangement	Square	
Tube pitch	1.5	

Table S2

Properties	Relevant process units	Applicable Range	Reference source	Ref
Absorption enthalpy	Absorber, regenerator	Temperature = 40-120 °C	Empirical equation	1
Absorption rate	Absorber, regenerator	T = 40-120 °C Concentration = 1-30 %-wt.	Empirical equation	2
Equivalent CO ₂ partial pressure in solution	Absorber, regenerator	Loading = 0-1 mole/mole Concentration = 30 %-wt. Temperature = 25-120 °C	Empirical equation	1
Solution density	Absorber, regenerator, HE	Temperature = 40-120 °C	Experimental work	2
Solution heat capacity	Absorber, HE, regenerator	Temperature = 40-120 °C	Experimental work	3
Solution viscosity	Absorber, regenerator	Temperature = 40-120 °C	Experimental work	2
Water vapor pressure	Regenerator	T = 40-120 °C	Empirical equation	1

Table S3

Parameter	Input parameters	This paper	Output from reference
Sensible heat duty of Na ₂ CO ₃ 30 % ^a (MJ/kg CO _{2,c})	Loadings Concentration Temperature	0.85	0.84 ⁴
Water vaporization duty of Na ₂ CO ₃ 30 % ^a (MJ/kg CO _{2,c})	Loadings Concentration Temperature	0.13	0.13 ⁵
Mass transfer rate of membrane resistance ^b (kmole/m ² .s.Pa)	Permeability Thickness Capsule diameter	1.1x10 ⁻⁷	1.1x10 ⁻⁷ ⁵
Overall absorption rate of Na ₂ CO ₃ 30 % ^c (kmole/m ² .s.Pa)	Loadings Concentration Temperature	2.0x10 ⁻⁸	2.0x10 ⁻⁸ ⁵
Specific surface area for 500 µm capsule (m ² /m ³)	Capsule diameter Void fraction	7440	7440 ⁵
PCO ₂ at rich loading of MEA = 0.46 (kPa) ^d	Loadings Concentration Temperature	1.25	1.25 ¹
PCO ₂ at lean loading of MEA = 0.23 (kPa) ^d	Loadings Concentration Temperature	0.06	0.06 ¹
Average void fraction of fixed-bed	Void fraction	0.38	0.38 ⁶
Average void fraction of bubbling-bed	Void fraction	0.50	0.45-0.55 ⁶
Average void fraction of CFB	Void fraction	0.91	0.80-0.95 ⁶

Supplementary Reference

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