

## Supporting Information

### Zeolite-Templated Carbon Catalysts for Adsorption and Hydrolysis of Cellulose-Derived Long-Chain Glucans: Effect of Post-Synthetic Surface Functionalization

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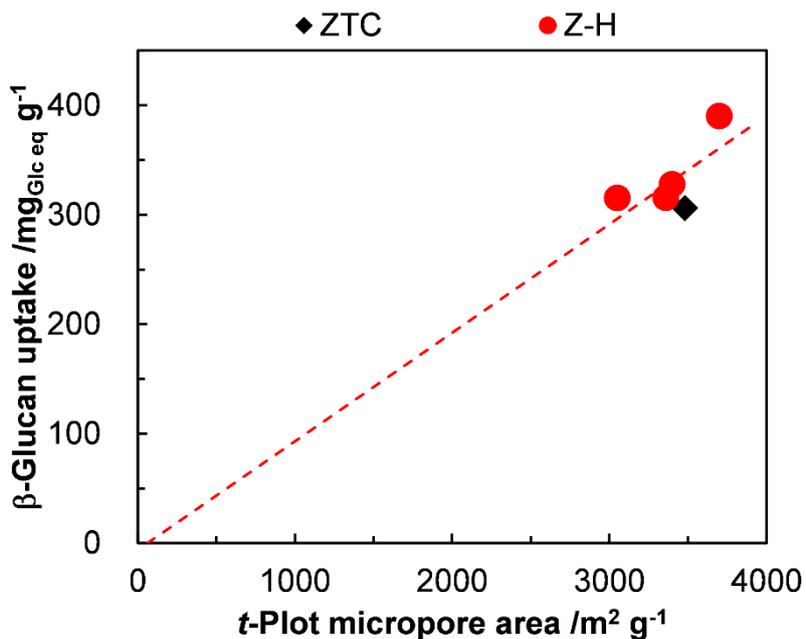
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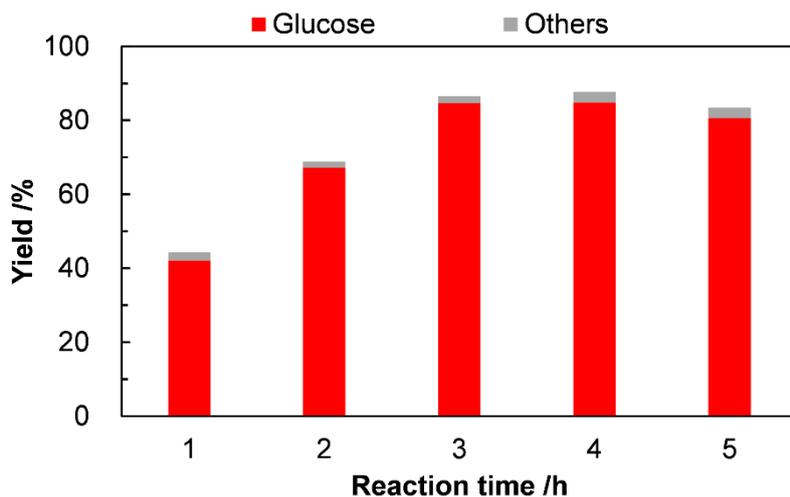
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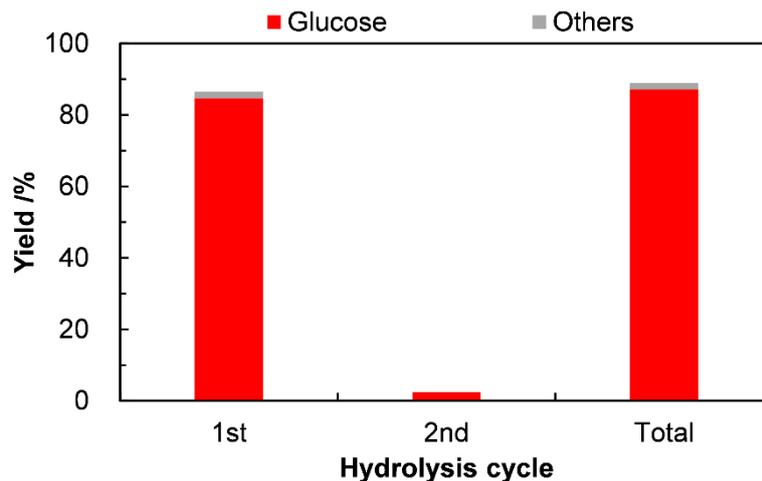


**Figure S1.**  $\beta$ -Glucan uptake of parent ZTC and Z-H materials as a function of  $t$ -plot micropore area.

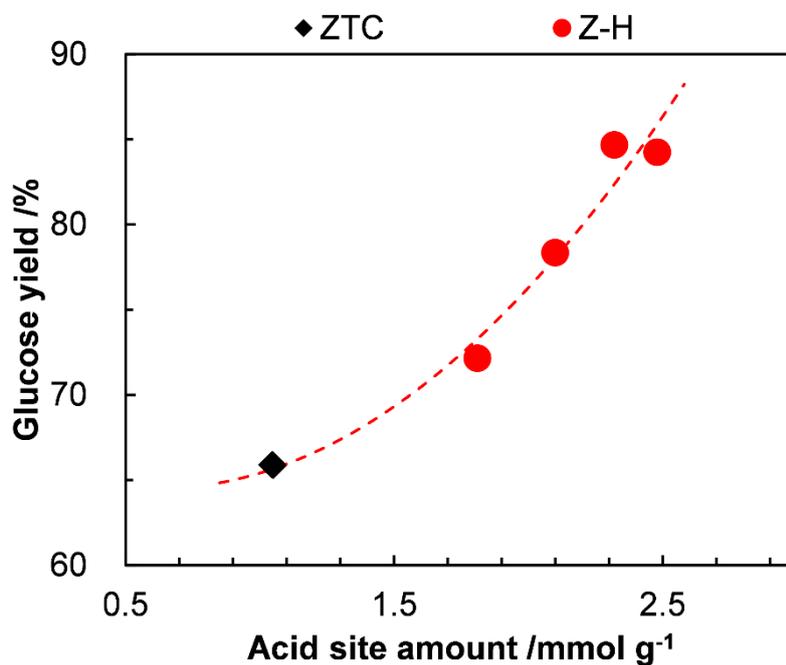
As demonstrated with Z-N(30) and Z-S(30) in Table 1, the narrow micropores of ZTC materials are unable to take  $\beta$ -glucan strands in, which results in a non-zero intercept in Figure S1. This trend is identical to non-zero intercepts in our previous studies consisting of mesoporous carbon nanoparticles as well as unfunctionalized ZTC materials.<sup>S1,S2</sup>



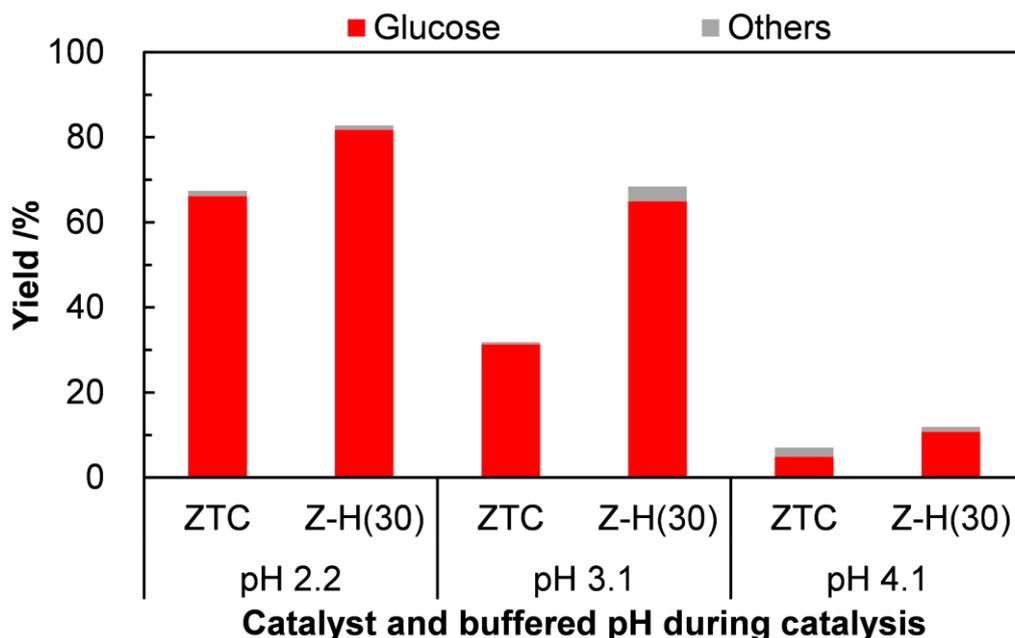
**Figure S2.** Effect of reaction time on adsorbed  $\beta$ -glucan hydrolysis on Z-H(30). *Others* include mannose, fructose, and HMF. Reaction conditions:  $\beta$ -glucan/Z-H(30) *ca.* 25 mg; water 1 mL; 453 K; 440 rpm.



**Figure S3.** Product yields in two cycles of adsorbed  $\beta$ -glucan hydrolysis on Z-H(30). *Others* include mannose, fructose, and HMF. In the second cycle, the residue consisting of unreacted  $\beta$ -glucan and Z-H(30) in the first run was employed without adding either fresh substrate or catalyst, and product yields were calculated on the basis of  $\beta$ -glucan amount in the first cycle. Reaction conditions:  $\beta$ -glucan/Z-H(30) *ca.* 25 mg; water 1 mL; 453 K; 3 h; 440 rpm.



**Figure S4.** Glucose yield in adsorbed  $\beta$ -glucan hydrolysis on parent ZTC and Z-H materials as a function of acid site amount. Reaction conditions:  $\beta$ -glucan/ZTC *ca.* 25 mg; water 1 mL; 453 K; 3 h; 440 rpm.



**Figure S5.** Adsorbed  $\beta$ -glucan hydrolysis on parent ZTC and Z-H(30) in buffer solutions. *Others* include mannose, fructose, and HMF. Reaction conditions:  $\beta$ -glucan/ZTC *ca.* 25 mg; solvent 1 mL; 453 K; 3 h; 440 rpm. The reactions at pH 2.2 and 3.1 were conducted in 20 mM of phosphate buffer and that at pH 4.1 was in 20 mM of acetate buffer.

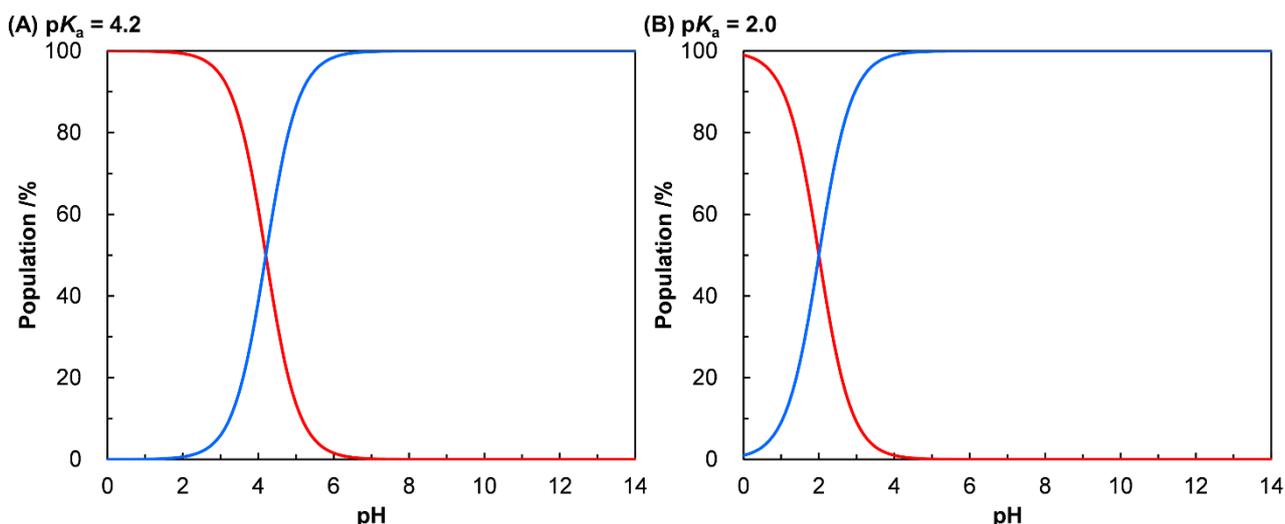
**Table S1.** pH Values After Adsorbed  $\beta$ -Glucan Hydrolysis on ZTC and Z-H(30)<sup>a</sup>

Catalyst	Reaction media	pH after reaction
ZTC	Water	2.4
	Acetate buffer <sup>b</sup>	3.9
	Phosphate buffer <sup>c</sup>	2.8
	Phosphate buffer <sup>d</sup>	2.5
Z-H(30)	Water	2.3
	Acetate buffer <sup>b</sup>	3.9
	Phosphate buffer <sup>c</sup>	2.8
	Phosphate buffer <sup>d</sup>	2.5

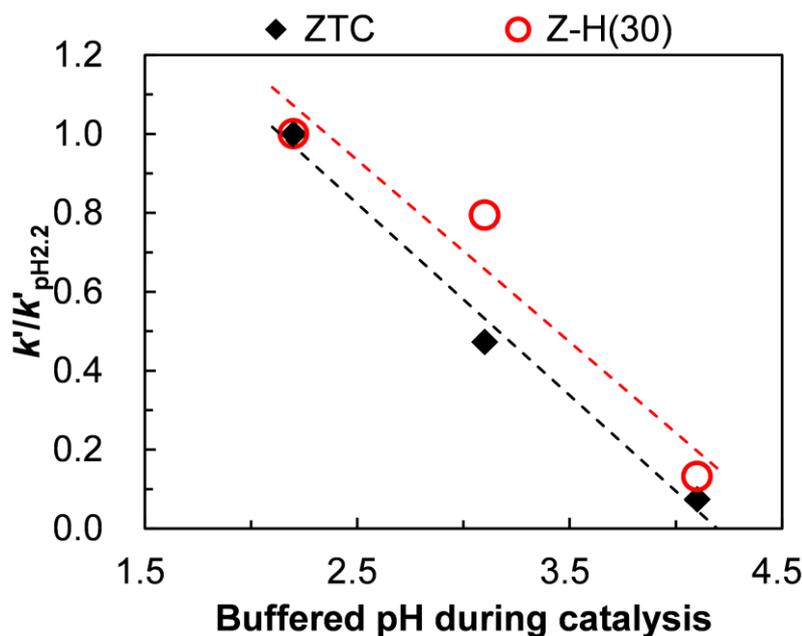
<sup>a</sup>Reaction conditions:  $\beta$ -glucan/ZTC *ca.* 25 mg; solvent 1 mL; 453 K; 3 h; 440 rpm.

<sup>b</sup>20 mM, initial pH 4.1. <sup>c</sup>20 mM, initial pH 3.1. <sup>d</sup>20 mM, initial pH 2.2.

Data for both acetate and phosphate buffers indicates a lack of appreciable pH change under buffered conditions of catalysis here.



**Figure S6.** Population of carboxylic acid (COOH) and conjugated carboxylate (COO<sup>-</sup>) at various pH, in the case of (A)  $pK_a = 4.2$  as typical aromatic carboxylic acid (*i.e.*, benzoic acid)<sup>S3</sup> and (B)  $pK_a = 2.0$ . Legends: red line = carboxylic acid; blue line = conjugated carboxylate.



**Figure S7.** Ratio of pseudo-zero-order rate constants in hydrolysis of  $\beta$ -glucan adsorbed on parent ZTC and Z-H(30) in buffer solutions as a function of initial pH value. The pseudo-zero-order rate constant  $k'$  is defined by eq. S1. Reaction conditions:  $\beta$ -glucan/ZTC *ca.* 25 mg; solvent 1 mL; 453 K; 3 h; 440 rpm.

$$k' = -\frac{X}{t_{\text{hyd}}} \quad (\text{S1})$$

where  $X$  is the glucose yield and  $t_{\text{hyd}}$  is the reaction time.

## References

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- (S2) Chung, P.-W.; Yabushita, M.; To, A. T.; Bae, Y.; Jankolovits, J.; Kobayashi, H.; Fukuoka, A.; Katz, A. Long-Chain Glucan Adsorption and Depolymerization in Zeolite-Templated Carbon Catalysts. *ACS Catal.* **2015**, *5*, 6422–6425.
- (S3) Jencks, W. P.; Regenstein, J. Ionization Constants of Acids and Bases. In *Handbook of Biochemistry and Molecular Biology*, 4th ed.; Lundblad, R. L.; MacDonald, F. M., Eds.; CRC Press: Cleveland, 2010.