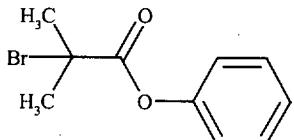
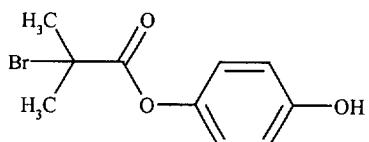


Supplementary Information

Synthesis of 2-bromo-2-methyl-propionic acid phenyl ester¹

18.85 g (0.20 mol) of phenol was added to 400 mL of tetrahydrofuran (THF). The mixture was then stirred to allow complete dissolution of the phenol. 30.7 mL (0.22 mol) of triethylamine was added to the mixture followed by the slow addition of 27.2 mL bromoisobutyryl bromide (0.22 mol). The reaction created a exotherm and a white precipitate of triethylammonium bromide was formed. The reaction was allowed to stir at room temperature for 4 hours. Triethylammonium bromide was removed by filtration and the mixture was concentrated to give a slightly orange liquid. This was vacuum distilled at 70 °C and 0.06 Torr to give a colorless liquid. Yield = 37.7g (77.5%)

¹H NMR (CDCl₃, 298K, 250.13 MHz) δ 7.41 (t, J 7.6 Hz, 2 H), 7.25 (t, J 7.5 Hz, 1H), 7.13 (d, J 8.3 Hz, 2 H), 2.06 (s, 6 H) : ¹³ C {¹H} NMR (CDCl₃, 298K 100.6 MHz) δ 169.88 (C-3), 150.51 (C-4), 129.23 (C-5), 125.88 (C-6), 120.77 (C-7), 55.24 (C-2), 30.34 (C-1). IR (Liquid, ATR Cell,) 2977, 1749 (C=O), 1591, 1493, 1463, 1262, 1185, 1161, 1135, 1100, 1007, 938, 910, 742, 688. CI MS 263, 261, 244, 242, 151, 149, 135, 123, 121, 93. **Anal Calcd.** for C₆H₁₁O₃ Br: C = 49.41, H = 4.56. **Found:** C = 49.26, H = 4.52.
BRN 2519108
CAS 114397-50-1

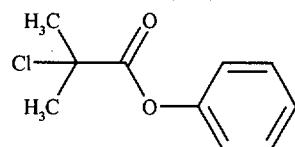
Synthesis of 4-(2'-methyl-2'-bromopropanoate)phenol

Hydroquinone 110.11 g (1.0 mol), tetrahydrofuran 800 mL and triethylamine 15.3 mL (0.11 mol) were placed in a 1 L round bottom and the flask was equipped with a pressure equilibrating dropping funnel. 2-Bromoisobutyryl bromide 12.4 mL (0.1 mol) and tetrahydrofuran 87.6 mL was placed into the dropping funnel. The 2-bromoisobut -yryl bromide solution was added dropwise over 2 hours with stirring which formed triethylammonium bromide and upon complete addition the reaction was stirred for 2 hours. The triethylammonium bromide was removed by filtration and the solvent was removed under reduced pressure. This resulted in a brown white crystalline mixture, which was placed into a round bottom flask with chloroform 600 mL and stirred overnight to separate the unreacted excess hydroquinone. The unreacted hydroquinone was removed from the solution by filtration and the filtrate was concentrated under reduced pressure to give a brown crystalline compound. The resulting brown crystalline solid was purified by column chromatography eluting with 100 % dichloromethane followed by 100 % methanol to give a pale brown crystalline solid. Yield = 18.5 g (71%), m.pt. 92.4 °C

¹H NMR (CDCl₃, 298K, 250.13 MHz) δ 6.98 (d, *J* 8.8 Hz, 2 H), 6.81 (d, *J* 9.1 Hz, 2 H), 4.84 (s, 1H), 2.04 (s, 6 H) : ¹³C {¹H} NMR (CDCl₃, 298K 100.6 MHz) δ 171.56, 153.69, 143.85, 121.75, 116.13, 55.29, 30.49 : IR (Solid, ATR Cell) 3464 (O-H, br), 2982, 1736 (C=O), 1601, 1506, 1461, 1442, 1393, 1374, 1265, 1203, 1183, 1160, 1145, 1097, 1010, 950, 936, 879, 822, 777, 752 : Mass Spectrometry (+CI/NH₃) (m/z) 278, 276 (M+NH₃), 260, 258 (mass peaks) 199, 197, 180, 151, 135, 127, 110, 71 : Anal. Calcd. for C₁₀H₁₁BrO₃: C = 46.36 , H = 4.28 . Found: C = 46.15, H = 4.25

Synthesis of phenyl 2'-chloro-2'-methyl propionate

This compound had been prepared previously by Mc Elvain.²

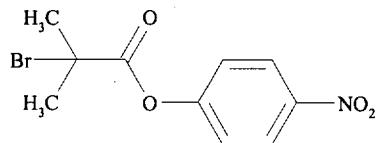


Phenol 18.85 g (0.20 mol), tetrahydrofuran 400 mL and triethylamine 30.6 mL (0.22 mol) were placed in a 500 mL round bottom flask. Chloroisobutyryl chloride 26.4 mL (0.22 mol) was added slowly. The reaction was followed as in 7.2.3 and the triethylammonium chloride was removed by filtration and the solvent was removed under reduced pressure to give a slightly yellow/brown liquid. This was vacuum distilled at 58 °C and 0.2 Torr to give a colourless liquid Yield = 28.9 g (72.7 %)

¹H NMR (CDCl₃, 298K, 250.13 MHz) δ (t, *J* 7.6 Hz, 2 H), 7.26 (t, *J* 6.9 Hz, 1H), 7.13 (d, *J* 8.7 Hz, 2 H), 1.93 (s, 6 H) ; ¹³C {¹H} NMR (CDCl₃, 298K 100.6 MHz) δ 169.40, 150.38, 129.09, 125.74, 120.74, 64.14, 29.09 ; IR (Liquid, ATR Cell,) 3044, 2985, 2936, 1754, 1591, 1456, 1389, 1371, 1265, 1186, 1161, 1140, 1107, 1070, 1006, 938, 911, 859, 745, 688 ; +EI MS (m/z) 200, 198 (mass peaks) 131, 94, 77, 65, 41

Anal Calcd. for C₁₀H₁₁O₂Cl : C = 60.46 , H= 5.58. Found: C = 60.36 , H = 5.58.

Synthesis of 4-Nitrophenyl 2'-bromo-2'-methyl propionate, 8³



4-Nitrophenol (0.2 moles), triethylamine, 30.6 mL (0.22 moles) and THF 400 mL were placed in a 3 neck round bottomed flask. Bromoisobutyryl bromide 27.2 mL (0.22 moles) was added slowly with stirring. A white precipitate of triethylammonium bromide was formed. The mixture was left to react for 6 hours with stirring. On completion of the reaction triethylammonium bromide was removed by filtration and the THF was removed by rotary evaporation. This gave a light brown powder, which was recrystallized from methanol. Yield = 50.6 g (88 %), m.pt. = 85.5 °C

¹H NMR (CDCl₃, 298K, 250.13 MHz) δ 8.30(d, *J* 9.5 Hz, 2 H), 7.32 (d, *J* 9.2 Hz, 2 H), 2.07 (s, 6 H) : ¹³C {¹H} NMR (CDCl₃, 298K 100.6 MHz) δ 169.23 , 155.28 , 145.53 , 125.17 , 121.98 , 54.73 , 30.30. IR (Solid ATR Cell) 2985, 1746 (C=O) (s), 1617, 1595 (N-O) (s), 1522, 1485, 1457, 1345, 1265, 1210, 1192, 1157, 1131, 1100, 1006, 936, 885, 863, 829, 744, 689.. Mass Spectrometry (+EI) (m/z) : 289, 287 (M+), 151, 149, 123, 121.

Anal Calcd. for $C_{10}H_{10}NO_4Br$; C = 41.69, H = 3.50, N = 4.86. **Found:** C = 41.68, H = 3.50, N = 4.70

2-Bromo-2-methyl-propionic acid 4-formyl-phenyl ester, 7.

Prepared as for compound 5. The product was recovered as a yellow oily liquid that crystallized upon standing and was recrystallized twice from diethyl ether. Yield = 18.95 g (69.9 %), m. pt. 42.6 °C

1H NMR ($CDCl_3$, 298K, 250.13 MHz) δ 10.00 (s, 1 H) (CHO), 7.94 (d, J 4.6 Hz 2 H), 7.31 (d, J 4.8 Hz 2 H), 2.06 (s, 6H); $^{13}C\{^1H\}$ NMR ($CDCl_3$, 298K 100.6 MHz) δ 190.59, 169.33, 155.08, 134.07, 131.02, 121.71, 54.94, 30.25; IR (Solid, ATR Cell) 2984, 2820, 2730, 1746 $\nu_{C=O}$, 1693 $\nu_{H-C=O}$, 1590, 1500, 1374, 1262, 1207, 1153, 1132, 1099, 1009, 932, 881, 808, 658 : EI MS (m/z) 273, 271 (mass peaks), 210, 193, 163, 151, 149, 140, 123, 121, 102; Anal Calcd. for $C_{11}H_{11}O_3Br$; C = 48.73, H = 4.09 ; Found: C = 48.63, H = 4.03

2-Bromo-2-methyl-propionic acid 4-benzyloxy-phenyl ester, 9.

Prepared as for compound 5. The product was recovered as an off white in colour and crystalline. The product was recrystallized from methanol : water (90 : 10) and dried to give a white crystalline product. Yield = 28.15 g (80.6 %), m.pt. 78.5°C.

1H NMR ($CDCl_3$, 298K, 250.13 MHz) δ 7.44 – 7.32 (m, 5 H), 7.04 (d, J 9.1 Hz, 2 H), 6.97 (d, J 9.1 Hz 2 H), 5.05 (s, 2 H), 2.05 (s, 6 H) ; $^{13}C\{^1H\}$ NMR ($CDCl_3$, 298K 100.6 MHz) δ 170.52, 156.62, 144.4, 136.68, 128.56, 127.99, 127.41, 121.79, 115.46, 70.36, 55.40, 30.60 ; IR (Solid, ATR Cell) 3063, 2979, 1742 (C=O), 1594, 1453, 1385, 1246, 1183, 1135, 1101, 1015, 941, 873, 811, 781, 738. : EI MS 349, 348 (mass peaks), 151, 149, 121, 123 Anal. Calcd. for $C_{17}H_{17}BrO_3$: C = 58.47, H = 4.91, Found: C = 58.45, H = 4.78.

Figure UV and DRI SEC chromatograms of PMMA initiated using, 2

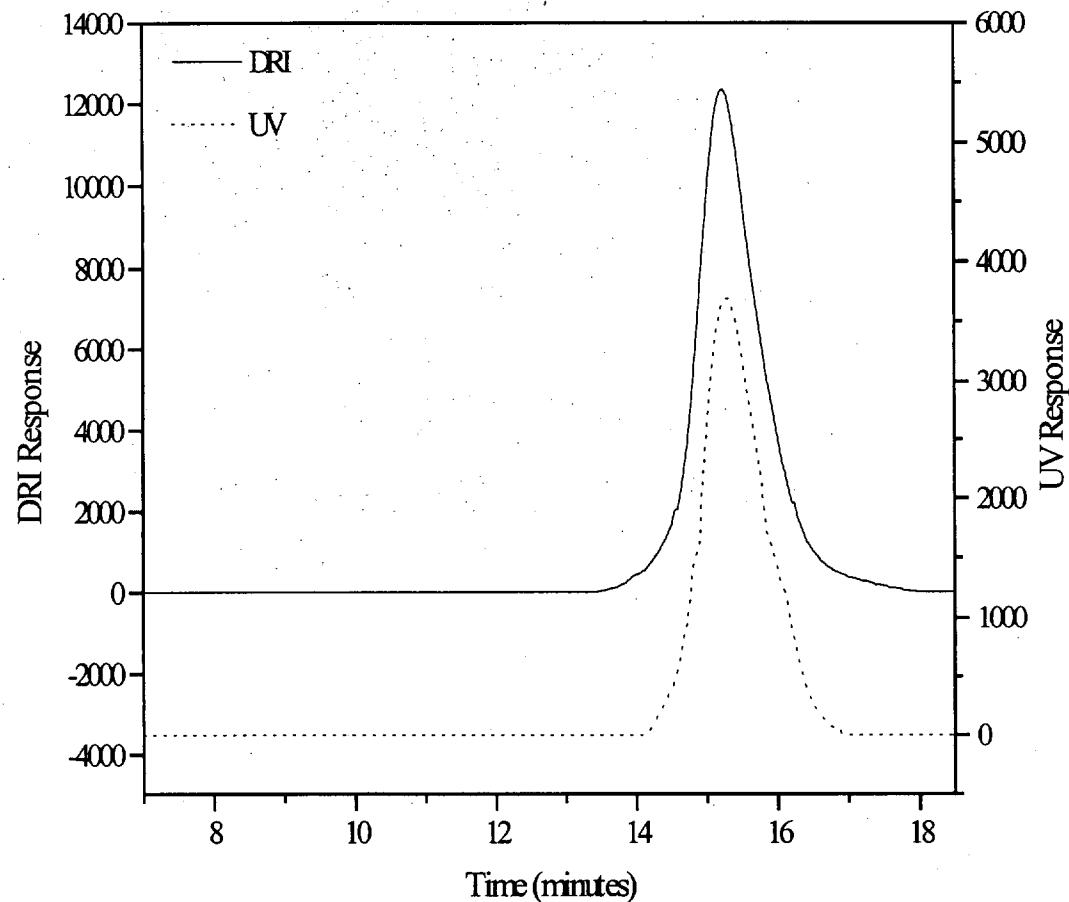


Figure Partial (3.2-7.9 ppm) 250MHz, ^1H NMR in CDCl_3 of PMMA initiated with, 2

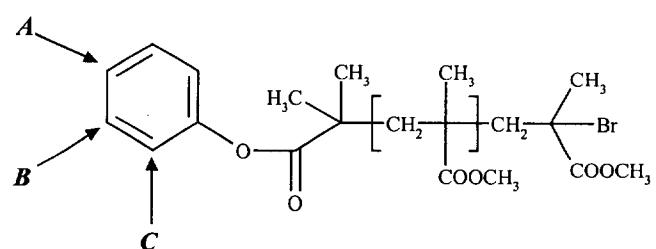
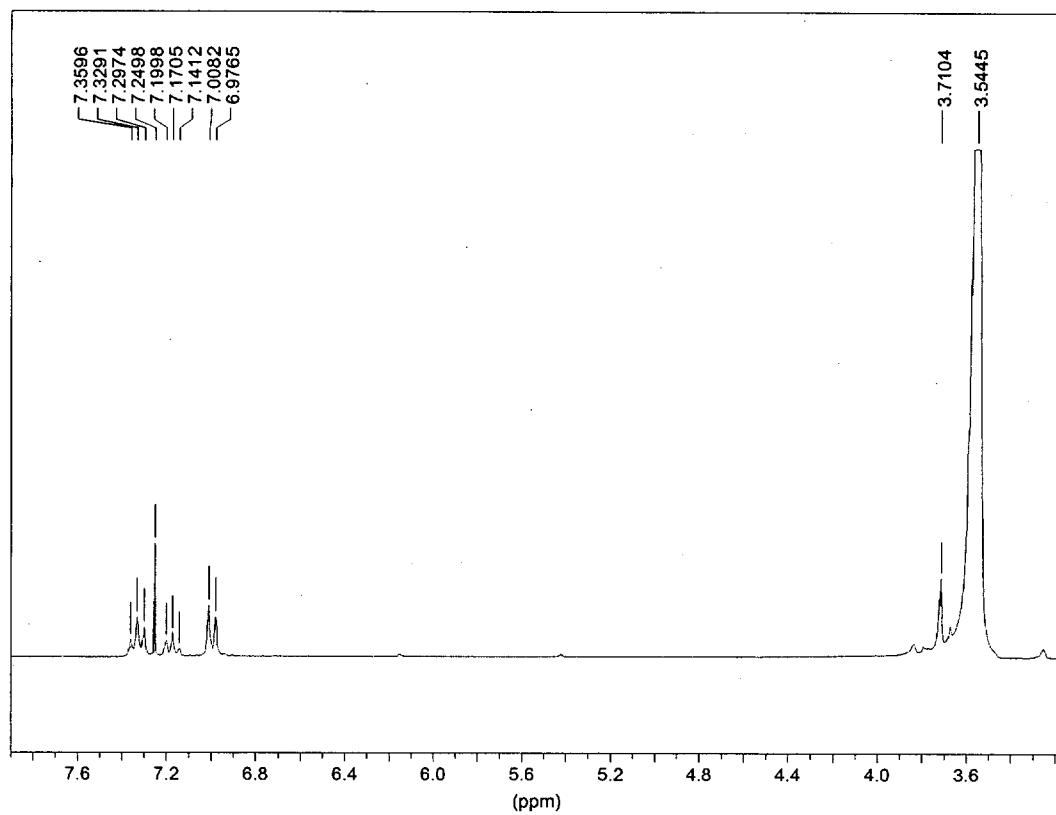
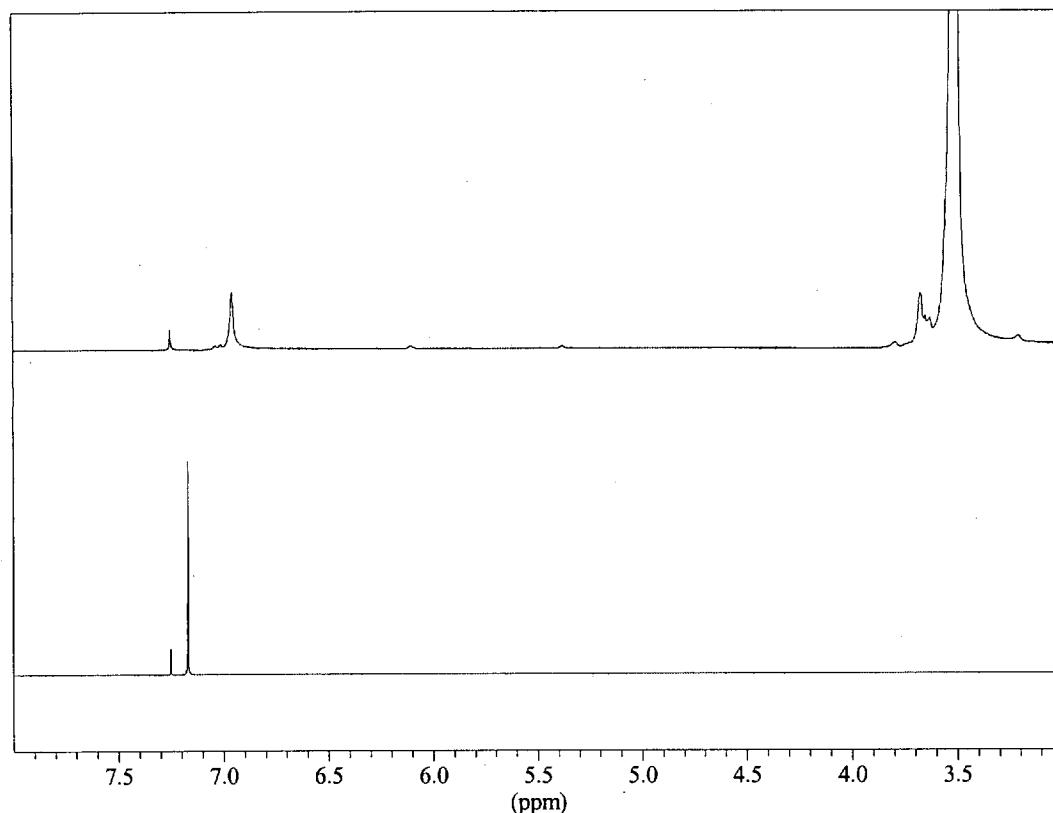


Figure Partial 250 MHz ^1H NMR (3.0-8.0 ppm) in CDCl_3 of PMMA initiated with **10**(top) and initiator **10** (bottom), small peak due to solvent.



MMA was polymerized under the conditions outlined in table 3-1 but the polymerization was terminated at 3600 s to produce a low M_n polymer to investigate if both initiator sites had reacted. The reaction was precipitated into petroleum ether and gave the NMR of the resulting polymer was obtained in CDCl_3 . If the polymer was propagating from one site on some initiator molecules then it would be expected that the aromatic region should contain two doublets shifted slightly upfield as the protons on the aromatic ring are inequivalent. If however, initiation is taking place on both sites the signal pattern obtained should be one singlet-shifted upfield from its original position in initiator **10**.

From the above figure it is noted that the singlet in the initiator at 7.16 ppm has shifted upfield to 6.95 ppm in the polymer. This demonstrates that the polymerization occurs on both sites as any partial initiation would have resulted in the presence of two doublets, which are not observed.

Full polymerisation data sets

Table 1 Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[2] = 100 : 1: 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 2250 | 1.14 | 23.5 | 0.267 |
| 3600 | 3670 | 1.13 | 42.3 | 0.550 |
| 5400 | 4470 | 1.12 | 53.9 | 0.775 |
| 7200 | 5170 | 1.12 | 63.2 | 0.999 |
| 9000 | 5650 | 1.12 | 68.6 | 1.160 |
| 10800 | 6110 | 1.12 | 73.5 | 1.327 |
| 14400 | 6620 | 1.11 | 84.2 | 1.846 |
| $k_p \text{ [pol } *] = 1.298 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 2 Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[1] = 100 : 1: 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|---|-------|------|--------|------------------|
| 1800 | 3030 | 1.14 | 15.9 | 0.174 |
| 3600 | 4080 | 1.16 | 27.9 | 0.327 |
| 5400 | 4660 | 1.18 | 38.1 | 0.480 |
| 7200 | 5260 | 1.17 | 47.7 | 0.649 |
| 9000 | 6000 | 1.17 | 56.1 | 0.822 |
| 10800 | 6650 | 1.17 | 64.7 | 1.041 |
| 14400 | 7290 | 1.18 | 76.9 | 1.466 |
| $k_p \text{ [pol } *] = 9.66 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 3. Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[3] = 100 : 1: 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 1400 | 1.15 | 11.1 | 0.118 |
| 3600 | 2000 | 1.29 | 17.6 | 0.193 |
| 5400 | 2500 | 1.30 | 23.2 | 0.264 |
| 7200 | 3240 | 1.31 | 29.3 | 0.347 |
| 9000 | 3670 | 1.32 | 34.3 | 0.420 |
| 10800 | 4150 | 1.32 | 39.4 | 0.500 |
| 14400 | 5120 | 1.34 | 48.7 | 0.667 |
| $k_p \text{ [pol } *] = 4.7 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 4 Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[4] = 100 : 1: 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 2450 | 1.19 | 17.0 | 0.187 |
| 3600 | 3270 | 1.17 | 25.5 | 0.294 |
| 5400 | 3730 | 1.16 | 36.2 | 0.449 |
| 7200 | 4190 | 1.16 | 44.3 | 0.585 |
| 9000 | 4650 | 1.15 | 51.7 | 0.729 |
| 10800 | 4960 | 1.14 | 57.5 | 0.856 |
| 14400 | 5427 | 1.14 | 66.9 | 1.104 |
| k_p [pol *] = $7.91 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 5 Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[5] = 100 : 1: 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|---|-------|------|--------|------------------|
| 1800 | 2360 | 1.22 | 25.9 | 0.300 |
| 3600 | 3830 | 1.14 | 46.0 | 0.615 |
| 5400 | 4700 | 1.14 | 56.7 | 0.837 |
| 7200 | 5130 | 1.14 | 64.7 | 1.050 |
| 9000 | 5640 | 1.13 | 71.1 | 1.240 |
| 10800 | 5960 | 1.13 | 75.6 | 1.412 |
| 14400 | 6580 | 1.12 | 85.1 | 1.907 |
| k_p [pol *] = $1.367 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 6 Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[6] = 100 : 1: 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|---|-------|------|--------|------------------|
| 1800 | 2680 | 1.22 | 18.6 | 0.206 |
| 3600 | 4030 | 1.24 | 33.2 | 0.403 |
| 5400 | 5250 | 1.26 | 45.4 | 0.604 |
| 7200 | 6220 | 1.23 | 60.7 | 0.935 |
| 9000 | 7150 | 1.22 | 67.9 | 1.138 |
| 10800 | 8060 | 1.19 | 77.5 | 1.494 |
| 14400 | 9340 | 1.19 | 86.6 | 2.014 |
| k_p [pol *] = $1.338 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 7 Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[7]
= 100 : 1; 2 : 1

| t/secs | M _n | PDi | Conv % | ln([M] ₀ /[M]) |
|--|----------------|------|--------|---------------------------|
| 1800 | 1940 | 1.09 | 20.3 | 0.227 |
| 3600 | 2656 | 1.10 | 30.8 | 0.368 |
| 5400 | 3589 | 1.09 | 40.0 | 0.512 |
| 7200 | 4525 | 1.07 | 52.0 | 0.733 |
| 9000 | 5429 | 1.08 | 61.0 | 0.942 |
| 10800 | 5948 | 1.08 | 68.1 | 1.142 |
| 14400 | 6436 | 1.10 | 76.7 | 1.456 |
| $k_p \text{ [pol } *] = 1.027 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 8 Polymerisation of MMA in xylene at 90 °C , [MMA]/[Cu(I)Br]/[18]/[8]
= 100 : 1; 2 : 1

| secs | M _n | PDi | Conv % | ln([M] ₀ /[M]) |
|--|----------------|------|--------|---------------------------|
| 1800 | 1990 | 1.11 | 25.4 | 0.280 |
| 3600 | 3500 | 1.09 | 43.4 | 0.570 |
| 5400 | 4450 | 1.09 | 55.4 | 0.807 |
| 7200 | 4990 | 1.09 | 64.2 | 1.027 |
| 9000 | 5530 | 1.09 | 70.6 | 1.223 |
| 10800 | 5780 | 1.09 | 75.4 | 1.404 |
| 14400 | 6530 | 1.09 | 85.2 | 1.911 |
| $k_p \text{ [pol } *] = 1.354 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 9 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[9]
= 100 : 1; 2 : 1

| t/secs | M _n | PDi | Conv % | ln([M] ₀ /[M]) |
|--|----------------|------|--------|---------------------------|
| 1800 | 2280 | 1.14 | 26.7 | 0.311 |
| 3600 | 3660 | 1.11 | 44.7 | 0.592 |
| 5400 | 4590 | 1.10 | 56.3 | 0.828 |
| 7200 | 5110 | 1.10 | 64.0 | 1.022 |
| 9000 | 5650 | 1.10 | 69.0 | 1.170 |
| 10800 | 5850 | 1.10 | 74.6 | 1.372 |
| 14400 | 6710 | 1.10 | 82.2 | 1.729 |
| $k_p \text{ [pol } *] = 1.290 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 10 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[10] = 100 : 1 : 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 3206 | 1.17 | 27.5 | 0.320 |
| 3600 | 4827 | 1.13 | 45.7 | 0.611 |
| 5400 | 5850 | 1.11 | 57.7 | 0.861 |
| 7200 | 6511 | 1.11 | 66.9 | 1.105 |
| 9000 | 7013 | 1.10 | 75.6 | 1.410 |
| 10800 | 7394 | 1.10 | 79.8 | 1.598 |
| 14400 | 7900 | 1.09 | 85.8 | 1.949 |
| $k_p \text{ [pol *]} = 1.46 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 11 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[10] = 100 : 2 : 4 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 3640 | 1.11 | 44.2 | 0.584 |
| 3600 | 4920 | 1.10 | 61.1 | 0.945 |
| 5400 | 5790 | 1.09 | 73.8 | 1.338 |
| 7200 | 6380 | 1.09 | 82.1 | 1.721 |
| 9000 | 6830 | 1.08 | 87.6 | 2.087 |
| 10800 | 7050 | 1.08 | 92.2 | 2.555 |
| 14400 | 7500 | 1.08 | 98.1 | 3.952 |
| $k_p \text{ [pol *]} = 2.54 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 12 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[10] = 100 : 2 : 4 : 2

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 2550 | 1.14 | 51.7 | 0.728 |
| 3600 | 3170 | 1.16 | 73.5 | 1.328 |
| 5400 | 3780 | 1.15 | 88.4 | 2.158 |
| 7200 | 4170 | 1.12 | 94.4 | 2.885 |
| 9000 | 4390 | 1.12 | 96.6 | 3.380 |
| 10800 | 4590 | 1.13 | 98.5 | 4.203 |
| 14400 | 4740 | 1.13 | 99.7 | 5.752 |
| $k_p \text{ [pol *]} = 3.92 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 13 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[11] = 100 : 2 : 4 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--------|-------|------|--------|------------------|
| 1800 | 4190 | 1.20 | 42.5 | 0.553 |
| 3600 | 5480 | 1.14 | 58.0 | 0.867 |
| 5400 | 6520 | 1.14 | 72.9 | 1.305 |
| 7200 | 7290 | 1.12 | 81.1 | 1.665 |
| 9000 | 7813 | 1.11 | 89.8 | 2.284 |
| 10800 | 8144 | 1.10 | 93.6 | 2.755 |
| 14400 | 8600 | 1.09 | 97.8 | 3.823 |

$$k_p \text{ [pol *]} = 2.56 \times 10^{-4} \text{ s}^{-1}$$

Table 14 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[12] = 100 : 2 : 4 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--------|-------|------|--------|------------------|
| 1800 | 3660 | 1.18 | 39.3 | 0.499 |
| 3600 | 5120 | 1.16 | 54.5 | 0.788 |
| 5400 | 6426 | 1.14 | 71.1 | 1.241 |
| 7200 | 7443 | 1.13 | 78.9 | 1.555 |
| 9000 | 7865 | 1.13 | 85.6 | 1.936 |
| 10800 | 8578 | 1.12 | 91.3 | 2.439 |
| 14400 | 8974 | 1.10 | 96.1 | 3.242 |

$$k_p \text{ [pol *]} = 2.23 \times 10^{-4} \text{ s}^{-1}$$

Table 15 Polymerisation of EMA in xylene at 90 °C, [EMA]/[Cu(I)Br]/[18]/[10] = 100 : 2 : 4 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--------|-------|------|--------|------------------|
| 1800 | 3740 | 1.10 | 39.0 | 0.494 |
| 3600 | 5510 | 1.09 | 58.3 | 0.875 |
| 5400 | 6530 | 1.09 | 70.1 | 1.207 |
| 7200 | 7170 | 1.09 | 77.9 | 1.512 |
| 9000 | 7630 | 1.09 | 82.9 | 1.768 |
| 10800 | 8050 | 1.09 | 87.6 | 2.091 |
| 14400 | 8460 | 1.10 | 93.6 | 2.743 |

$$k_p \text{ [pol *]} = 1.98 \times 10^{-4} \text{ s}^{-1}$$

Table 16 Polymerisation of IPMA in xylene at 90 °C, [IPMA]/[Cu(I)Br]/[18]/[10] = 100 : 2 : 4 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 2880 | 1.12 | 18.4 | 0.204 |
| 3600 | 3590 | 1.10 | 29.8 | 0.354 |
| 5400 | 4250 | 1.10 | 36.9 | 0.461 |
| 7200 | 4910 | 1.10 | 48.4 | 0.661 |
| 9000 | 5420 | 1.10 | 53.4 | 0.764 |
| 10800 | 5740 | 1.11 | 57.4 | 0.853 |
| 14400 | 6320 | 1.12 | 67.8 | 1.133 |
| $k_p \text{ [pol *]} = 8.22 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 17 Polymerisation of *t*-BMA in xylene at 90 °C, [*t*-BMA]/[Cu(I)Br]/[18]/[10] = 100 : 2 : 4 : 1

| t/hrs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|-------|-------|------|--------|------------------|
| 0.5 | 4838 | 1.12 | 38.5 | 0.4859 |
| 1 | 6358 | 1.15 | 49.9 | 0.6929 |
| 1.5 | 6864 | 1.21 | 53.9 | 0.7764 |
| 2 | 7021 | 1.25 | 54.9 | 0.7959 |
| 2.5 | 7117 | 1.28 | 56.8 | 0.8402 |
| 3 | 7170 | 1.30 | 56.9 | 0.8409 |
| 4 | 7130 | 1.31 | 57.5 | 0.8557 |

Table 18 Polymerisation of n-BMA in xylene at 90 °C, [n-BMA]/[Cu(I)Br]/[18]/[10] = 100 : 2 : 4 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 5770 | 1.14 | 56.5 | 0.833 |
| 3600 | 8050 | 1.12 | 79.3 | 1.576 |
| 5400 | 9170 | 1.12 | 89.7 | 2.269 |
| 7200 | 9930 | 1.12 | 95.8 | 3.168 |
| 9000 | 10210 | 1.13 | 97.8 | 3.818 |
| 10800 | 10420 | 1.14 | 99.0 | 4.654 |
| 14400 | 10790 | 1.15 | 99.8 | 6.250 |
| $k_p \text{ [pol *]} = 4.32 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 19 Polymerisation of *i*-BMA in xylene at 90 °C, [i-BMA]/[Cu(I)Br]/[18][10] = 100 : 2 : 4 : 1

| t/hrs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 5360 | 1.13 | 53.6 | 0.768 |
| 3600 | 7550 | 1.13 | 75.8 | 1.417 |
| 5400 | 8600 | 1.12 | 86.4 | 1.998 |
| 7200 | 9220 | 1.13 | 92.8 | 2.631 |
| 9000 | 9810 | 1.13 | 96.6 | 3.393 |
| 10800 | 9870 | 1.12 | 98.6 | 4.234 |
| 14400 | 10370 | 1.13 | 99.7 | 5.730 |
| $k_p \text{ [pol}^*] = 3.88 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 20 Polymerisation of BzMA in xylene at 90 °C, [BzMA]/[Cu(I)Br]/[18][10] = 100 : 2 : 4 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 9590 | 1.21 | 87.1 | 2.048 |
| 3600 | 11440 | 1.13 | 98.6 | 4.251 |
| 5400 | 12780 | 1.11 | 99.8 | 6.336 |
| $k_p \text{ [pol}^*] = 1.17 \times 10^{-3} \text{ s}^{-1}$ | | | | |

Table 21 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Cl]/[18]/[15] = 100 : 2 : 4 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|---|-------|------|--------|------------------|
| 1800 | 4010 | 1.37 | 21.3 | 0.240 |
| 3600 | 4640 | 1.45 | 33.3 | 0.405 |
| 5400 | 5610 | 1.42 | 46.9 | 0.634 |
| 7200 | 6290 | 1.38 | 57.0 | 0.845 |
| 9000 | 7089 | 1.36 | 68.1 | 1.144 |
| 10800 | 7540 | 1.30 | 75.5 | 1.405 |
| 14400 | 8350 | 1.21 | 84.6 | 1.869 |
| $k_p \text{ [pol}^*] = 1.270 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 22. Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[13] = 100 : 1 : 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|---|-------|------|--------|------------------|
| 1800 | 2710 | 1.10 | 22.1 | 0.250 |
| 3600 | 3700 | 1.13 | 34.9 | 0.429 |
| 5400 | 4770 | 1.11 | 47.0 | 0.635 |
| 7200 | 5670 | 1.10 | 58.5 | 0.879 |
| 9000 | 6230 | 1.09 | 64.9 | 1.048 |
| 10800 | 6750 | 1.10 | 71.8 | 1.266 |
| 14400 | 7220 | 1.09 | 80.6 | 1.642 |
| $k_p \text{ [pol *]} = 1.165 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 23 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Cl]/[18]/[14] = 100 : 1 : 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 3260 | 1.23 | 8.4 | 0.087 |
| 3600 | 4190 | 1.27 | 20.8 | 0.233 |
| 5400 | 5070 | 1.29 | 29.2 | 0.345 |
| 7200 | 5820 | 1.28 | 38.2 | 0.481 |
| 9000 | 6410 | 1.29 | 48.8 | 0.669 |
| 10800 | 6820 | 1.29 | 56.1 | 0.823 |
| 14400 | 7415 | 1.23 | 64.6 | 1.039 |
| $k_p \text{ [pol *]} = 7.21 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 24 Polymerisation of styrene in xylene 50% (v/v) at 110 °C, [STY]/[Cu(I)Br]/[18]/[16] = 100 : 3 : 6 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 2180 | 1.09 | 21.5 | 0.242 |
| 3600 | 3090 | 1.11 | 33.8 | 0.413 |
| 5400 | 3680 | 1.11 | 39.3 | 0.499 |
| 7200 | 4500 | 1.14 | 45.2 | 0.602 |
| 10800 | 5850 | 1.15 | 56.5 | 0.833 |
| 14400 | 7054 | 1.15 | 68.2 | 1.146 |
| 18800 | 8340 | 1.17 | 78.9 | 1.558 |
| 21600 | 9710 | 1.17 | 82.8 | 1.761 |
| 25200 | 10350 | 1.24 | 89.8 | 2.280 |
| 28800 | 11000 | 1.28 | 91.7 | 2.490 |
| $k_p \text{ [pol *]} = 8.58 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 25 Polymerisation of styrene in xylene 50% (v/v) at 110 °C, [STY]/[Cu(I)Cl]/[18]/[17] = 100 : 3 : 6 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 3720 | 1.32 | 30.6 | 0.366 |
| 3600 | 4370 | 1.33 | 36.3 | 0.452 |
| 5400 | 4900 | 1.33 | 41.7 | 0.540 |
| 7200 | 5380 | 1.33 | 47.2 | 0.638 |
| 10800 | 6300 | 1.34 | 57.0 | 0.844 |
| 14400 | 7080 | 1.35 | 65.6 | 1.066 |
| 18800 | 7990 | 1.35 | 74.6 | 1.369 |
| 21600 | 8570 | 1.35 | 84.7 | 1.877 |
| 25200 | 9450 | 1.35 | 88.8 | 2.193 |
| 28800 | 9680 | 1.37 | 91.2 | 2.549 |
| $k_p \text{ [pol *]} = 8.52 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 26 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Br]/[18]/[16] = 100 : 3 : 6 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|---|-------|------|--------|------------------|
| 1800 | 5460 | 1.18 | 55.0 | 0.798 |
| 3600 | 7460 | 1.18 | 77.6 | 1.495 |
| 5400 | 8640 | 1.17 | 88.0 | 2.120 |
| 7200 | 8980 | 1.11 | 95.0 | 2.991 |
| 9000 | 9250 | 1.12 | 97.2 | 3.564 |
| 10800 | 9600 | 1.12 | 98.8 | 4.452 |
| $k_p \text{ [pol *]} = 4.068 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 27 Polymerisation of MMA in xylene at 90 °C, [MMA]/[Cu(I)Cl]/[18]/[17] = 100 : 3 : 6 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|---|-------|------|--------|------------------|
| 1800 | 5320 | 1.34 | 34.6 | 0.425 |
| 3600 | 7400 | 1.42 | 57.8 | 0.863 |
| 5400 | 7980 | 1.41 | 70.4 | 1.216 |
| 7200 | 8020 | 1.24 | 76.8 | 1.460 |
| 9000 | 8440 | 1.21 | 83.6 | 1.807 |
| 10800 | 8570 | 1.21 | 87.6 | 2.089 |
| $k_p \text{ [pol *]} = 2.028 \times 10^{-4} \text{ s}^{-1}$ | | | | |

Table 28 Polymerisation of styrene in xylene 50% (v/v) at 110 °C, [STY]/[Cu(I)Br]/[18]/[1] = 100 : 1 : 2 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 690 | 1.06 | 8.3 | 0.087 |
| 3600 | 880 | 1.07 | 10.3 | 0.109 |
| 5400 | 1040 | 1.09 | 12.3 | 0.132 |
| 7200 | 1230 | 1.10 | 15.3 | 0.166 |
| 10800 | 1570 | 1.10 | 23.2 | 0.264 |
| 14400 | 1950 | 1.10 | 29.5 | 0.350 |
| 18000 | 2380 | 1.10 | 32.1 | 0.387 |
| 21600 | 2510 | 1.10 | 36.4 | 0.452 |
| 25200 | 2840 | 1.11 | 41.4 | 0.534 |
| 28800 | 2870 | 1.12 | 44.2 | 0.584 |
| $k_p \text{ [pol *]} = 2.14 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 29 Polymerisation of styrene in xylene 50% (v/v) at 110 °C, [STY]/[Cu(I)Br]/[18]/[10] = 100 : 2 : 4 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 1770 | 1.10 | 10.6 | 0.112 |
| 3600 | 2360 | 1.10 | 19.1 | 0.211 |
| 5400 | 2910 | 1.09 | 25.3 | 0.292 |
| 7200 | 3480 | 1.10 | 31.8 | 0.383 |
| 10800 | 4290 | 1.10 | 41.8 | 0.540 |
| 14400 | 4950 | 1.11 | 48.6 | 0.666 |
| 18800 | 5770 | 1.11 | 54.5 | 0.788 |
| 21600 | 6420 | 1.12 | 60.1 | 0.918 |
| 25200 | 6880 | 1.15 | 67.1 | 1.113 |
| 28800 | 7460 | 1.17 | 71.6 | 1.258 |
| $k_p \text{ [pol *]} = 4.45 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 30 Polymerisation of styrene in xylene 50% (v/v) at 110 °C, [STY]/[Cu(I)Cl] /[17]/[14] = 100 : 2 : 4 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 3040 | 1.47 | 18.2 | 0.200 |
| 3600 | 3430 | 1.47 | 24.5 | 0.280 |
| 5400 | 3760 | 1.48 | 33.7 | 0.411 |
| 7200 | 4080 | 1.47 | 37.4 | 0.469 |
| 10800 | 4690 | 1.46 | 48.3 | 0.660 |
| 14400 | 5360 | 1.45 | 55.8 | 0.816 |
| 18800 | 5850 | 1.44 | 62.9 | 0.991 |
| 21600 | 6320 | 1.44 | 70.0 | 1.203 |
| 25200 | 6890 | 1.44 | 76.3 | 1.441 |
| 28800 | 7150 | 1.44 | 81.9 | 1.709 |
| $k_p \text{ [pol *]} = 5.80 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 31 Polymerisation of styrene in xylene 50% (v/v) at 110 °C, [STY]/[Cu(I)Br] /[18]/[16] = 100 : 3 : 6 : 1

| t/secs | M_n | PDi | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 2180 | 1.09 | 21.5 | 0.242 |
| 3600 | 3090 | 1.11 | 33.8 | 0.413 |
| 5400 | 3680 | 1.11 | 39.3 | 0.499 |
| 7200 | 4500 | 1.14 | 45.2 | 0.602 |
| 10800 | 5850 | 1.15 | 56.5 | 0.833 |
| 14400 | 7054 | 1.15 | 68.2 | 1.146 |
| 18800 | 8340 | 1.17 | 78.9 | 1.558 |
| 21600 | 9710 | 1.17 | 82.8 | 1.761 |
| 25200 | 10350 | 1.24 | 89.8 | 2.280 |
| 28800 | 11000 | 1.28 | 91.7 | 2.490 |
| $k_p \text{ [pol *]} = 8.58 \times 10^{-5} \text{ s}^{-1}$ | | | | |

Table 32 Polymerisation of styrene in xylene 50% (v/v) at 110 °C, [STY]/[Cu(I)Cl] / [18]/[17] = 100 : 3 : 6 : 1

| t/secs | M_n | PDI | Conv % | $\ln([M]_0/[M])$ |
|--|-------|------|--------|------------------|
| 1800 | 3720 | 1.32 | 30.6 | 0.366 |
| 3600 | 4370 | 1.33 | 36.3 | 0.452 |
| 5400 | 4900 | 1.33 | 41.7 | 0.540 |
| 7200 | 5380 | 1.33 | 47.2 | 0.638 |
| 10800 | 6300 | 1.34 | 57.0 | 0.844 |
| 14400 | 7080 | 1.35 | 65.6 | 1.066 |
| 18800 | 7990 | 1.35 | 74.6 | 1.369 |
| 21600 | 8570 | 1.35 | 84.7 | 1.877 |
| 25200 | 9450 | 1.35 | 88.8 | 2.193 |
| 28800 | 9680 | 1.37 | 91.2 | 2.549 |
| $k_p \text{ [pol}^*] = 8.52 \times 10^{-5} \text{ s}^{-1}$ | | | | |

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Table. Atomic coordinates ($\times 10^4$) and equivalent isotropic displacement parameters ($\text{\AA}^2 \times 10^3$) for 10.

| | x | y | z | U(eq) |
|-------|------------|------------|------------|-------|
| Br(1) | -5876.5(7) | 5665.5(5) | -3143.7(3) | 35(1) |
| C(11) | 1167(8) | 5865(5) | -682(3) | 35(1) |
| C(12) | -719(7) | 5349(5) | -943(3) | 30(1) |
| C(13) | -1909(8) | 4493(6) | -280(3) | 37(1) |
| O(14) | -1500(6) | 5794(3) | -1911(2) | 33(1) |
| C(15) | -1549(6) | 4777(4) | -2472(3) | 24(1) |
| O(16) | -789(6) | 3561(3) | -2212(2) | 35(1) |
| C(17) | -2642(6) | 5384(4) | -3460(3) | 24(1) |
| C(18) | -1975(8) | 6826(5) | -3914(3) | 33(1) |
| C(19) | -2319(8) | 4296(5) | -4120(3) | 38(1) |
| Br(2) | 5452.9(7) | -1176.4(5) | 8323.4(4) | 38(1) |
| C(21) | 2175(7) | -502(4) | 5333(3) | 28(1) |
| C(22) | 599(7) | 59(4) | 5934(3) | 26(1) |
| C(23) | -1556(7) | 555(4) | 5614(3) | 27(1) |
| O(24) | 1124(5) | 38(4) | 6919(2) | 33(1) |
| C(25) | 2659(6) | 874(4) | 7110(3) | 25(1) |
| O(26) | 3428(5) | 1720(3) | 6501(2) | 33(1) |
| C(27) | 3290(6) | 591(4) | 8196(3) | 26(1) |
| C(28) | 1357(7) | 274(5) | 8867(3) | 34(1) |
| C(29) | 4485(8) | 1777(5) | 8452(3) | 35(1) |

Table. Selected bond lengths [Å] and angles [deg] for 10.

| | |
|-------------------|-----------|
| Br(1)-C(17) | 1.997 (4) |
| Br(2)-C(27) | 1.994 (4) |
| C(19)-C(17)-Br(1) | 108.0 (3) |
| C(18)-C(17)-Br(1) | 107.7 (3) |
| C(15)-C(17)-Br(1) | 102.9 (2) |
| C(29)-C(27)-Br(2) | 108.7 (3) |
| C(28)-C(27)-Br(2) | 108.1 (3) |
| C(25)-C(27)-Br(2) | 102.2 (3) |

Table. Bond lengths [Å] and angles [deg] for 10.

| | |
|------------------------|-----------|
| Br(1) -C(17) | 1.997 (4) |
| C(11) -C(12) | 1.373 (6) |
| C(11) -C(13) #1 | 1.385 (6) |
| C(12) -C(13) | 1.382 (6) |
| C(12) -O(14) | 1.405 (5) |
| C(13) -C(11) #1 | 1.385 (6) |
| O(14) -C(15) | 1.361 (5) |
| C(15) -O(16) | 1.194 (5) |
| C(15) -C(17) | 1.515 (5) |
| C(17) -C(19) | 1.507 (6) |
| C(17) -C(18) | 1.517 (6) |
| Br(2) -C(27) | 1.994 (4) |
| C(21) -C(22) | 1.388 (6) |
| C(21) -C(23) #2 | 1.384 (6) |
| C(22) -C(23) | 1.378 (6) |
| C(22) -O(24) | 1.407 (5) |
| C(23) -C(21) #2 | 1.384 (6) |
| O(24) -C(25) | 1.356 (5) |
| C(25) -O(26) | 1.198 (5) |
| C(25) -C(27) | 1.531 (5) |
| C(27) -C(29) | 1.516 (6) |
| C(27) -C(28) | 1.517 (6) |
| | |
| C(12) -C(11) -C(13) #1 | 118.8 (4) |
| C(11) -C(12) -C(13) | 122.4 (4) |
| C(11) -C(12) -O(14) | 117.4 (4) |
| C(13) -C(12) -O(14) | 120.1 (4) |
| C(12) -C(13) -C(11) #1 | 118.9 (4) |
| C(15) -O(14) -C(12) | 117.5 (3) |
| O(16) -C(15) -O(14) | 123.4 (4) |
| O(16) -C(15) -C(17) | 124.9 (4) |
| O(14) -C(15) -C(17) | 111.8 (3) |
| C(19) -C(17) -C(18) | 113.8 (4) |
| C(19) -C(17) -C(15) | 110.2 (3) |
| C(18) -C(17) -C(15) | 113.6 (3) |
| C(19) -C(17) -Br(1) | 108.0 (3) |
| C(18) -C(17) -Br(1) | 107.7 (3) |
| C(15) -C(17) -Br(1) | 102.9 (2) |
| C(22) -C(21) -C(23) #2 | 118.8 (4) |
| C(23) -C(22) -C(21) | 121.8 (4) |
| C(23) -C(22) -O(24) | 117.8 (4) |
| C(21) -C(22) -O(24) | 120.3 (4) |
| C(22) -C(23) -C(21) #2 | 119.4 (4) |
| C(25) -O(24) -C(22) | 117.4 (3) |
| O(26) -C(25) -O(24) | 124.0 (4) |
| O(26) -C(25) -C(27) | 124.5 (4) |
| O(24) -C(25) -C(27) | 111.4 (3) |
| C(29) -C(27) -C(28) | 112.3 (4) |
| C(29) -C(27) -C(25) | 111.1 (3) |
| C(28) -C(27) -C(25) | 113.9 (3) |
| C(29) -C(27) -Br(2) | 108.7 (3) |
| C(28) -C(27) -Br(2) | 108.1 (3) |
| C(25) -C(27) -Br(2) | 102.2 (3) |

Table. Anisotropic displacement parameters ($\text{Å}^2 \times 10^3$) for **10**.

| | U11 | U22 | U33 | U23 | U13 | U12 |
|-------|--------|--------|--------|---------|---------|-------|
| Br(1) | 22 (1) | 50 (1) | 32 (1) | -6 (1) | 0 (1) | 6 (1) |
| C(11) | 38 (2) | 41 (2) | 29 (2) | -6 (2) | 0 (2) | 4 (2) |
| C(12) | 33 (2) | 31 (2) | 24 (2) | -6 (2) | -5 (2) | 1 (2) |
| C(13) | 35 (2) | 52 (3) | 26 (2) | -6 (2) | -6 (2) | 4 (2) |
| O(14) | 49 (2) | 29 (2) | 19 (1) | -4 (1) | -11 (1) | 2 (1) |
| C(15) | 22 (2) | 28 (2) | 21 (2) | -3 (1) | -2 (1) | 4 (1) |
| O(16) | 45 (2) | 26 (2) | 29 (2) | -2 (1) | -6 (1) | 6 (1) |
| C(17) | 21 (2) | 30 (2) | 22 (2) | -4 (2) | -2 (1) | 3 (1) |
| C(18) | 35 (2) | 35 (2) | 25 (2) | 6 (2) | 0 (2) | 8 (2) |
| C(19) | 42 (3) | 43 (3) | 30 (2) | -16 (2) | -2 (2) | 2 (2) |
| Br(2) | 32 (1) | 35 (1) | 44 (1) | -6 (1) | -2 (1) | 2 (1) |
| C(21) | 23 (2) | 28 (2) | 32 (2) | -2 (2) | -4 (2) | 8 (2) |
| C(22) | 30 (2) | 26 (2) | 23 (2) | -3 (2) | -1 (2) | 2 (2) |
| C(23) | 24 (2) | 30 (2) | 28 (2) | -5 (2) | 2 (2) | 6 (2) |
| O(24) | 32 (2) | 47 (2) | 24 (1) | -4 (1) | 0 (1) | 4 (1) |
| C(25) | 23 (2) | 30 (2) | 23 (2) | -4 (2) | 0 (1) | 8 (2) |
| O(26) | 38 (2) | 38 (2) | 26 (2) | 0 (1) | 1 (1) | 8 (1) |
| C(27) | 21 (2) | 29 (2) | 27 (2) | -5 (2) | 0 (1) | 2 (2) |
| C(28) | 28 (2) | 49 (3) | 22 (2) | 2 (2) | 3 (2) | 4 (2) |
| C(29) | 41 (2) | 34 (2) | 34 (2) | -6 (2) | -8 (2) | 3 (2) |

Table 5. Hydrogen coordinates ($\times 10^4$) and isotropic displacement parameters ($\text{\AA}^2 \times 10^3$) for arm2.

| U(eq) | X | Y | Z |
|--------|-------|------|-------|
| H(11A) | 1948 | 6457 | -1152 |
| H(13A) | -3215 | 4155 | -481 |
| H(18A) | -365 | 6734 | -4025 |
| H(18B) | -2353 | 7503 | -3472 |
| H(18C) | -2776 | 7173 | -4537 |
| H(19A) | -720 | 4014 | -4191 |
| H(19B) | -2994 | 4709 | -4762 |
| H(19C) | -3031 | 3456 | -3835 |
| H(21A) | 3651 | -844 | 5567 |
| H(23A) | -2607 | 930 | 6040 |
| H(28A) | 204 | 1100 | 8769 |
| H(28B) | 1888 | 77 | 9547 |
| H(28C) | 730 | -558 | 8718 |
| H(29A) | 3450 | 2659 | 8374 |
| H(29B) | 5750 | 1921 | 8017 |
| H(29C) | 5028 | 1518 | 9130 |