

Environ. Sci. Technol., 1998, 32(7), 876-881, DOI:10.1021/es970743t

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Supplementary Figure 1. Diagram of the apparatus used for the recirculation experiments involving low nitric oxide concentrations.

Supplementary Figure 2. Plot of catalytic efficiency as a function of palladium loading on the activated carbon. A) Overall rates, as moles of N_2O product per min. B) Palladium efficiency measured as turnovers of NO per min (0.1 g catalyst, 10 mL 3 M NaOH, 840 torr NO, 22°C).

Supplementary Figure 3. Plot demonstrating the increase in catalysis rate obtained by reducing Pd(II) to Pd(0) on an activated carbon support (0.1 g catalyst, 10 mL 3 M NaOH, 840 torr NO, 22°C).

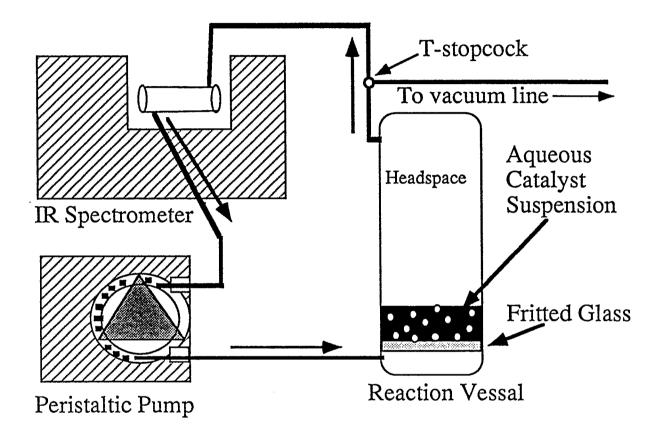
Supplementary Figure 4. Plot demonstrating the increase in catalysis rate obtained by reducing Pd(II) to Pd(0) on a barium sulfate support (0.1 g catalyst, 10 mL 3 M NaOH, 840 torr NO, 22°C).

Supplementary Figure 5. Plot of the pH of a solution over time when the NaOH concentration was the limiting reagent. Product formation became negligible below pH 8. The horizontal line at pH 6.3 represents the position of E = 0 calculated by the Nernst

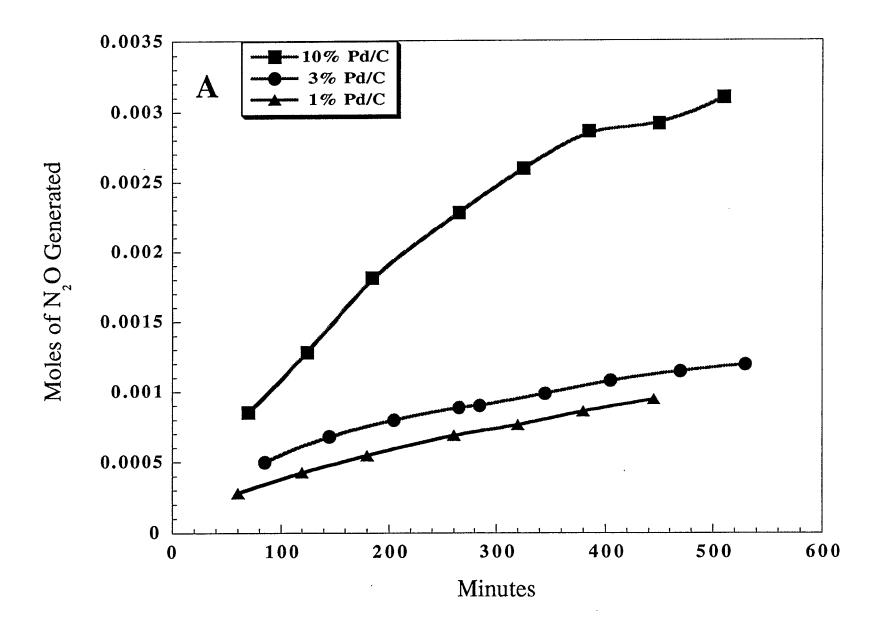
equation and assuming a hyponitrite intermediate (0.1 g catalyst, 10 mL initial pH 13, 840 torr NO, 22°C).

Supplementary Figure 6. Rate of N_2O formation above a dry, base-impregnated catalyst in H_2O -saturated nitric oxide. The plateau region where no additional N_2O forms corresponds to complete depletion of hydroxide (22°C).

Supplementary Figure 1.



Supplementary Figure 2A.



Supplementary Figure 2B.

