From Original Version 2.3 Correction Version 1\_5 (4/7/04)

#### SUPPORTING INFORMATION

### **ADDITION / CORRECTION FOR:**

Hornstein, B. J.; Finke, R. G. Chem. Mater, 2004, 16, 139-150.

Transition-Metal Nanocluster Kinetic and Mechanistic Studies Emphasizing Nanocluster Agglomeration: Demonstration of a Kinetic Method that Allows Monitoring of All Three Phases of Nanocluster Formation and Aging

Brooks J. Hornstein and Richard G. Finke\*

Colorado State University, Department of Chemistry, Fort Collins, Colorado 80523

# Appendix A: Treatment of the Kinetic Data

The following is a corrected version of the Supporting Information accompanying the original paper;<sup>1</sup> it replaces that Supporting Information except for the section entitled "The Experimental Methods to Determine y", Figures S1, S2 and S3.<sup>1</sup>

The revised equations are (3a)-(3e) and (4) below, six total equations which replace the five prior equations (3a)-(3d) and (4) in the main text elsewhere:<sup>1</sup>

$$\alpha x \quad \left[ \quad A \xrightarrow{k_1} \quad B \quad \right] \tag{3a}$$

$$\alpha(1-x) \left[ A + B \xrightarrow{k_2} 2B \right]$$
 (3b)

1400 
$$\left[ \begin{array}{c} \text{fast} \\ \text{B + cyclohex} ene + \text{H}_2 \rightarrow \text{B + cyclohex} ane \end{array} \right]$$
 (3c)

SUM: 
$$\alpha A + 1400 \text{ cyclohex} ene + 1400 \text{ H}_2 \rightarrow \alpha B + 1400 \text{ cyclohex} ene$$
 (3d)

$$1/2 \quad \left[ \begin{array}{c} B+B \xrightarrow{k_3} 2(1-y)B + 2yC \\ \text{(or } yB \rightarrow yC) \end{array} \right]$$
 (3e)

$$\frac{\text{NET}}{\text{REACTION:}} \qquad A \rightarrow (1-y)B + yC \tag{4}$$

The variable,  $\alpha$ , is experimentally the amount of A converted (measured as the amount of cyclooctane released; determined by GLC) at the time the cyclohexene has been fully consumed

<sup>&</sup>lt;sup>1</sup> Hornstein, B. J.; Finke, R. G. Chem. Mater, 2004, 16, 139-150.

(see equation (3d) above); that is,  $\alpha \approx 0.7$  for the experiment in Figure 2 of the main text with 2 equivalents of pyridine<sup>1</sup> (i.e., at ~2.5 h when the cyclohexene concentration is zero, only about 0.7 eq. of cyclooctane has evolved corresponding to the consumption of 0.7 eq A; approximately 10 h is required for the full consumption of A, see Figure S4).

From equation (3d) we can see equation A.1

A.1 
$$\left(\frac{1}{\alpha}\right) \frac{d[A]}{dt} = \left(\frac{1}{1400}\right) \frac{d[cyclohexene]}{dt}$$

Integrating from  $A = [A]_0$  to  $[A]_t$  and cyclohexene = [cyclohexene]\_0 to [cyclohexene]\_t yields equation A.2.

A.2 
$$\frac{1}{\alpha} ([A]_t - [A]_o) = \frac{1}{1400} ([cyclohexene]_t - [cyclohexene]_o)$$

A.3(a) but for 1400  $A_0 = \alpha[cyclohexene]_0$ , it follows that

A.3(b) [cyclohexene]<sub>t</sub> = 
$$\frac{1400}{\alpha}$$
[A]<sub>t</sub>

Differentiating equation A.3(b) with respect to time yields equation A.3 (c)

A.3(c) 
$$\frac{d[cyclohexene]}{dt} = \frac{1400}{\alpha} \frac{d[A]}{dt}$$

# MacKinetics Numerical Integration Treatment of the Cyclohexene vs Time Data

The  $H_2$  loss vs time for the cyclohexene hydrogenation, equation (3d), is followed vs time with a high precision pressure transducer. Those  $H_2$  vs time data are then converted to [cyclohexene] loss vs time data via PV = nRT, the known volume of the system, and using the 1:1  $H_2$  to cyclohexene stoichiometry, equation (3d).

The kinetic equations entered into MacKinetics correspond to equations (3a), (3b) and (3e), namely equations A.4-A.6:

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A.4 A 
$$\xrightarrow{k_1}$$
 B

A.5 A + B  $\xrightarrow{k_2}$  2B

A.6 B + B  $\xrightarrow{k_3}$  C (where C = B·B, i.e., B<sub>2</sub>)

(i.e., 2B  $\xrightarrow{}$  C)

The corresponding differential equations are A.7-A.9:

A.7 
$$\frac{-d[A]}{dt} = k_1[A] + k_2[A][B]$$
A.8 
$$\frac{d[B]}{dt} = k_1[A] + k_2[A][B] - 2k_3[B]^2$$

$$= \frac{-d[A]}{dt} - 2k_3[B]^2$$
A.9 
$$\frac{d[C]}{dt} = k_3[B]^2$$

$$= -\frac{1}{2} \left( \frac{d[A]}{dt} + \frac{d[B]}{dt} \right)$$

The mass balance equation is A.10

A.10 
$$[A]_0 = [A]_t + [B]_t + 2[C]_t$$

(As a check d[A]/dt = 0 = d[A]/dt + d[B]/dt + 2d[C]/dt, and if one adds -A.7 + A.8 + 2A.9, that sum in fact = 0.)

However, for the ease of analysis of the data, we enter the [cyclohexene]<sub>0</sub> and [cyclohexene]<sub>1</sub> vs time data into MacKinetics. That is, the actual system numerically integrated is:

A.11 cyclohexene 
$$\xrightarrow{k_{1 \text{ obs}}}$$
 B'

(i.e., A'  $\xrightarrow{k_{1 \text{ obs}}}$  B' where A' = cyclohexene)

A.12 cyclohexene + B'  $\xrightarrow{k_{2 \text{ obs}}}$  2B'

(i.e., A' + B'  $\xrightarrow{k_{2 \text{ obs}}}$  2B')

A.13 B' + B'  $\xrightarrow{k_{3 \text{ obs}}}$  C'

The differential equations corresponding to A.11-A.13 are:

A.14 
$$\frac{-\text{d[cyclohexene]}}{\text{dt}} = \frac{-\text{d[A']}}{\text{dt}} = k_{1\text{obs}}[A'] + k_{2\text{obs}}[A'][B']$$
A.15 
$$\frac{d[B']}{dt} = k_{1\text{obs}}[A'] + k_{2\text{obs}}[A'][B'] - 2k_{3\text{obs}}[B']^2$$
A.16 
$$\frac{\text{d[C']}}{\text{dt}} = k_{3\text{obs}}[B']^2$$

The mass balance equation A.17 is easily derived by adding  $\frac{d[A']}{dt} + \frac{d[B']}{dt} + 2\frac{d[C']}{dt}$ , showing

this equals zero, and then integrating (where  $[B]_o = [C]_o = 0$ ).

A.17 
$$[A]_o = [A]_t + [B]_t + 2[C]_t \text{ or } [A]_o - [A]_t = [B]_t + 2[C]_t$$

From equations A.3(a) and A.3(b) we are reminded that:

A.3(a) [cyclohexene]<sub>0</sub> = 
$$[A']_0 = \frac{1400}{\alpha} [A]_0$$
  
A.3(b) [cyclohexene]<sub>t</sub> =  $[A']_t = \frac{1400}{\alpha} [A]_t$ 

Combining these equations with A.17 yields:

A.18(a) 
$$[A']_o - [A']_t = \frac{1400}{\alpha} ([A]_o - [A]_t) = [B']_t + 2[C']_t$$

But substituting equation A.10 yields

A.18(b) 
$$\frac{1400}{G}([B]_t + 2[C]_t) = [B']_t + 2[C']_t$$

From which is follows that

A.18(c) 
$$\frac{1400}{\alpha} [B]_t + \left(\frac{1400}{\alpha}\right) 2[C]_t = [B']_t + 2[C']_t$$

Which leads to the following identities:

A.18(d) 
$$\frac{1400}{\alpha}$$
[B]<sub>t</sub> = [B']<sub>t</sub>

A.18(e) 
$$\frac{1400}{\alpha} [C]_t = [C']_t$$

Now we can substitute A.3(b), A.18(d) and A.18(e) into equations A.14, A.15 and A.16 to derive, ultimately, the desired relationship between  $k_{1obs}$ ,  $k_{2obs}$ ,  $k_{3obs}$  and  $k_1$ ,  $k_2$  and  $k_3$ .

A.19(a) 
$$\frac{1400}{\alpha} \frac{-d[A]}{dt} = \left(\frac{1400}{\alpha}\right) k_{1obs}[A] + \left(\frac{1400}{\alpha}\right)^2 k_{2obs}[A][B]$$
for A.19(b) 
$$\frac{-d[A]}{dt} = k_{1obs}[A] + \left(\frac{1400}{\alpha}\right) k_{2obs}[A][B]$$
A.20(a) 
$$\left(\frac{1400}{\alpha}\right) \frac{d[B]}{dt} = \left(\frac{1400}{\alpha}\right) k_{1obs}[A] + \left(\frac{1400}{\alpha}\right)^2 k_{2obs}[A][B] - \left(\frac{1400}{\alpha}\right)^2 2k_{3obs}[B]^2$$
or A.20(b) 
$$\frac{d[B]}{dt} = k_{1obs}[A] + \left(\frac{1400}{\alpha}\right) k_{2obs}[A][B] - \left(\frac{1400}{\alpha}\right) 2k_{3obs}[B]^2$$
A.21(a) 
$$\left(\frac{1400}{\alpha}\right) \frac{d[C]}{dt} = \left(\frac{1400}{\alpha}\right)^2 k_{3obs}[B]^2$$
or A.21(b) 
$$\frac{d[C]}{dt} = \left(\frac{1400}{\alpha}\right) k_{3obs}[B]^2$$

Finally, a comparison of equations A.7, A.8 and A.9 with A.19(b), A.20(b) and A.21(b) yields the identities:

A.22 
$$k_{1} = k_{1\text{obs}}$$
A.23 
$$k_{2} = \left(\frac{1400}{\alpha}\right) k_{2\text{obs}}$$
A.24 
$$k_{3} = \left(\frac{1400}{\alpha}\right) k_{3\text{obs}}$$

## **Experimental Methods to Determine y**

This section is unchanged from the prior Supporting Information. Note that for the net reaction,  $A \rightarrow (1-y)B + yC$  (equation 4 herein), where y = y(t), the estimate of y = 0.45 determined on p. 146 elsewhere<sup>1</sup> ) for the case where 2 equivalents of pyridine were added) is just

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a single value of the variable y as detailed in the main text and the Experimental section elsewhere.<sup>1</sup>

# Actual MacKinetics Treatment of the Raw Data Set Prior to Measuring y

This section can be completely discarded; it is replaced by, for example, equations A.22 - A.24 in this revised Supporting Information.

### Figures S1, S2 and S3

Each of these Figures given in the prior Supporting Information is correct and remains unchanged.