Supporting Information

Figure S1. Ir L_{III} -edge XANES spectra for $(Ir^{3+})_{40}G4OH$ complex and $IrCl_3$ aqueous solutions before and after reduction with NaBH₄.

Figure S2. CO adsorption after a) H_2 at different temperatures, b) H_2 at 400 °C for different times.

Figure S3. HRTEM micrographs and particle size distribution histograms of 1 wt.% a) $Ir_{40}G4OH/\gamma-Al_2O_3$, b) $Ir/\gamma-Al_2O_3$ treated with reduction treatment and c) $Ir_{40}G4OH/\gamma-Al_2O_3$, d) $Ir/\gamma-Al_2O_3$ treated with oxidation/reduction treatment.

Figure S4. Typical benzonitrile concentration versus time plot obtained for the hydrogenation of benzonitrile over supported Ir catalysts.

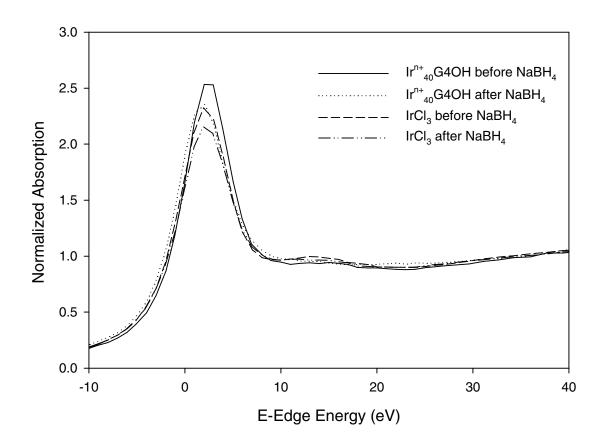


Figure S1.

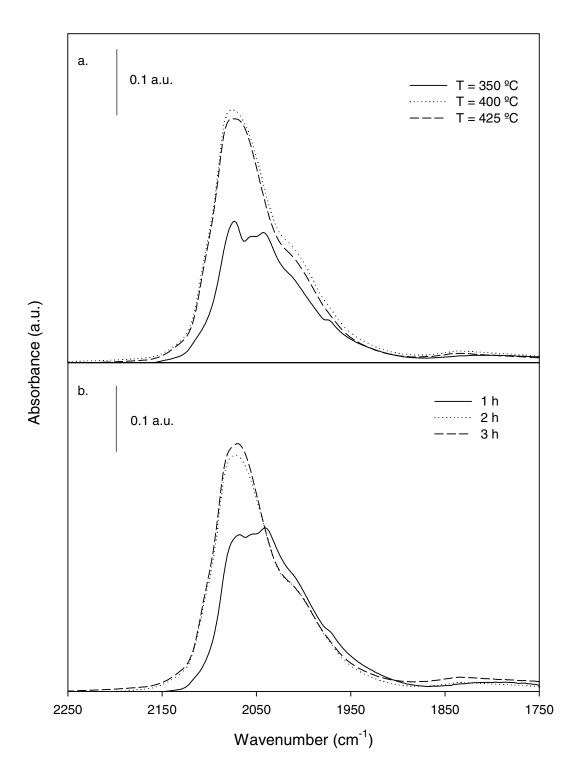


Figure S2.

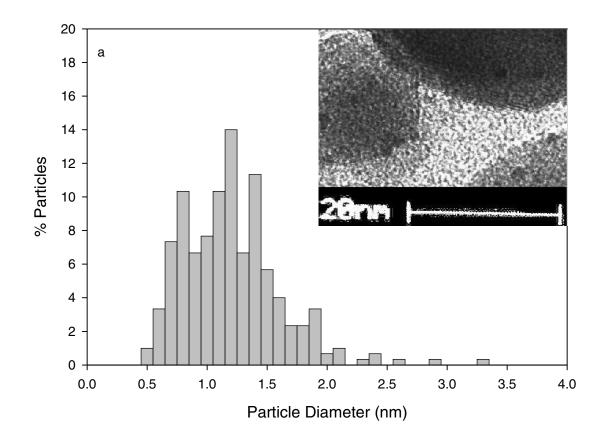


Figure S3.

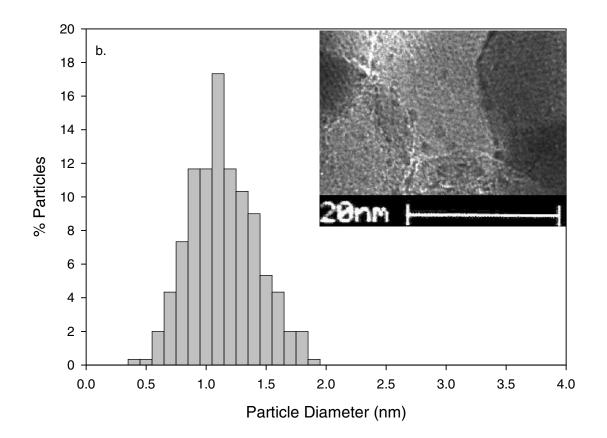


Figure S3. (cont.)

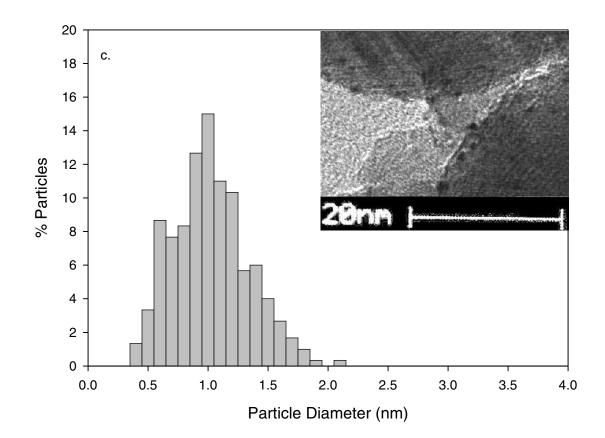


Figure S3. (cont.)

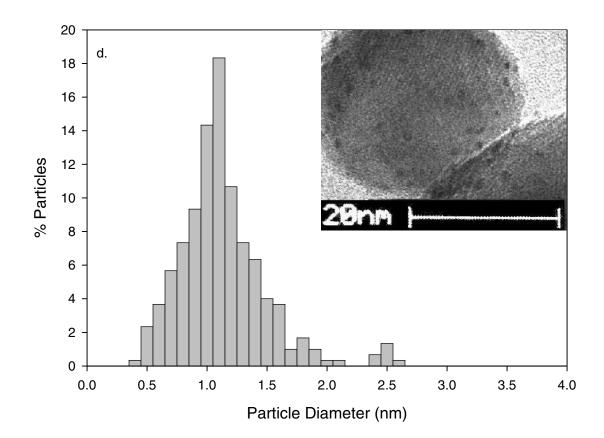
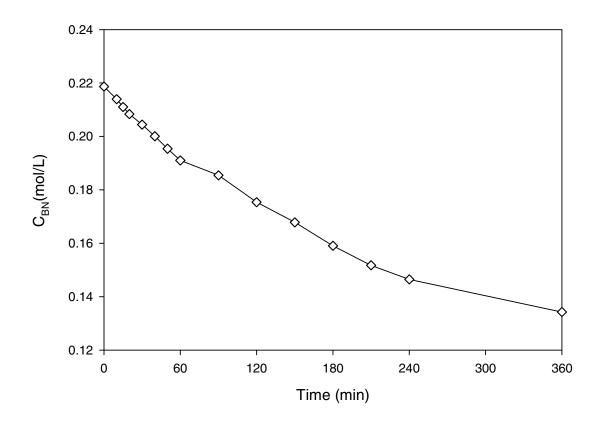


Figure S3. (cont.)



Initial rate was calculated by fitting the benzonitrile concentration versus time with an appropriate polynomial during the initial stages of the reaction and determining $-\left(\frac{dC_{BN}}{dt}\right)_{t=0}$.

Selectivity toward dibenzylamine (DBA) was calculated at 20 % benzonitrile conversion using the following formula:

$$S_{DBA} = \frac{n_{DBA}}{\sum v_i n_i}$$

where, n_i is the moles of the product, v_i is the stoichiometric number of the product

Figure S4.