Production of fatty acid butyl esters using the low cost naturally immobilized

Carica papaya lipase

Erzheng Su^{a,b,*}, Dongzhi Wei^{c,**}

^aEnzyme and Fermentation Technology Laboratory, College of Light Industry Science and Engineering,

Nanjing Forestry University, Nanjing 210037, P. R. China.

^bDepartment of Chemistry, Massachusetts Institute of Technology Cambridge, Massachusetts 02139, USA.

^cState Key Laboratory of Bioreactor Engineering, New World Institute of Biotechnology, East China University of Science and Technology, Shanghai 200237, P.R. China.

* Corresponding author:

Erzheng Su

Tel. +86 25 85428906 Fax: +86 25 85428906 E-mail address: ezhsu@njfu.edu.cn

****** Corresponding author:

Dongzhi Wei

Tel. +86 21 64252078 Fax: +86 21 64250068 E-mail address: dzhwei@ecust.edu.cn



Figure S1. The schematic diagram of naturely immobilized CPL packed-bed reactor for continuous biodiesel production. (1) Substrate reservoir, (2) reactor temperature controller, (3) peristaltic pump, (4) water jacket, (5) bed of CPL, (6) three-way valve, (7) product reservoir, (8) sampling, (9) cooling/heating water; and (10) recirculation. The dashed line describes the flow of materials for recirculating operation; the dotted line describes the flow for the continuous mode.



Figure S2. pCPL-GD-catalyzed alcoholysis of soybean oil with butanol as the solvent and acyl acceptor at the same time. Reaction conditions: 50 °C, 150 rpm, 10% pCPL-GD based on oil weight, a_w =0.225.



Figure S3. Residence time course of the pCPL-GD-catalyzed alcoholysis of soybean oil with n-butanol in the packed bed reactor. Reaction condition: 55° C, alcohol/oil molar ratio of 12:1, a_w =0.225.