## Supporting Information

## Rh/ZrP<sub>2</sub>O<sub>7</sub> as an Efficient Automotive Catalyst for NO<sub>x</sub> Reduction under Slightly Lean Conditions

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**Figure S1.** XRD patterns of as-prepared a) AlPO<sub>4</sub>, b) YPO<sub>4</sub>, c)  $ZrP_2O_7$  and d) LaPO<sub>4</sub>. **Figure S2.** *In situ* diffuse reflectance FT-IR spectra of adsorbed species formed on  $ZrP_2O_7$  and  $ZrO_2$  powders in gas mixtures of a) 0.8% C<sub>3</sub>H<sub>6</sub>, 0.5% O<sub>2</sub>, and He balance (rich), b) 0.35% C<sub>3</sub>H<sub>6</sub> + 3.25% O<sub>2</sub>, and He balance (lean), and c) 1% C<sub>3</sub>H<sub>6</sub> and He balance at 300 °C.

**Figure S3.** Fourier transforms of  $k^3$ -weighted Rh K-edge EXAFS of supported Rh catalysts without phase shift corrections.

**Figure S4.** FT-IR differential spectra of pyridine adsorbed onto  $ZrP_2O_7$  and  $ZrO_2$  at 50 °C and subsequent evacuation.

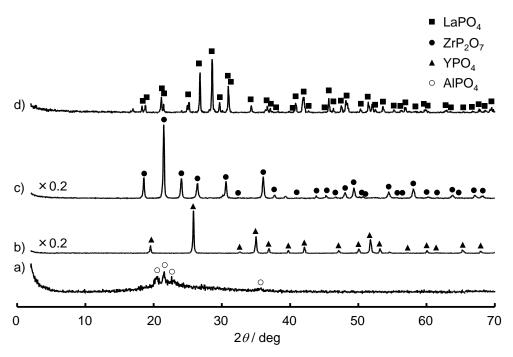
**Table S1**. Composition of simulated exhaust gas mixtures (NO-CO-C<sub>3</sub>H<sub>6</sub>-O<sub>2</sub>-H<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for  $14.2 \leq A/F \leq 14.8$  in test mode A.

**Table S2**. Composition of simulated exhaust gas mixtures (NO-CO-C<sub>3</sub>H<sub>6</sub>-O<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for 14.6  $\leq$  A/F  $\leq$  15.3 in test mode B.

**Table S3**. Composition of simulated exhaust gas mixtures (NO-CO-O<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for  $14.6 \leq A/F \leq 15.3$  in test mode C.

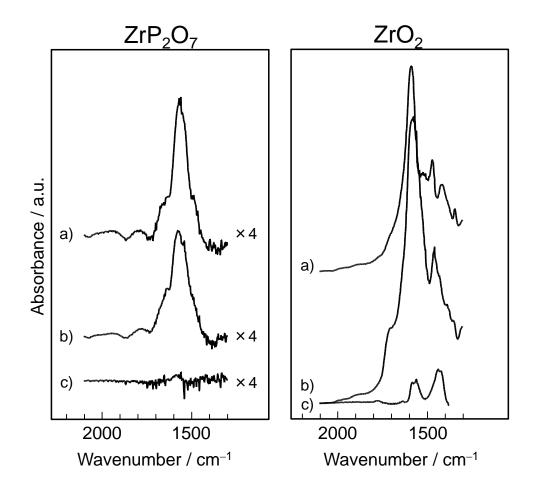
**Table S4.** Composition of simulated exhaust gas mixtures (NO-C<sub>3</sub>H<sub>6</sub>-O<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for 14.6  $\leq$  A/F  $\leq$  15.3 in test mode D.

Table S5. Fitting results of Rh K-edge EXAFS analysis



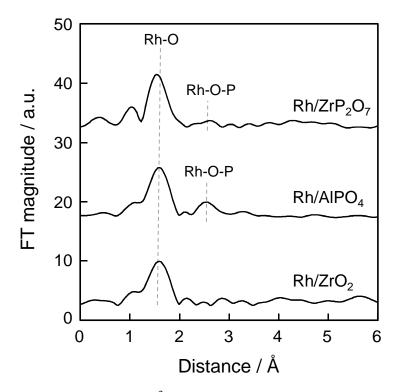
**Figure S1.** XRD patterns of as-prepared a) AlPO<sub>4</sub>, b) YPO<sub>4</sub>, c) ZrP<sub>2</sub>O<sub>7</sub> and d) LaPO<sub>4</sub>.

Figure S1 shows the XRD patterns of four types of metal phosphates after calcination. Diffraction peaks are attributed to monophasic metal phosphates with hexagonal AlPO<sub>4</sub> tridymite-type structure ( $P6_3mc$ , 5.097 Å, 8.344 Å)<sup>1</sup>, tetragonal YPO<sub>4</sub> with xenotime-type structure, ( $I4_1/amdZ$ , 6.882 Å, 6.882 Å, 6.018 Å)<sup>2</sup>, monoclinic LaPO<sub>4</sub> with monazite-type structure, ( $P12_1/n$  1, 6.825 Å, 7.057 Å, 6.482 Å, 103.2°)<sup>3</sup> and cubic ZrP<sub>2</sub>O<sub>7</sub> (Pa-3, 8.293 Å)<sup>4</sup>.

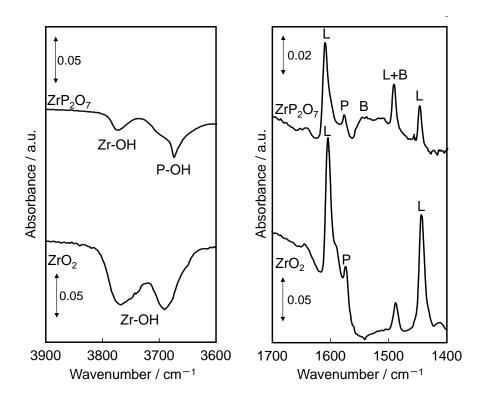


**Figure S2.** In situ diffuse reflectance FT-IR spectra of adsorbed species formed on  $ZrP_2O_7$  and  $ZrO_2$  powders in gas mixtures of a) 0.8%  $C_3H_6$ , 0.5%  $O_2$ , and He balance (rich), b) 0.35%  $C_3H_6$  + 3.25%  $O_2$ , and He balance (lean), and c) 1%  $C_3H_6$  and He balance at 300 °C.

 $C_3H_6$  was adsorbed onto  $ZrP_2O_7$  and  $ZrO_2$  in the presence of  $O_2$  to form aldehyde and carboxylate species, respectively. The intensity of observed bands for these Rh-unloaded support materials were as the same as those for Rh-loaded catalysts (**Figures 8** and 9). These partially oxidized species were therefore adsorbed on the surface of support materials. Also, these species were formed in a similar way under the rich and lean conditions (a and b), but they were significantly decreased in the absence of  $O_2$  (c).



**Figure S3.** Fourier transforms of  $k^3$ -weighted Rh K-edge EXAFS of supported Rh catalysts without phase shift corrections. See **Table S5** for curve-fitting results and explanation of this figure.



**Figure S4**. FT-IR differential spectra of pyridine adsorbed onto  $ZrP_2O_7$  and  $ZrO_2$  at 50 °C and subsequent evacuation. P: physisorbed pyridine, B: pyridine chemisorbed on Brønsted acid sites, L: pyridine chemisorbed on Lewis acid sites.

In situ FT-IR of pyridine chemisorption was carried out at 50 °C after dehydration at 500 °C in a He flow. The spectra obtained after subsequent evacuation at 50 °C were referenced to that of the sample in a He flow just before pyridine adsorption.  $ZrP_2O_7$  yielded bands assignable to pyridine coordinated to Lewis acid site (L: 1610, 1492, and 1448 cm<sup>-1</sup>) and to pyridinium ion adsorbed on Brønsted site (B: 1545, 1492 cm<sup>-1</sup>) as reported by several researchers.<sup>5-7</sup> Simultaneously with the appearance of these bands, P–OH (3676 cm<sup>-1</sup>) and Zr–OH (3773 cm<sup>-1</sup>) bands were weakened. These results suggest that surface hydroxyl groups of  $ZrP_2O_7$  act as both Lewis and Brønsted acid sites. By contrast,  $ZrO_2$  yielded bands assigned only to Lewis acid site (L: 1604, 1488, and 1444 cm<sup>-1</sup>).

$\Pi_2(0)$ for $\Pi_2(2)$ and $\Pi_2$								
A/F <sup>a</sup>	14.2	14.4	14.5	14.6	14.7	14.8		
CO / %	1.00	0.73	0.60	0.50	0.44	0.40		
H <sub>2</sub> / %	0.33	0.24	0.20	0.17	0.15	0.13		
C <sub>3</sub> H <sub>6</sub> / ppm	400	Ļ	$\leftarrow$	$\leftarrow$	Ļ	$\leftarrow$		
NO / ppm	500	$\leftarrow$	$\leftarrow$	$\leftarrow$	$\leftarrow$	$\leftarrow$		
O <sub>2</sub> / %	0.35	0.41	0.45	0.50	0.55	0.60		
CO <sub>2</sub> / %	14.0	Ļ	$\leftarrow$	$\leftarrow$	Ļ	$\leftarrow$		
H <sub>2</sub> O / %	10.0	$\leftarrow$	$\leftarrow$	$\leftarrow$	$\leftarrow$	$\leftarrow$		

Table S1. Composition of simulated exhaust gas mixtures (NO-CO-C<sub>3</sub>H<sub>6</sub>-O<sub>2</sub>-H<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for  $14.2 \leq A/F \leq 14.8$  in test mode A.

<sup>a</sup> The A/F value is calculated according to the literature<sup>8</sup> using following excess oxygen ratio of the simulated gas feed.

Amount of oxygen in gas feed Excess oxygen ratio  $= \frac{\text{Amount of oxygen in gas recu$  $Amount of oxygen required for complete oxidation}$ 

 $=\frac{2 \times p_{02} + p_{N0}}{9 \times p_{C3H6} + p_{C0} + p_{H2}}$ 

Table S2. Composition of simulated exhaust gas mixtures (NO-CO-C<sub>3</sub>H<sub>6</sub>-O<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for 14.6  $\leq$  A/F  $\leq$  15.3 in test mode B.

A/F <sup>a</sup>	14.6	14.7	14.8	14.9	15.0	15.1	15.2	15.3
CO / %	0.69	0.59	0.52	0.52	0.50	0.40	0.40	0.30
C <sub>3</sub> H <sub>6</sub> / ppm	400	$\leftarrow$	$\downarrow$	$\downarrow$	$\downarrow$	$\downarrow$	$\downarrow$	$\leftarrow$
NO / ppm	500	$\leftarrow$	Ļ	$\downarrow$	$\downarrow$	$\downarrow$	$\downarrow$	$\leftarrow$
O <sub>2</sub> / %	0.50	0.55	0.60	0.69	0.81	0.84	0.96	0.93
CO <sub>2</sub> / %	14.0	$\leftarrow$	Ļ	$\downarrow$	$\downarrow$	Ļ	Ļ	$\leftarrow$
H <sub>2</sub> O / %	10.0	$\leftarrow$						

<sup>*a*</sup> See Table S1.

A/F <sup>a</sup>	14.6	14.7	14.8	14.9	15.0	15.1	15.2	15.3
CO / %	0.69	0.59	0.52	0.52	0.50	0.40	0.40	0.30
NO / ppm	500	Ļ	Ļ	Ļ	Ļ	Ļ	Ļ	$\leftarrow$
O <sub>2</sub> / %	0.32	0.33	0.34	0.40	0.46	0.43	0.49	0.41
CO <sub>2</sub> / %	14.0	Ļ	Ļ	Ļ	$\downarrow$	Ļ	Ļ	$\downarrow$
$H_2O$ / %	10.0	$\leftarrow$						

**Table S3**. Composition of simulated exhaust gas mixtures (NO-CO-O<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for  $14.6 \le A/F \le 15.3$  in test mode C.

<sup>*a*</sup> See **Table S1**.

**Table S4**. Composition of simulated exhaust gas mixtures (NO-C<sub>3</sub>H<sub>6</sub>-O<sub>2</sub>-CO<sub>2</sub>-H<sub>2</sub>O) for 14.6  $\leq$  A/F  $\leq$  15.3 in test mode D.

A/F <sup>a</sup>	14.6	14.7	14.8	14.9	15.0	15.1	15.2	15.3
C <sub>3</sub> H <sub>6</sub> / ppm	400	Ļ	$\leftarrow$	Ļ	Ļ	Ļ	Ļ	$\leftarrow$
NO / ppm	500	Ļ	$\leftarrow$	Ļ	Ļ	Ļ	Ļ	$\leftarrow$
O <sub>2</sub> / %	0.16	0.19	0.23	0.27	0.33	0.38	0.44	0.50
CO <sub>2</sub> / %	14.0	Ļ	$\leftarrow$	Ļ	Ļ	Ļ	$\downarrow$	$\downarrow$
H <sub>2</sub> O / %	10.0	$\leftarrow$	$\leftarrow$	$\leftarrow$	$\downarrow$	$\leftarrow$	$\leftarrow$	$\leftarrow$

<sup>*a*</sup> See **Table S1**.

Catalust	chall	CN <sup><i>a</i></sup>	r/Å <sup>b</sup>	$\sigma^2 / 10^{-2} \text{ Å}^{2 c}$
Catalyst	shell	(±0.2)	(±0.03)	(±0.02)
2 wt% Rh/ZrP <sub>2</sub> O <sub>7</sub>	Rh–O	2.9	2.01	0.15
	Rh–O–P	0.89	3.12	0.36
0.4 wt% Rh/AlPO <sub>4</sub>	Rh–O	4.3	2.03	0.15
	Rh–Rh	0.32	2.69	0.42
	Rh–O–P	1.4	3.09	0.36
	Rh–O–Rh	0.19	3.54	0.64
2 wt% Rh/ZrO <sub>2</sub>	Rh–O	4.1	2.04	0.15

Table S5. Fitting results of Rh K-edge EXAFS analysis

Interval of *k*-space to *r*-space of FT is 3.0-14.0 Å<sup>-1</sup>.

<sup>*a*</sup>Coordination number.

<sup>*b*</sup>Atomic distance.

<sup>*c*</sup>Debye-Waller factor.

**Table S5** compares structural parameters for as-prepared supported Rh catalysts in **Figure S3**. These catalysts showed an intense peak at approximately 0.2 nm, which was attributed to a Rh–O shell of Rh oxide (Rh<sub>2</sub>O<sub>3</sub>). In the second coordination, a contribution of the Rh–O–P shell was observed in Rh/ZrP<sub>2</sub>O<sub>7</sub> as was reported for Rh/AlPO<sub>4</sub> in our previous manuscript,<sup>9</sup> suggesting interfacial bonding between Rh and a phosphate unit (PO<sub>4</sub>). Rh/ZrO<sub>2</sub> showed no such second coordination shell indicative of the metal-support bonding. The higher Rh loading (2 wt%) was used for Zr-containing supports to ensure the to ensure a good quality signal for curve fitting analysis.

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