The Superior Performance of Sol-Gel Made Ce-O-P Catalyst for Selective Catalytic Reduction of NO with NH₃

Weiyuan Yao,^{1†} Yue Liu,^{*1†} Xiaoqiang Wang,^{1†} Xiaole Weng,^{1†} Haiqiang Wang,^{1†} and Zhongbiao Wu^{1†,2‡}

^{1†}Department of Environmental Engineering, Zhejiang University, 866 Yuhangtang Road, Hangzhou, 310058, P. R. China

^{2‡}Zhejiang Provincial Engineering Research Center of Industrial Boiler & FurnaceFlue Gas Pollution Control, 866 Yuhangtang Road, Hangzhou, 310058, P. R. China

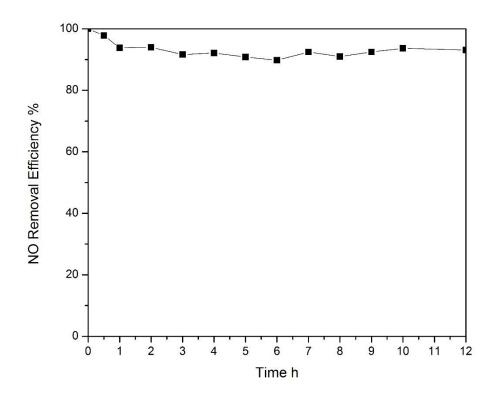
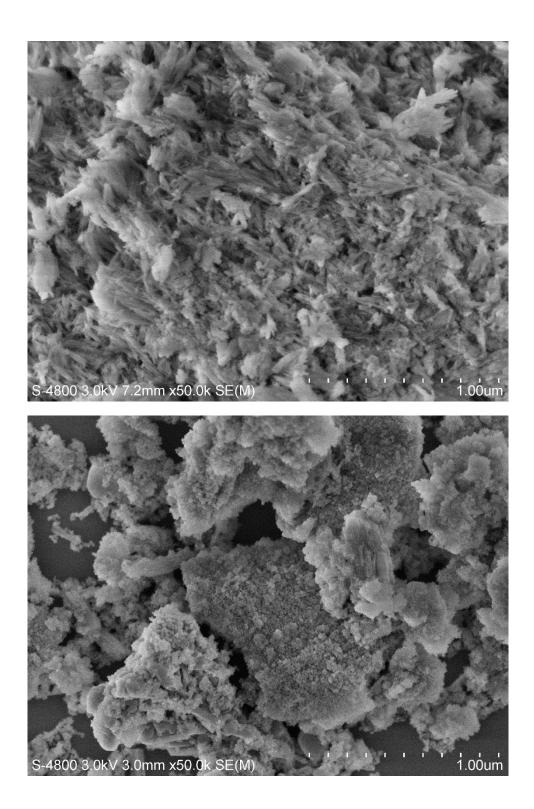


Figure S1. H₂O duration of Ce–O–P-SG catalyst in SCR process. ($[NH_3] = [NO] = 600 \text{ ppm}, [O_2] = 3 \%, [H_2O] = 5 \text{ vol }\%, N_2 \text{ balance, GHSV} = 40000 \text{ h}^{-1}$)



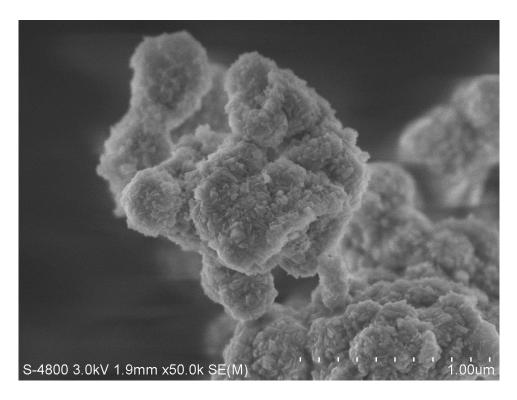


Figure S2. SEM results of the Ce–O–P catalysts: (a) Ce–O–P-SG, (b) Ce–O–P-HT, (c) Ce–O–P-CP.

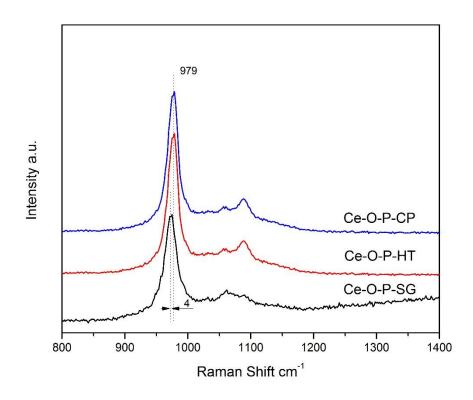


Figure S3. Raman spectra (n = 514 nm) of Ce–O–P-SG, Ce–O–P-HT and Ce–O–P-CP catalysts.

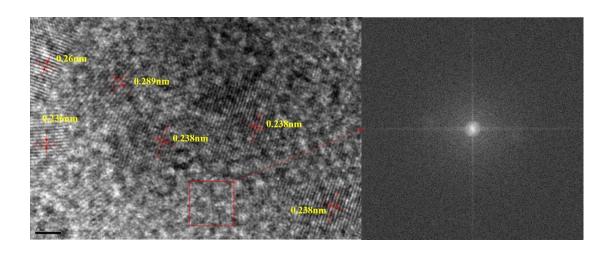


Figure S4. HR-TEM image of Ce–O–P-SG catalyst, the image in right is the FFT

pattern of region in red square and reveals no crystal in the region.

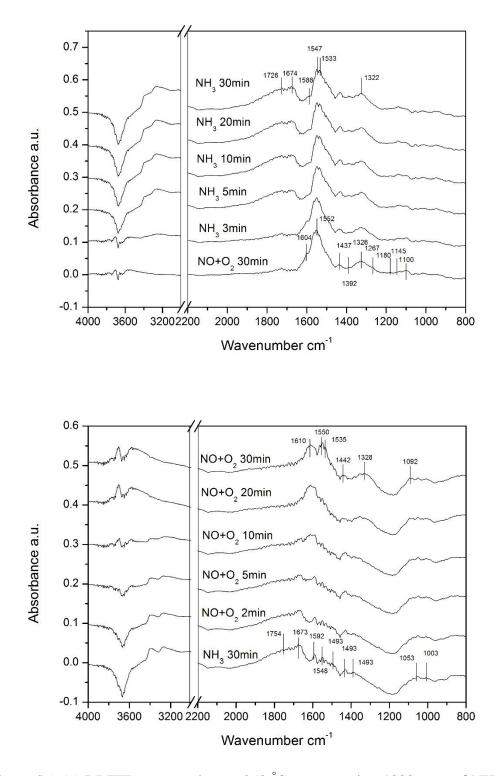


Figure S5. (a) DRIFT spectra taken at 250 °C upon passing 1000 ppm of $NH_3 + 3 \%$ O₂/He over the NO + O₂ pre-sorbed on Ce–O–P-SG catalyst at different time; (b) DRIFT spectra taken at 250 °C upon passing 1000 ppm of NO₂ + 3 % O₂/He over the NH₃ pre-sorbed on Ce–O–P-SG catalyst at different time.

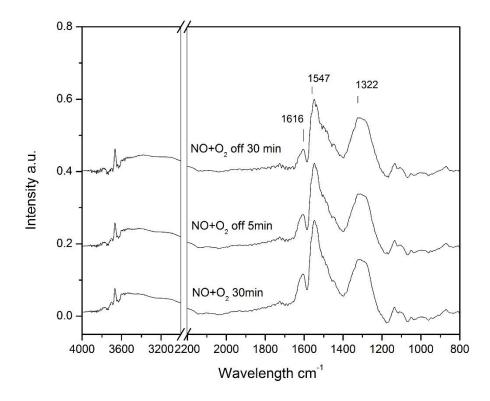


Figure S6. DRIFT spectra taken at 250 $^{\circ}$ C upon passing pure He over 1000 ppm of NO + 3 % O₂ pre-sorbed on Ce–O–P-SG catalyst at different time.

Catalysts	Ce %	Р%	Ce/P	0 %
Ce-O-P-SG	16.7	18.7	0.89	64.6
Ce-O-P-HT	17.5	19.6	0.89	63.0
Ce-O-P-CP	19.2	21.7	0.88	59.1

 Table S1 Bulk atomic concentration of the Ce-O-P catalysts.

Table S2 S deposition on the Ce-O-P catalysts which were pretreated in SCR processat the presence of 100 ppm SO2 and 5 vol. % H2O for 10 h

Catalysts	EDX %	XPS %
Ce-O-P-SG	1.56	1.37
Ce-O-P-HT	0.65	0.87
Ce-O-P-CP	0.59	0.58