Supplementary information

Table 8 of the paper. The bio-oil components distribution. In this version with data on wet basis

included.

| | On wet basis | | | On dry basis | | | | |
|-------------------------------------|--------------|-------|--------|--------------|------|-------|--------|-------|
| Pyrolysis temperature (°C) | Wood | Straw | Lignin | Algae | Wood | Straw | Lignin | Algae |
| | oil | oil | oil | Oil | oil | oil | oil | oil |
| Water (wt.%) ^a | 27.3 | 25.7 | 27.4 | 26.6 | - | - | - | - |
| Light fraction (wt %) ^b | 29.7 | 28.8 | 25.5 | 16.1 | 40.9 | 38.8 | 35.2 | 21.9 |
| Medium fraction (wt %) ^c | 22.5 | 22.9 | 28.6 | 30.8 | 30.9 | 30.8 | 39.4 | 42.0 |
| Heavy fraction (wt %) ^d | 3.0 | 2.8 | 2.5 | 3.8 | 4.1 | 3.8 | 3.4 | 5.2 |
| Residual ^e (char) | 17.5 | 19.8 | 15.9 | 22.7 | 24.1 | 26.6 | 21.9 | 30.9 |

^adetermined by Karl Fischer, ^bdetermined as the mass loss appearing from room temperature to 200 °C of the TGA curve and substrated the water content, ^cdetermined as the mass loss from 200 to 500 °C on TGA curve, ^ddetermined as the mass loss from 500 to 950 °C on TGA curve, ^ethe residual char after heating to 950 °C.

Table 10 of the paper. The bio-oil components distribution. In this version with data on wet basis

included.

| | On | wet basis | On dry basis | | |
|-------------------------------------|------------|-------------------|--------------|-------------------|--|
| Pyrolysis temperature (°C) | Lignin oil | Lignin bottom oil | Lignin oil | Lignin bottom oil | |
| Water (wt.%) ^a | 27.4 | 15.3 | - | - | |
| Light fraction (wt %) ^b | 25.5 | 7.7 | 35.2 | 9.1 | |
| Medium fraction (wt %) ^c | 28.6 | 50.4 | 39.4 | 59.5 | |
| Heavy fraction (wt %) ^d | 2.5 | 4.1 | 3.4 | 4.8 | |
| Residual ^e (char) | 15.9 | 22.5 | 21.9 | 26.6 | |

^adetermined by Karl Fischer, ^bdetermined as the mass loss appearing from room temperature to 200 $^{\circ}$ of the TGA curve and substrated the water content, ^cdetermined as the mass loss from 200 to 500 $^{\circ}$ on TGA curve, ^ddetermined as the mass loss from 500 to 950 $^{\circ}$ on TGA curve, ^e the residual char after heating to 950 $^{\circ}$ C.

Some comments regarding the use of isopropanol for condensation of the bio oil from the pyrolysis gas

In this study isopropanol was used as a condensing solvent, and after the pyrolysis experiments the isopropanol was removed by a rotary vacuum evaporator at a temperature of 30 °C and using a soft sub-pressure. The isopropanol solvent removal procedure are mentioned by I.Fonts et al. (Ind. Eng. Chem. Res., Vol 48, No .4, 2009; Anal. Appl. Pyrolysis 85 (2009) 184-191). A pure isopropanol (having a boiling point of 82 °C at atmospheric pressure) was used to determine a set point pressure (the temperature is fixed 30 °C to avoid an aging of the bio-oil) in which the isopropanol start to evaporate. The mixture of isopropanol and bio-oil was distilled at those conditions. Regarding low boiling point species in the bio oil acetic acid is considered to be present at a relatively high concentration in the bio-oil and has a boiling point of 119 °C (at atmospheric pressure) next to water with a boiling point of 100 °C (at atmosphere pressure). The bio-oil components were identified with GC-MS (The GC-MS identified components of lignin and wood oil are shown in table 1). We used a wood bio-oil (that has the highest acetic acid concentration in the bio-oil) to quantify the acetic acid concentrations of a bio-oil liquid sample including isopropanol and the bio-oil sample after solvent removal (see figure 1). It was observed that 37% the acetic acid (corresponding to 1.9 % wt of the wood bio-oil) is lost during solvent removal. Also wood oil was used as condensing solvent during a wood pyrolysis experiment and the pH value of the obtained bio-oil was 3.04. This is slightly lower than when using isopropanol as solvent where a pH value of 3.2 is obtained. Thus the isopropanol solvent removal has a small influence on the pH value of bio-oil.

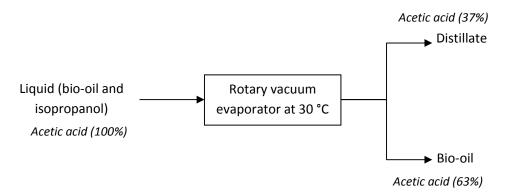


Figure 1: Distribution of acetic acid after removing solvent

| | Lignin oil | Wood oil | Boiling point (°C) |
|--|------------|----------|--------------------|
| Acids | 6.15 | 25.88 | |
| Acetic acid | 6.15 | 25.88 | 119 |
| Nonaromatic ketones | 2.55 | 13.3 | |
| Hydroxyacetone | 2.55 | 7.16 | 146 |
| 1,2-ethanediol, monoacetate | a | 3.93 | 182 |
| 1-(acetyloxy)-2-propanone | - | 0.73 | 176 |
| 2,3-butanedione | - | - | |
| 2-hydroxy-3-methyl- 2-cyclopenten-1-one | - | 0.69 | |
| 2-methyl-cyclopentanone | - | 0.79 | 141 |
| Furans | 1.01 | 8.61 | |
| Furfural | 0.51 | 5.16 | 162 |
| 5-methyl-furfural | - | - | |
| Furfuryl alcohol | 0.50 | 1.35 | 170 |
| 5-hydroxymethylfurfural | - | - | |
| γ-crotonolactone | - | - | |
| Carbohydrates | 5.5 | 7.1 | |
| Glycerol | 2.91 | - | 290 |
| Levoglucosan | 2.55 | 7.10 | 384 |
| Lignin-derived phenols | 2.89 | 0.48 | |
| Phenol | 1.52 | 0.48 | 182 |
| 2,4-dimethyl-phenol | - | - | |
| 4-methyl-phenol | - | - | |
| p-ethylphenol | 0.73 | - | 219 |
| 2,4,6-trihydroxyphenyl-2-pentanone | 0.64 | - | |
| Guaiacols | 27.4 | 11.4 | |
| o-guaiacol | 6.18 | 1.85 | 205 |
| p-methylguaiacol | 3.21 | 1.27 | 222 |
| p-ethylguaiacol | 2.95 | 0.75 | 236 |
| p-vinylguaiacol | 9.35 | 2.12 | 224 |
| Isoeugenol | 2.29 | 2.48 | 266 |
| Acetoguaiacon | 0.80 | - | |
| Coniferyl alcohol | 2.62 | 2.93 | |
| Syringols | 18.3 | 10.3 | |
| Syringol | 9.03 | 3.08 | 261 |
| Methoxyeugenol | 3.57 | 2.50 | |
| 3',5'-dimethoxyacetophenone | 3.37 | 2.09 | |
| Syringaldehyde | 0.72 | 0.74 | |
| Acetosyringone | 1.61 | 1.89 | |
| Methoxy benzenes | 4.43 | 3.05 | |
| Trimethoxybenzene | 1.95 | 1.29 | |
| 1,2,3-trimethoxy-5-methyl-benzene | 0.80 | - | |
| Benzenemethanol, 2,5-dimethoxy-, acetate | 1.68 | 1.76 | |

Table 1: The GC-MS results on % identified peak area^a

^aComponents with a peak area less than 0.5% are not listed in the table