

Supporting Information

Improved catalytic transfer hydrogenation of biomass-derived aldehydes with metal-loaded aluminum phosphate

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Number of pages	10
Number of figures	14
Number of tables	3

Content

Figure S1. XRD patterns of AEM-loaded APO1.5 catalysts.....	S3
Figure S2. SEM image of APO1.5 catalyst.....	S3
Figure S3. SEM images of 5Mg/APO1.5, 5Ca/APO1.5, 5Sr/APO1.5, and 5Ba/APO1.5 catalysts.....	S4
Figure S4. EDS mapping of 5Mg/APO1.5, 5Ca/APO1.5, 5Sr/APO1.5, and 5Ba/APO1.5 catalysts.....	S5
Figure S5. FT-IR spectra of APO1.5 and AEM-loaded APO1.5 catalysts.....	S6
Figure S6. N ₂ adsorption-desorption isotherms of APO1.5 and AEM-loaded APO1.5 catalyst..	S6
Figure S7. CO ₂ -TPD profiles of APO1.5, 5Mg/APO1.5, 5Ca/APO1.5, 5Sr/APO1.5 and 5Ba/APO1.5 catalysts.....	S7
Figure S8. FT-IR spectra of APO1.5 and AEM-loaded APO1.5 catalysts with pre-adsorbed FF and FA.....	S7

Figure S9. Correlations between acidity/basicity, FF consumption rate and FA/DIPF/IPF formation rate of the APO1.5 and AEM-loaded APO1.5 catalysts.....	S8
Figure S10. CTH of FF to FA with 3Ca/APO1.5 catalyst.....	S8
Figure S11. XRD patterns of fresh and reused 3Ca/APO1.5 catalyst.....	S9
Figure S12. TG curves of fresh and reused 3Ca/APO1.5 catalyst.....	S9
Figure S13. N ₂ adsorption-desorption isotherms of fresh and reused 3Ca/APO1.5 catalyst....	S10
Figure S14. NH ₃ -TPD and CO ₂ -TPD profiles of calcined 3Ca/APO1.5 catalyst.....	S10
Table S1. Crystalline size and unit cell size of APO1.5 and AEM-loaded APO1.5 catalysts....	S11
Table S2. The conversion of FF using 2-propanol as H-donor over APO1.5 catalysts.....	S11
Table S3. Physical properties and compositions of 3Ca/APO1.5 catalysts.....	S12

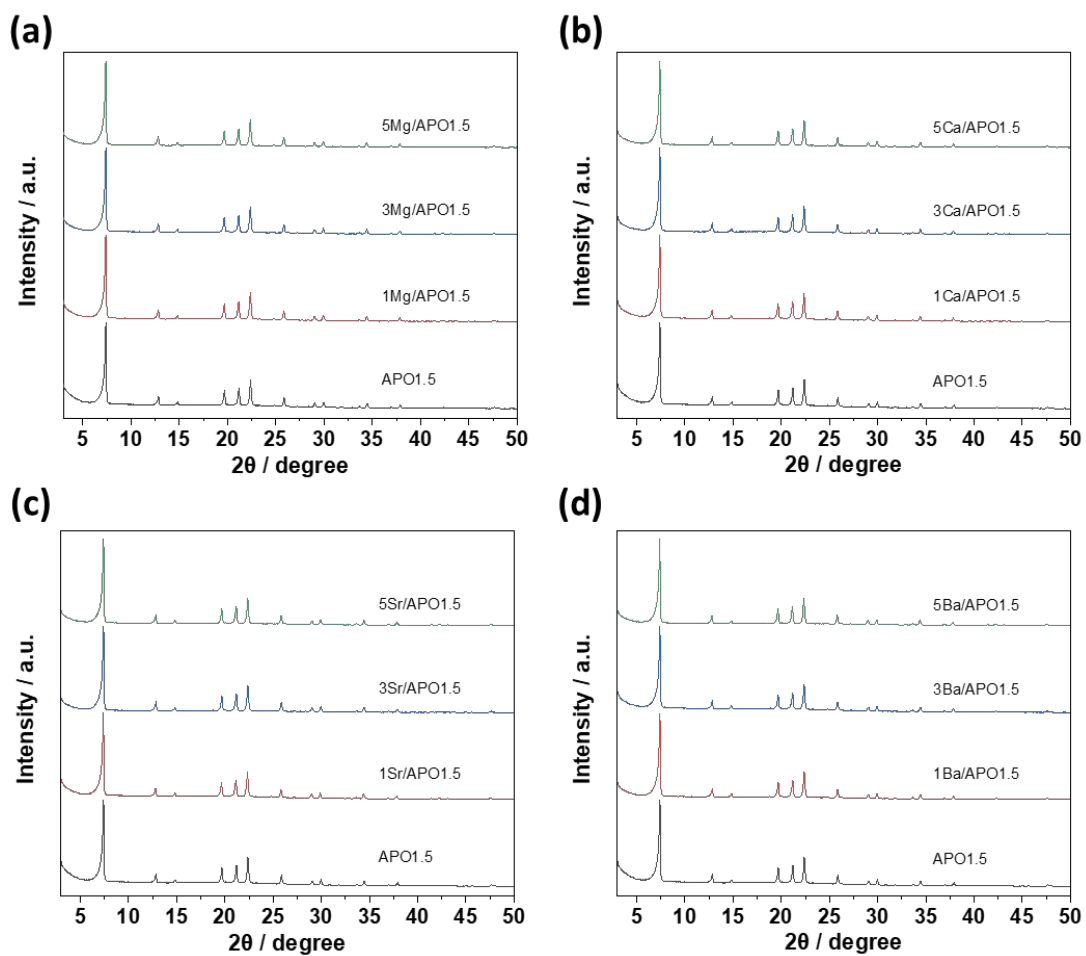


Figure S1. XRD patterns of AEM-loaded APO1.5 catalysts.

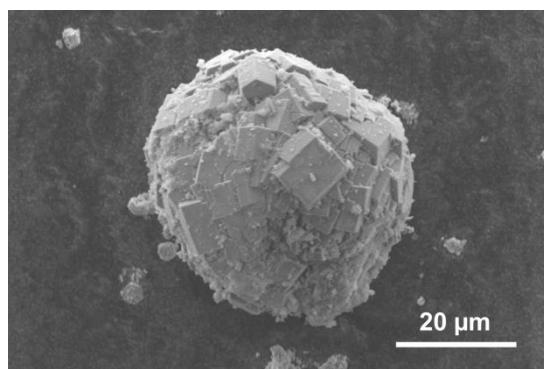


Figure S2. SEM image of APO1.5 catalyst.

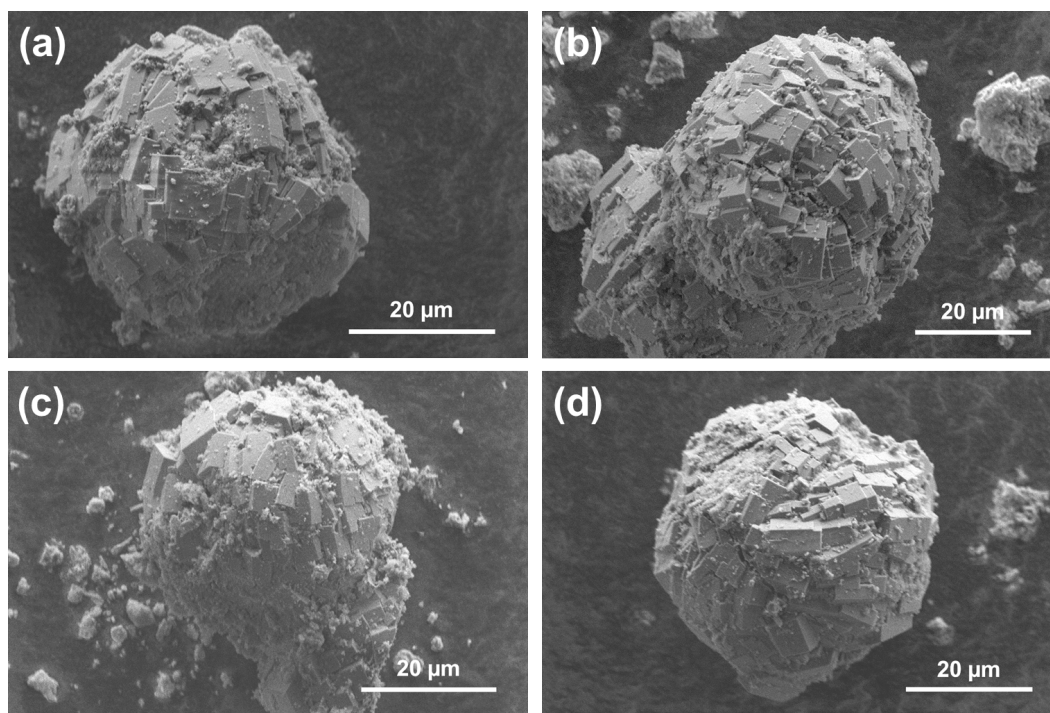


Figure S3. SEM images of (a) 5Mg/APO1.5, (b) 5Ca/APO1.5, (c) 5Sr/APO1.5, and (d) 5Ba/APO1.5 catalysts.

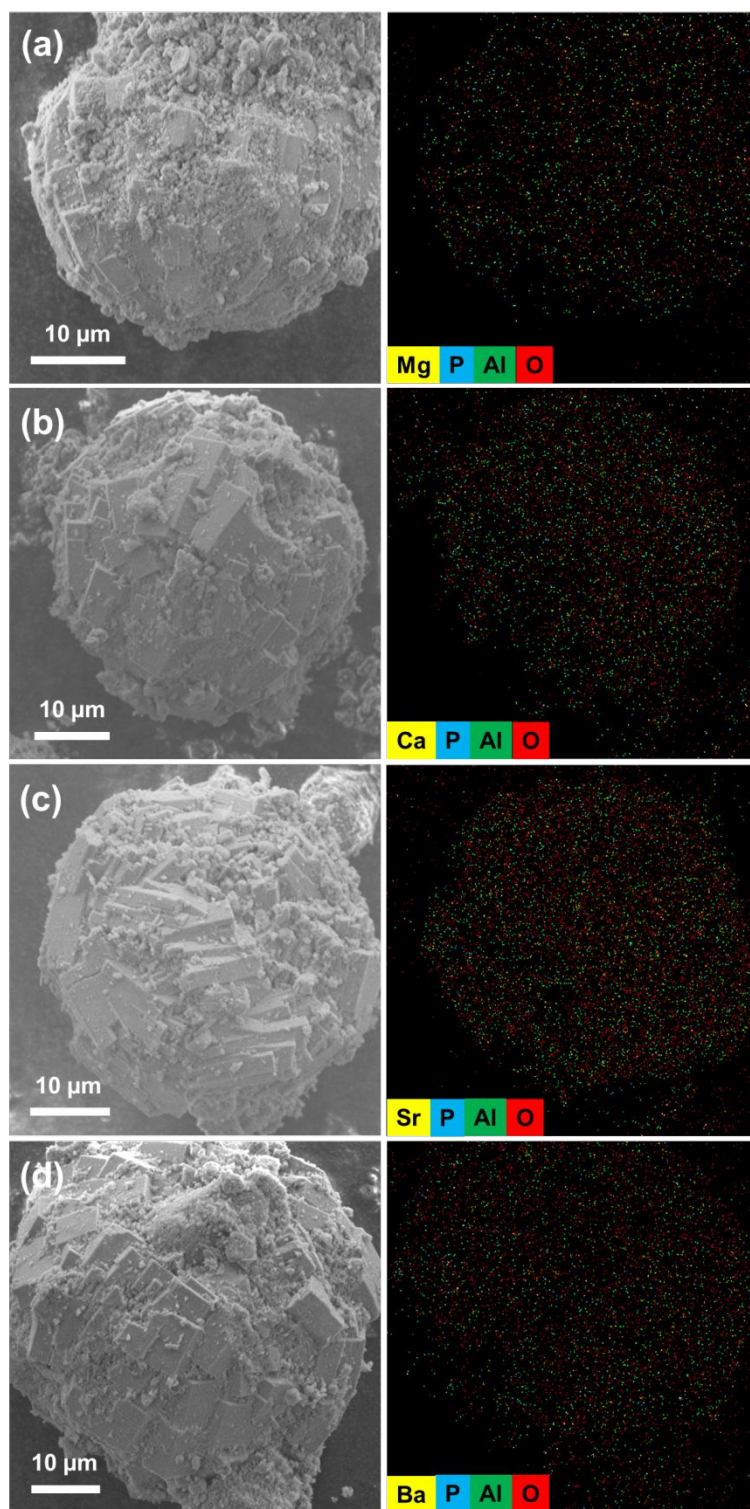


Figure S4. EDS mapping of (a) 5Mg/APO1.5, (b) 5Ca/APO1.5, (c) 5Sr/APO1.5, and (d) 5Ba/APO1.5 catalysts.

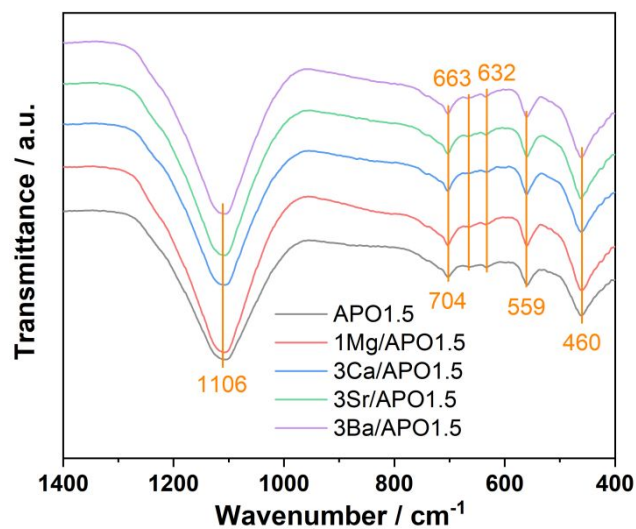


Figure S5. FT-IR spectra of APO1.5 and AEM-loaded APO1.5 catalysts.

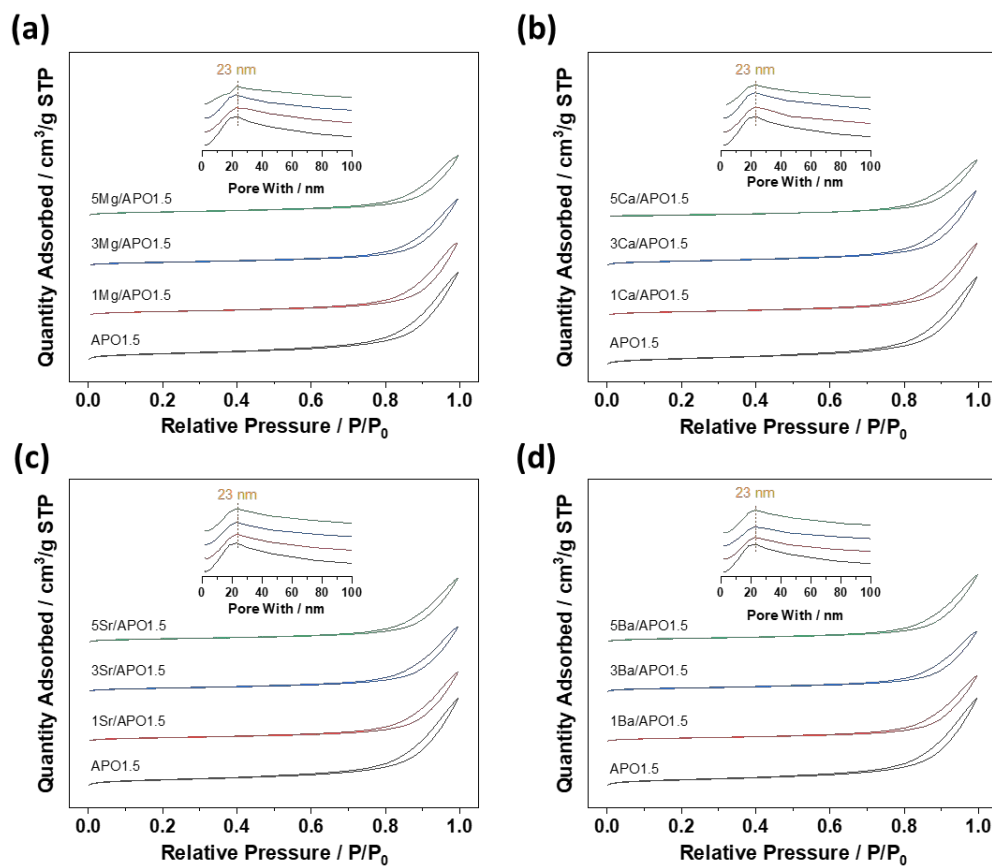


Figure S6. N₂ adsorption-desorption isotherms (inset: BJH mesopore size distribution) of APO1.5 and AEM-loaded APO1.5 catalysts.

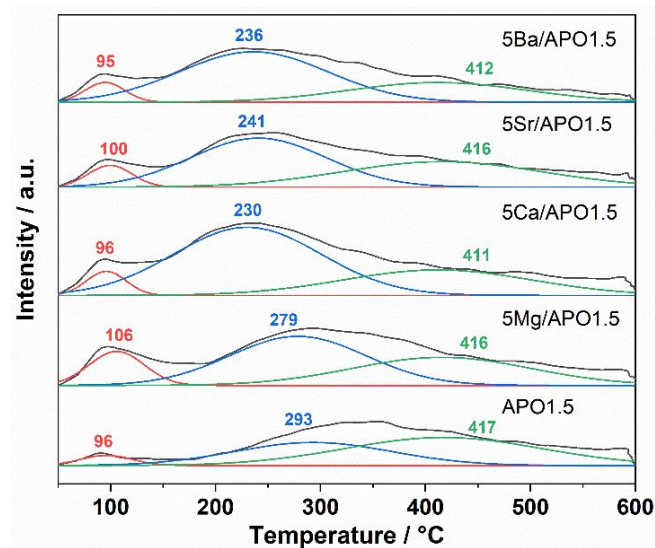


Figure S7. CO₂-TPD profiles of APO1.5, 5Mg/APO1.5, 5Ca/APO1.5, 5Sr/APO1.5 and 5Ba/APO1.5 catalysts.

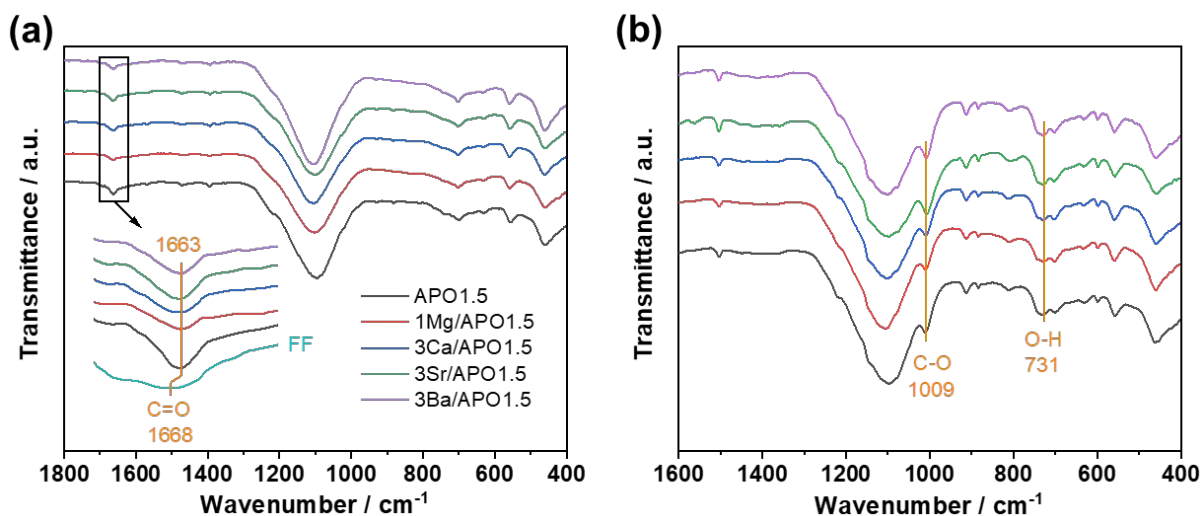


Figure S8. FT-IR spectra of APO1.5 and AEM-loaded APO1.5 catalysts with pre-adsorbed (a) FF and (b) FA.

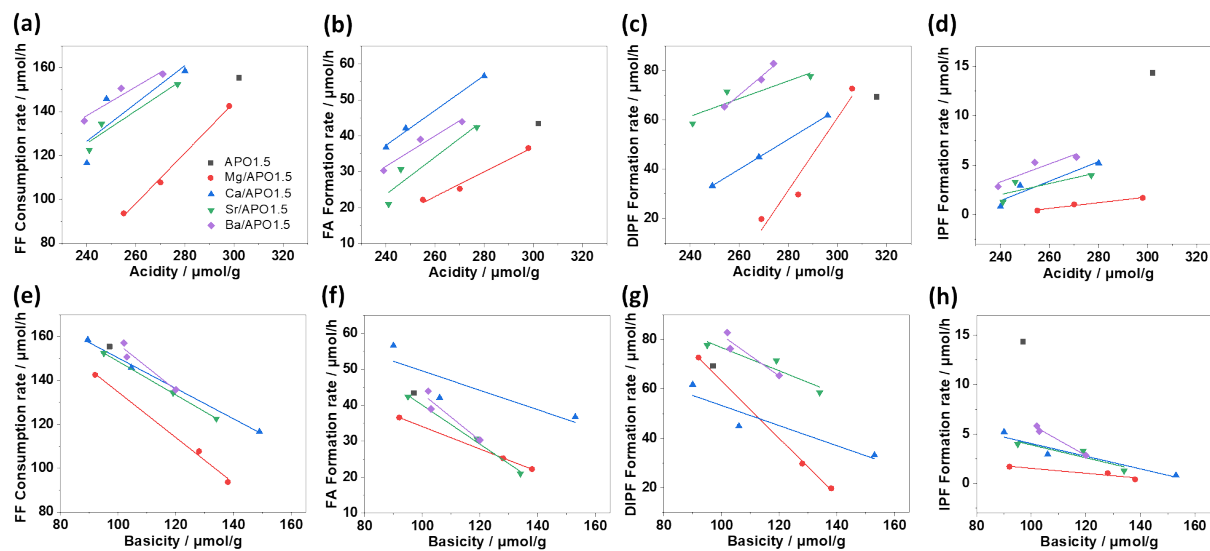


Figure S9. Correlations between acidity/basicity, FF consumption rate and FA/DIPF/IPF formation rate of the APO1.5 and AEM-loaded APO1.5 catalysts. Reaction conditions: (a)-(c) and (e)-(g) FF (96 mg, 1 mmol), catalyst (50 mg), 2-propanol (5 mL), 140°C, 2 h; (d) and (h) FA (98 mg, 1 mmol), catalyst (50 mg), 2-propanol (5 mL), 140°C, 6 h.

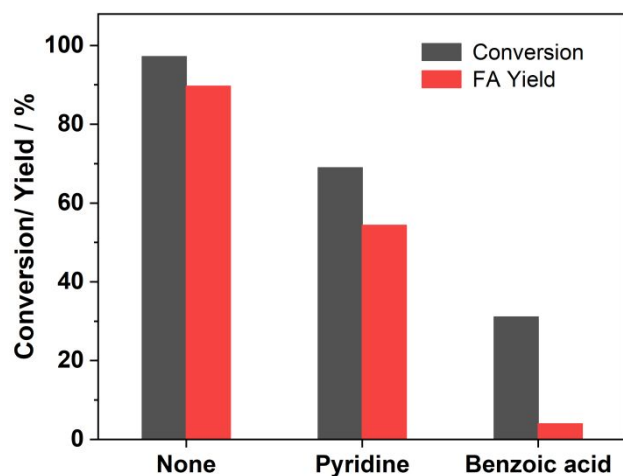


Figure S10. CTH of FF to FA with 3Ca/APO1.5 catalyst. Reaction conditions: FF (96 mg, 1 mmol), 3Ca/APO1.5 (50 mg), additive (100 mg), 2-propanol (5 mL), 140°C, 48 h.

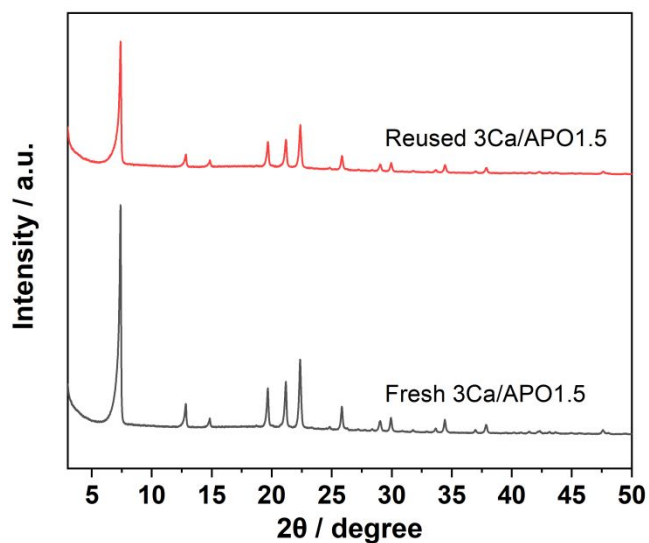


Figure S11. XRD patterns of fresh and reused (after four reaction cycles) 3Ca/APO1.5 catalyst.

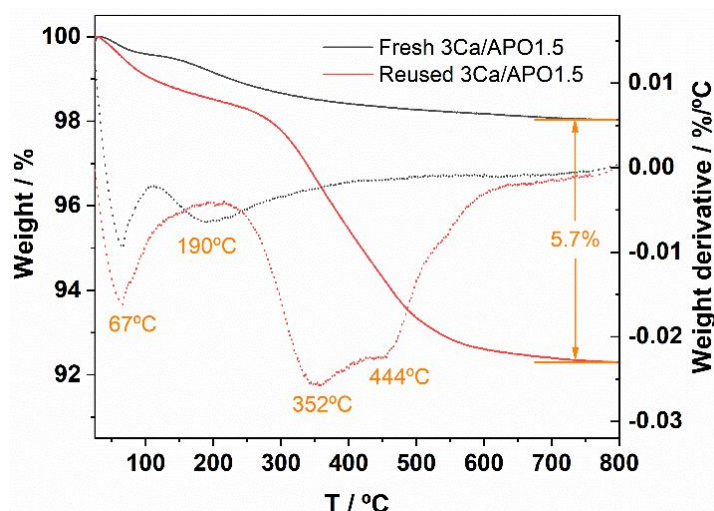


Figure S12. TG curves of fresh and reused (after four reaction cycles) 3Ca/APO1.5 catalyst.

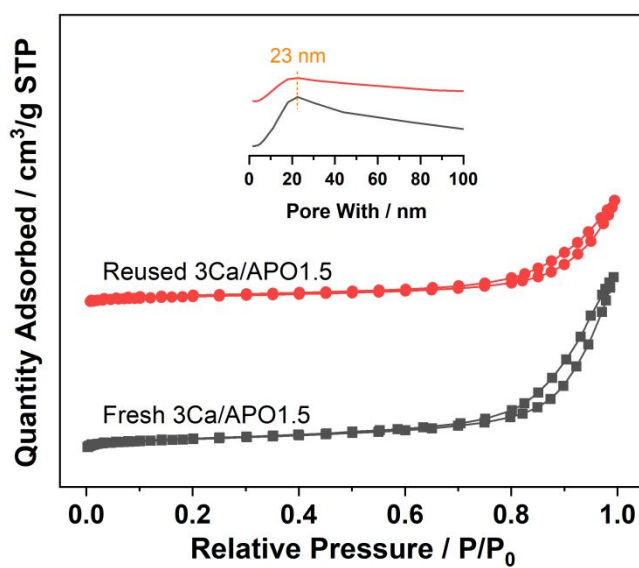


Figure S13. N₂ adsorption-desorption isotherms (inset: BJH mesopore size distribution) of fresh and reused (after four reaction cycles) 3Ca/APO1.5 catalyst.

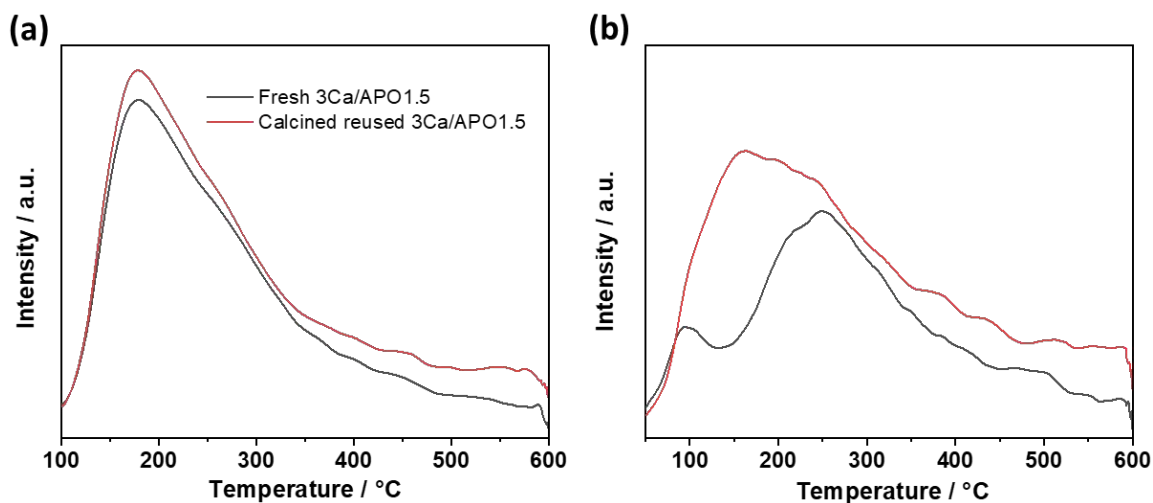


Figure S14. NH₃-TPD and CO₂-TPD profiles of calcined 3Ca/APO1.5 catalyst (after four reaction cycles).

Table S1. Crystalline size and unit cell size of APO1.5 and AEM-loaded APO1.5 catalysts.

Catalyst	Unit cell parameter		
	a (Å)	c (Å)	V (Å ³)
APO1.5	13.78	8.38	1378.08
1Mg/APO1.5	13.78	8.38	1378.08
3Mg/APO1.5	13.78	8.38	1378.08
5Mg/APO1.5	13.79	8.39	1381.72
1Ca/APO1.5	13.78	8.38	1378.08
3Ca/APO1.5	13.78	8.38	1378.08

5Ca/APO1.5	13.78	8.38	1378.08
1Sr/APO1.5	13.80	8.39	1383.73
3Sr/APO1.5	13.78	8.38	1378.08
5Sr/APO1.5	13.78	8.38	1378.08
1Ba/APO1.5	13.78	8.38	1378.08
3Ba/APO1.5	13.78	8.39	1379.72
5Ba/APO1.5	13.80	8.39	1383.73

Table S2. The conversion of FF using 2-propanol as H-donor over APO1.5 catalysts.^a

Catalyst	Conversion (%) ^b	Product yield (%) ^b			
		FA	DIPF	IPF	IPL
APO1.5+CaO	58.3	27.1	5.8	5.95	0

^a Reaction conditions: FF (96 mg, 1 mmol), catalyst (50 mg), 2-propanol (5 mL), 140°C, 24 h. ^b Conversion and yield were quantified using GC. FA: furfuryl alcohol, DIPF: 2-(diisopropoxymethyl)furan, IPF: 2-(isopropoxymethyl)furan, IPL: isopropyl levulinate.

Table S3. Physical properties and compositions of 3Ca/APO1.5 catalysts.

Catalyst	Ca content (wt.%) ^a	S _{BET} (m ² /g) ^b	V _{total} (cm ³ /g) ^c	V _{micro} (cm ³ /g) ^d	V _{meso} (cm ³ /g) ^e	Acidity (μmol/g) ^f	Basicity (μmol/g) ^g
3Ca/APO1.5	2.9	106	0.30	0.01	0.29	248	106
3Ca/APO1.5 (reused) ^h	2.2 ⁱ	49	0.17	0.00	0.17	264 ⁱ	198 ⁱ

^a Determined by XRF. ^b Calculated by Brunauer-Emmett-Teller (BET) method. ^c Calculated by single point adsorption at P/P₀ = 0.95. ^d Estimated by the t-plot method. ^e Calculated by subtraction of the micro pore volume from the total volume. ^f Determined by NH₃-TPD. ^g Determined by CO₂-TPD. ^h 3Ca/APO1.5 catalyst after four reaction cycles. ⁱ Calcined 3Ca/APO1.5 catalyst (after four reaction cycles).