Supporting Information

Liquid–Liquid Equilibrium Data for Cyclohexane–Ethanol–Solvent Ternary Systems and Their Correlation with the Nonrandom Two-Liquid Model

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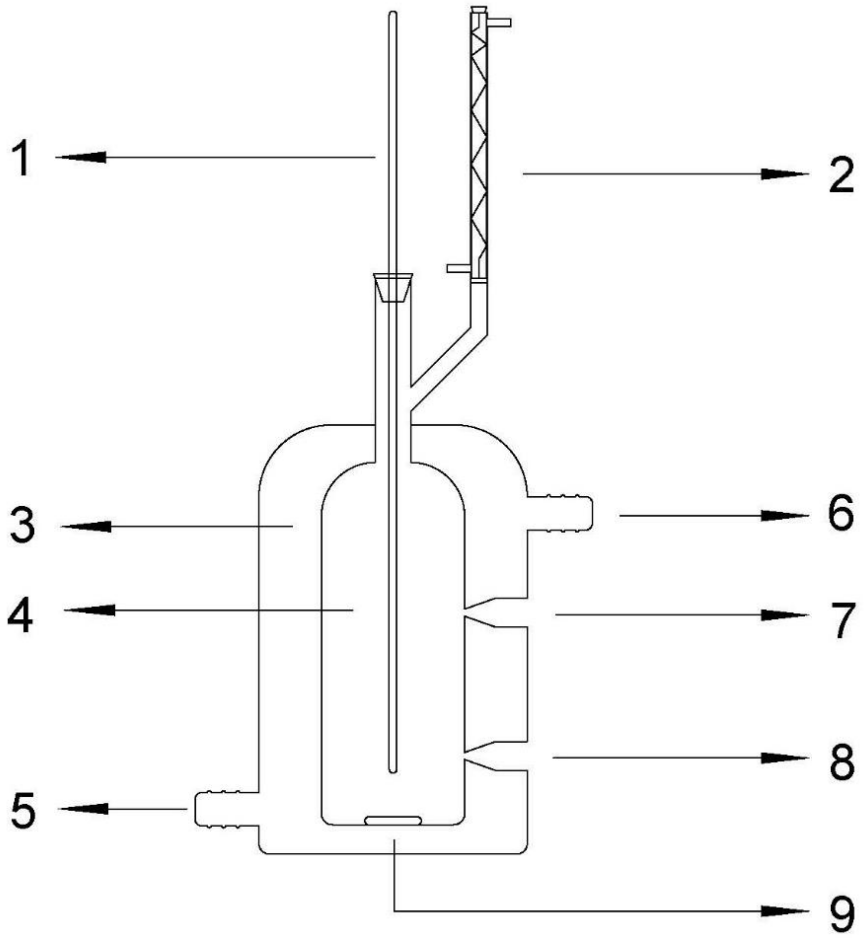

Figure S1. Experimental set-up of the vessel for obtaining the LLE data: 1. Thermometer, 2. condenser tube, 3. circulating water chamber, 4. equilibrium cell chamber, 5. circulating water inlet, 6. circulating water outlet, 7. super-stratum sampling port, 8. substratum sampling port, 9. magnetic stirrer.

Table S1. Mole Fractions (x) Corresponding to the Calculated LLE Values using the NRTL Model for the Cy (1)–EtOH (2)–Solvent (3) Ternary System at T = 303.15 K and P = 100.3 kPa

solvent	solvent-rich phase			Cy-rich phase		
	x_1^β	x_2^β	x_3^β	x_1^α	x_2^α	x_3^α
BDO	0.0491	0.1017	0.8492	0.9911	0.0043	0.0046
	0.0574	0.1894	0.7532	0.9893	0.0062	0.0045
	0.0663	0.2705	0.6632	0.9867	0.0091	0.0042
	0.0759	0.3352	0.5889	0.9837	0.0123	0.0040
	0.0883	0.3985	0.5132	0.9800	0.0164	0.0036
	0.1057	0.4633	0.4310	0.9751	0.0216	0.0033
	0.1237	0.5132	0.3631	0.9705	0.0266	0.0029
DMSO	0.0642	0.0910	0.8448	0.9771	0.0038	0.0191
	0.0726	0.1759	0.7515	0.9770	0.0061	0.0169
	0.0920	0.2446	0.6634	0.9702	0.0113	0.0185
	0.1206	0.2914	0.5880	0.9570	0.0196	0.0234
	0.1451	0.3464	0.5085	0.9463	0.0290	0.0247
	0.1769	0.3847	0.4384	0.9306	0.0415	0.0279
	0.2271	0.3835	0.3894	0.8992	0.0609	0.0399
DMF	0.2494	0.0580	0.6926	0.8891	0.0078	0.1031
	0.2765	0.0866	0.6369	0.8855	0.0140	0.1005
	0.3009	0.1105	0.5886	0.8797	0.0210	0.0993
	0.3249	0.1318	0.5433	0.8718	0.0291	0.0991
	0.3412	0.1451	0.5137	0.8650	0.0354	0.0996
	0.3629	0.1604	0.4767	0.8546	0.0443	0.1011