

## Supporting Information

### **Hierarchical Porous Catalytic Pyrolysis Char Derived from Oily Sludge for Enhanced Adsorption**

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## Explanations and formulas for isotherm models

The Langmuir model assumes that the adsorbent surface is homogeneous, and the adsorption energy is the same on the surface. The adsorption is monolayer adsorption. When the adsorption equilibrium reached, the number of molecules entering the adsorption site is equal to the number of molecules leaving in unit time, in other words, the adsorption rate is equal to the desorption rate [1]. The linear formula of the Langmuir model is expressed as follows:

$$\frac{c_e}{q_e} = \frac{1}{q_m K_L} + \frac{c_e}{q_m}$$

Where,  $q_e$  is the equilibrium adsorption capacity (mg/g),  $c_e$  is the equilibrium concentration of the dye solution (mg/L),  $q_m$  is the saturated adsorption capacity (mg/g) and  $K_L$  is the Langmuir constant (L/mg).

The dimensionless constant  $R_L$  normally known as separation factor expressed as follows:

$$R_L = \frac{1}{1 + K_L c_e}$$

When  $R_L > 1$ ,  $R_L = 1$ ,  $0 < R_L < 1$ , and  $R_L = 0$ , the adsorption process is predicted to be non-favorable, linear, favorable and non-reversible, respectively [2].

The Freundlich model is an empirical formula without any assumptions, because the constants in the formula have no definite physical meaning [3]. The linear formula of

Freundlich model is shown as follows:

$$\ln q_e = \ln K_F + \frac{1}{n} \ln c_e$$

Where,  $K_F$  is the Freundlich constant  $[(\text{mg/g})(\text{L/mg})^{1/n}]$  related to the adsorption interaction and the adsorption capacity,  $n$  is a constant related to the adsorption intensity.

### **Explanations and formulas for kinetic models:**

The linear formula of Pseudo-first-order model is shown as follows:

$$\ln(q_{e.\text{exp}} - q_t) = \ln q_{e.\text{cal}} - k_1 t$$

Where,  $q_{e.\text{exp}}$  is the experimental equilibrium adsorption capacity (mg/g),  $q_{e.\text{cal}}$  is the calculated equilibrium adsorption capacity (mg/g),  $q_t$  is the adsorption capacity at time  $t$  (mg/g),  $k_1$  is the Pseudo-first-order rate constant ( $\text{min}^{-1}$ ),  $t$  is the pre-set time intervals (min).

The linear formula of Pseudo-second-order model is shown as follows:

$$\frac{t}{q_t} = \frac{1}{k_2 q_{e.\text{cal}}^2} + \frac{1}{q_{e.\text{cal}}} t$$

Where,  $k_2$  is the Pseudo-second-order rate constant ( $\text{g mg}^{-1}\text{min}^{-1}$ ).

**Table S1** Characteristics of the OS used in this paper.

Ultimate analysis						
element	C	H	O	N	S	Si
wt%	16.38	4.25	8.91	0.32	2.34	20.47
Proximate analysis						
component	moisture	Volatile matter		ash	fixed carbon	
wt%	16.61	27.38		51.19	4.82	

**Table S2** Fit summary of sequential model.

Sequential Model Sum of Squares						
Source	Sum of squares	DF	Mean square	F-value	Prob>F	
Mean vs Total	7.337E+005	1	7.337E+005			
Linear vs Mean	4707.93	3	1569.31	0.30	0.8268	
2FI vs Linear	3460.47	3	1153.49	0.18	0.9096	
Quadratic vs 2FI	65138.26	3	21712.75	2798.24	<0.0001	Suggested
Cubic vs Quadratic	10.76	3	3.59	0.33	0.8058	Aliased
Residual	43.56	4	10.89			
Total	8.071E+005	17	47476.00			
Lack of Fit tests						
Linear	68609.49	9	7623.28	700.08	<0.0001	
2FI	65149.02	6	10858.17	997.16	<0.0001	
Quadratic	10.76	3	3.59	0.33	0.8058	Suggested
Cubic	0.000	0				Aliased
Pure Error	43.56	4	10.89			
Model Summary Statistics						
source	Std. Dev.	R <sup>2</sup>	R <sup>2</sup> <sub>Adj</sub>	R <sup>2</sup> <sub>Pred</sub>	PRESS	
Linear	72.67	0.0642	-0.1518	-0.3689	1.004E+005	
2FI	80.74	0.1113	-0.4218	-1.1132	1.550E+005	
Quadratic	2.79	0.9993	0.9983	0.9967	240.21	Suggested
Cubic	3.30	0.9994	0.9976			Aliased

**Table S3** Analysis of variance (ANOVA) of the experimental results of RSM-BBD.

Source	Sum of squares	DF	Mean square	F-value	Prob>F	
<b>Model</b>	73306.66	9	8145.18	1049.72	<0.0001	<b>significant</b>
<b>A</b>	2778.14	1	2778.14	358.03	<0.0001	
<b>B</b>	1454.36	1	1454.36	187.43	<0.0001	
<b>C</b>	475.43	1	475.43	61.27	0.0001	
<b>AB</b>	308.79	1	308.79	39.80	0.0004	
<b>AC</b>	3149.79	1	3149.79	405.93	<0.0001	
<b>BC</b>	1.89	1	1.89	0.24	0.6372	
<b>A<sup>2</sup></b>	29270.40	1	29270.40	3772.24	<0.0001	
<b>B<sup>2</sup></b>	13766.04	1	13766.04	1774.11	<0.0001	
<b>C<sup>2</sup></b>	15500.73	1	15500.73	1997.66	<0.0001	
<b>Residual</b>	54.32	7	7.76			
<b>Lack of Fit</b>	10.76	3	3.59	0.33	0.8058	<b>not significant</b>
<b>Pure Error</b>	43.56	4	10.89			
<b>Cor Total</b>	73360.97	16				

**Table S4** Statistical analysis for the quadratic model.

Statics	Value
Determination coefficient	0.9993
Adjusted determination coefficient	0.9983
Predicted determination coefficient	0.9967
Coefficient of variation (CV, %)	1.34
Adequate precision	92.892

**Table S5**

Adsorption isotherm parameters for MB adsorbed onto PC at different temperature.

Temperature (K)			298	308	318
Experimental $q_e$ (mg/g)			282.69	305.51	322.89
<b>Langmuir</b>	$q_m$	mg/g	285.71	304.88	327.87
	$K_L$	L/mg	0.4094	0.3388	0.2032
	$R_L$		0.003~0.789	0.003~0.850	0.007~0.960
	$R^2$		0.9999	0.9999	0.9997
<b>Freundlich</b>	$K_F$	(mg/g)(L/mg) <sup>1/n</sup>	178.95	183.06	193.37
	$1/n$		0.0844	0.0897	0.0905
	$R^2$		0.5635	0.6255	0.7153

**Table S6**

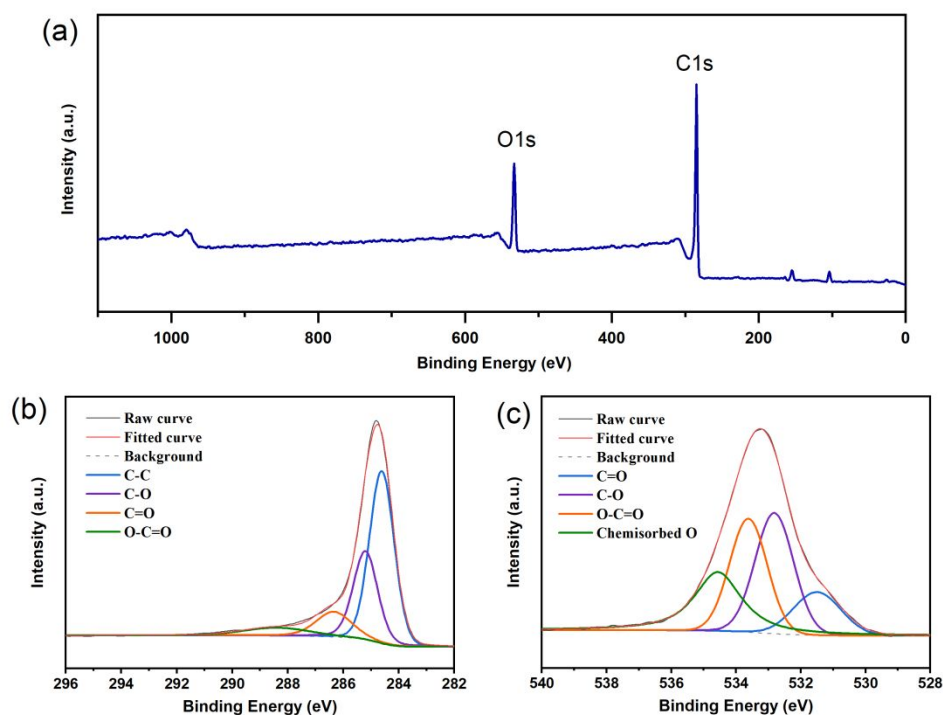
Adsorption kinetic parameters for MB adsorbed onto PC at different temperature.

Temperature (K)			298	308	318
Experimental $q_{e.exp}$ (mg/g)			282.69	305.51	322.89
<b>Pseudo-first-order</b>	$q_{e.cal}$	mg/g	275.03	299.62	308.34
	$k_1$	min <sup>-1</sup>	5.0817	5.5723	5.1104
	$R^2$		0.9948	0.9972	0.9941
<b>Pseudo-second-order</b>	$q_{e.cal}$	mg/g	281.69	304.88	317.46
	$k_2$	g mg <sup>-1</sup> min <sup>-1</sup>	0.027	0.033	0.015
	$R^2$		0.9999	0.9999	0.9999

**Table S7**

Comparison of the MB adsorption capacity of various adsorbents

Adsorbents	adsorption capacity (mg g <sup>-1</sup> )	Reference
<b>Oily sludge-based PC</b>	<b>322.89</b>	<b>This work</b>
Nanoporous polymer	57.74	[4]
Hollow spherical sludge carbon	149	[5]
Cellulose nanocrystal-alginate hydrogel	256.41	[6]
<i>Prosopis juliflora</i> -based activated carbon	91	[7]
Corn stalk-based activated carbon	144	[8]
Eucalyptus sawdust-based activated carbon	178.57	[9]
Chitosan-clay composite	193.23	[10]
Wheat straw-based activated carbon	208	[11]
Wheat straw-based activated carbon	396.9	[12]



**Figure S1.** The XPS survey (a) and the high resolution of C1s (b) and O1s(c) spectrum of PC

As shown in Figure S1a, C1s, and O1s peaks can be observed clearly in the XPS survey. The high resolution C1s and O1s XPS spectra of PC are shown in Figure S1b and c, respectively. The C1s spectrum can be deconvoluted into four peaks which representing C-C (284.5 eV), C-O (285.7eV), C=O (287.3 eV) and C-C (288.7 eV), respectively [13]. The O1s spectrum can also be divided into four peaks which attributing to C=O (531.4 eV), C-O (532.3 eV), O-C=O (533.5 eV) and chemisorbed Oxygen (534.8 eV), respectively [14]. These O-containing functional group especially hydroxyl and carboxyl groups could generate electrostatic interactions and hydrogen bonding effect with MB ions, which promotes the adsorption performance of PC material.



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