Supporting information

Characterizing Carbon Ring-C₃N₄ Nanosheets as a Light Harvesting and Charge Carrier Transfer Agent: Photodegradation of Methylene Blue and Photoconversion of CO₂ to CH₄ as Case Studies

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Photocatalytic reduction of CO₂

Photocatalytic activity of the synthesized catalysts for CO_2 reduction was evaluated in a batch circulation water reactor (Pyrex tubular reactor) with a 300W Xe lamp as the light source. The reactor was double-walled for circulating water between these walls to maintain the solution at around 25°C. An amount of 40 mg photocatalyst powder and 100 mL H₂O were placed in the reactor. Then, the mixture was stirred under strong magnetic force for 10 min to homogenize the solution. The CO_2 (99.999%) gas was purged into the reactor for 40 min to saturate water with CO_2 and remove the dissolved air. After irradiation, the gas phase products were taken from the reactor in every 1 h by using a 1-mL Hamilton gas tight syringe to analyze it by gas chromatography equipped with flame ionisation detector. The isotope-labeled examination was carry out by gas chromatography-mass spectrometry (GC-MS, 7890A and 5875C, Agilent).

Electrochemical measurements

Electrochemical measurements were performed by a PGSTAT302N (Metrohm Autolab B.V., Utrecht, The Netherlands). The electrochemical cell was assembled with a conventional threeelectrode system. The working electrodes were prepared by using samples coated on FTO glass. A saturated Ag/AgCl (saturated KCl) and a platinum wire were used as reference and auxiliary electrodes, respectively. The electrolyte was Na₂SO₄ solution (0.5 mol L^{-1}) and the solution was purged with argon for 1h to remove O₂ before light irradiation. Electrochemical impedance spectroscopy (EIS) was performed using 5 mmol L^{-1} K₃[Fe(CN)₆]/K₄[Fe(CN)₆] solution as the reversible redox probe with 0.1 mol L^{-1} KCl as the electrolyte.

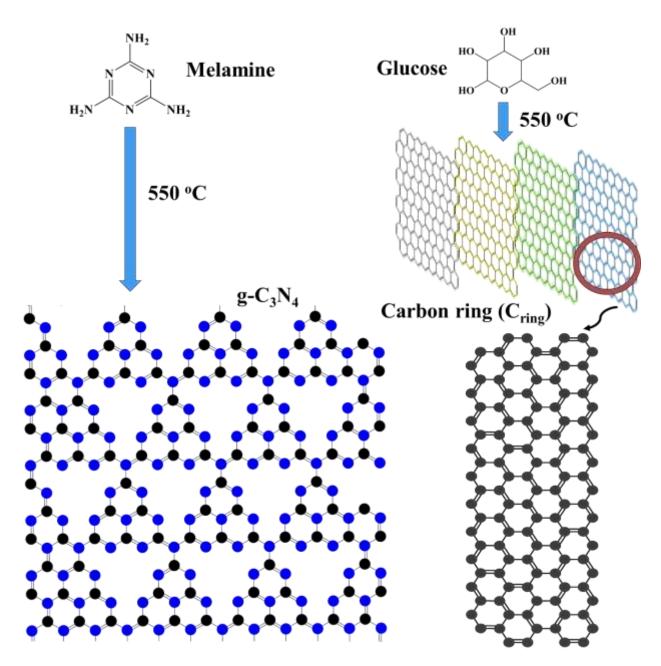


Figure S1. When glucose and melamine are heated to high temperatures, carbon and tri-s-triazine rings produce having sp^2 hybrid (two-dimensional domains in-plane with a similar aromatic structure).

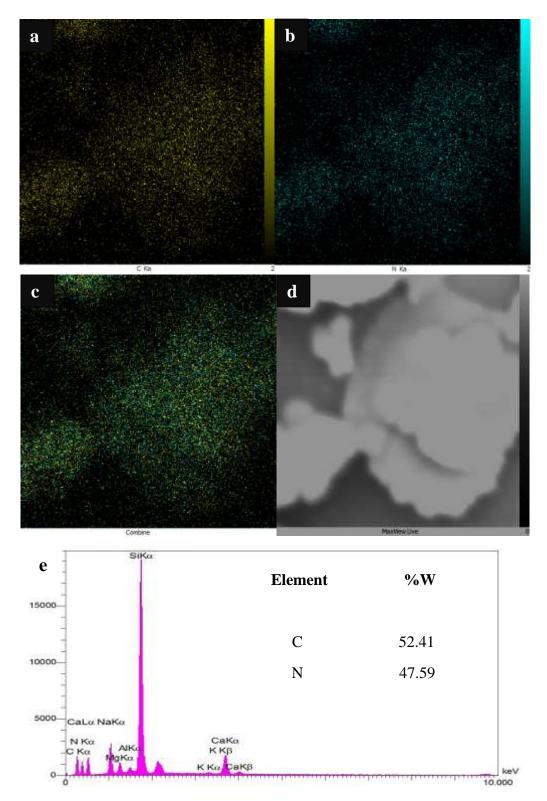


Figure S2. The SEM-EDS mapping images and spectra of C_{ring} - C_3N_4 . (a), the C mapping image; (b), the N mapping image; (c), the combined C and N mapping image; (d), the SEM image shows the corresponding region for mapping; and (e), the EDS spectra of C_{ring} - C_3N_4 .

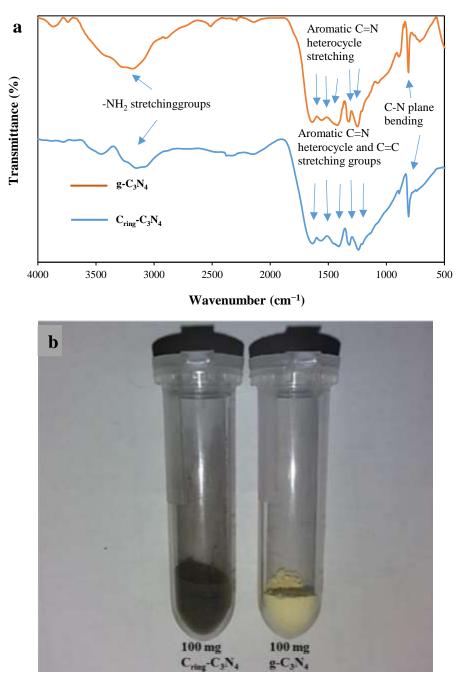


Figure S3. (a), the FT-IR spectra of C_{ring} - C_3N_4 and bulk g- C_3N_4 . (b), Comparison between color of C_{ring} - C_3N_4 and bulk g- C_3N_4 .

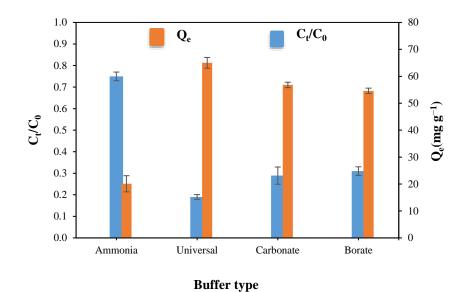


Figure S4. Effect of buffer type. Experimental conditions: 40.0 mL of 20.0 mg L^{-1} MB, 4.0 mg of C_{ring} - C_3N_4 with 0.01 mol L^{-1} universal buffer at pH=11.0.

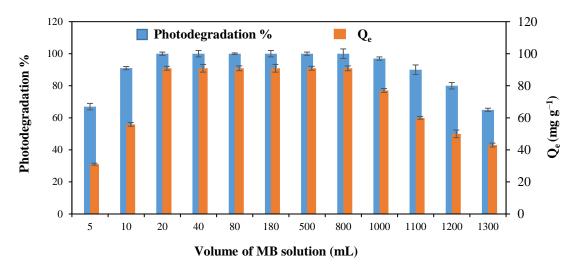


Figure S5. Breakthrough volume in adsorption/photodegradation of MB.

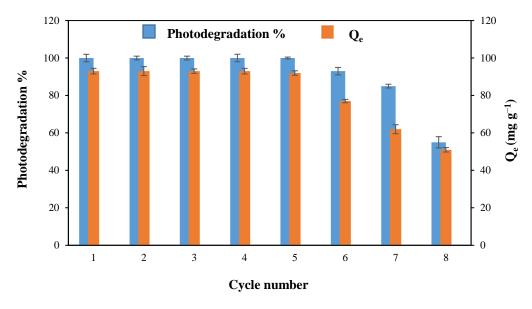


Figure S6. Reusability of the photocatalysts in several successive processes in the adsorption/photodegradation of MB.

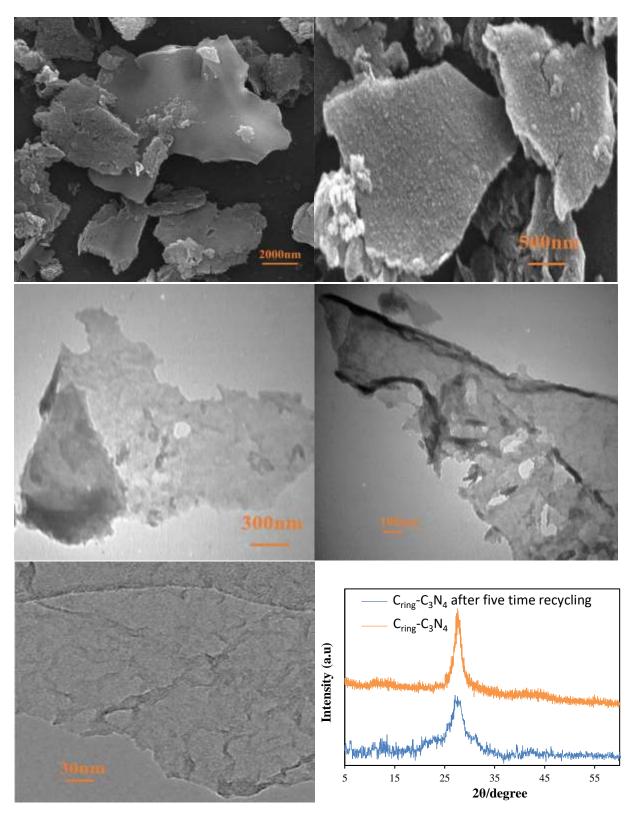


Figure S7. SEM, TEM, and XRD analyses after 5-time usage of C_{ring} - C_3N_4 photocatalyst.

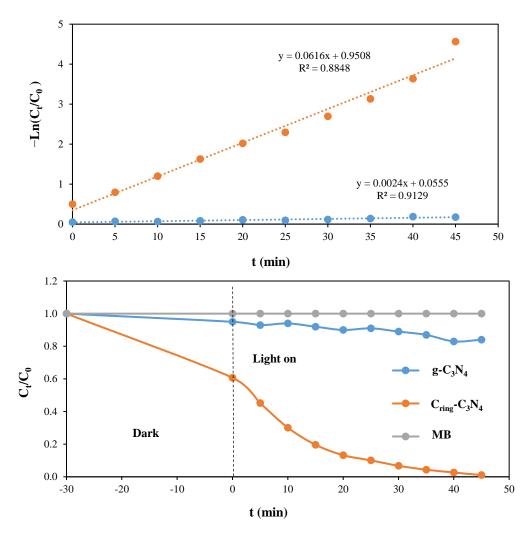


Figure S8. The kinetic simulation curves of MB photodegradation under visible light irradiation. Experimental conditions: 4.0 mg C_{ring} - C_3N_4 , 40.0 mL of 20.0 mg L^{-1} MB with 0.05 M universal buffer at pH=11.0).

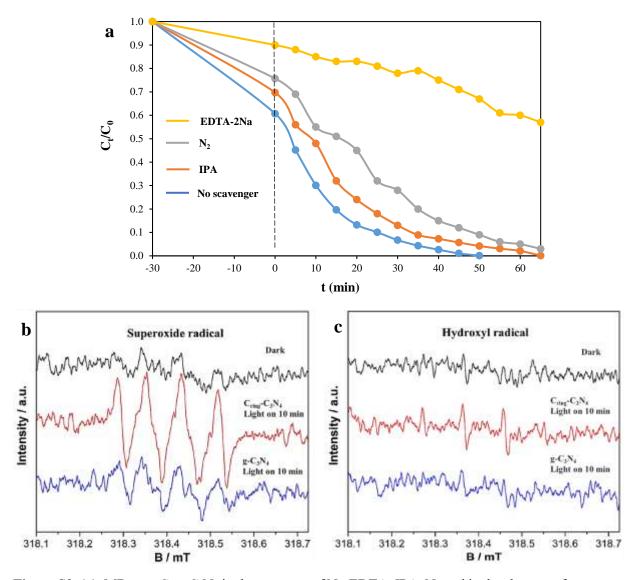


Figure S9. (a), MB over C_{ring} - C_3N_4 in the presence of Na₂EDTA, IPA, N₂ and in the absence of scavengers; (b), ESR spectra of DMPO- $O_2^{\circ-}$ for C_{ring} - C_3N_4 and bulk g- C_3N_4 ; (c), ESR spectra of DMPO- $^{\circ}OH$ for C_{ring} - C_3N_4 and bulk g- C_3N_4 .



Figure S10. Picture of the employed photo-reactor for photoreduction of CO₂ to CH₄.

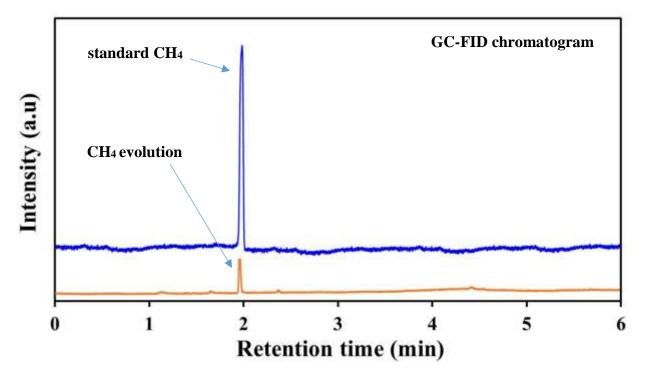


Figure S11. The chromatogram of the standard methane sample and the reaction mixture.

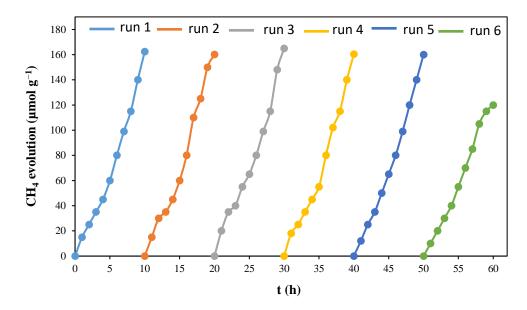


Figure S12. Reusability study of C_{rng}-C₃N₄ in the photocatalytic conversion of CO₂ to CH₄.

Calculation of AQY: Photocatalytic reaction with Cring-C3N4 nanosheet photocatalyst from [1]:

Main product: CH₄ Reactor type: Batch circulation water reactor (pyrex tubular reactor) Product yield: 162.4 μ mol g_{cat}⁻¹ after 10 h Apparent light input (H): 438 mW/cm² Area of irradiation (A): computed from tubular reactor dimensions (length: 10.0 cm × diameter: 6.0 cm) A = 0.006 m² Band gap: 2.7 eV

The number of reacted electrons is computed by:

Number of reacted electrons = $\begin{bmatrix} mol \text{ of product} \\ produced \text{ in time, t} \end{bmatrix} * \begin{bmatrix} Number \text{ of electrons} \\ required \text{ to produce} \\ 1 \text{ mol of product} \end{bmatrix} * N_A$

Since $CO_2 + 8H^+ + 8e^- \rightarrow CH_4 + 2H_2O$, it requires 8 electrons to produce 1 mole of CH₄ as the product

Number of reacted electrons = $\left[\frac{162.4 * 10^{-6}}{10} \frac{\text{mol}}{\text{g h}}\right] * [8] * 6.022 * 10^{23}$

Number of reacted electrons = $7.82 * 10^{19}$

The number of incident photons is computed by:

Effective number of incident photons = $\left[\frac{\text{Light absorbed by the photocatalyst}}{\text{Average photon energy}}\right] * t$

where

Light absorbed by the photocatalyst = H * A = 43.8
$$\frac{W}{m^2}$$
 * 0.006 m² = 0.2628 W

Average photon energy $= \frac{hC}{\lambda}$

And, λ is the average wavelength of the absorption range of the photocatalyst. The maximum wavelength from the band gap is computed by:

$$\lambda_{\max} = \frac{hC}{E_g} = \frac{(6.626 * 10^{-34} j.s) * (3 * 10^8 m/s)}{2.7 \text{ eV}} * \frac{1 \text{ eV}}{1.6 * 10^{-19} j} * 10^9 = 460.1 \text{ nm}$$

Therefore, the average wavelength would be:

$$\lambda = \frac{\lambda_{\min} + \lambda_{\max}}{2} = \frac{250 + 460.1}{2} = 355.05$$

The average photon energy is then computed to be:

Average photon energy =
$$\frac{(6.626 * 10^{-34} j.s) * (3 * 10^8 m/s)}{355.05 * 10^{-9} m} = 5.6 * 10^{-19}$$

Effective number of incident electrons = $\left[\frac{0.2628 \text{ W}}{5.6 * 10^{-19} j} \frac{3600 \text{ s}}{1 \text{ h}}\right] = 1.689 * 10^{21}$

AQY calculation:

$$AQY (\%) = \left[\frac{\text{number of reacted electrons}}{\text{Effective number of incident electrons}}\right] * 100$$

AQY (%) =
$$\left[\frac{7.82 * 10^{19}}{1.689 * 10^{21}}\right] * 100 = 4.63 \%$$

Photocatalytic reaction with bulk g-C₃N₄ photocatalyst:

Reactor type: Batch circulation water reactor (pyrex tubular reactor) Product yield: 6.875 μ mol g_{cat}⁻¹ after 10 h Apparent light input (H): 438 mW/cm² Area of irradiation (A): computed from tubular reactor dimensions (length: 10.0 cm × diameter: 6.0 cm) A = 0.006 m² Band gap: 2.7 eV

The number of reacted electrons is computed by:

Number of reacted electrons =
$$\begin{bmatrix} mol \text{ of product} \\ produced \text{ in time, t} \end{bmatrix} * \begin{bmatrix} Number \text{ of electrons} \\ required \text{ to produce} \\ 1 \text{ mol of product} \end{bmatrix} * N_A$$

Since $CO_2 + 8H^+ + 8e^- \rightarrow CH_4 + 2H_2O$, it requires 8 electrons to produce 1 mole of CH_4

Number of reacted electrons =
$$\left[\frac{6.875 * 10^{-6}}{10} \frac{\text{mol}}{\text{g h}}\right] * [8] * 6.022 * 10^{23}$$

Number of reacted electrons = $3.3121 * 10^{18}$

The number of incident photons is computed by:

 $Effective number of incident photons = \left[\frac{\text{Light absorbed by the photocatalyst}}{\text{Average photon energy}}\right] * t$

Wherein light absorbed by the photocatalyst and average photon energy is found to be:

Light absorbed by the photocatalyst = H * A = 43.8 $\frac{w}{m^2}$ * 0.006 m² = 0.2628 W

Average photon energy $= \frac{hC}{\lambda}$

where λ is the average wavelength of the absorption range of the photocatalyst. The maximum wavelength from the band gap was computed by:

$$\lambda_{\max} = \frac{hC}{E_g} = \frac{(6.626 * 10^{-34} j.s) * (3 * 10^8 m/s)}{2.7 \text{ eV}} * \frac{1 \text{ eV}}{1.6 * 10^{-19} j} * 10^9 = 460.1 \text{ nm}$$

Therefore, the average wavelength would be

$$\lambda = \frac{\lambda_{\min} + \lambda_{\max}}{2} = \frac{250 + 460.1}{2} = 355.05$$

The average photon energy is then computed to be

Average photon energy =
$$\frac{(6.626 * 10^{-34} \text{ j. s}) * (3 * 10^8 \text{ m/s})}{355.05 * 10^{-9} \text{ m}} = 5.6 * 10^{-19}$$

Effective number of incident electrons =
$$\left[\frac{0.2628 \text{ W}}{5.6 * 10^{-19} \text{ j}} \frac{3600 \text{ s}}{1 \text{ h}}\right] = 1.689 * 10^{21}$$

AQY calculation:

$$AQY (\%) = \left[\frac{\text{number of reacted electrons}}{\text{Effective number of incident electrons}}\right] * 100$$

AQY (%) =
$$\left[\frac{3.3121 * 10^{18}}{1.689 * 10^{21}}\right] * 100 = 0.1961 \%$$

$$\left[\frac{\text{AQY (\%) } C_{\text{ring}} - C_3 N_4}{\text{AQY (\%) } g - C_3 N_4}\right] = \left[\frac{4.63}{0.1961}\right] = 23.61$$

Name of models isotherm	Equations	Plots for isotherms	
	Linear adsorption isotherms		
Langmuir model ¹	$\frac{C_{e}}{Q_{e}} = \frac{1}{Q_{m}}C_{e} + \frac{1}{k_{L}Q_{m}}$	$\frac{C_e}{Q_e}$ vs. C_e	
Freundlich model ²	$\ln q_e = \ln k_f + \frac{1}{n} \ln C_e$	ln Q _e vs. ln C _e	
Temkin model ³	$\ln q_e = \ln k_f + \frac{1}{n} \ln C_e$ $Q_e = \left(\frac{RT}{b}\right) \ln k_T + \left(\frac{RT}{b}\right) \ln C_e$ $B_T = \frac{RT}{b}$	Q _e vs. ln C _e	
Dubinin-radushkevich model ³	$B_{T} = \frac{RT}{b}$ $ln Q_{e} = ln Q_{m} - \beta \epsilon^{2}$ $E = \frac{1}{\sqrt{(-2\beta)}}$	$ln Q_e vs. \epsilon^2$	
	$\varepsilon = RT \ln \left(1 + \frac{1}{C_e}\right)$ Nonlinear adsorption isotherms		
Langmuir model ¹		Q _e vs. C _e	
Freundlich model ²	$Q_e = k_f C_e^{\frac{1}{n}}$	Q _e vs. C _e	
Temkin model ³	$Q_{e} = Q_{m}k_{L}\frac{C_{e}}{1 + k_{L}C_{e}}$ $Q_{e} = k_{f}C_{e}^{\frac{1}{n}}$ $Q_{e} = \frac{RT}{b}(ln k_{T}C_{e})$ $B_{T} = \frac{RT}{b}$	Q _e vs. C _e	
Dubinin-radushkevich model ³	$Q_e = q_m e^{-\beta \epsilon^2}$	Q _e vs. C _e	

 Table S1. Linear and nonlinear equations of absorption isotherms.

Table S2. Linear and nonlinear equations of kinetic isotherms.

Name of models isotherm	Equations	Plots for isotherms					
linear kinetic isotherms							
Pseudo-first-order model ⁴	$ln\left(\mathbf{Q}_{\mathrm{e}}-\mathbf{Q}_{\mathrm{t}}\right)=\ln\mathbf{Q}_{\mathrm{e}}-\mathrm{tk}_{\mathrm{1}}$	$ln (Q_e - Q_t) vs. t$					
Pseudo-second-order model ⁵	$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{t}{Q_e}$	$\frac{t}{Q_t}$ vs. t					
Elovich model ⁶	$Q_t = \frac{1}{\beta} \ln (\alpha \beta) + \frac{1}{\beta} \ln t$	Q _t vs. ln t					
Intraparticle diffusion model ⁷	$Q_t = k_{id}t^{\frac{1}{2}} + k_0$	$Q_t vs. t^{\frac{1}{2}}$					
I	Nonlinear kinetic isotherms						
Pseudo-first-order model ⁴	$Q_t = Q_e(1 - \exp - kt)$	Q _t vs. t					
Pseudo-second-order model ⁵	$Q_t = \frac{k_2 Q_e^2 t}{1 + k_2 Q_e t}$	Q _t vs. t					
Elovich model ⁶	$Q_t = \beta \ln (\alpha \beta t)$	Q _t vs. t					
Intraparticle diffusion model ⁷	$Q_t = k_{id}t^{\frac{1}{2}} + k_0$	Q _t vs. t					

Adsorption	Sum Sq	Sum Sq	Mean	Mean Sq	F	Pvalue	ACI
isotherm		Error	Sq	Error			
Langmuir	6.9×10 ⁻²	5.3×10 ⁻⁴	6.9×10 ⁻²	8.89×10 ⁻⁵	783.24	1.4×10^{-7}	-22.1812
Freundlich	1.35	5.3×10 ⁻²	1.35	8.98×10 ⁻³	152.23	1.7×10 ⁻⁵	-6.1914
Temkin	5309.6	690.11	5309.6	115.02	46.16	4.9×10 ⁻⁴	26.7114
Dubinin- radushkevich	1.03	0.37	1.03	6.3×10 ⁻²	16.45	6.7×10 ⁻³	0.593
Kinetics							
modeling							
Pseudo first order	9.42	8.9×10 ⁻²	9.42	1.3×10^{-2}	738.91	2.3×10 ⁻⁸	-5.447
Pseudo second order	0.31	3.8×10 ⁻²	3.1×10 ⁻¹	5.5×10 ⁻³	56.32	1.4×10 ⁻⁴	-8.7281
Elovich	12295	259.14	12295	37.02	332.11	3.7×10 ⁻⁷	25.7218
Intraparticle diffusion	5666.7	333.08	5666.7	55.51	102.08	5.5×10 ⁻⁵	26.8826

Table S3. Anova and Akaike information criterion tests for linear kinetic and adsorption isotherms.

Photocatalyst	CH4 Yield (µmol/g h)	Light input (W/m ²)	Area of irradiation (m ²)	Band gap (eV)	Wavel	C	Ave. λ (nm)	No. of reacted electrons	Average photon energy (J)	No. of incident photons	AQY (%)
					λmin	λmax					
Pt-XG/RBT ⁸	37	1000	0.00049	2.41	250	515.5	383	1.78×10^{20}	5.19×10 ⁻¹⁹	3.4×10 ²¹	5.2479
C,N-TNT06 ⁹	9.75	1000	0.00071	2.8	250	443.7	347	4.7×10 ¹⁹	5.73×10 ⁻¹⁹	4.46×10 ²¹	1.0532
In ₂ O ₃ -C ₃ N ₄ ¹⁰	7.991	12000	0.00063	2.8	250	444	347	3.85×10 ¹⁹	5.73×10 ⁻¹⁹	4.71×10 ²¹	0.082
CZTS-ZnO ¹¹	0.095	1000	0.00041	1.74	250	714	482	4.58×10 ¹⁷	4.12×10 ⁻¹⁹	3.58×10 ²¹	0.0128
HCP-TiO ₂ -FG ¹²	27.62	4330	0.00031	2.34	420	531	475	1.33×10 ²⁰	4.18×10 ⁻¹⁹	1.17×10 ²²	1.14
Pd _x Cu ₁ -TiO ₂ ¹³	19.6	20	0.0064	-	250	400	325	9.44×10 ¹⁹	6.12×10 ⁻¹⁹	7.53×10 ²⁰	12.53
Pt-X-RT ¹⁴	1.13	1000	0.00071	2.85	250	435.9	343	5.44×10 ¹⁸	5.8×10 ⁻¹⁹	4.41×10 ²¹	0.1234
Pt/TiO ₂ ¹⁵	2.85	348	0.0084	3.18	250	391	320	1.37×10 ¹⁹	6.21×10 ⁻¹⁹	1.69×10 ²²	0.081
Cu _x O-TiO ₂ ¹⁶	0.152	1000	0.00071	3.15	250	394.4	322	7.32×10 ¹⁷	6.17×10 ⁻¹⁹	4.14×10 ²¹	0.0177
C _{ring} -C ₃ N ₄ In this work	16.24	43.8	0.006	2.7	250	460.1	355.05	7.82×10 ¹⁹	5.6×10 ⁻¹⁹	1.689×10 ²¹	4.63

Table S4. A comparison between the various photocatalysts for photoreduction of CO₂ to CH₄.

Table S5. The comparison of the synthesized photocatalyst with some literature-reported photocatalysts in term of their ability for

Photocatalyst	WCatalyst (g)	Volume and concentration of MB	Irradiation Time (h)	mg MB/W _{Catalyst}	Degradation efficiency ^a	Reference
Nanoporous Graphitic Carbon Nitride	0.025	50 mL 10 mg/L	3	20	0.11	17
TiO ₂ nano-sized particles	1	600 mL 20 mg/L	9	12	0.02	18
TiO ₂ /ZnO	0.3	10 mL 10 mg/L	5	0.3	0.001	19
Al ₂ O ₃ /Fe ₂ O ₃	0.2	100 mL 25 mg/L	1.5	12.5	0.14	20
Fe3O4@rGO@ TiO2	0.05	50 mL 10 mg/L	2	10	0.08	21
TiO ₂ /polyacryl amide	0.025	25 mL 10 mg/L	5	10	0.03	22
SnO ₂ /S-doped g-C ₃ N ₄	0.14	500 mL 6 mg/L	2.5	21.4	0.14	23
Ag/g-C ₃ N ₄	0.1	300 mL 10 mg/L	1	30	0.5	24
C ₃ N ₄ /ZnO	0.15	150 mL 3.2 mg/L	2	3.2	0.03	25
npg-C ₃ N ₄	0.001	20 mL 20 mg/L	0.75	400	8.9	26
Cring-C3N4	0.004	40 mL 20 mg/L	0.75	200	4.4	This work

^aDegradation efficiency was defined as (mg MB/W_{Catalyst}) per minute of the irradiation time in this table.

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