Production of cyanide using thermal plasma: thermodynamic analysis and experimental specific energy consumption Supporting information Figure SI F1 Detailed Thermodynamic profile of C-N-H species (1:2:4), e.g. feed of nitrogen and methane Figure SI F2: Detailed Thermodynamic profile of C-H-N species same as figure 1 but excluding condensed carbon Figure SI F3: Process diagram Table SI T1: Experimental data and mass balance (Nitrogen and Propane) Table SI T2: Experimental data and mass balance (Nitrogen and Methane)

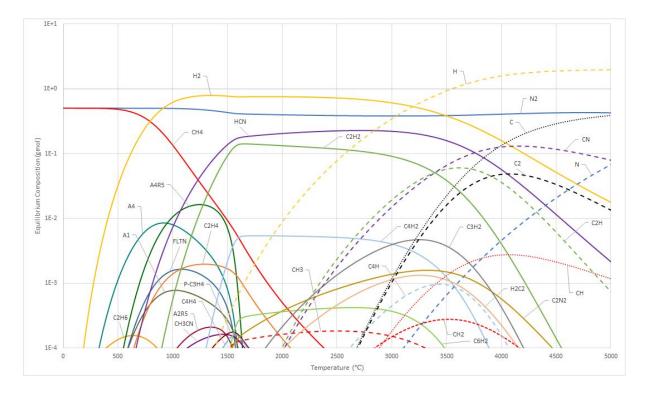


Figure SI-F1 Detailed Thermodynamic profile of C-N-H species (1:2:4), e.g. feed of nitrogen and methane

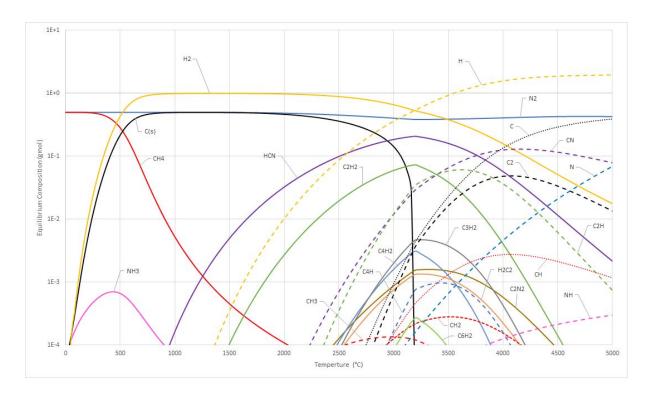


Figure SI-F2: Detailed Thermodynamic profile of C-H-N species same as figure 1 but excluding condensed carbon

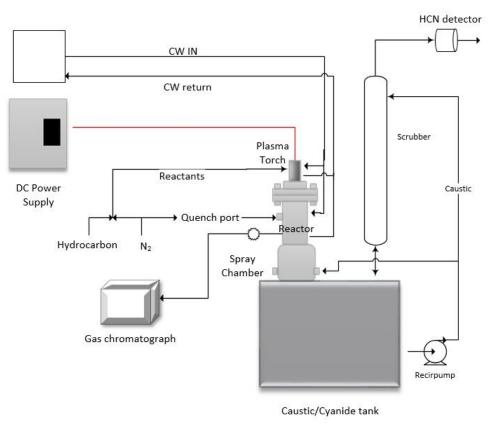


Figure SI-F3: Process flow diagram

Table SI-T1: Experimental parameters and mass balance – Nitrogen and Propane

| Test No | Nitrogen Flow | Propan e Flow | N:C | Nitroge n Mol % | Power | HCN yield | Cyanide conv | SEC (NaCN) | N2 | СЗН8 | Carbon ** | Carbon to Acetylene | Carbon to Soot |
|------------|------------------|------------------|-------|--------------------|-------|-----------|--------------|------------|-------|---------|-----------|------------------------|-------------------|
| | SLPM | SLPM | | % | kW | g/min | % | kw-hr/Kg | mol/m | mol/min | mol/min | | |
| 1 | 46.5 | 7.75 | 4.00 | 85.7 % | 23 | 9.25 | 37% | 22.8 | 1.88 | 0.31 | 0.94 | 36% | 27% |
| 2 | 51 | 6.25 | 5.44 | 89.1 % | 23 | 9.67 | 47% | 21.8 | 2.06 | 0.25 | 0.76 | | |
| 3 | 64 | 7 | 6.10 | 90.1 % | 23 | 11.44 | 50% | 18.5 | 2.58 | 0.28 | 0.85 | | |
| 4 | 64.25 | 6 | 7.14 | 91.5 % | 23 | 13.57 | 69% | 15.57 | 2.59 | 0.24 | 0.73 | 19% | 12% |
| 5 | 63.5 | 4 | 10.58 | 94.1 % | 23 | 9.70 | 74% | 21.8 | 2.56 | 0.16 | 0.48 | 16% | 10% |
| 6 | 64 | 4 | 10.67 | 94.1 % | 23 | 9.73 | 74% | 21.7 | 2.58 | 0.16 | 0.48 | | |
| 7 | 63.5 | 2 | 21.17 | 96.9 % | 23 | 5.19 | 79.45 % | 40.8 | 2.56 | 0.08 | 0.24 | 12% | 9% |
| 8 | 57.5 | 8 | 4.79 | 87.8 % | 27 | 12.27 | 47% | 20.2 | 2.32 | 0.32 | 0.97 | | |
| 9 | 64 | 9 | 4.74 | 87.7 % | 27 | 13.16 | 45% | 18.8 | 2.58 | 0.36 | 1.09 | | |
| | | | | | | | | | | | | | |
| 11 | 72 | 8.9 | 5.39 | 89.0 % | 27 | 15.30 | 53% | 16.2 | 2.91 | 0.36 | 1.08 | | |

| 12 | 72 | 9 | 5.33 | 88.9 % | 27 | 16.06 | 55% | 15.4 | 2.91 | 0.36 | 1.09 | | |
|----|------|-----|------|--------|------|-------|-------|-------|------|------|------|-----|-----|
| | 72 | 10 | | | | | | | | | | | |
| 13 | | | 4.8 | 87.8 | 27 | 12.40 | 37.93 | 19.99 | 2.91 | 0.41 | 1.25 | | |
| | | | | | | | | | | | | | |
| | | | | | | | | | | | | | |
| 14 | | | | | | | | | | | | | |
| | 32 | 1 | 21.3 | 97.0 % | 14.5 | 2.42 | 74% | 55.0 | 1.29 | 0.04 | 0.12 | 15% | 11% |
| 15 | | | | | | | | | | | | | |
| | 32 | 2 | 10.6 | 94.1 % | 14.5 | 4.1 | 63% | 32.5 | 1.29 | 0.08 | 0.24 | | |
| 16 | | | | | | | | | | | | | |
| | 32 | 3 | 7.1 | 91.4 % | 14.5 | 7.17 | 73% | 18.57 | 1.29 | 0.12 | 0.36 | 19% | 8% |
| 17 | | | | | | | | | | | | | |
| | 33.5 | 4.2 | 5.3 | 88.9 % | 14.5 | 6.62 | 48% | 20.1 | 1.35 | 0.17 | 0.51 | 35% | 17% |
| 18 | | | | | | | | | | | | | |
| 1 | 32 | 4.2 | 5.1 | 88.4 % | 14.5 | 6.57 | 48% | 20.3 | 1.29 | 0.17 | 0.51 | 34% | 18% |

** The carbon (soot) production was not measured experimentally. It is determined by the mass balance after deducting moles of acetylene and cyanide produced from total carbon supplied. Almost 100% propane was consumed since no major peak was observed in the product analysis. Trace amounts (<10ppm) of benzene was detected. A few small peaks of long chain compounds were found but not characterised.

| Test No | Nitrogen Flow | Propane Flow | N:C | Nitrogen Mol % | Power | HCN yield | Cyanide conv | SEC (NaCN) | N2 | CH4 | Carbon ** |
|---------|---------------|-----------------|------|-------------------|-------|-----------|--------------|------------|--------|--------|-----------|
| | SLPM | SLPM | | % | kW | g/min | % | kw-hr/Kg | mol/mi | mol/mi | mol/mi |
| | | | | | | | | | n | n | n |
| M1 | 64 | 19 | 6.74 | 77.1 % | 25 | 12.2 | 59.5 % | 18.7 | 2.58 | 0.77 | 0.77 |
| M2 | 64 | 17 | 7.53 | 79 % | 25 | 12.07 | 65 % | 19 | 2.58 | 0.69 | 0.69 |
| МЗ | 64 | 17 | 7.53 | 79 % | 25 | 12.1 | 65 % | 19 | 2.58 | 0.69 | 0.69 |
| M4 | 64.75 | 13 | 9.96 | 83 % | 25 | 11.57 | 82 % | 19.75 | 2.61 | 0.52 | 0.52 |
| M5 | 65 | 14 | 9.15 | 82% | 26 | 12.95 | 85% | 19.13 | 2.85 | 0.62 | 0.62 |
| M6 | 64 | 10 | 13 | 87% | 25 | 9.21 | 85% | 24.92 | 2.90 | 0.44 | 0.44 |
| M7 | 64 | 7.5 | 17 | 90% | 25 | 7.15 | 87% | 32.12 | 2.90 | 0.33 | 0.33 |
| M8 | 64 | 7.5 | 17 | 90% | 25 | 6.82 | 85% | 34.96 | 2.85 | 0.33 | 0.33 |
| M9 | 64 | 5 | 25.5 | 93% | 25 | 5.04 | 92% | 45.62 | 2.85 | 0.22 | 0.22 |

^{**} The carbon (soot) production was not measured experimentally. It is determined by the mass balance after deducting moles of acetylene and cyanide produced from total carbon supplied. 100% methane was consumed since no major peak was observed in the product analysis.