

Supplementary information for

Hydrogenation of CO/CO₂ Mixtures on Nickel Catalysts: Kinetics and Flexibility for Nickel Catalysts

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Criteria for absence of transfer limitations

Table S1: Criteria for the exclusion of transfer limitations (symbols see Table S2).

	mass-transfer	heat-transfer
internal transfer limitations	Mears criterion ¹ : $\frac{r_{\text{CH}_4} r_p}{c_i D_{i,\text{eff}}} \leq \frac{1}{ n } \quad i \in \text{CO, CO}_2$	Anderson criterion ² : $\frac{r_{\text{CH}_4} \Delta H \rho_{\text{cat}} d_{\text{cat}}^2}{4 \lambda_{\text{eff}} T} \leq \frac{0.75 R T}{E_A}$
external transfer limitations	Carberry criterion ³ : $Ca = \frac{r_{\text{CH}_4} \rho_{\text{cat}}}{k_g a c_i} \leq 0.05$	Mears criterion ¹ : $\frac{r_{\text{CH}_4} \Delta H \rho_{\text{cat}} d_{\text{cat}}}{h_t T} \leq \frac{0.3 R T}{E_A}$

Table S2: Symbols used in equations in Table S1.

Latin symbols		
Carberry Number	Ca	1
Concentration of component i	c_i	mol m ⁻³
Effective diffusion coefficient of component i	$D_{i,\text{eff}}$	m ² s ⁻¹
Catalyst particle diameter	d_{cat}	m
Activation energy	E_A	J mol ⁻¹
Enthalpy of reaction	ΔH	J mol ⁻¹
Heat transfer coefficient between gas and particle	h_t	W m ⁻² K ⁻¹
Mass transfer coefficient	$k_g a$	m s ⁻¹
Reaction order	n	1
Universal gas constant	R	J mol ⁻¹ K ⁻¹
Observed reaction rate	r_{CH_4}	mol s ⁻¹
Catalyst particle radius	r_p	m
Reaction temperature	T	K
Greek symbols		
Effective heat conductivity	λ_{eff}	W m ⁻¹ K ⁻¹
Catalyst particle density	ρ_{cat}	kg m ⁻³

Additional Figures

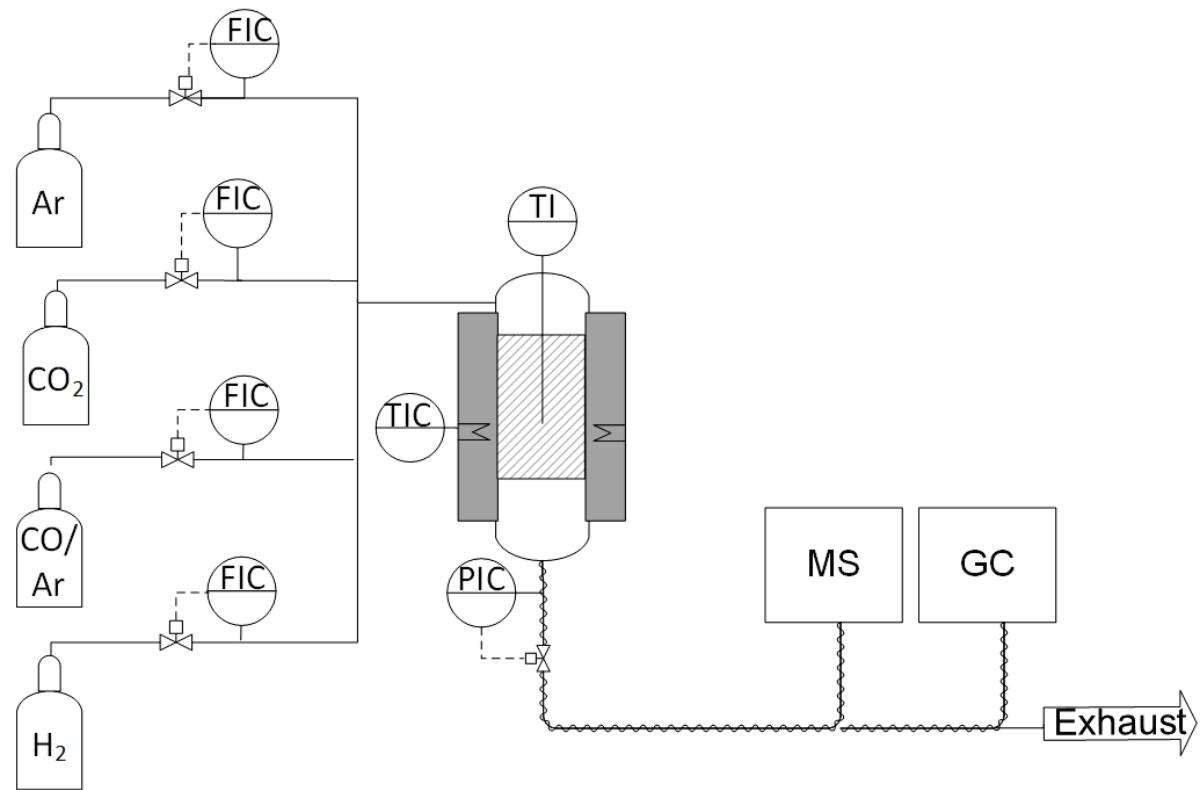


Figure S1: Flowsheet of the fixed bed reactor setup.

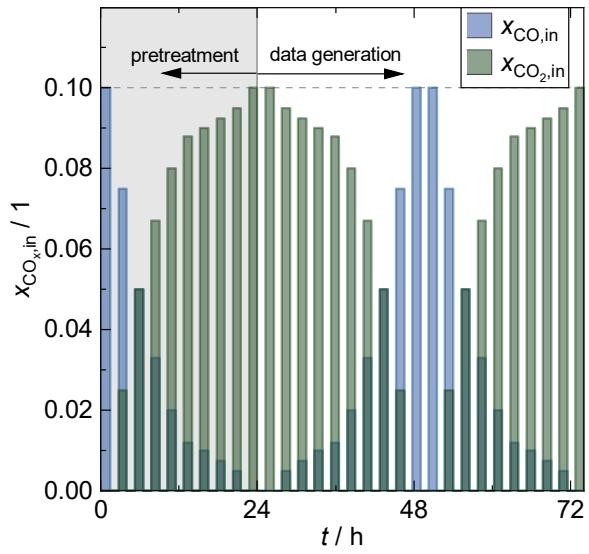


Figure S2: Typical variation of the specific inlet carbon oxide composition in one experimental run.

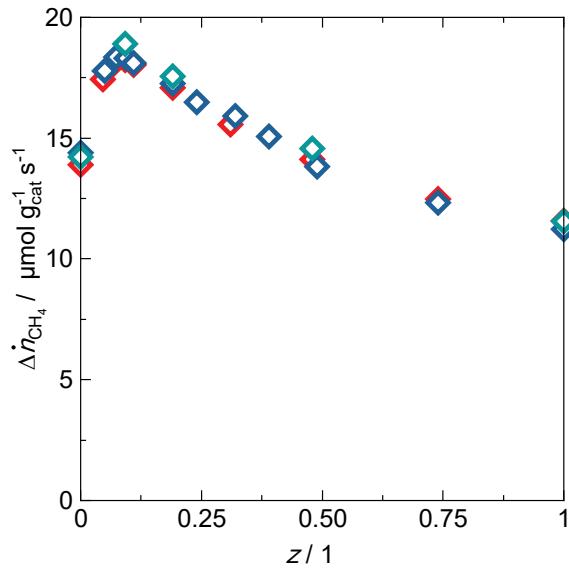


Figure S3: CH₄ formation rates of three different campaigns indicated with different colors; for sake of clarity average values of single experiments within one run are shown as symbols; reaction conditions: 556 K, 2 bar, 250 mL_{STP} min⁻¹ total flow rate, 800 mbar H₂ inlet partial pressure.

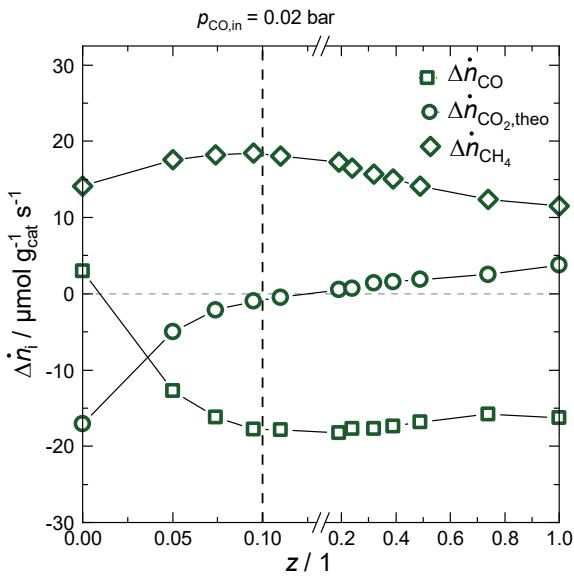


Figure S4: Measured conversion rates $\Delta\dot{n}_i$ for CO and CH₄, as well as the theoretical CO₂ conversion rate during CO_x methanation; shaded background indicates 95 % confidence interval; reaction conditions: 556 K, 2 bar(a), total flow rate 250 mL_{STP} min⁻¹, 800 mbar H₂ inlet partial pressure.

The theoretical CO₂ conversion rate is calculated as follows:

$$\Delta\dot{n}_{\text{CO}_2, \text{theo}} = \dot{n}_{\text{CO,in}} - (\dot{n}_{\text{CO,out}} + \dot{n}_{\text{CH}_4,out} + 2 \dot{n}_{\text{C}_2\text{H}_6,out} + 3 \dot{n}_{\text{C}_3\text{H}_8,out}).$$

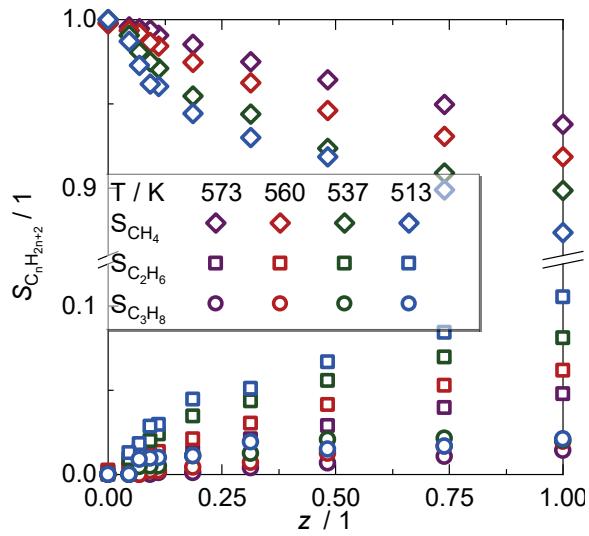


Figure S5: Hydrocarbon selectivity at different temperatures; reaction conditions: 2 bar, total flow rate $250 \text{ mL}_{\text{STP}} \text{ min}^{-1}$, 800 mbar H_2 inlet partial pressure.

The selectivity $S_{C_nH_{2n+2}}$ is calculated as follows: $S_{C_nH_{2n+2}} = \frac{\dot{n}_{C_nH_{2n+2}}}{\dot{n}_{CH_4} + \dot{n}_{C_2H_4} + \dot{n}_{C_3H_6}}$.

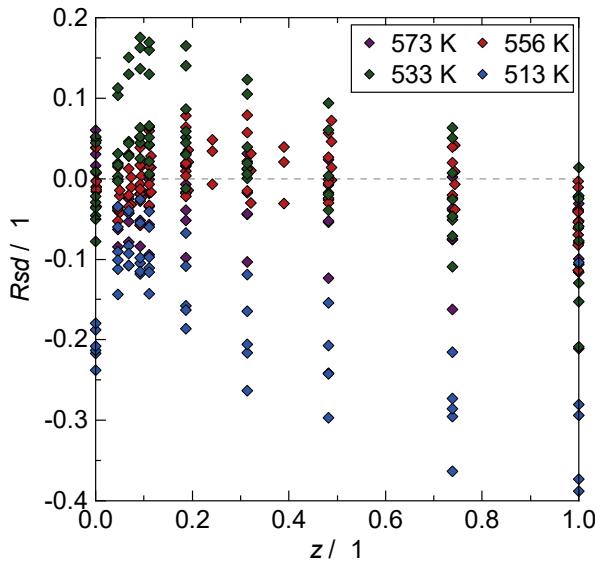


Figure S6: Residuals Rsd for the simulated methane formation rate over the complete range of CO_x inlet compositions between pure CO and pure CO_2 methanation at different temperatures; residuals at 556 K for parameter estimation; residuals at 513, 533, and 573 K for model validation; reaction conditions: 2 bar, total flow rate $250 \text{ mL}_{\text{STP}} \text{ min}^{-1}$, 800 mbar H_2 inlet partial pressure.

Residuals are calculated as follows:

$$RSD = \frac{r_{\text{CH}_4,\text{sim}} - r_{\text{CH}_4,\text{obs}}}{r_{\text{CH}_4,\text{obs}}}$$

with $r_{\text{CH}_4,\text{sim}}$ as the simulated methane formation rate and $r_{\text{CH}_4,\text{obs}}$ as the observed methane formation rate.

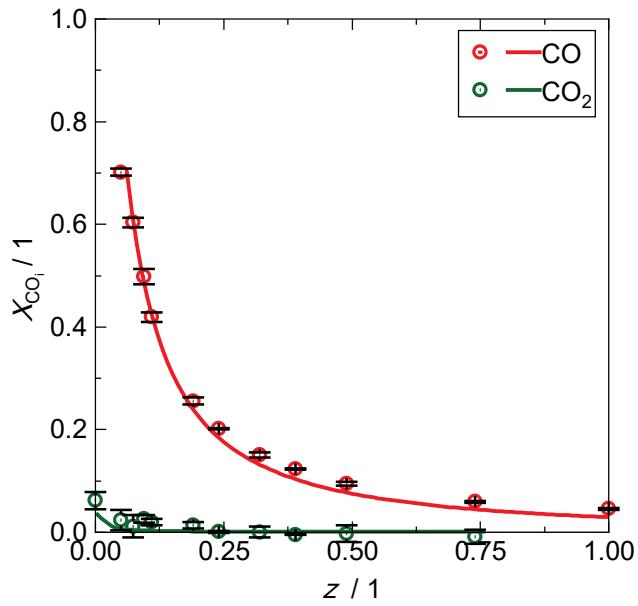


Figure S7: Comparison between simulated (lines) and experimental (symbols) CO and CO_2 conversion X_{CO_i} observed during CO_x methanation; reaction conditions: 556 K, 2 bar, total flow rate 250 mL_{STP} min⁻¹, 800 mbar H_2 inlet partial pressure.

The individual conversion X_{CO_i} for CO and CO_2 is calculated as follows: $X_{\text{CO}_i} = 1 - \frac{\dot{n}_{\text{CO}_i,\text{out}}}{\dot{n}_{\text{CO}_i,\text{in}}}$.

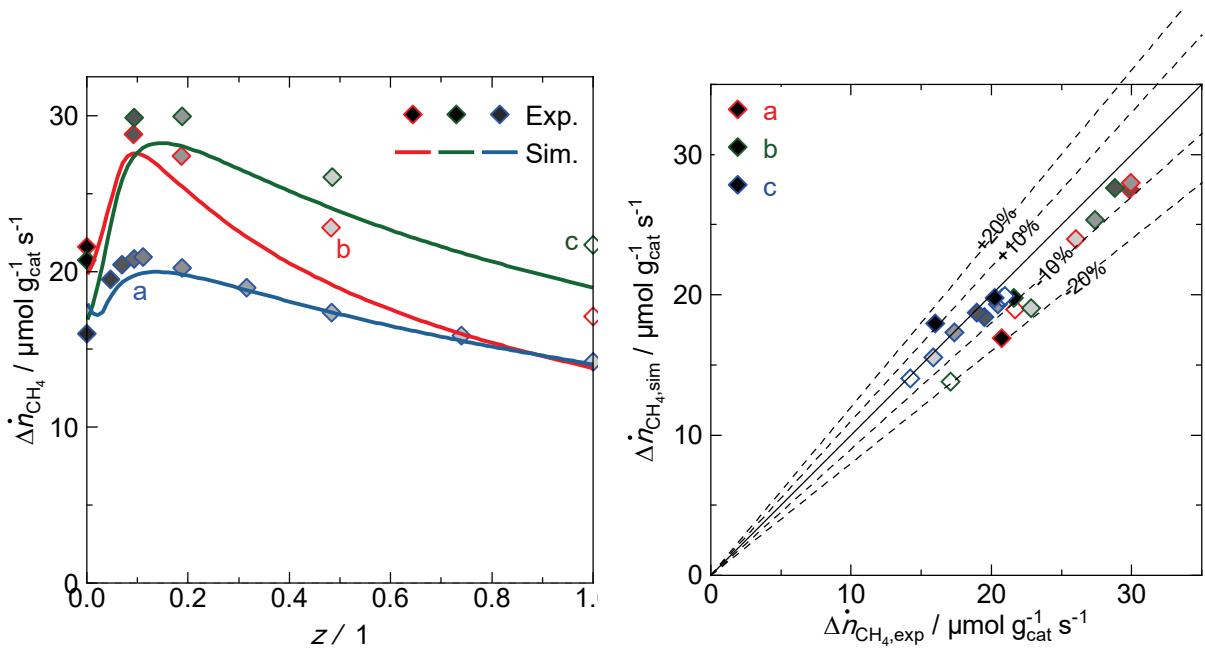


Figure S8: Comparison between experimental (symbols) and simulated (lines) results under different reaction conditions in dependency on the carbon oxide composition (left) and corresponding parity plot (right); for these experiments only two hysteresis are conducted with respect to the carbon oxide composition and the second one is shown; reaction conditions:

- a) 570 K, 2 bar, 500 mbar H₂ and 166 mbar CO_x inlet partial pressure, total flow rate 300 mL_{STP} min⁻¹
- b) 556 K, 3.85 bar, 1540 mbar H₂ and 385 mbar CO_x inlet partial pressure, total flow rate 250 mL_{STP} min⁻¹
- c) 556 K, 2 bar, 1600 mbar H₂ and 200 mbar CO_x inlet partial pressure, total flow rate 250 mL_{STP} min⁻¹.

Data used for optimization of f_{CO} , f_{CO_2} and f_{KC}

Table S3: Experimental data sets with z and r_{CH_4} used for estimation of f_{CO} , f_{CO_2} , and f_{KC} ; reaction conditions: 556 K, 2 bar, 250 mL_{STP} min⁻¹ total flow rate, 800 mbar H₂ inlet partial pressure.

$z / 1$	$r_{\text{CH}_4} / \text{mol/g}_{\text{cat}} \text{s}^{-1}$	$z / 1$	$r_{\text{CH}_4} / \text{mol/g}_{\text{cat}} \text{s}^{-1}$	$z / 1$	$r_{\text{CH}_4} / \text{mol/g}_{\text{cat}} \text{s}^{-1}$
0.00	$1.46 \cdot 10^{-5}$	0.11	$1.86 \cdot 10^{-5}$	0.49	$1.43 \cdot 10^{-5}$
0.00	$1.43 \cdot 10^{-5}$	0.11	$1.80 \cdot 10^{-5}$	0.49	$1.41 \cdot 10^{-5}$
0.00	$1.42 \cdot 10^{-5}$	0.11	$1.78 \cdot 10^{-5}$	0.49	$1.36 \cdot 10^{-5}$
0.00	$1.43 \cdot 10^{-5}$	0.11	$1.89 \cdot 10^{-5}$	0.49	$1.33 \cdot 10^{-5}$
0.00	$1.41 \cdot 10^{-5}$	0.11	$1.84 \cdot 10^{-5}$	0.49	$1.47 \cdot 10^{-5}$
0.00	$1.40 \cdot 10^{-5}$	0.11	$1.82 \cdot 10^{-5}$	0.49	$1.43 \cdot 10^{-5}$
0.00	$1.36 \cdot 10^{-5}$	0.11	$1.80 \cdot 10^{-5}$	0.49	$1.40 \cdot 10^{-5}$
0.00	$1.35 \cdot 10^{-5}$	0.11	$1.75 \cdot 10^{-5}$	0.49	$1.36 \cdot 10^{-5}$
0.00	$1.43 \cdot 10^{-5}$	0.11	$1.72 \cdot 10^{-5}$	0.49	$1.48 \cdot 10^{-5}$
0.00	$1.41 \cdot 10^{-5}$	0.19	$1.78 \cdot 10^{-5}$	0.49	$1.44 \cdot 10^{-5}$
0.05	$1.81 \cdot 10^{-5}$	0.19	$1.71 \cdot 10^{-5}$	0.74	$1.28 \cdot 10^{-5}$
0.05	$1.77 \cdot 10^{-5}$	0.19	$1.69 \cdot 10^{-5}$	0.74	$1.24 \cdot 10^{-5}$
0.05	$1.76 \cdot 10^{-5}$	0.19	$1.79 \cdot 10^{-5}$	0.74	$1.22 \cdot 10^{-5}$
0.05	$1.80 \cdot 10^{-5}$	0.19	$1.74 \cdot 10^{-5}$	0.74	$1.19 \cdot 10^{-5}$
0.05	$1.78 \cdot 10^{-5}$	0.19	$1.72 \cdot 10^{-5}$	0.74	$1.30 \cdot 10^{-5}$
0.05	$1.71 \cdot 10^{-5}$	0.19	$1.73 \cdot 10^{-5}$	0.74	$1.27 \cdot 10^{-5}$
0.05	$1.69 \cdot 10^{-5}$	0.19	$1.65 \cdot 10^{-5}$	0.74	$1.26 \cdot 10^{-5}$
0.07	$1.87 \cdot 10^{-5}$	0.19	$1.63 \cdot 10^{-5}$	0.74	$1.21 \cdot 10^{-5}$
0.07	$1.83 \cdot 10^{-5}$	0.19	$1.80 \cdot 10^{-5}$	0.74	$1.19 \cdot 10^{-5}$
0.07	$1.81 \cdot 10^{-5}$	0.19	$1.75 \cdot 10^{-5}$	1.00	$1.15 \cdot 10^{-5}$
0.07	$1.87 \cdot 10^{-5}$	0.19	$1.72 \cdot 10^{-5}$	1.00	$1.12 \cdot 10^{-5}$
0.07	$1.84 \cdot 10^{-5}$	0.24	$1.70 \cdot 10^{-5}$	1.00	$1.14 \cdot 10^{-5}$
0.07	$1.78 \cdot 10^{-5}$	0.24	$1.63 \cdot 10^{-5}$	1.00	$1.09 \cdot 10^{-5}$
0.07	$1.75 \cdot 10^{-5}$	0.24	$1.61 \cdot 10^{-5}$	1.00	$1.23 \cdot 10^{-5}$
0.10	$1.87 \cdot 10^{-5}$	0.32	$1.65 \cdot 10^{-5}$	1.00	$1.16 \cdot 10^{-5}$
0.10	$1.82 \cdot 10^{-5}$	0.32	$1.58 \cdot 10^{-5}$	1.00	$1.13 \cdot 10^{-5}$
0.10	$1.80 \cdot 10^{-5}$	0.32	$1.55 \cdot 10^{-5}$	1.00	$1.19 \cdot 10^{-5}$
0.10	$1.94 \cdot 10^{-5}$	0.32	$1.63 \cdot 10^{-5}$	1.00	$1.14 \cdot 10^{-5}$
0.10	$1.86 \cdot 10^{-5}$	0.32	$1.59 \cdot 10^{-5}$	1.00	$1.10 \cdot 10^{-5}$
0.10	$1.84 \cdot 10^{-5}$	0.32	$1.57 \cdot 10^{-5}$	1.00	$1.17 \cdot 10^{-5}$
0.10	$1.80 \cdot 10^{-5}$	0.32	$1.52 \cdot 10^{-5}$	1.00	$1.14 \cdot 10^{-5}$
0.10	$1.76 \cdot 10^{-5}$	0.32	$1.49 \cdot 10^{-5}$		
0.10	$1.74 \cdot 10^{-5}$	0.39	$1.57 \cdot 10^{-5}$		
0.10	$1.94 \cdot 10^{-5}$	0.39	$1.49 \cdot 10^{-5}$		
0.10	$1.88 \cdot 10^{-5}$	0.39	$1.46 \cdot 10^{-5}$		
0.10	$1.85 \cdot 10^{-5}$				

CO _x methanation @556 K for kinetic parameter estimation, continued										
feed ratio CO/(CO+CO ₂) z 1	consumption or formation rates for			conversion for		selectivity for				
	CO	CO ₂	CH ₄	X _{CO}	X _{CO₂}	CH ₄	C ₂ H ₆	C ₃ H ₈	S _{CH₄}	S _{C₂H₆}
	Δn _{CO} mol g ⁻¹ s ⁻¹	Δn _{CO₂} mol g ⁻¹ s ⁻¹	Δn _{CH₄} mol g ⁻¹ s ⁻¹							
1,000E+00	1,606E-05	-1,836E-07	1,153E-05	4,544E-02	-	9,181E-01	6,433E-02	1,754E-02		
1,000E+00	1,553E-05	-1,101E-07	1,116E-05	4,396E-02	-	9,184E-01	6,344E-02	1,813E-02		
1,000E+00	1,592E-05	-1,103E-07	1,136E-05	4,506E-02	-	9,196E-01	6,250E-02	1,786E-02		
1,000E+00	1,508E-05	-1,101E-07	1,094E-05	4,269E-02	-	9,198E-01	6,173E-02	1,852E-02		
1,000E+00	1,745E-05	-1,825E-07	1,230E-05	4,865E-02	-	9,158E-01	6,250E-02	2,174E-02		
1,000E+00	1,666E-05	-1,096E-07	1,162E-05	4,643E-02	-	9,191E-01	6,069E-02	2,023E-02		
1,000E+00	1,616E-05	-7,295E-08	1,134E-05	4,504E-02	-	9,201E-01	5,917E-02	2,071E-02		
1,000E+00	1,705E-05	-1,094E-07	1,189E-05	4,753E-02	-	9,183E-01	6,197E-02	1,972E-02		
1,000E+00	1,599E-05	-1,097E-07	1,137E-05	4,456E-02	-	9,174E-01	6,195E-02	2,065E-02		
1,000E+00	1,563E-05	-7,300E-08	1,102E-05	4,355E-02	-	9,207E-01	6,098E-02	1,829E-02		
1,000E+00	1,722E-05	-1,107E-07	1,173E-05	4,801E-02	-	9,164E-01	6,340E-02	2,017E-02		
1,000E+00	1,674E-05	-7,389E-08	1,138E-05	4,667E-02	-	9,167E-01	6,250E-02	2,083E-02		

parameter	catalyst mass	5,000E-02 g	reaction temperature	573 K	reaction pressure	2,000E+05 Pa	volumetric inlet flow rate	2,500E+02 mL _{STP} min ⁻¹
feed ratio CO/(CO+CO ₂)	consumption or formation rates for			conversion for		selectivity for		
z	CO Δn_{CO} mol g ⁻¹ s ⁻¹	CO ₂ Δn_{CO_2} mol g ⁻¹ s ⁻¹	CH ₄ Δn_{CH_4} mol g ⁻¹ s ⁻¹	CO χ_{CO}	CO ₂ χ_{CO_2}	CH ₄ S_{CH_4}	C ₂ H ₆ S_{C2H_6}	C ₃ H ₈ S_{C3H_8}
1	-5,154E-06	3,030E-05	2,308E-05	-	7,766E-02	9,968E-01	3,226E-03	0,000E+00
0,000E+00	-4,995E-06	4,279E-05	2,326E-05	-	1,097E-01	9,968E-01	3,195E-03	0,000E+00
0,000E+00	-5,113E-06	4,045E-05	2,281E-05	-	1,037E-01	9,967E-01	3,263E-03	0,000E+00
0,000E+00	-5,052E-06	4,108E-05	2,260E-05	-	1,053E-01	9,983E-01	1,653E-03	0,000E+00
4,590E-02	1,187E-05	2,796E-05	2,696E-05	6,657E-01	7,547E-02	9,959E-01	4,127E-03	0,000E+00
4,590E-02	1,190E-05	2,741E-05	2,684E-05	6,675E-01	7,399E-02	9,959E-01	4,149E-03	0,000E+00
6,892E-02	1,880E-05	1,649E-05	2,918E-05	7,058E-01	4,582E-02	9,949E-01	5,089E-03	0,000E+00
6,892E-02	1,866E-05	1,437E-05	2,864E-05	7,007E-01	3,993E-02	9,948E-01	5,175E-03	0,000E+00
6,892E-02	1,866E-05	1,195E-05	2,853E-05	7,008E-01	3,322E-02	9,948E-01	5,242E-03	0,000E+00
9,237E-02	2,398E-05	1,727E-05	2,984E-05	6,745E-01	4,943E-02	9,926E-01	7,426E-03	0,000E+00
9,237E-02	2,394E-05	1,673E-05	2,984E-05	6,734E-01	4,788E-02	9,938E-01	6,219E-03	0,000E+00
1,109E-01	2,688E-05	9,081E-06	3,096E-05	6,315E-01	2,662E-02	9,905E-01	8,323E-03	1,189E-03
1,109E-01	2,662E-05	7,499E-06	3,044E-05	6,254E-01	2,198E-02	9,903E-01	8,464E-03	1,209E-03
1,109E-01	2,649E-05	3,871E-06	3,039E-05	6,223E-01	1,135E-02	9,902E-01	8,547E-03	1,221E-03
1,109E-01	2,623E-05	1,490E-07	2,992E-05	6,162E-01	4,367E-04	9,913E-01	7,500E-03	1,250E-03
1,871E-01	3,149E-05	1,307E-06	3,156E-05	4,416E-01	4,216E-03	9,838E-01	1,392E-02	2,320E-03
1,871E-01	3,107E-05	-1,072E-06	3,082E-05	4,357E-01	-3,461E-03	9,845E-01	1,310E-02	2,381E-03
1,871E-01	3,077E-05	9,402E-06	3,053E-05	4,314E-01	3,034E-02	9,855E-01	1,332E-02	1,211E-03
1,871E-01	3,013E-05	7,102E-06	2,986E-05	4,224E-01	2,292E-02	9,851E-01	1,361E-02	1,238E-03
3,139E-01	3,277E-05	6,184E-06	3,037E-05	2,782E-01	2,402E-02	9,750E-01	2,143E-02	3,571E-03
3,139E-01	3,204E-05	4,418E-06	2,955E-05	2,720E-01	1,716E-02	9,755E-01	2,083E-02	3,676E-03
3,139E-01	3,130E-05	-2,707E-06	2,888E-05	2,657E-01	-1,051E-02	9,747E-01	2,146E-02	3,788E-03
3,139E-01	3,038E-05	-5,483E-06	2,818E-05	2,579E-01	-2,129E-02	9,753E-01	2,078E-02	3,896E-03
4,823E-01	3,203E-05	-1,108E-07	2,844E-05	1,797E-01	-5,794E-04	9,622E-01	3,023E-02	7,557E-03
4,823E-01	3,101E-05	-1,036E-06	2,768E-05	1,740E-01	-5,415E-03	9,637E-01	2,979E-02	6,477E-03
4,823E-01	3,056E-05	2,391E-07	2,715E-05	1,715E-01	1,250E-03	9,642E-01	2,918E-02	6,631E-03
4,823E-01	2,936E-05	-4,906E-07	2,633E-05	1,647E-01	-2,565E-03	9,644E-01	2,877E-02	6,849E-03
7,388E-01	3,108E-05	1,235E-06	2,611E-05	1,163E-01	1,307E-02	9,475E-01	4,038E-02	1,211E-02
7,388E-01	2,949E-05	5,298E-07	2,513E-05	1,103E-01	5,607E-03	9,495E-01	3,927E-02	1,122E-02
7,388E-01	2,967E-05	1,231E-06	2,507E-05	1,110E-01	1,303E-02	9,493E-01	3,944E-02	1,127E-02
7,388E-01	2,812E-05	5,201E-07	2,411E-05	1,052E-01	5,504E-03	9,500E-01	3,971E-02	1,029E-02
1,000E+00	3,066E-05	-2,610E-07	2,423E-05	8,545E-02	-	9,366E-01	4,899E-02	1,441E-02
1,000E+00	2,885E-05	-1,866E-07	2,303E-05	8,041E-02	-	9,391E-01	4,718E-02	1,370E-02
1,000E+00	3,005E-05	-2,240E-07	2,371E-05	8,375E-02	-	9,366E-01	4,867E-02	1,475E-02
1,000E+00	2,825E-05	-1,871E-07	2,252E-05	7,872E-02	-	9,392E-01	4,680E-02	1,404E-02

CO_x methanation @513 K

Parameter	catalyst mass	5,000E-02 g
	reaction temperature	513 K
	reaction pressure	2,000E+05 Pa
	volumetric inlet flow rate	2,500E+02 mL _{STP} min ⁻¹

feed ratio CO/(CO+CO ₂) z	consumption or formation rates for			conversion for		selectivity for		
	CO	CO ₂	CH ₄	CO	CO ₂	CH ₄	C ₂ H ₆	C ₃ H ₈
	$\Delta\dot{n}_{CO}$ mol g ⁻¹ s ⁻¹	$\Delta\dot{n}_{CO_2}$ mol g ⁻¹ s ⁻¹	$\Delta\dot{n}_{CH_4}$ mol g ⁻¹ s ⁻¹	X _{CO}	X _{CO₂}	S _{CH₄}	S _{C₂H₆}	S _{C₃H₈}
0,000E+00	-8,874E-07	1,227E-05	3,882E-06	-	3,145E-02	1,000E+00	0,000E+00	0,000E+00
0,000E+00	-8,529E-07	1,177E-05	3,857E-06	-	3,016E-02	1,000E+00	0,000E+00	0,000E+00
0,000E+00	-8,111E-07	6,252E-06	3,761E-06	-	1,602E-02	1,000E+00	0,000E+00	0,000E+00
0,000E+00	-8,482E-07	4,451E-06	3,725E-06	-	1,141E-02	1,000E+00	0,000E+00	0,000E+00
4,590E-02	4,468E-06	6,199E-06	4,489E-06	2,507E-01	1,673E-02	9,837E-01	1,626E-02	0,000E+00
4,590E-02	4,543E-06	4,975E-06	4,712E-06	2,549E-01	1,343E-02	9,845E-01	1,550E-02	0,000E+00
4,590E-02	4,248E-06	4,262E-06	4,291E-06	2,383E-01	1,150E-02	9,915E-01	8,547E-03	0,000E+00
4,590E-02	4,397E-06	3,188E-06	4,180E-06	2,467E-01	8,605E-03	9,826E-01	1,739E-02	0,000E+00
6,892E-02	4,324E-06	4,070E-06	4,262E-06	1,623E-01	1,131E-02	9,746E-01	1,695E-02	8,475E-03
6,892E-02	4,536E-06	3,122E-06	4,190E-06	1,703E-01	8,677E-03	9,741E-01	1,724E-02	8,621E-03
6,892E-02	4,143E-06	5,455E-06	3,971E-06	1,556E-01	1,516E-02	9,727E-01	1,818E-02	9,091E-03
6,892E-02	4,319E-06	4,627E-06	3,960E-06	1,622E-01	1,286E-02	9,727E-01	1,818E-02	9,091E-03
9,237E-02	4,262E-06	7,840E-07	4,037E-06	1,199E-01	2,244E-03	9,646E-01	2,655E-02	8,850E-03
9,237E-02	4,425E-06	3,083E-08	3,961E-06	1,245E-01	8,825E-05	9,640E-01	2,703E-02	9,009E-03
9,237E-02	4,010E-06	6,242E-06	3,781E-06	1,128E-01	1,787E-02	9,623E-01	2,830E-02	9,434E-03
9,237E-02	4,252E-06	5,163E-06	3,667E-06	1,196E-01	1,478E-02	9,612E-01	2,913E-02	9,709E-03
1,109E-01	4,147E-06	-1,581E-06	3,856E-06	9,744E-02	-4,636E-03	9,630E-01	2,778E-02	9,259E-03
1,109E-01	4,338E-06	-4,128E-06	3,778E-06	1,019E-01	-1,210E-02	9,623E-01	2,830E-02	9,434E-03
1,109E-01	3,886E-06	9,499E-06	3,627E-06	9,131E-02	2,784E-02	9,608E-01	2,941E-02	9,804E-03
1,109E-01	4,167E-06	8,442E-06	3,554E-06	9,791E-02	2,475E-02	9,600E-01	3,000E-02	1,000E-02
1,871E-01	4,192E-06	7,613E-06	3,447E-06	5,879E-02	2,457E-02	9,490E-01	4,082E-02	1,020E-02
1,871E-01	3,382E-06	6,533E-06	3,235E-06	4,743E-02	2,108E-02	9,457E-01	4,348E-02	1,087E-02
1,871E-01	3,964E-06	2,780E-06	3,094E-06	5,558E-02	8,970E-03	9,432E-01	4,545E-02	1,136E-02
3,139E-01	4,163E-06	-5,571E-06	2,935E-06	3,534E-02	-2,163E-02	9,405E-01	4,762E-02	1,190E-02
3,139E-01	3,155E-06	-3,173E-06	2,790E-06	2,678E-02	-1,232E-02	9,259E-01	4,938E-02	2,469E-02
3,139E-01	3,885E-06	-6,736E-06	2,647E-06	3,298E-02	-2,616E-02	9,342E-01	5,263E-02	1,316E-02
4,823E-01	3,435E-06	1,467E-06	2,490E-06	1,928E-02	7,667E-03	9,178E-01	6,849E-02	1,370E-02
4,823E-01	2,754E-06	-1,714E-06	2,380E-06	1,545E-02	-8,960E-03	9,143E-01	7,143E-02	1,429E-02
4,823E-01	3,351E-06	-2,389E-06	2,232E-06	1,880E-02	-1,249E-02	9,231E-01	6,154E-02	1,538E-02
7,388E-01	3,129E-06	1,286E-08	2,045E-06	1,171E-02	1,361E-04	9,016E-01	8,197E-02	1,639E-02
7,388E-01	2,632E-06	-7,165E-07	2,080E-06	9,845E-03	-7,583E-03	9,032E-01	8,065E-02	1,613E-02
7,388E-01	2,954E-06	-1,065E-06	1,894E-06	1,105E-02	-1,127E-02	8,947E-01	8,772E-02	1,754E-02
1,000E+00	2,135E-06	-1,113E-07	1,966E-06	5,950E-03	-	8,833E-01	1,000E-01	1,667E-02
1,000E+00	4,670E-06	-3,714E-08	1,746E-06	1,302E-02	-	8,868E-01	9,434E-02	1,887E-02
1,000E+00	3,008E-06	-3,718E-08	1,376E-06	8,384E-03	-	8,605E-01	1,163E-01	2,326E-02
1,000E+00	3,540E-06	-3,724E-08	1,713E-06	9,867E-03	-	8,846E-01	9,615E-02	1,923E-02

Parameter	catalyst mass	5,000E-02 g
z	reaction temperature	556 K
	reaction pressure	2,000E+05 Pa
	volumetric inlet flow rate	2,500E+02 mL _{STP} min ⁻¹
feed ratio CO/(CO+CO ₂)		consumption or formation rates for
z	CO $\Delta\dot{n}_{CO}$ mol g ⁻¹ s ⁻¹	CO ₂ $\Delta\dot{n}_{CO_2}$ mol g ⁻¹ s ⁻¹
1		CH ₄ $\Delta\dot{n}_{CH_4}$ mol g ⁻¹ s ⁻¹
0,000E+00	6,489E-05	-2,364E-04
0,000E+00	6,567E-05	-2,233E-04
0,000E+00	6,562E-05	-2,124E-04
0,000E+00	6,583E-05	-3,981E-04
0,000E+00	6,593E-05	-3,703E-04
0,000E+00	6,758E-05	-3,497E-04
0,000E+00	6,421E-05	-2,579E-04
0,000E+00	6,484E-05	-2,324E-04
0,000E+00	6,492E-05	-1,508E-04
0,000E+00	6,536E-05	-1,218E-04
0,000E+00	6,585E-05	-1,044E-04
4,763E-02	6,202E-05	-2,441E-04
4,763E-02	6,271E-05	-2,301E-04
4,763E-02	6,263E-05	-2,239E-04
4,763E-02	6,371E-05	-2,386E-04
4,763E-02	6,442E-05	-2,232E-04
4,763E-02	6,527E-05	-2,220E-04
7,368E-02	6,063E-05	-2,398E-04
7,368E-02	6,113E-05	-2,307E-04
7,368E-02	6,116E-05	-2,280E-04
7,368E-02	6,212E-05	-2,522E-04
7,368E-02	6,295E-05	-2,376E-04
7,368E-02	6,307E-05	-2,335E-04
1,002E-01	5,898E-05	-2,370E-04
1,002E-01	5,969E-05	-2,310E-04
1,002E-01	6,048E-05	-2,171E-04
1,002E-01	6,079E-05	-2,435E-04
1,002E-01	6,067E-05	-2,287E-04
1,002E-01	6,145E-05	-2,319E-04
1,207E-01	5,588E-05	-3,939E-04
1,207E-01	5,812E-05	-3,810E-04
1,207E-01	5,893E-05	-3,623E-04
1,207E-01	5,931E-05	-2,577E-04
1,207E-01	6,017E-05	-2,465E-04
1,207E-01	5,993E-05	-2,401E-04
1,207E-01	5,714E-05	-2,172E-04
1,207E-01	5,860E-05	-1,937E-04
2,024E-01	5,290E-05	-3,307E-04
2,024E-01	5,431E-05	-3,117E-04
2,024E-01	5,366E-05	-3,055E-04
2,024E-01	5,469E-05	-2,505E-04
2,024E-01	5,484E-05	-2,414E-04
3,344E-01	4,535E-05	-3,024E-04
3,344E-01	4,554E-05	-2,843E-04
3,344E-01	4,638E-05	-2,774E-04
3,344E-01	4,645E-05	-2,550E-04
3,344E-01	4,672E-05	-2,459E-04
5,054E-01	3,688E-05	-2,402E-04
5,054E-01	3,683E-05	-2,149E-04
5,054E-01	3,608E-05	-2,564E-04
5,054E-01	3,629E-05	-2,499E-04
7,549E-01	1,987E-05	-2,601E-04
7,549E-01	1,916E-05	-2,570E-04
7,549E-01	1,992E-05	-2,450E-04
7,549E-01	1,988E-05	-2,397E-04

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