

## Supporting Information

### **Iron–Potassium on Single-Walled Carbon Nanotubes as Efficient Catalyst for CO<sub>2</sub> Hydrogenation to Heavy Olefins**

Shunwu Wang,<sup>†</sup> Tijun Wu,<sup>†</sup> Jun Lin,<sup>‡</sup> Yushan Ji,<sup>†</sup> Shirun Yan,<sup>†</sup> Yan Pei,<sup>†</sup> Songhai

Xie,<sup>\*,†</sup> Baoning Zong,<sup>§</sup> Minghua Qiao<sup>\*,†</sup>

<sup>†</sup>Collaborative Innovation Center of Chemistry for Energy Materials, Department of Chemistry and  
Shanghai Key Laboratory of Molecular Catalysis and Innovative Materials, Fudan University,  
Shanghai 200438, P. R. China

<sup>‡</sup>Key Laboratory of Nuclear Analysis Techniques, Shanghai Institute of Applied Physics, Chinese  
Academy of Sciences, Shanghai 201800, P. R. China

<sup>§</sup>State Key Laboratory of Catalytic Materials and Chemical Engineering, Research Institute of  
Petroleum Processing, SINOPEC, Beijing 100083, P. R. China

**Table S1. Comparison of the Results in Literature Works for CO<sub>2</sub> Hydrogenation to Olefins with the Selectivity to Heavy Olefins being Available**

catalyst	<i>T</i> (K)	<i>P</i> (MPa)	H <sub>2</sub> /CO <sub>2</sub> (v/v)	CO <sub>2</sub> conv. (%)	FTY <sub>H<sub>Cs</sub></sub> (μmol <sub>CO<sub>2</sub></sub> g <sub>Fe<sup>-1</sup></sub> s <sup>-1</sup> )	CO sel. (%)	hydrocarbon distribution (%)				FTY <sub>C<sub>2-C<sub>4</sub>=</sub></sub> (μmol <sub>CO<sub>2</sub></sub> g <sub>Fe<sup>-1</sup></sub> s <sup>-1</sup> )	FTY <sub>C<sub>5+</sub>=</sub> (μmol <sub>CO<sub>2</sub></sub> g <sub>Fe<sup>-1</sup></sub> s <sup>-1</sup> )	
							CH <sub>4</sub>	C <sub>2</sub> -C <sub>4</sub> <sup>=</sup>	C <sub>2</sub> -C <sub>4</sub> <sup>0</sup>	C <sub>5+</sub> <sup>=</sup>	C <sub>5+</sub> <sup>0</sup>		
Fe/C-Bio <sup>1</sup>	593	1.0	3	31	11.6	23.2	11.8	21.7 <sup>a</sup>	2.7 <sup>b</sup>	50.3 <sup>c</sup>	13.5 <sup>d</sup>	2.5 <sup>a</sup>	5.9 <sup>c</sup>
Fe/C-K <sup>1</sup>	593	1.0	3	28	9.2	22.6	24	29.9 <sup>a</sup>	8.2 <sup>b</sup>	30.5 <sup>c</sup>	7.4 <sup>d</sup>	2.7 <sup>a</sup>	2.8 <sup>c</sup>
Fe/Co-Y <sub>K</sub> <sup>2</sup>	573	1.0	3	25.9	2.0	21.1	13.9	25.0 <sup>a</sup>	5.2 <sup>b</sup>	45.9 <sup>c</sup>	10 <sup>d</sup>	0.5 <sup>a</sup>	0.9 <sup>c</sup>
CAT A <sup>3</sup>	533	13.7	2	27.2	26.7	21.5	28.2	36.4 <sup>a</sup>	4.9 <sup>b</sup>	29.5 <sup>c</sup>	1.1 <sup>d</sup>	9.7 <sup>a</sup>	7.9 <sup>c</sup>
K-Fe/ZrO <sub>2</sub> <sup>4</sup>	613	2.0	3	43.0	13.6	15.0	18	44	9.2	19	9.8	6.0	2.6
K-Fe/CNT <sup>4</sup>	613	2.0	3	35.0	11.5	12.0	26	34	10	19	11	3.9	2.2
FeK+3Ca-ZSM-5 <sup>5</sup>	648	3.0	3	45.9	24.3	17.3	19.6	43.2	10.1 <sup>e</sup>	27.1	N.A.	10.5	6.6

FeK/SWNTs									39.8			
	613	2.0	3	52.7	66.5	9.6	13.5	22.5	8.6	15.6	15.0	26.5
(This work)									(47.5 <sup>c</sup> )			

<sup>a</sup>C<sub>2</sub>–C<sub>3</sub>= products. <sup>b</sup>C<sub>2</sub>–C<sub>3</sub><sup>0</sup> products. <sup>c</sup>C<sub>4+</sub>= products. <sup>d</sup>C<sub>4+</sub><sup>0</sup> products. <sup>e</sup>C<sub>2</sub>–C<sub>10</sub><sup>0</sup> and aromatics products.

**Table S2.** Product Distribution over the FeK/SWNTs Catalyst in CO Hydrogenation<sup>a</sup>

catalyst	CO conv.	CO <sub>2</sub> sel. (%)	hydrocarbon selectivity (wt%)				
			CH <sub>4</sub>	C <sub>2</sub> –C <sub>4</sub> <sup>=</sup>	C <sub>2</sub> –C <sub>4</sub> <sup>0</sup>	C <sub>5+</sub> <sup>=</sup>	C <sub>5+</sub> <sup>0</sup>
	(%)						
FeK/SWNTs	69.5	44.7	16.2	21.6	8.9	35.9	17.4

<sup>a</sup>Reaction conditions: 200 mg of catalyst,  $T = 613$  K,  $P = 2.0$  MPa, H<sub>2</sub>/CO = 1, GHSV

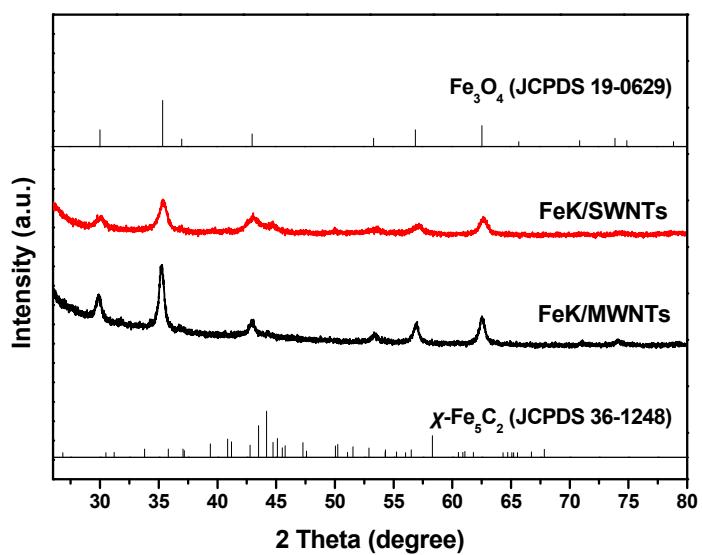
= 9000 mL g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, and TOS = 24 h.

**Table S3.** Product Distribution over the FeK/rGO Catalyst in CO<sub>2</sub> Hydrogenation<sup>a</sup>

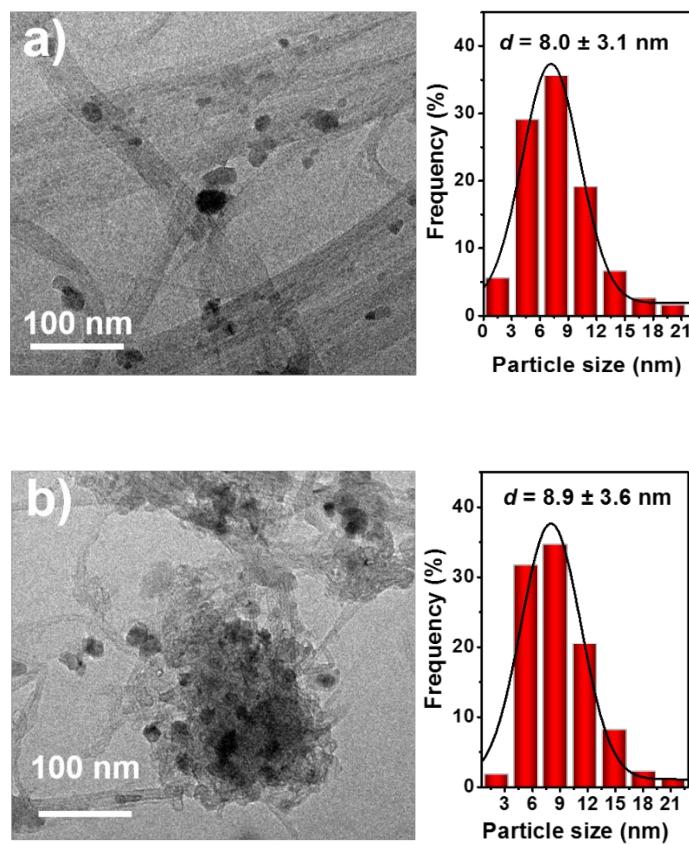
catalyst	CO <sub>2</sub> conv. (%)	CO sel. (%)	hydrocarbon selectivity (wt%)				
			CH <sub>4</sub>	C <sub>2</sub> –C <sub>4</sub> <sup>=</sup>	C <sub>2</sub> –C <sub>4</sub> <sup>0</sup>	C <sub>5+</sub> <sup>=</sup>	C <sub>5+</sub> <sup>0</sup>
FeK/rGO	39.4	34.2	24.8	50.3	12.1	8.5	4.3

<sup>a</sup>Reaction conditions: 200 mg of catalyst,  $T = 613$  K,  $P = 2.0$  MPa, H<sub>2</sub>/CO<sub>2</sub> = 3, GHSV

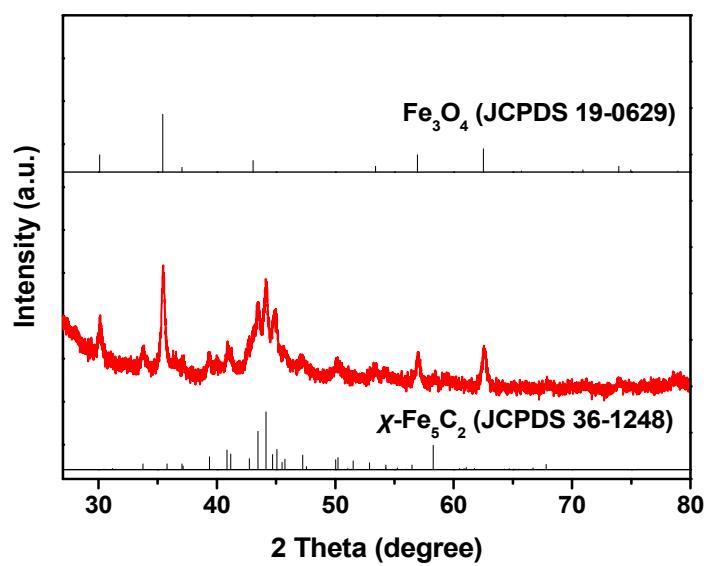
= 9000 mL g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, and TOS = 24 h.



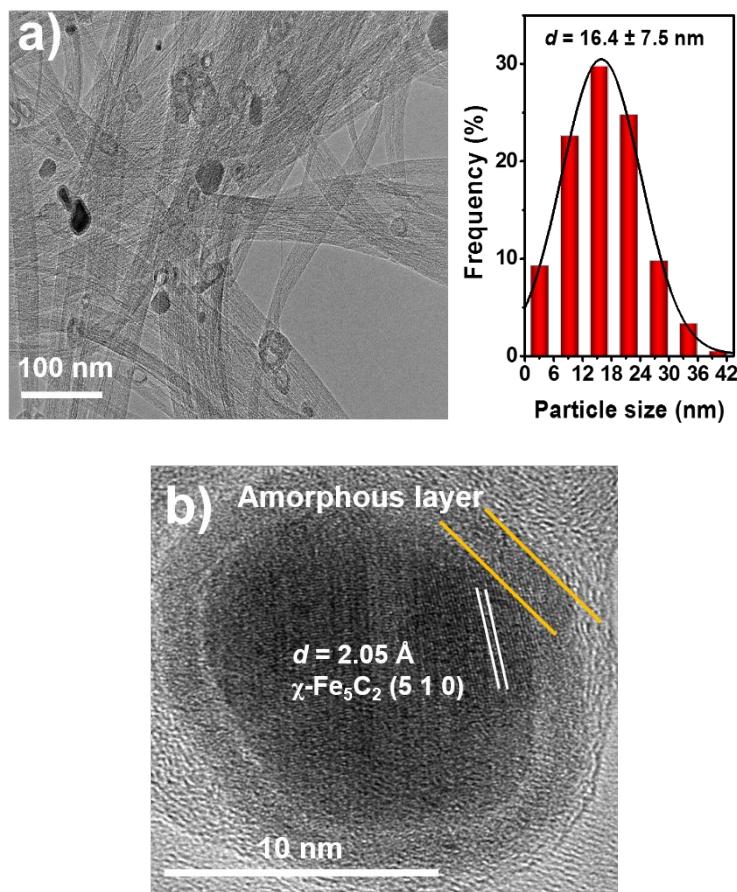
**Figure S1.** XRD patterns of the FeK/SWNTs and FeK/MWNTs catalysts after CO activation.



**Figure S2.** TEM images and PSD histograms with Gaussian analysis fittings of the (a) FeK/SWNTs and (b) FeK/MWNTs catalysts after CO activation.



**Figure S3.** XRD pattern of the FeK/SWNTs catalyst after 120 h on stream in  $\text{CO}_2$  hydrogenation.



**Figure S4.** (a) TEM image and particle size distribution histograms with Gaussian analysis fitting and (b) HRTEM image of the FeK/SWNTs catalyst after 120 h on stream in CO<sub>2</sub> hydrogenation.

## References

- [1] Guo, L. S.; Sun, J.; Ji, X. W.; Wei, J.; Wen, Z. Y.; Yao, R. W.; Xu, H.Y.; Ge, Q. J. Directly Converting Carbon Dioxide to Linear  $\alpha$ -Olefins on Bio-Promoted Catalysts. *Commun. Chem.* **2018**, *1*, 11.
- [2] Guo, L. S.; Cui, Y.; Li, H. J.; Fang, Y.; Prasert, R.; Wu, J. H.; Yang, G. H.; Yoneyama, Y.; Tsubaki, N. Selective Formation of Linear-Alpha Olefins (LAOs) by CO<sub>2</sub> Hydrogenation over Bimetallic Fe/Co-Y Catalyst. *Catal. Commun.* **2019**, *130*, 105759.
- [3] Hu, B. X.; Frueh, S.; Garces, H. F.; Zhang, L. C.; Aindow, M.; Brooks, C.; Kreidler, E.; Suib, S. L. Selective Hydrogenation of CO<sub>2</sub> and CO to Useful Light Olefins over Octahedral Molecular Sieve Manganese Oxide Supported Iron Catalysts. *Appl. Catal. B* **2013**, *132–133*, 54–61.
- [4] Wang, J. J.; You, Z. Y.; Zhang, Q. H.; Deng, W. P.; Wang, Y. Synthesis of Lower Olefins by Hydrogenation of Carbon Dioxide over Supported Iron Catalysts. *Catal. Today* **2013**, *215*, 186–193.
- [5] Dokania, A.; Chowdhury, A. D.; Ramirez, A.; Telalovic, S.; Abou-Hamad, E.; Gevers, L.; Ruiz-Martinez, J.; Gascon, J. Acidity Modification of ZSM-5 for Enhanced Production of Light Olefins from CO<sub>2</sub>. *J. Catal.* **2020**, *381*, 347–354.