

Supporting Information

Zeolitic Imidazolate Framework-67 Derived $\text{CeO}_2@\text{Co}_3\text{O}_4$ Core-shell Microspheres with Enhanced Catalytic Activity towards Toluene Oxidation

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Preparation of the CoCe-P catalyst

The CoCe-P catalyst was synthesized with a modified co-precipitation method.¹ Firstly, 667.6 mg $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ and 306.4 mg $\text{Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ were dissolved in 40 ml ethanol and water mixed solution (v/v=1:1). Then, 10 vol.% aqueous ammonia solution was added dropwise to the above solution with continuous stirring until the pH was 9.30 ± 0.02 . Subsequently, the precipitants were collected by centrifugation, washed for at least 3 times and dried at 80 °C overnight. Finally, the product was calcined at 400 °C for 2 h and marked as CoCe-P.

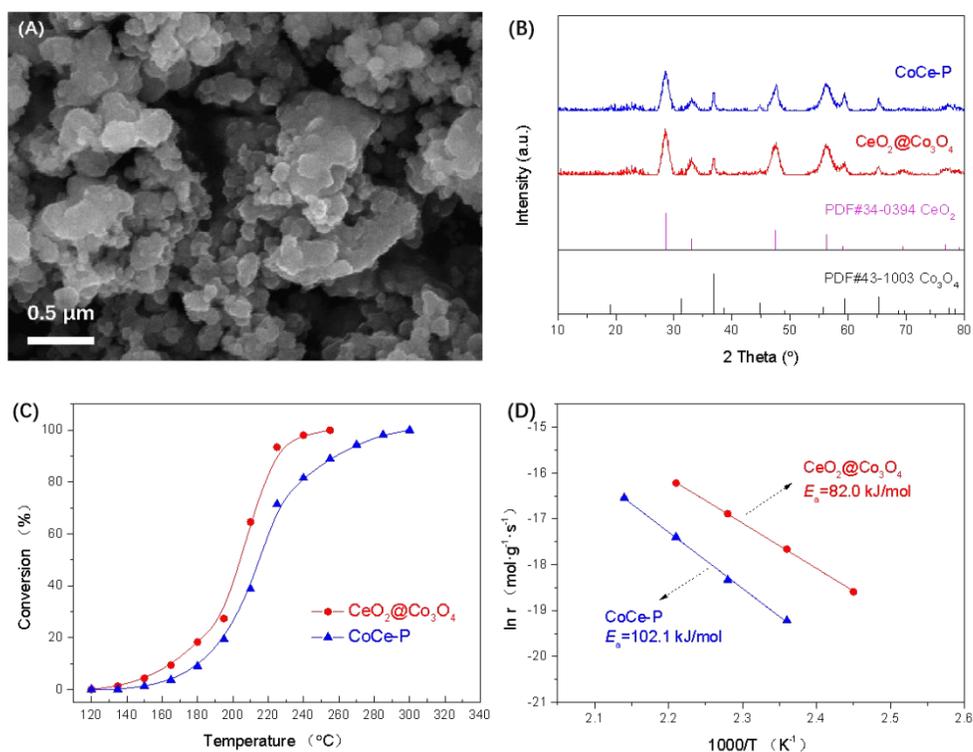


Figure S1. SEM image (A) of CoCe-P; XRD pattern (B), Toluene conversion (C) and Arrhenius plots (D) of CeO₂@Co₃O₄ and CoCe-P.

As shown in Figure S1A, the SEM image of CoCe-P exhibited clusters of irregular particles,

which was similar with the previous work.² From Figure S1B, the XRD pattern of CoCe-P could be ascribed to CeO₂ and Co₃O₄. No other phases were detected.

Furthermore, the catalytic activity towards toluene oxidation (C) and Arrhenius plots (D) of CoCe-P were also given in Figure 1, and the results were summarized in Table 1. From Figure 1C-D and Table 1, the CeO₂@Co₃O₄ sample showed better activity than CoCe-P. Additionally, the E_a of the core-shell catalyst was lower than that of the CoCe-P sample, which further verified that core-shell CeO₂@Co₃O₄ was superior to the CeCo catalyst prepared by the co-precipitation method.

Table S1: The catalytic activity results of CeO₂@Co₃O₄ and CoCe-P for toluene

Sample	T_{50} (°C)	T_{90} (°C)	E_a^a (kJ/mol)
CeO ₂ @Co ₃ O ₄	204	225	82.0
CoCe-P	215	259	102.1

^a Apparent activation energy for toluene oxidation obtained from the Arrhenius plot.

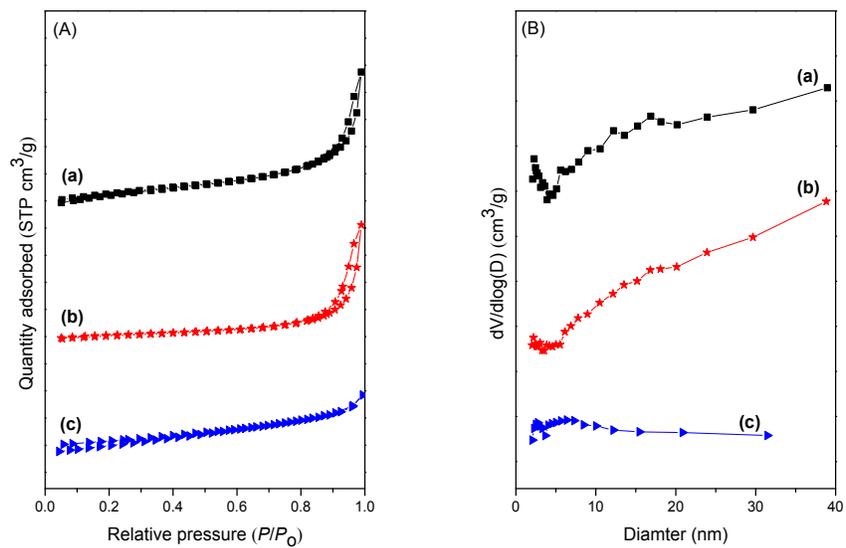


Figure S2. N₂ adsorption/desorption isotherms (A) and pore size distributions (B) of (a) Co₃O₄, (b) CeO₂@Co₃O₄ and (c) CeO₂.

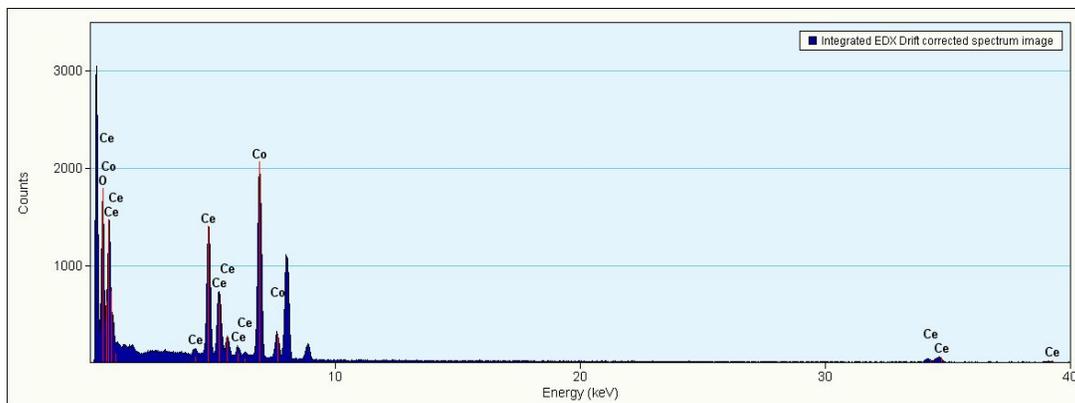


Figure S3. EDX image of the $\text{CeO}_2@\text{Co}_3\text{O}_4$ sample.

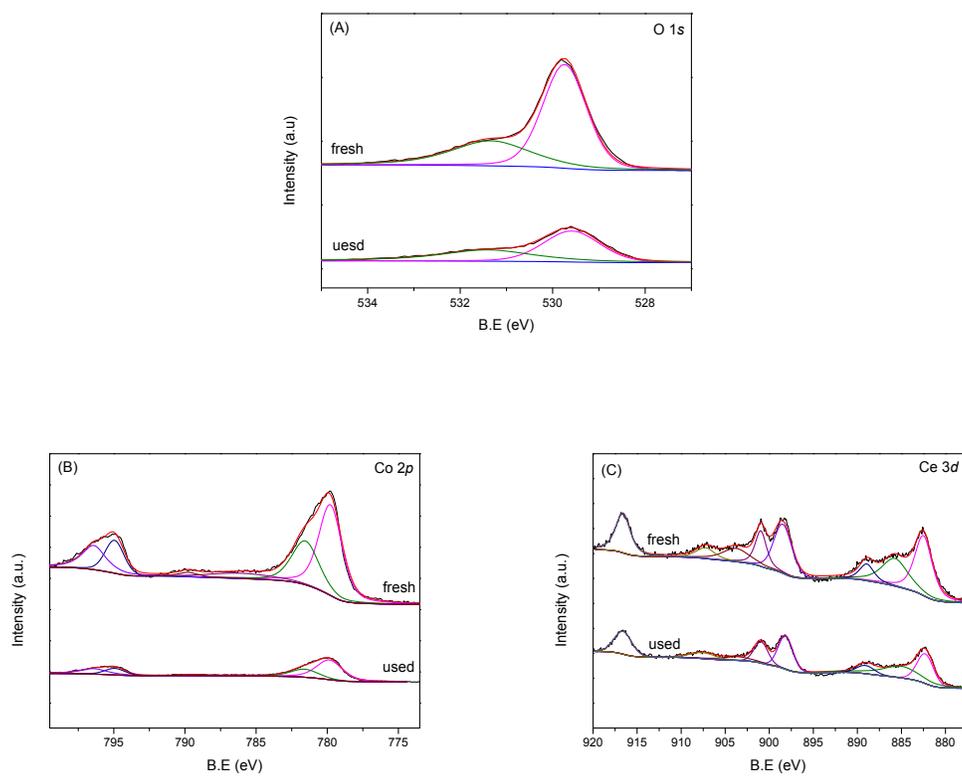


Figure S4. XPS spectra of $\text{CeO}_2@ \text{Co}_3\text{O}_4$ before and after reaction.

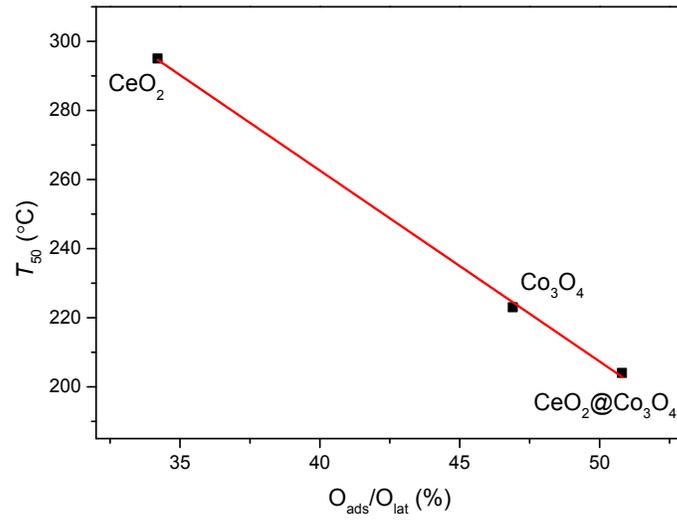


Figure S5. Correlations between the O_{ads}/O_{lat} ratios and the catalytic activity at 50% conversion of the three catalysts.

References

- (1) Chen, J.; Zhang, X.; Arandiyani, H.; Peng, Y.; Chang, H.; Li, J., Low temperature complete combustion of methane over cobalt chromium oxides catalysts. *Catal. Today* **2013**, *201*, 12-18.
- (2) Liotta, L. F.; Ousmane, M.; Di Carlo, G.; Pantaleo, G.; Deganello, G.; Marci, G.; Retailleau, L.; Giroir-Fendler, A., Total oxidation of propane at low temperature over $\text{Co}_3\text{O}_4\text{-CeO}_2$ mixed oxides: Role of surface oxygen vacancies and bulk oxygen mobility in the catalytic activity. *App. Catal., A* **2008**, *347* (1), 81-88.