Quantitative Analysis of Attachment Time of Air Bubbles to Solid

Surfaces in Water

Seongsoo Han^{1,2}, Anh V. Nguyen^{3*}, Kwanho Kim¹, Jaikoo Park², Kwangsuk You^{1*}

¹ Convergence Research Center for Development of Mineral Resources (DMR), Korea Institute of Geoscience and Mineral Resources (KIGAM), 124 Gwahak-ro, Yuseong-gu, Daejeon 34132, Republic of Korea

² Department of Earth Resources and Environmental Engineering, Hanyang University, 222, Wangsimni-ro, Seongdong-gu, Seoul 04763, Republic of Korea

³School of Chemical Engineering, The University of Queensland, Brisbane, Queensland 4072, Australia

*Corresponding Author Information

Kwangsuk You (youks@kigam.re.kr) Anh.V. Nguyen (Anh.Nguyen@eng.uq.edu.au)

Number of pages: #8

Number of figures: #5

S1

SUPPORTING INFORMATION

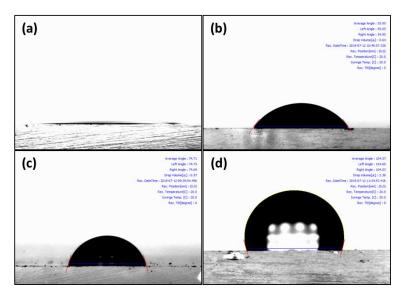


Figure S1. Images of the water droplet static contact angles (a) 0° (pristine glass slide), (b) 55° (0.01 mM OTS in toluene for 10 min), (c) 75° (0.1 mM OTS in toluene for 10 min), and (d) 105° (1 mM OTS in toluene for 10 min)

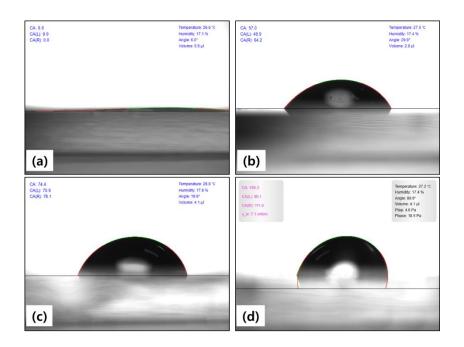


Figure S2. Images of the hysteresis of the water contact angles (a) 0° (pristine glass slide) (b) $55 \pm 10^{\circ}$ (0.01 mM OTS in toluene for 10 min), (c) $75 \pm 5^{\circ}$ (0.1 mM OTS in toluene for 10 min), and (d) $105 \pm 5^{\circ}$ (1 mM OTS in toluene for 10 min)

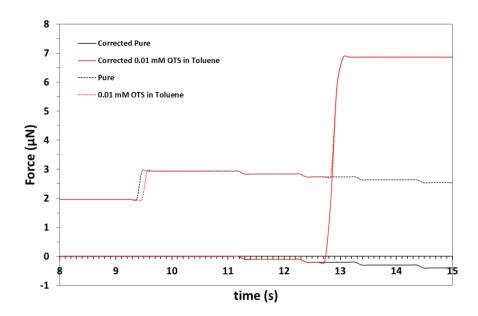


Figure S3. Corrected force curves incorporating the capillary effect of the needle produced by the water in the cell (solid line: after correction, dotted line: before correction)

Conversion to dimensionless forms

Capillary number: $Ca = \mu V / \sigma$

$$x = \frac{r}{R}Ca^{-1/4}; \quad y = \frac{h}{R}Ca^{-1/2}; \quad Y = \frac{H}{R}Ca^{-1/2}; \quad p = \frac{R}{\sigma}P; \quad \tau = \frac{\sigma\sqrt{Ca}}{R\mu}t; \quad \tau_0 = \frac{\sigma\sqrt{Ca}}{R\mu}t_0;$$

$$\wp = \frac{R}{\sigma}\Pi$$
 ; $\Phi = \frac{F}{2\pi R\sigma Ca^{1/2}}$;

$$\frac{\partial y}{\partial \tau} = \frac{1}{4x} \frac{\partial}{\partial x} \left\{ xy^3 \frac{\partial p}{\partial x} \right\} + \frac{d^*}{x} \frac{\partial}{\partial x} \left\{ xy^2 \frac{\partial p}{\partial x} \right\} = \frac{1}{4} \left\{ \frac{y^3}{x} \frac{\partial p}{\partial x} + 3y^2 \frac{\partial y}{\partial x} \frac{\partial p}{\partial x} + y^3 \frac{\partial^2 p}{\partial x^2} \right\} + \dots$$

$$p(y,x) = 2 - \frac{1}{x} \frac{\partial}{\partial x} \left\{ x \frac{\partial y}{\partial x} \right\} - \wp(y) = 2 - \left\{ \frac{\partial^2 y}{\partial x^2} + \frac{1}{x} \frac{\partial y}{\partial x} \right\} - \wp(y)$$

$$y(x,\tau=0) = Y + x^2 / 2$$

$$p(x, y, \tau = 0) = 0$$

$$\frac{\partial y_N}{\partial \tau} = -1 - \frac{\partial \Phi}{\partial \tau} \left\{ \log \frac{x_{\infty} C a^{1/4}}{2} + B(\theta_o) \right\}$$

$$p(y, x \to \infty) = 0$$

$$\Phi = \int_0^{r_\infty} \left\{ p(x,\tau) + \wp(x,\tau) \right\} x dx$$

At x = 0, we obtain the following limits:

$$\left(\frac{\partial Y}{\partial x}\right)_{x=0} = 0; \quad \left(\frac{\partial p}{\partial x}\right)_{x=0} = 0$$

$$p(Y,0) = 2 - 2\left(\frac{\partial^2 Y}{\partial x^2}\right)_{x=0} - \wp(Y)$$

$$\frac{\partial Y}{\partial \tau} = \left\{ \frac{3}{2} Y^3 + d^* Y^2 \right\} \left\{ \frac{\partial^2 p}{\partial x^2} \right\}_{x=0}$$

Numerical Solution by the three-point Finite Difference Method

We divide the film radius into N-1 sections (stages) and consider N points on the 1D mesh. Applying the three-point FDM, we obtain the following ordinary differential equations (ODEs):

Section 1 (around the film symmetry): $Y = y_1$; $\Delta = \text{film radius } / (N-1)$

$$\frac{\partial y_1}{\partial \tau} = \left\{ \frac{3}{2} y_1^3 + d^* y_1^2 \right\} \frac{-2p_1 + 2p_2}{\Delta^2} ; \quad p_1 = 2 - \frac{-4y_1 + 4y_2}{\Delta^2} - \wp(y_1)$$

Section k = 2 to N-1 (intermediate sections):

$$\frac{\partial y_k}{\partial \tau} = \frac{m}{12} \left\{ \frac{y_k^3}{x_k} \frac{p_{k+1} - p_{k-1}}{2\Delta} + 3y_k^2 \frac{y_{k+1} - y_{k-1}}{2\Delta} \frac{p_{k+1} - p_{k-1}}{2\Delta} + y_k^3 \frac{p_{k+1} - 2p_k + p_{k-1}}{\Delta^2} \right\} + \dots$$

$$p_k = 2 - \left\{ \frac{y_{k+1} - 2y_k + y_{k-1}}{\Delta^2} + \frac{y_{k+1} - y_{k-1}}{2x_k \Delta} \right\} - \wp(y_k)$$

Section N (at the film boundary):

$$\frac{\partial y_N}{\partial \tau} = -1 - \frac{\partial \Phi}{\partial \tau} \left\{ \log \frac{x_{\infty} C a^{1/4}}{2} + B(\theta_c) \right\}; \quad p_N = 0$$

This system of ODEs can be solved using the Matlab ODE solver "ODE15S."

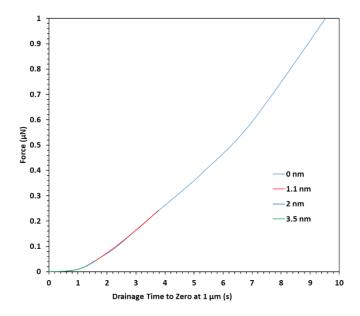


Figure S4. Force with respect to the drainage time calculated by Eq. 15 (before attachment) The y-axis in Figure S3 is the force calculated by Eq. (15) in the manuscript:

$$F(t) = 2\pi \int_0^{r_{\infty}} \left\{ P(x,t) + \Pi(x,t) \right\} x dx \tag{15}$$

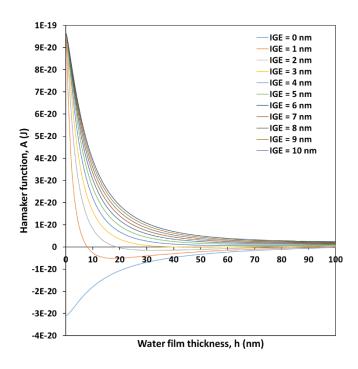


Figure S5. Hamaker function of silica showing increment with the IGE thickness.