Supporting Information

Hollow and yolk-shell Co-N-C@SiO₂ nanoreactors: Controllable synthesis with high selectivity and activity for nitroarene hydrogenation

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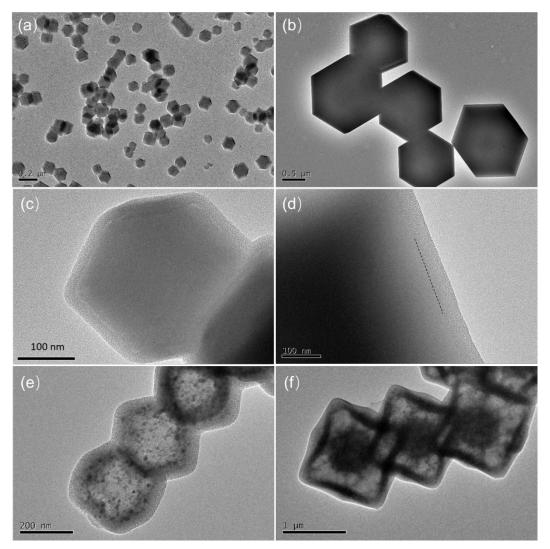


Figure S1. TEM images of (a) S-ZIF-67, (b) L-ZIF-67, (c) S-ZIF-67@SiO₂, (d) L-ZIF-67@SiO₂, (e) H-Co-N-C@SiO₂-20, and (f) Y-Co-N-C@SiO₂-40.

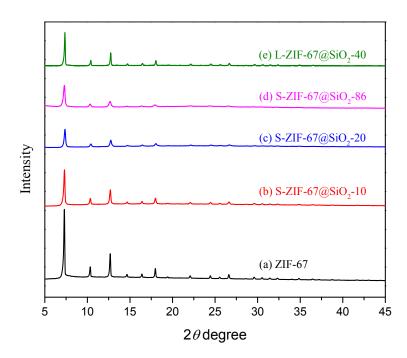


Figure S2. XRD patterns of ZIF-67 and ZIF-67@SiO₂.

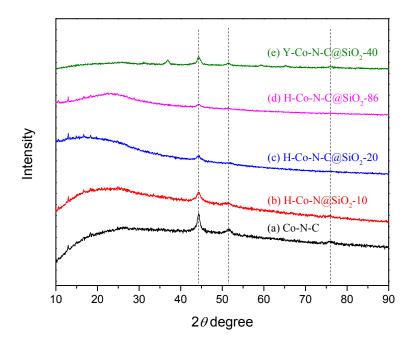


Figure S3. XRD patterns of Co-N-C, H-Co-N-C@SiO₂-*x*, and Y-Co-N-C@SiO₂-*x*.

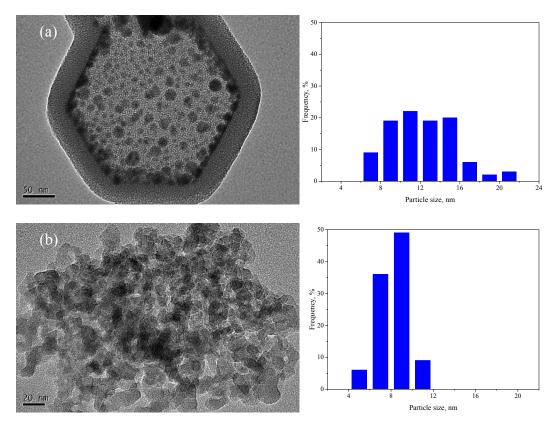


Figure S4. TEM and Co particle size distribution of (a) $Co@SiO_2$ and (b) Co/SiO_2 .

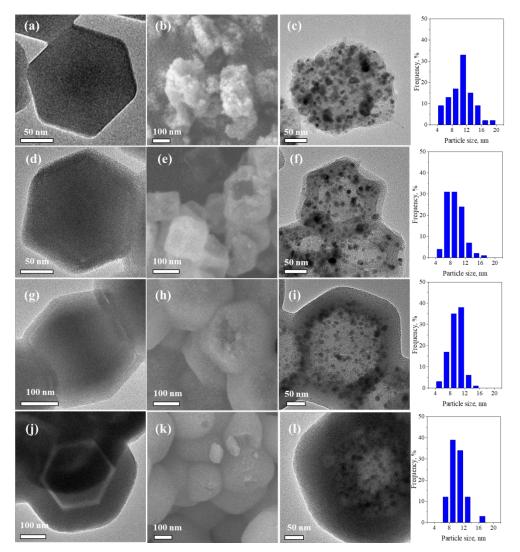


Figure S5. Characterization of HSN with different SiO₂ shell thickness. TEM images of (a) ZIF-67, (c) Co-N-C, (d) ZIF-67@SiO₂-10, (f) H-Co-N-C@SiO₂-10, (g) ZIF-67@SiO₂-20, (i) H-Co-N-C@SiO₂-20, (j) ZIF-67@SiO₂-86, and (l) H-Co-N-C@SiO₂-86. SEM images of (b) Co-N-C, (e) H-Co-N-C@SiO₂-10, (h) H-Co-N-C@SiO₂-20, and (k) H-Co-N-C@SiO₂-86.

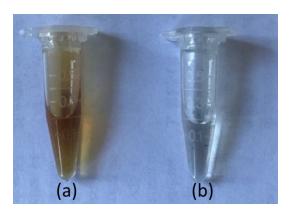


Figure S6. Typical reaction samples after reaction. (a) Co@SiO₂, (b) H-Co-N-C@SiO₂-20.

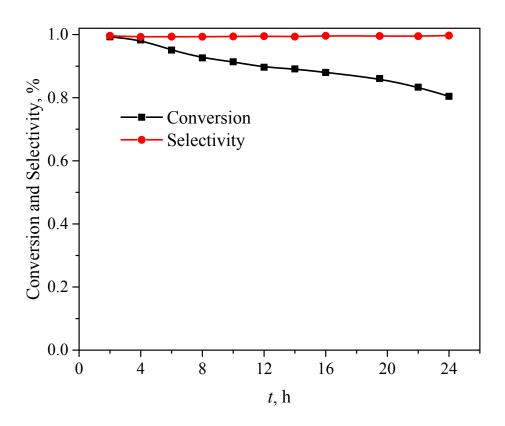


Figure S7. Long-term stability of H-Co-N-C@SiO₂-20. Reaction conditions: 35 mg catalyst, 0.5 mL reactant dissolved in 30 mL solvent (24 mL ethanol + 6 mL H₂O), 110 °C, 2.7 MPa hydrogen pressure with a gas flow of 50 mL/min, and 0.1 mL/min feeding rate.

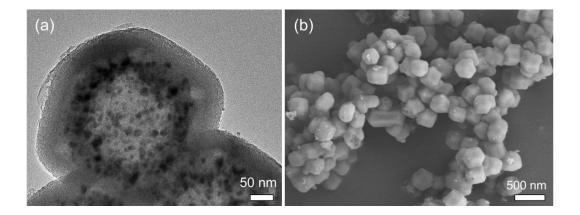


Figure S8. (a) TEM and (b) SEM images of the spent H-Co-N-C@SiO₂-20 catalyst.

| | | H-Co-N-C@SiO ₂ -20 | Co@SiO ₂ | |
|----------------------|---------------------------|-------------------------------|---------------------|--|
| N/Co. molor ratio | XPS | 1.75 | 0.34 | |
| N/Co, molar ratio | EDS | 1.54 | 0.27 | |
| | Co, % | 9.7 | 2.5 | |
| Co 2p _{3/2} | Co-O _x , % | 22.9 | 63.3 | |
| - | Co-N _x , % | 67.4 | 34.2 | |
| | Pyridinic-N, % | 9.4 | 11.8 | |
| | Cobalt-N _x , % | 32.9 | 8.3 | |
| N 1s | Pyrrolic-N, % | 15.9 | 22.1 | |
| | Graphitic-N, % | 35.7 | 35.7 | |
| - | Oxidized-N, % | 6.0 | 22.0 | |

Table S1. N/Co molar ratio and proportion of deconvoluted peaks

Table S2. TOFs of Co⁰ and Co-N_x active sites

| | <i>r,</i> h⁻ | <i>d</i> _{TEM} ^a , nm | D ^b , % | TOF ^{<i>c</i>} , h⁻¹ | $P_{\text{Co-Nx}}d, \%$ | TOF _{Co} , h ⁻¹ | TOF _{Co-Nx} , h ⁻ |
|-----------------------------|--------------|---|--------------------|-------------------------------|-------------------------|-------------------------------------|---------------------------------------|
| | 1 | | | | | | 1 |
| Co/SiO ₂ | 11.8 | 8.2 | 12.2 | 46 | 0.0 | 46 | |
| H-Co-N-C@SiO ₂ - | 32.8 | 9.3 | 10.8 | 146 | 67.5 | 46 | 194 |
| 20 | | | | | | | |

^{*a*} Particle size was calculated based on TEM results, ^{*b*} Metal dispersion was calculated by $D = 1.00 / d_{TEM}^{[1]}$, ^{*c*}TOF was the turnover frequency based on surface Co atoms, ^{*d*} P_{Co-Nx} was the proportion of Co-N_x identified from XPS results.

The TOF of the H-Co-N-C@SiO₂-20 catalyst was defined as the total activity of Co⁰ and Co-N_x active sites. In order to quantitatively compare the activity of different active sites, we assumed that the TOF_{Co} of Co⁰ was equal for Co/SiO₂ and H-Co-N-C@SiO₂-20. Thus, the TOF of Co-N_x species (TOF_{Co-Nx}) was calculated as:

$$\mathsf{TOF}_{\mathsf{Co-Nx}} = (\mathsf{TOF} - \mathsf{TOF}_{\mathsf{Co}} \times (1 - P_{\mathsf{Co-Nx}})) / P_{\mathsf{Co-Nx}}$$
(S-1)

| Entry | Catalysts | Co, mg | <i>t</i> , h | <i>X</i> , % | <i>S</i> , % | <i>r</i> , h ⁻¹ |
|-------|-------------------------------|--------|--------------|--------------|--------------|----------------------------|
| 1 | Co-N-C | 4.8 | 2.5 | 82.4 | >99 | 28.2 |
| 2 | H-Co-N-C@SiO ₂ -10 | 5.5 | 2.5 | 100.0 | >99 | 35.3 |
| 3 | H-Co-N-C@SiO ₂ -20 | 5.3 | 2.5 | 98.6 | 98.6 | 32.8 |
| 4 | H-Co-N-C@SiO ₂ -86 | 4.6 | 2.5 | 68.2 | 92.0 | 23.2 |

Table S3. Effect of SiO₂ shell on hydrogenation of nitrobenzene ^{*a*}

^a Reaction conditions: reactant 3 mmol, internal standard (isopropyl benzene) 0.15 mL, solvent (ethanol) 30 mL.

Table S4. Substrate scope of H-Co-N-C@SiO₂-20 in hydrogenation of nitroarenes.^a

| Entry | Nitroarenes | <i>t</i> , h | <i>X</i> , % | <i>S</i> , % |
|-------|-----------------------|--------------|--------------|--------------|
| 1 | NO ₂ | 2 | 99.5 | >99 |
| 2 | | 3 | 100 | >99 |
| 3 | | 2 | 80.5 | >99 |
| 4 | BrNO2 | 3 | 99.4 | >99 |
| 5 | Br NO2 | 2 | 95.2 | >99 |
| 6 | Br NO ₂ | 2 | 62.8 | >99 |

^a Reaction conditions: reactant 3 mmol, internal standard (isopropyl benzene) 0.15 mL, solvent: 24 mL ethanol + 6 mL H₂O.

Experimental details

1. Catalyst characterization

The morphology and element distribution line scan of the samples were obtained by a scanning electron microscope (SEM, JSM7401) and transmission electron microscope (TEM, JEM2010) equipped with an energy dispersive spectrometer (EDS, OXFORD). HRTEM and elemental mapping images were obtained by high angle annular dark field scanning transmission electron microscopy (HAADF-STEM, FEI Titan Cubed G2 300) at 300 kV. All of the samples were ultrasonically dispersed in ethanol for 30 min and then dropped onto a carbon film supported on copper grid. The particle size distribution was analyzed by collecting 100 particles. The elemental chemical states of Co@SiO2 and H-Co-N-C@SiO2-x were determined by XPS (Thermal Scientific ESCALAB 250Xi) with a CAE pass energy 100.0 eV analyser mode and an Al Ka X-ray source. The deconvolution of N 1s and Co 2p were based on previous works^[2-5]. The X-ray diffraction (XRD) powder patterns of ZIF-67@SiO₂, Co-N-C, H-Co-N-C@SiO₂x and Y-Co-N-C@SiO₂-x were obtained by a Bruker Advance D8 X-ray diffractometer with Cu K α (λ = 1.5406 Å) monochromatic radiation. The samples were prepared by tableting the powder on a single crystal Si substrate. The metal loading of Co on the catalysts was confirmed by inductively coupled plasma (ICP) analysis, where the metal was dissolved by boiling the catalyst powder in aqua regia. The porosity of the samples was determined by N_2 adsorption at -196 °C on an Autosorb-IQ₂-MP-C system (Quantachrome, USA). The samples were evacuated at 300 °C for 10 h before analysis.

References

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