

# **Supporting Information (SI)**

## **Migration and emission characteristics of ammonia/ammonium through flue gas cleaning devices in coal-fired power plants of China**

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### **Supplementary Information Contents:**

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**Table S1. Parameters and Components of Flue Gas at Each Sampling Points and Key Operation Parameters of APCDs**

Sampling points	#a*	PP1			PP2			PP3			PP4		
		#b*	#c*	#a	#b	#c	#a	#b	#c	#a	#b	#c	
SO <sub>2</sub>	mg/Nm <sup>3</sup>	-	5269	13	-	1468	14	-	1785	19	-	1554	6
NO <sub>x</sub>	mg/Nm <sup>3</sup>	43	-	-	39	-	-	33	-	-	34	-	-
O <sub>2</sub>	%		5.9	5.8	4.5	6	7.5	3.7	8.4	8.4	4.9	7	7
T		368	108	49	155	134	48	327	137	48	342	152	49
W	%	-	6.5	7	-	4.5	7.5	-	5.5	11	-	4.5	10
<b>Denitrification process</b>													
Denitrification efficiency	%	93.9			-			93.3			94.3		
Number of Catalyst layers		4			-			3			3		
Ammonia consumption	kg/h	263			20			38			68		
Ammonia slip(online measurement)	mg/Nm <sup>3</sup>	0.49			ND*			ND			ND		
<b>Desulfurization process</b>													
Number of desulfurization tower		2			1			1			1		
Number of spraying layers		4+3			5			3			3		
Desulfurization sorbent		Limestone			Limestone			Aqueous ammonia			Liquefied ammonia		
Desulfurization absorbent consumption	kg/h	20510			416			991			234		
Desulfurization efficiency	%	99.8			99			98.9			99.6		

2 \*#a: denitrification outlet, #b: desulfurization inlet, #c: final outlet, ND: not detected.

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4      **Table S2. Comparison of NH<sub>3</sub>/NH<sub>4</sub><sup>+</sup> average concentration in flue gas from our**  
 5      **study with other published results**

	After denitrification devices		After dedusting devices		Final outlet	
	NH <sub>3</sub>	NH <sub>4</sub> <sup>+</sup>	NH <sub>3</sub>	NH <sub>4</sub> <sup>+</sup>	NH <sub>3</sub>	NH <sub>4</sub> <sup>+</sup>
PP1	0.54±0.01	21.35±1.57	0.17± 0.007	0.34±0.14	0.14±0.01	0.21±0.11
PP2	0.15±0.008	15.08±0.48	0.18±0.002	0.18±0.32	0.16±0.03	0.22±0.05
PP3	0.44±0.11	4.98±0.11	0.49±0.03	0.42±0.20	0.44±0.20	1.07±0.09
PP4	0.41±0.05	6.85±1.00	0.28±0.06	0.05±0.007	4.07±0.30	6.27±1.87
Li et al. <sup>1</sup>					0.26	0.15 (PM <sub>2.5</sub> )
Cheng et al. <sup>2</sup>	0.53	1.19 (PM <sub>2.5</sub> ) <sup>*</sup>	0.35	0.32 (PM <sub>2.5</sub> )	0.04	0.41 (PM <sub>2.5</sub> )
Ruan et al. <sup>3</sup>		0.32 (PM <sub>10</sub> ) <sup>*</sup>		0.05 (PM <sub>10</sub> )		0.005(PM <sub>10</sub> )
		0.19 (PM <sub>2.5</sub> ) <sup>*</sup>		0.03 (PM <sub>2.5</sub> )		0.005(PM <sub>2.5</sub> )
		0.17 (PM <sub>1</sub> ) <sup>*</sup>		0.03 (PM <sub>1</sub> )		0.004 (PM <sub>1</sub> )

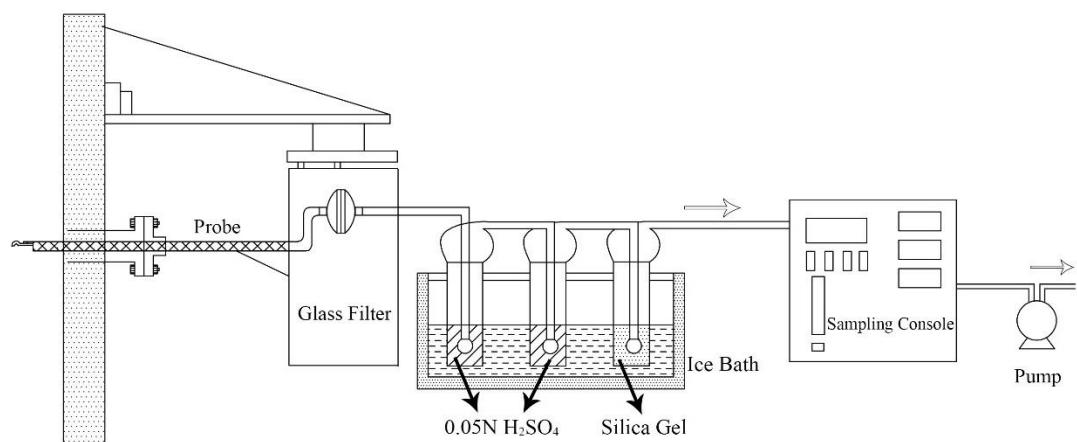
6      \*The PM<sub>10</sub>, PM<sub>2.5</sub> and PM<sub>1</sub> in brackets means the NH<sub>4</sub><sup>+</sup> concentration in the three diameters.

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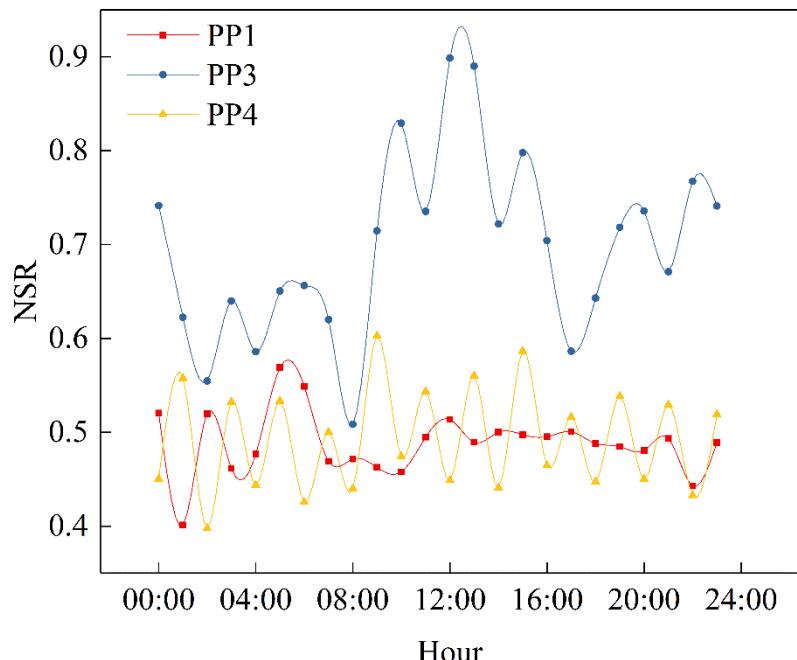
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**Figure S1 Schematic of the Ammonia/Ammonium Sampling system**

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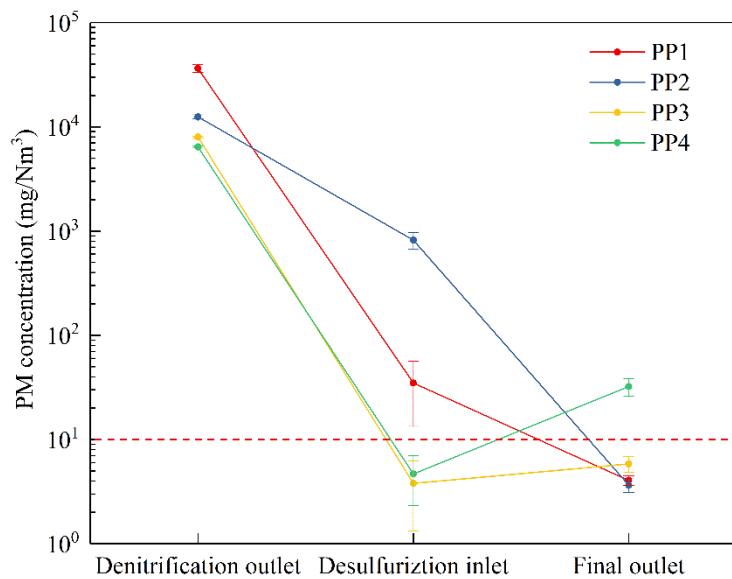
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**Figure S2. The hourly variations of NH<sub>3</sub>/NO<sub>x</sub> normalized stoichiometric ratio (NSR) in three tested plants**

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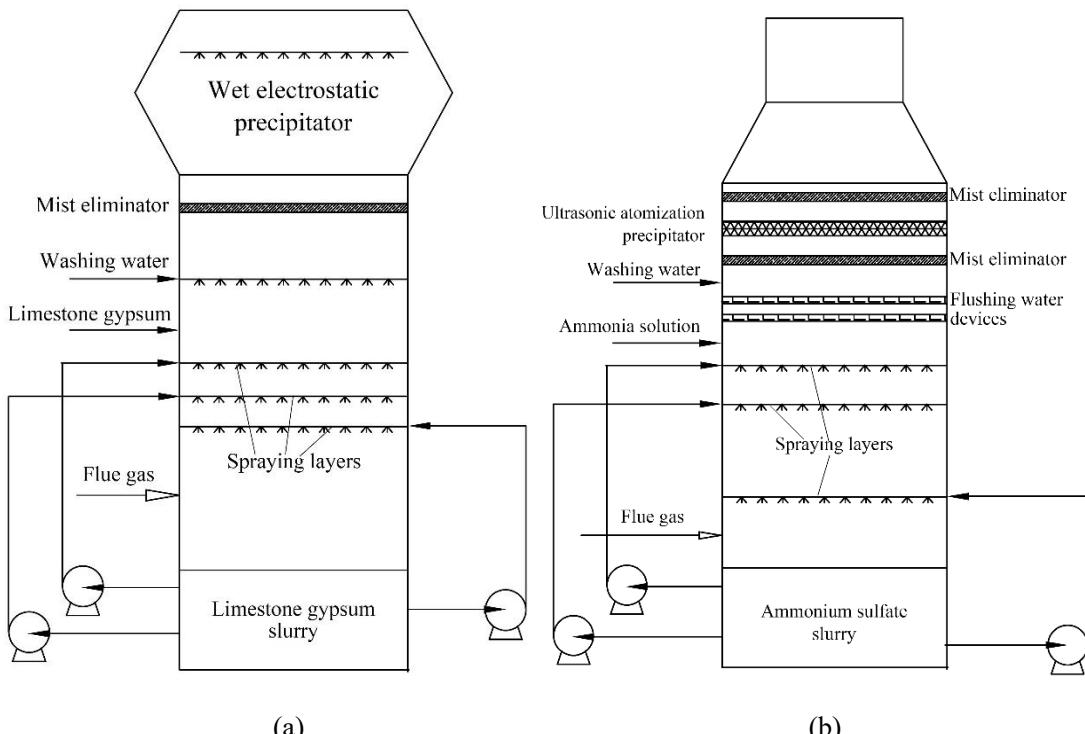
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19 **Figure S3. Average PM concentration with standard deviation at sampling points  
of four tested plants**

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(a)

(b)

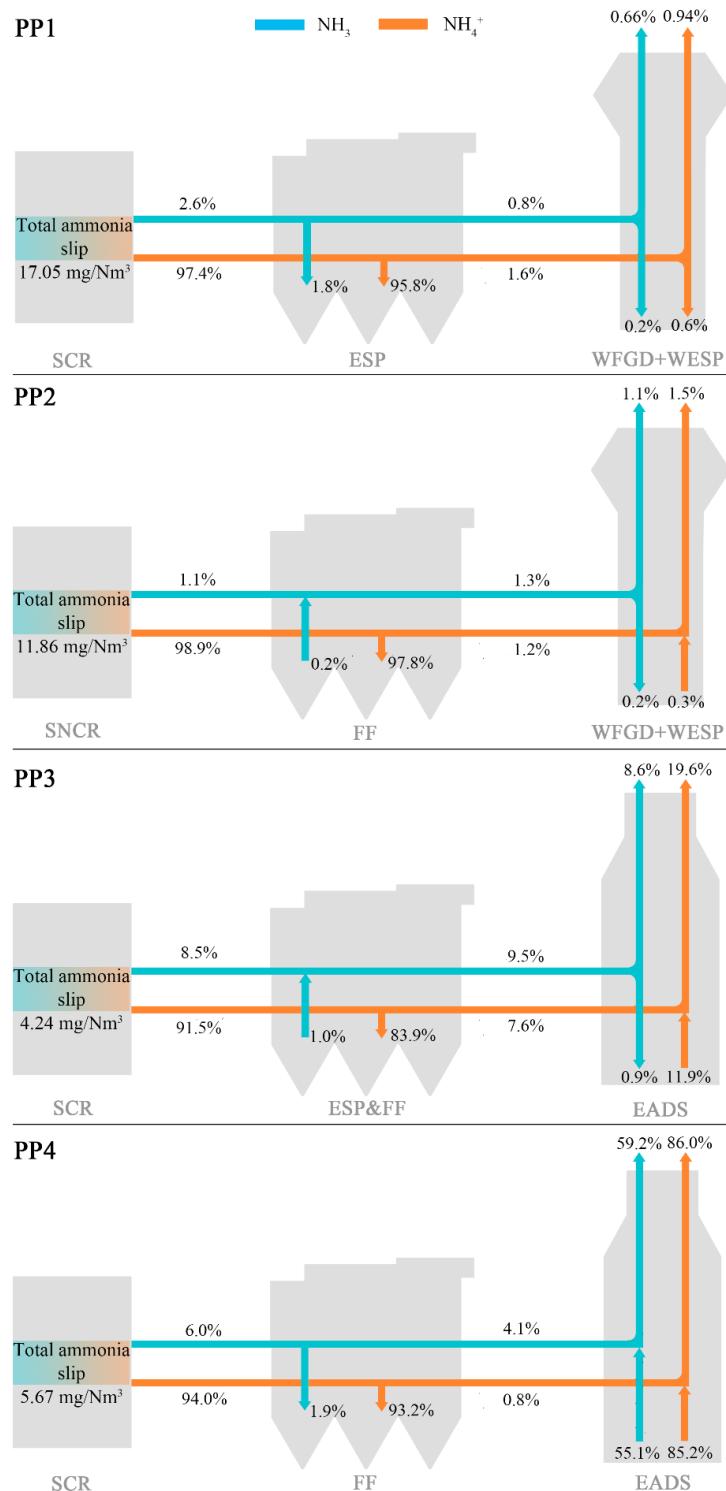
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**Figure S4. The Schematic of Desulfurization tower (a) Limestone-based WFGD,**

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**(b) Ammonia-based WFGD**

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29 **Figure S5. Quantitative migration and transformation laws of NH<sub>3</sub> in flue gas  
30 and particle-bound NH<sub>4</sub><sup>+</sup> for the four tested plants**

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34      **Equation S1**

35      Because there are no proper sampling conditions before the SCR, hourly NO<sub>x</sub>  
36      concentration of SCR inlet and the amount of injecting ammonia were derived from the  
37      denitrification flue gas continuous emission monitoring system, and used to calculate  
38      the NSR based on the following equation<sup>4</sup>:

39      
$$\text{NSR} = W / \left( \frac{V_q \times C_{NO} \times 17}{30 \times 10^6} + \frac{V_q \times C_{NO_2} \times 34}{46 \times 10^6} \right) \quad (\text{eq S1})$$

40      Where  $W$  is the ammonia consumption per hour in the denitrification system,  $V_q$  is  
41      the flux of the flue gas at the inlet of SCR reactor,  $C_{NO}$  and  $C_{NO_2}$  are the NO and NO<sub>2</sub>  
42      concentration at the inlet of SCR reactor, “17” and “34” are determined based on the  
43      reaction molar ratio of NO/NH<sub>3</sub> and NO<sub>2</sub>/NH<sub>3</sub>, respectively.

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47      **References**

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