## Supporting Information

## Mechanism of the H<sub>2</sub> Effect on NH<sub>3</sub>-Selective Catalytic Reduction over Ag/Al<sub>2</sub>O<sub>3</sub>: Kinetic and Diffuse Reflectance Infrared Fourier Transform Spectroscopy Studies

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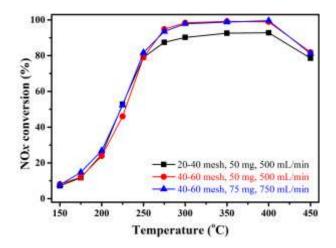


Figure S1. NOx conversion over Ag/Al<sub>2</sub>O<sub>3</sub> during H<sub>2</sub>-NH<sub>3</sub>-SCR at different gas flow rates and with different particle size. Feed composition: 500 ppm NO, 520 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, 1500 ppm H<sub>2</sub>, and N<sub>2</sub> balance. GHSV: 450 000  $h^{-1}$ .

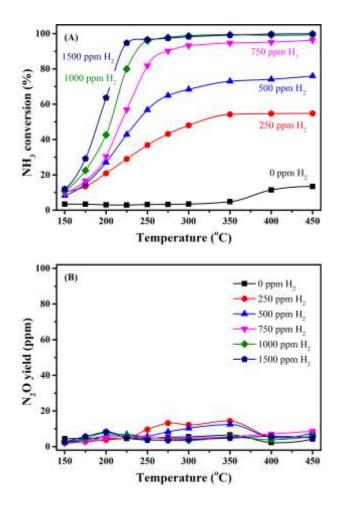
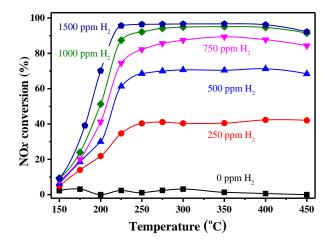
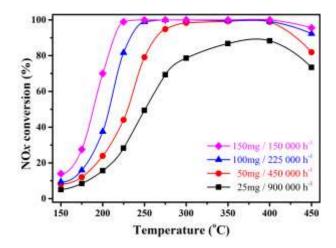


Figure S2. NH<sub>3</sub> conversion (A) and N<sub>2</sub>O yield (B) over Ag/Al<sub>2</sub>O<sub>3</sub> during H<sub>2</sub> assisted NH<sub>3</sub>-SCR with various amount of H<sub>2</sub>. Feed composition: 500 ppm NO, 520 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, 0-1500 ppm H<sub>2</sub>, and N<sub>2</sub> balance. GHSV: 150,000  $h^{-1}$ .



**Figure S3.** NOx conversion over  $Ag/Al_2O_3$  during  $H_2$ -NH<sub>3</sub>-SCR in the presence of  $H_2O$ . Feed composition: 500 ppm NO, 520 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, 0-1500 ppm H<sub>2</sub>, 2% H<sub>2</sub>O, and N<sub>2</sub> balance. GHSV: 150,000 h<sup>-1</sup>.



**Figure S4.** NO*x* conversion over Ag/Al<sub>2</sub>O<sub>3</sub> during H<sub>2</sub>-NH<sub>3</sub>-SCR under different GHSV. Feed composition: 500 ppm NO, 520 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, 1500 ppm H<sub>2</sub>, and N<sub>2</sub> balance.

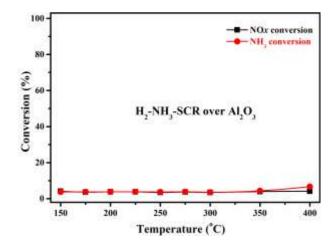
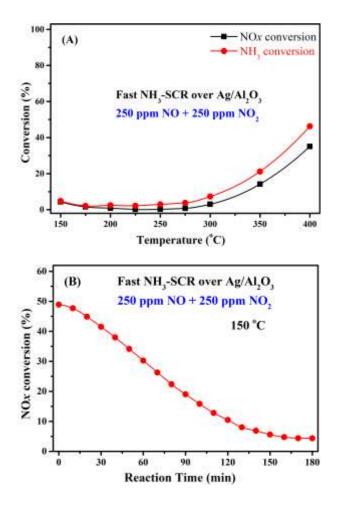


Figure S5. NOx and NH<sub>3</sub> conversions over  $Al_2O_3$  during H<sub>2</sub>-NH<sub>3</sub>-SCR. Feed composition: 500 ppm NO, 520 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, 1500 ppm H<sub>2</sub>, and N<sub>2</sub> balance. GHSV: 150,000 h<sup>-1</sup>.



**Figure S6.** NOx and NH<sub>3</sub> conversions over Ag/Al<sub>2</sub>O<sub>3</sub> during fast NH<sub>3</sub>-SCR (A) and NOx conversion at 150 °C (B). Feed composition: 250 ppm NO, 250 ppm NO<sub>2</sub>, 520 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, and N<sub>2</sub> balance. GHSV: 150,000 h<sup>-1</sup>.

As shown in the Figure S6B, the Ag/Al<sub>2</sub>O<sub>3</sub> catalyst was gradually deactivated at 150 °C during the fast NH<sub>3</sub>-SCR. Therefore, the NOx conversion was measured at 150 °C for 180 min until the reaction reached a steady state. Afterward, the experiment was further performed at each temperature point for 40 min because the reaction reached a steady state more quickly at a higher temperature. Besides, other activity tests were performed at each temperature point for 40 min because those reactions reached a steady state more quickly.

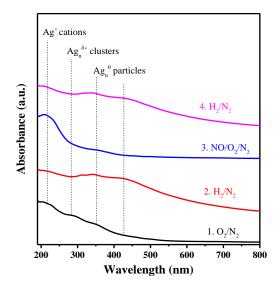
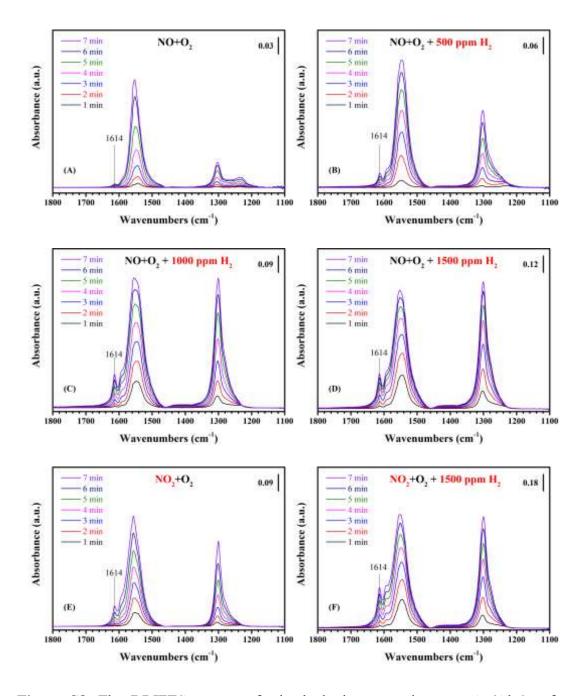
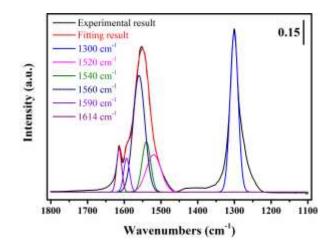


Figure S7. UV-vis spectra of Ag/Al<sub>2</sub>O<sub>3</sub> catalyst pretreated in  $O_2/N_2$  (a),  $H_2/N_2$  (b),  $NO/O_2/N_2$  (c), and  $H_2/N_2$  (d) at 200 °C for 1 hour, respectively. Feed composition: 500 ppm NO, 1500 ppm H<sub>2</sub>, 5% O<sub>2</sub>, and N<sub>2</sub> balance.

Figure S7 shows the UV-vis spectra of Ag/Al<sub>2</sub>O<sub>3</sub> catalyst pretreated in different atmosphere. Four adsorption peaks (220, 290, 350, and 425 nm) were observed on the Ag/Al<sub>2</sub>O<sub>3</sub>, and they were attributed to dispersed Ag cations (Ag<sup>+</sup>, 220 nm), oxidized Ag clusters (Ag<sub>n</sub><sup> $\delta$ +</sup>, 290 nm), and metallic Ag particles (Ag<sub>n</sub><sup>0</sup>, 350 and 425 nm). On the fresh sample, dispersed Ag cations were predominant, and Ag<sub>n</sub><sup> $\delta$ +</sup> and Ag<sub>n</sub><sup>0</sup> were also observed. After exposure to H<sub>2</sub>, the oxidized silver species were reduced and thus increased the amount of metallic silver species. Afterward, the metallic silver species were converted to oxidized species in a flow of NO+O<sub>2</sub>, possibly due to the formation of AgNO<sub>3</sub>. Moreover, the oxidized silver species were further converted to metallic silver species in a flow of H<sub>2</sub>/N<sub>2</sub>. Therefore, metallic silver species catalytically oxidized NO to produce nitrates, and H<sub>2</sub> reduced the oxidized silver species, thus completing the redox cycle for the oxidized and reduced states of Ag species.



**Figure S8.** The DRIFTS spectra of adsorbed nitrate species over  $Ag/Al_2O_3$  after exposure to a flow of  $H_2$ +NO+O<sub>2</sub> or  $H_2$ +NO<sub>2</sub>+O<sub>2</sub> with different amount of  $H_2$ . Feed composition: 500 ppm NO (or NO<sub>2</sub>), 5% O<sub>2</sub>, 0-1500 ppm H<sub>2</sub>, N<sub>2</sub> balance, 200 °C.



**Figure S9.** The deconvolution and curve fitting results for DRIFTS spectra in Figure 6 and S8.

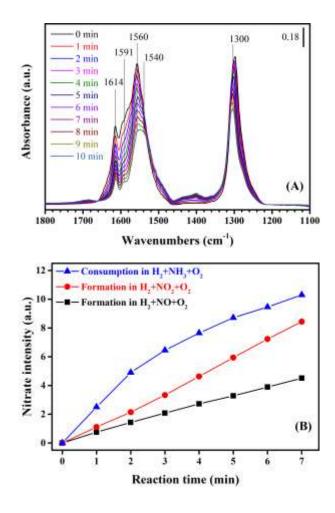
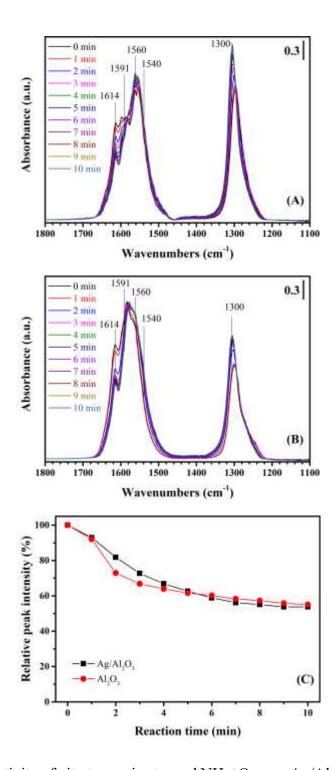


Figure S10. Reactivity of nitrate species toward  $H_2+NH_3+O_2$  over Ag/Al<sub>2</sub>O<sub>3</sub> at 200 °C (A). Comparison of the formation rate of bridge nitrate (1614 cm<sup>-1</sup>) in a flow of  $H_2+NO+O_2$  or  $H_2+NO_2+O_2$  and the consumption rate of bridge nitrate in a flow of  $H_2+NH_3+O_2$  over Ag/Al<sub>2</sub>O<sub>3</sub> (B).



**Figure S11.** Reactivity of nitrate species toward NH<sub>3</sub>+O<sub>2</sub> over Ag/Al<sub>2</sub>O<sub>3</sub> (A) and Al<sub>2</sub>O<sub>3</sub> (B) at 200 °C. Comparison of the consumption rate of bridge nitrate (1614 cm<sup>-1</sup>) over Ag/Al<sub>2</sub>O<sub>3</sub> and Al<sub>2</sub>O<sub>3</sub> (C).

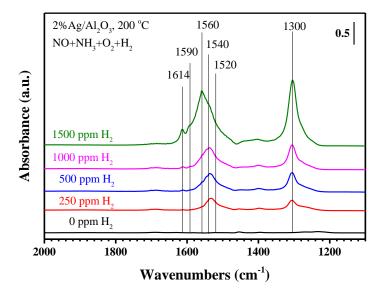


Figure S12. In situ DRIFTS of H<sub>2</sub>-NH<sub>3</sub>-SCR over Ag/Al<sub>2</sub>O<sub>3</sub> with different concentration of H<sub>2</sub>. Feed composition: 500 ppm NO, 500 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, 0-1500 ppm H<sub>2</sub>, N<sub>2</sub> balance, 200 °C.

Figure S12 shows in situ DRIFTS of the H<sub>2</sub>-NH<sub>3</sub>-SCR over Ag/Al<sub>2</sub>O<sub>3</sub> with different amount of H<sub>2</sub> at 200 °C. In this experiment, bridging nitrates (1614 cm<sup>-1</sup>), bidentate nitrates (1590 cm<sup>-1</sup>), and monodentate nitrates (1560, 1540, 1520, and 1300 cm<sup>-1</sup>) were observed on the surface of catalyst. Adsorbed NH<sub>3</sub> species was not observed possibly due to its low intensity (as shown in Figure 7). As the H<sub>2</sub> concentration increased, the amount of adsorbed nitrates gradually increased. Notably, the reactive nitrate species (bridging nitrate and bidentate nitrate) were only observed when a high concentration of H<sub>2</sub> (1500 ppm) was employed. As demonstrated in Figure 6, the formation rate of nitrate species on the Ag/Al<sub>2</sub>O<sub>3</sub> was determined by the H<sub>2</sub> concentration. During the H<sub>2</sub>-NH<sub>3</sub>-SCR reaction with low concentration of H<sub>2</sub> ( $\leq$  1000 ppm), the formation of reactive nitrates was slower than its further reaction with NH<sub>3</sub> species, thus resulting in the absence of these reactive nitrate species. When the H<sub>2</sub> concentration was rather high (1500 ppm), the formation of reactive nitrates was fast enough and thus resulted in the accumulation of these species. This experiment further confirmed that the formation of reactive nitrates was the rate-determining step for the H<sub>2</sub>-NH<sub>3</sub>-SCR reaction.