

Supporting Information

Air-water partitioning of C5 and C6 alkanones. Measurement, Critical Compilation, Correlation, and Recommended Data

Štěpán Hovorka^a, Pavel Vrbka^a, Carolina Bermúdez-Salguero^b, Alexander Böhme^c, and Vladimír Dohnal^a

^a Department of Physical Chemistry, University of Chemistry and Technology, Technická 5, 166 28 Prague 6, Czech Republic

^b Departamento de Fisicoquímica, Facultad de Química, Universidad Nacional Autónoma de México, México, D.F. 04510, Mexico

^c UFZ Department of Ecological Chemistry, Helmholtz Centre for Environmental Research, Permoserstr. 15, 04318 Leipzig, Germany

E-mail: Stepan.Hovorka@vscht.cz

Table S1. Parameters for Estimation of the Second Virial Coefficients by the Hayden-O'Connell Method: Critical Temperature T_c , Critical Pressure P_c , Radius of Gyration R_D , Dipole Moment μ , Association Constant η_{ii} , and Solvation Constant $\eta_{i,\text{water}}$

Liquid	$T_c / \text{K}^{\text{a}}$	$P_c / \text{MPa}^{\text{a}}$	$R_D / \text{\AA}^{\text{b}}$	$\mu / \text{D}^{\text{c}}$	η_{ii}^{d}	$\eta_{i,\text{water}}^{\text{d}}$
pentan-2-one	561	3.70	3.618	2.77	0.9	1.0
pentan-3-one	562	3.73	3.583	2.82	0.9	1.0
3-methylbutan-2-one	555	3.79	3.465	2.76	0.9	1.0
hexan-2-one	587	3.32	4.093	2.68	0.9	1.0
hexan-3-one	583	3.32	4.009	2.87	0.9	1.0
3-methylpentan-2-one	573 ^f	3.32 ^f	3.828	2.77	0.9	1.0
4-methylpentan-2-one	575 ^g	3.27 ^g	3.572	2.69	0.9	1.0
2-methylpentan-3-one	567 ^f	3.32 ^f	3.892	3.12	0.9	1.0
3,3-dimethylbutan-2-one	567	3.47	3.800	2.75	0.9	1.0
water	647.14	21.491	0.615	1.83	1.7 ^e	—

^a From reference 1.

^b From reference 2.

^c From reference 3.

^d From reference 4, the value assumed to be the same as for butan-2-one.

^e From reference 4.

^f From reference 5.

^g From reference 6.

Table S2. Experimental Values of Air-Water Partition Coefficient and Activity Coefficient of Alkanones at Infinite Dilution in Water Reported in the Literature^a along with Their Estimated Standard Uncertainties^b and Experimental Method^c

T/ K	$1000 \cdot K_{\text{aw}}$	$u_{\text{rel}}(K_{\text{aw}})$	γ_1^∞	$u_{\text{rel}}(\gamma_1^\infty)$	method	ref
pentan-2-one						
301.15	4.4	0.1	111	0.1	EPICS	68NEL/HOF ⁷
298.15	2.6	0.2	75.8	0.2	HSA	69BUT/LIN ⁸
303.15	4.1	0.1	93.8	0.1	HSA	71NAW ⁹
310.15	6.02	0.1	99.8	0.1	PRV	79SAT/NAK ¹⁰
298.15	3.39	0.03	98.9	0.03	GLC	80MAS/PEM ¹¹
310.2	7.24	0.05	120	0.05	IGS	81KUH/BOC ¹²
298.15	4.63	0.2	135.1	0.2	GLC/LLC	86JAN/QAD ¹³
303.15	5.46	0.2	125.0	0.2	GLC/LLC	86JAN/QAD ¹³
308.15	7.15	0.2	129.7	0.2	GLC/LLC	86JAN/QAD ¹³
298.15	3.52	0.05	102.5	0.05	GLC/LLC	88DJE/LAU ¹⁴
298.15	3.50	0.05	102	0.05	NSGLC	91LAN/BEL ¹⁵
298.15	3.23	0.03	94.3	0.02	HSA	93DAL ¹⁶
298.15	3.42	0.03	99.7	0.03	IGS	97SHI/MAC ¹⁷
303.25	4.61	0.03	105	0.03	IGS	04ATI/GRU ¹⁸
313.25	8.30	0.03	120	0.03	IGS	04ATI/GRU ¹⁸
323.25	13.5	0.03	128	0.03	IGS	04ATI/GRU ¹⁸

333.25	21.0	0.03	135	0.03	IGS	04ATI/GRU ¹⁸
297.85	4.36	0.2	129	0.2	RGLC	05STR/DEL ¹⁹
298.15	5.08	0.5	148	0.2	RGLC	05STR/DEL ¹⁹
298.15	3.41	0.03	99.4	0.03	MHE	05BRA/CHA ²⁰
323.15	12.3	0.05	117	0.05	RHSA	05CHA/FAL ²¹
333.15	18.7	0.05	121	0.05	RHSA	05CHA/FAL ²¹
343.15	27.8	0.05	125	0.05	RHSA	05CHA/FAL ²¹
353.15	39.7	0.03	127	0.03	RHSA	05CHA/FAL ²¹
278.15	0.67	0.2	57.5	0.2	HSA	07JL/EVA ²²
283.15	0.95	0.2	61.1	0.2	HSA	07JL/EVA ²²
288.15	1.30	0.2	63.5	0.2	HSA	07JL/EVA ²²
293.15	1.82	0.2	68.3	0.2	HSA	07JL/EVA ²²
298.15	2.45	0.2	71.4	0.2	HSA	07JL/EVA ²²

pentan-3-one

310.15	5.53	0.2	91.5	0.2	PRV	79SAT/NAK ¹⁰
298.15	3.87	0.03	113	0.03	GLC	80MAS/PEM ¹¹
310.2	8.32	0.03	137	0.03	IGS	81KUH/BOC ¹²
298.15	4.62	0.2	134.8	0.2	GLC/LLC	86JAN/QAD ¹³
303.15	6.10	0.2	139.6	0.2	GLC/LLC	86JAN/QAD ¹³
308.15	9.94	0.2	180	0.2	GLC/LLC	86JAN/QAD ¹³

298.15	3.87	0.03	113	0.03	NSGLC	91LAN/BEL ¹⁵
298.15	3.68	0.03	107.4	0.03	HSA	93DAL ¹⁶
278.15	0.72	0.2	62.1	0.2	RHSA	07JI/EVA ²²
283.15	0.99	0.2	64.0	0.2	RHSA	07JI/EVA ²²
288.15	1.39	0.2	68.1	0.2	RHSA	07JI/EVA ²²
293.15	1.93	0.2	72.5	0.2	RHSA	07JI/EVA ²²
298.15	2.56	0.5	74.7	0.2	RHSA	07JI/EVA ²²
293.2	1.93^d	0.2	72.2	0.2	TENS	10OFA/WAG ²³
3-methylbutan-2-one						
298.15	4.20	0.05	84	0.05	HSA	93DAL ¹⁶
hexan-2-one						
303.15	5.3	0.1	359	0.1	HSA	71NAW ⁹
310.15	9.0	0.1	425	0.1	PRV	79SAT/NAK ¹⁰
298.15	4.14	0.03	368	0.03	GLC	80MAS/PEM ¹¹
310.2	9.33	0.02	439	0.02	IGS	81KUH/BOC ¹²
298	3.67	0.1	329	0.1	GLC/LLC	88DJE/LAU ¹⁴
298.15	4.00	0.05	355.7	0.03	HSA	93DAL ¹⁶
298.15	2.98	0.2	265	0.2	RGLC	05STR/DEL ¹⁹
297.85	3.53	0.2	319	0.2	RGLC	05STR/DEL ¹⁹
323.15	16.5	0.1	419	0.1	RHSA	05CHA/FAL ²¹

333.15	25.3	0.1	416	0.1	RHSA	05CHA/FAL ²¹
343.15	37.0	0.1	406	0.1	RHSA	05CHA/FAL ²¹
353.15	59.2	0.05	446	0.05	RHSA	05CHA/FAL ²¹
298.15	4.3	0.03	382	0.03	MHE	05BRA/CHA ²⁰

hexan-3-one

298.15	5.66	0.03	412	0.03	GLC	80MAS/PEM ¹¹
310.2	12.9	0.01	507	0.03	IGS	81KUH/BOC ¹²
275.15	39	— ^e	11000	— ^e	EPICS	99DEW/LAN ²⁴
279.15	55	— ^e	12030	— ^e	EPICS	99DEW/LAN ²⁴
283.15	54	— ^e	9230	— ^e	EPICS	99DEW/LAN ²⁴
291.15	50	— ^e	5350	— ^e	EPICS	99DEW/LAN ²⁴
298.15	52	— ^e	3780	— ^e	EPICS	99DEW/LAN ²⁴

4-methylpentan-2-one

310.15	12.7	0.05	358	0.05	PRV	79SAT/NAK ¹⁰
310.2	14.1	0.02	396	0.02	IGS	81KUH/BOC ¹²
283.15	28.4^f	— ^e	3350	— ^e	EPICS	88ASH ²⁵
288.15	15.6	1	1380	1	EPICS	88ASH ²⁵
293.15	12.1	1	804	1	EPICS	88ASH ²⁵
298.15	15.9	1	814	1	EPICS	88ASH ²⁵
303.15	27.3	1	1080	1	EPICS	88ASH ²⁵

313.15	18.4	0.1	451	0.1	HSA	92KOL/WEL ²⁶
333.15	43.9	0.05	459	0.05	HSA	92KOL/WEL ²⁶
343.15	61.7	0.05	441	0.05	HSA	92KOL/WEL ²⁶
353.15	84.7	0.05	424	0.05	HSA	92KOL/WEL ²⁶
298.15	10.4^g	0.5	531	0.5	EPICS	14KIM/KIM ²⁷

^a The property value reported in the original literature is given in bold, the other one was obtained from the interconversion formula $K_{\text{aw}} = \gamma_1^\infty p_1^s v_2^L / (RT)$ assuming the ideal behavior of gas phase.

^b The uncertainties were assigned in this work.

^c EPICS, equilibrium partitioning in closed system; HSA, headspace analysis; RHSA, relative headspace analysis; PRV, phase ratio variation; GLC gas-liquid chromatography; RGLC relative gas-liquid chromatography; LLC liquid-liquid chromatography; NSGLC non-steady state gas-liquid chromatography; IGS, inert gas stripping; MHE, multiple headspace extraction; TENS, tensimetry.

^d The original source reports the Henry's law constant $H_{12} = p_1 / x_1$ which was converted here to K_{aw} by $K_{\text{aw}} = H_{12} v_2^L / (RT)$.

^e Rejected wrong value.

^f The original source reports the Henry's law constant $H_c = p_1 / c_1$ which was converted here to K_{aw} by $K_{\text{aw}} = H_c / (RT)$.

^g The original source reports the inverse Henry's law constant $1/H_c = c_1 / p_1$ which was converted here to K_{aw} by $K_{\text{aw}} = H_c / (RT)$.

Table S3. Values of Infinite Dilution Partial Molar Excess Enthalpy $\bar{H}_1^{E,\infty}$ ^a and Hydration Enthalpy $\Delta_{hyd}H_1$ ^b Used in the Simultaneous Correlation with Data on Limiting Activity Coefficient and Air-Water Partition Coefficient, Respectively, along with Their Estimated Standard Uncertainties (in Parentheses)

alkanone	T / K	$\frac{\bar{H}_1^{E,\infty}}{\text{kJ} \cdot \text{mol}^{-1}}$ ^a	ref	$\frac{\Delta_{hyd}H_1}{\text{kJ} \cdot \text{mol}^{-1}}$ ^b
pentan-2-one	298.15	-10.21 (0.15)	81DEL/STR ²⁸	-46.38 (0.5)
	288.15	-12.76 (0.05)	17DOH/REH ²⁹	
	298.15	-10.42 (0.05)	17DOH/REH ²⁹	-46.59 (0.5)
	308.15	-8.20 (0.03)	17DOH/REH ²⁹	
	318.15	-5.95 (0.02)	17DOH/REH ²⁹	
pentan-3-one	298.15	-10.9 (0.1)	81DEL/STR ²⁸	-47.29 (0.4)
	288.15	-13.01 (0.08)	17DOH/REH ²⁹	
	298.15	-10.68 (0.06)	17DOH/REH ²⁹	-47.07 (0.4)
	308.15	-8.37 (0.06)	17DOH/REH ²⁹	
	318.15	-6.09 (0.05)	17DOH/REH ²⁹	
3-methylbutan-2-one	298.15	-10.63 (0.1)	81DEL/STR ²⁸	-45.21 (0.4)
	288.15	-12.61 (0.05)	17DOH/REH ²⁹	
	298.15	-10.47 (0.04)	17DOH/REH ²⁹	-45.05 (0.4)
	308.15	-8.25 (0.03)	17DOH/REH ²⁹	
	318.15	-6.13 (0.03)	17DOH/REH ²⁹	
hexan-2-one	298.15	-9.46 (0.1)	81DEL/STR ²⁸	-50.32 (0.4)

	288.15	-12.23 (0.10)	17DOH/REH ²⁹	
	298.15	-9.46 (0.08)	17DOH/REH ²⁹	-50.32 (0.4)
	308.15	-6.58 (0.06)	17DOH/REH ²⁹	
	318.15	-3.92 (0.05)	17DOH/REH ²⁹	
4-methylpentan-2-one	288.15	-12.77 (0.08)	17DOH/REH ²⁹	
	298.15	-9.97 (0.08)	17DOH/REH ²⁹	-48.33 (0.4)
	308.15	-7.25 (0.05)	17DOH/REH ²⁹	
	318.15	-4.73 (0.04)	17DOH/REH ²⁹	
3,3-dimethylbutan-2-one	298.15	-9.5 (0.1)	81DEL/STR ²⁸	-45.08(0.5)

^a Direct calorimetric measurements in the highly dilute region.

^b Determined from $\Delta_{\text{hyd}} H_1 = \bar{H}_1^{\text{E},\infty} - \Delta_{\text{vap}} H_1^0 + RT(1 - \alpha_w T)$ where $\Delta_{\text{vap}} H_1^0$ is the pure solute standard vaporization enthalpy (taken from reference 30) and α_w is the thermal expansion coefficient of water.

Table S4. Values of Infinite Dilution Partial Molar Excess Heat Capacity $\bar{C}_{p,1}^{E,\infty}$ and Hydration Heat Capacity $\Delta_{hyd}C_{p,1}$ at 298.15 K Used in the Simultaneous Correlation with Data on Limiting Activity Coefficient and Air-Water Partition Coefficient, Respectively, along with Their Estimated Standard Uncertainties (in Parentheses)

alkanone	$\frac{\bar{C}_{p,1}^{E,\infty}}{J \cdot K^{-1} \cdot mol^{-1}}$		$\frac{\Delta_{hyd}C_{p,1}}{J \cdot K^{-1} \cdot mol^{-1}}$	ref
pentan-2-one			290 (10) ^a	17DOH/REH ²⁹
pentan-3-one	237 ^b (6)	78ROU/PER ³¹ 96ZAB/RUZ ³²	301 (25) ^c	78ROU/PER ³¹ 81BUR ³³
			292 (15) ^a	17DOH/REH ²⁹
3-methylbutan-2-one			273 (10) ^a	17DOH/REH ²⁹
hexan-2-one			348 (10) ^a	17DOH/REH ²⁹
hexan-3-one	289 ^d (29)	04PLY/PLY ³⁴ 96ZAB/RUZ ³² 81BUR ³³	356 ^e (36)	04PLY/PLY ³⁴
3-methylpentan-2-one	296 ^d (30)	04PLY/PLY ³⁴ 08KOL/KUK ³⁵ 81BUR ³³	357 ^e (36)	04PLY/PLY ³⁴
4-methylpentan-2-one			337 (10) ^a	17DOH/REH ²⁹
2-methylpentan-3-one	292 ^d	04PLY/PLY ³⁴ 08KOL/KUK ³⁵ 81BUR ³³	357 ^e (36)	04PLY/PLY ³⁴
3,3-dimethylbutan-2-one	277 ^d	04PLY/PLY ³⁴ 96ZAB/RUZ ³² 81BUR ³³	336 ^e (34)	04PLY/PLY ³⁴

^a The value of $\Delta_{hyd}C_{p,1}$ reported here was taken from ref 29.

^b The value of $\bar{C}_{p,1}^{E,\infty}$ reported here was calculated from $\bar{C}_{p,1}^{E,\infty} = \bar{C}_{p,1}^{\infty} - C_{p,1}^{\bullet}$ where $\bar{C}_{p,1}^{\infty}$ is the solute partial molar heat capacity at infinite dilution determined by direct calorimetric measurements in ref 31 and $C_{p,1}^{\bullet}$ is the solute heat capacity in the pure liquid state taken from ref 32.

^c The value of $\Delta_{hyd}C_{p,1}$ reported here was calculated from $\Delta_{hyd}C_{p,1} = \bar{C}_{p,1}^{\infty} - C_{p,1}^0$ where $\bar{C}_{p,1}^{\infty}$ is the solute partial molar heat capacity at infinite dilution determined by direct calorimetric

measurements in ref 31 and $C_{p,1}^0$ is the pure solute heat capacity in the ideal gas state taken from ref 33.

^d The value of $\bar{C}_{p,1}^{E,\infty}$ reported here was calculated from $\bar{C}_{p,1}^{E,\infty} = \Delta_{\text{hyd}} C_{p,1} + (C_{p,1}^0 - C_{p,1}^\bullet)$ where $\Delta_{\text{hyd}} C_{p,1}$ is the hydration heat capacity as estimated by the first order group contribution method of Plyasunov et al.³⁴, and $C_{p,1}^0$, and $C_{p,1}^\bullet$ are the pure solute heat capacity in the ideal gas state, and that in the liquid state, respectively. The $C_{p,1}^\bullet$ data were taken from ref 32 or estimated by the method of Kolská et al.³⁵ and $C_{p,1}^0$ data were taken from ref 33.

^e Estimated by the first order group contribution method of Plyasunov et al.³⁴

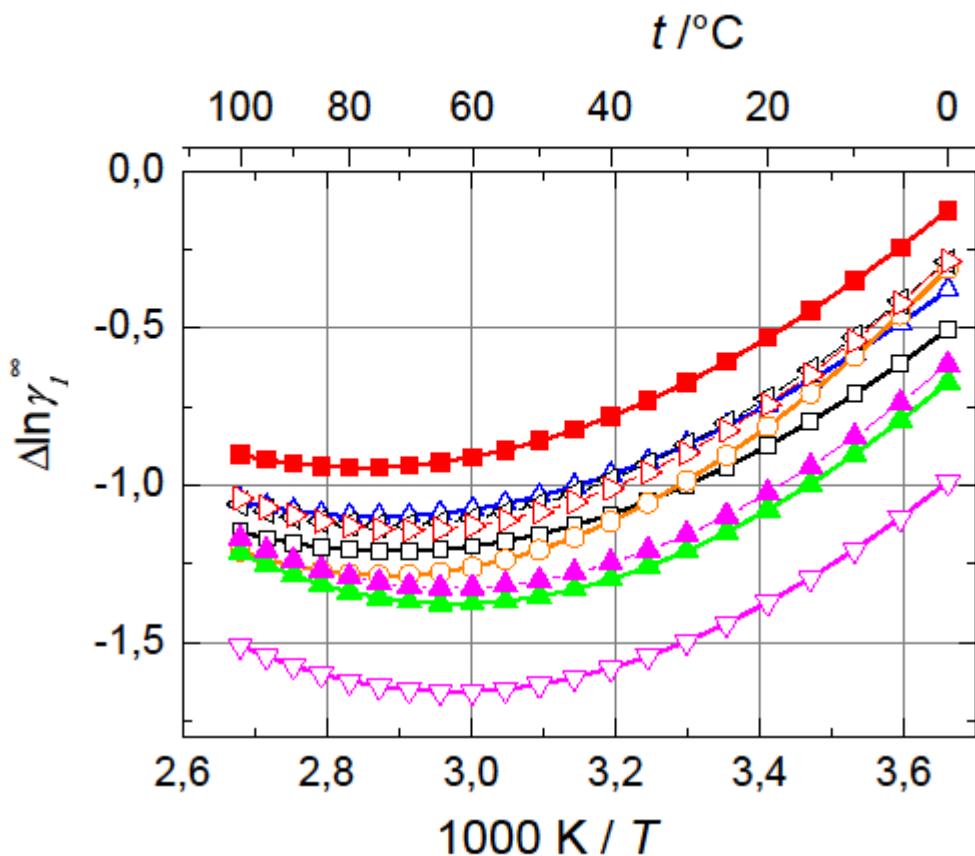


Figure S1. Deviation $\Delta \ln \gamma_1^\infty = \ln \gamma_1^\infty(\text{predicted}) - \ln \gamma_1^\infty(\text{recommended})$ as a function of temperature for the COSMO-SAC method: (□), pentan-2-one; (■), pentan-3-one; (△), 3-methylbutan-2-one; (▽), hexan-2-one; (○), hexan-3-one; (▲), 3-methylpentan-2-one; (◀), 4-methylpentan-2-one; (▷), 2-methylpentan-3-one; (▲), 3,3-dimethylbutan-2-one.

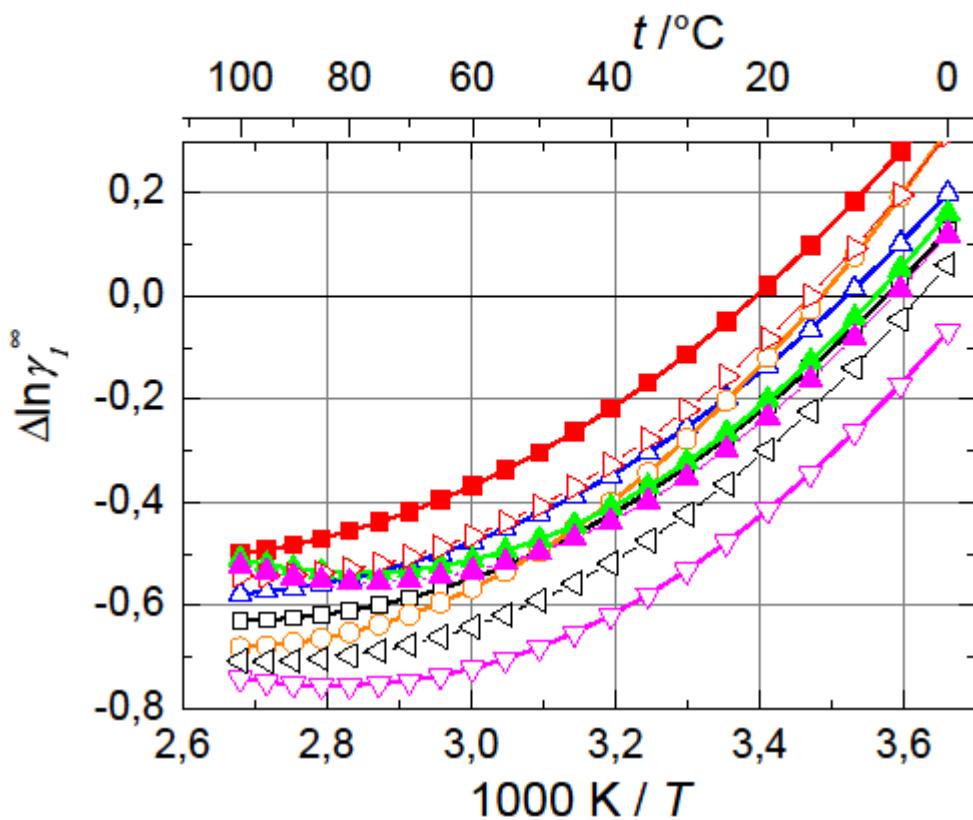


Figure S2. Deviation $\Delta \ln \gamma_1^\infty = \ln \gamma_1^\infty(\text{predicted}) - \ln \gamma_1^\infty(\text{recommended})$ as a function of temperature for the modified UNIFAC (Dortmund): (\square), pentan-2-one; (\blacksquare), pentan-3-one; (\triangle), 3-methylbutan-2-one; (∇), hexan-2-one; (\circ), hexan-3-one; (\blacktriangle), 3-methylpentan-2-one; (\lhd), 4-methylpentan-2-one; (\triangleright), 2-methylpentan-3-one; (\blacktriangleup), 3,3-dimethylbutan-2-one.

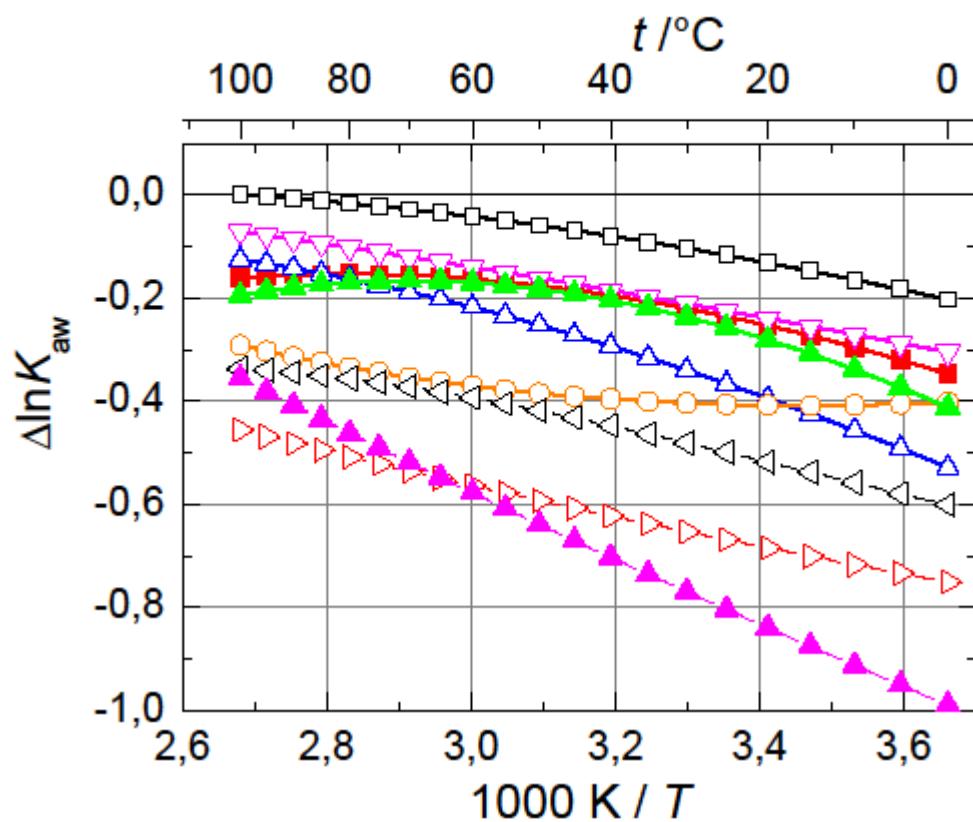


Figure S3. Deviation $\Delta \ln K_{aw} = \ln K_{aw}(\text{predicted}) - \ln K_{aw}(\text{recommended})$ as a function of temperature for the Abraham LFER-L method: (□), pentan-2-one; (■), pentan-3-one; (△), 3-methylbutan-2-one; (▽), hexan-2-one; (○), hexan-3-one; (▲), 3-methylpentan-2-one; (◀), 4-methylpentan-2-one; (▷), 2-methylpentan-3-one; (▲), 3,3-dimethylbutan-2-one.

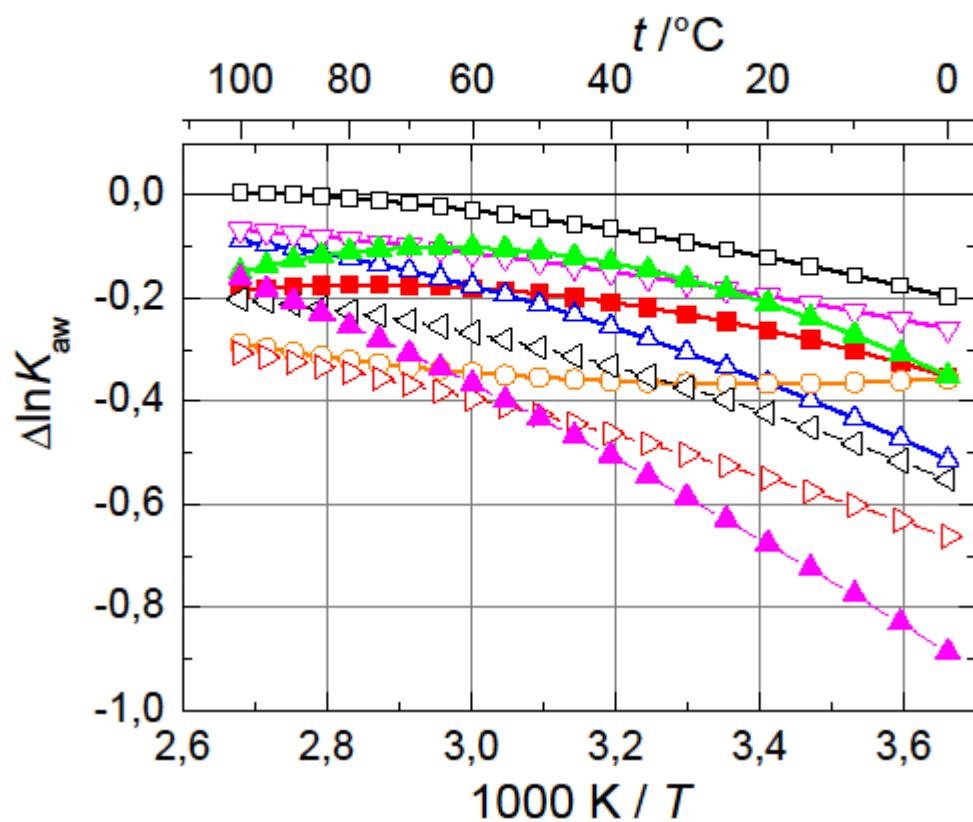


Figure S4. Deviation $\Delta \ln K_{\text{aw}} = \ln K_{\text{aw}}(\text{predicted}) - \ln K_{\text{aw}}(\text{recommended})$ as a function of temperature for the Abraham LFER-V method: (\square), pentan-2-one; (\blacksquare), pentan-3-one; (\triangle), 3-methylbutan-2-one; (∇), hexan-2-one; (\circ), hexan-3-one; (\blacktriangle), 3-methylpentan-2-one; (\triangleleft), 4-methylpentan-2-one; (\triangleright), 2-methylpentan-3-one; (\blacktriangledown), 3,3-dimethylbutan-2-one.

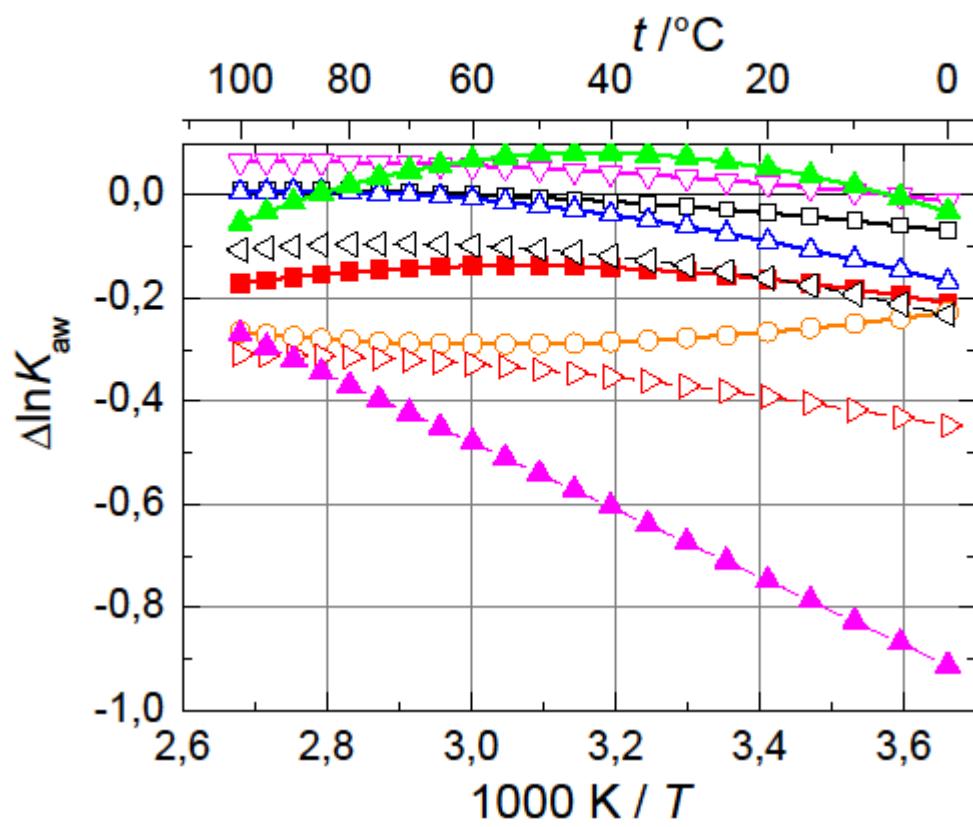


Figure S5. Deviation $\Delta \ln K_{aw} = \ln K_{aw}(\text{predicted}) - \ln K_{aw}(\text{recommended})$ as a function of temperature for the Cabani group contribution method: (□), pentan-2-one; (■), pentan-3-one; (△), 3-methylbutan-2-one; (▽), hexan-2-one; (○), hexan-3-one; (▲), 3-methylpentan-2-one; (◁), 4-methylpentan-2-one; (▷), 2-methylpentan-3-one; (▲), 3,3-dimethylbutan-2-one.

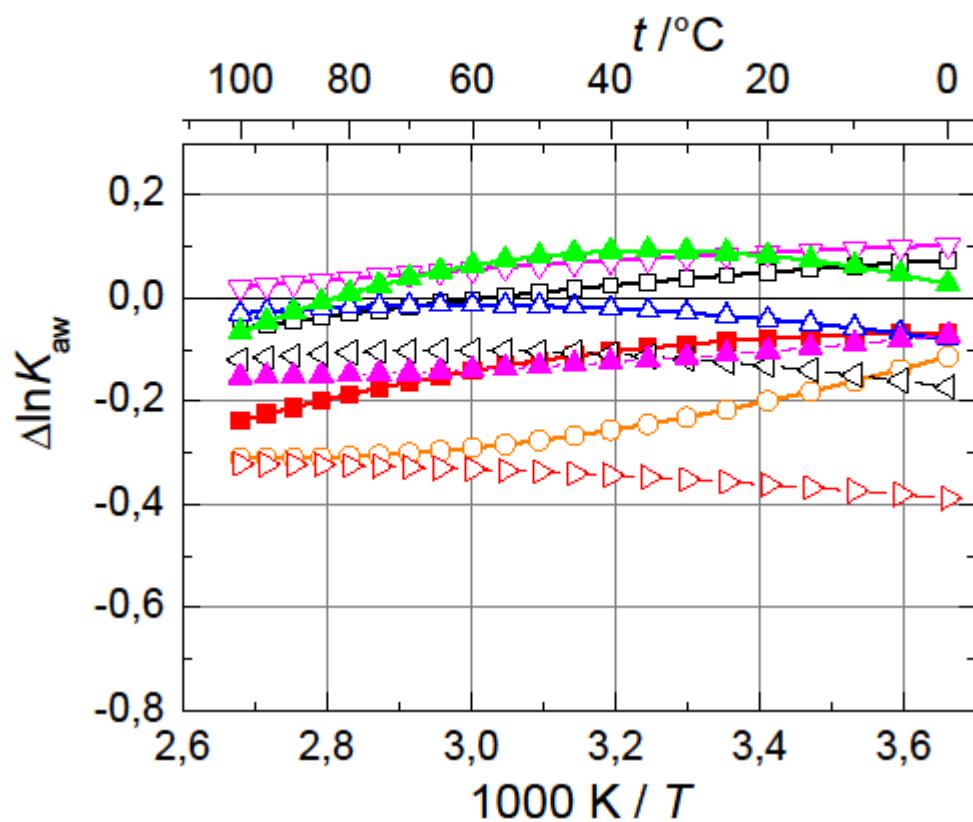


Figure S6. Deviation $\Delta \ln K_{\text{aw}} = \ln K_{\text{aw}}(\text{predicted}) - \ln K_{\text{aw}}(\text{recommended})$ as a function of temperature for the Plyasunov first-order group contribution method: (\square), pentan-2-one; (\blacksquare), pentan-3-one; (\triangle), 3-methylbutan-2-one; (∇), hexan-2-one; (\circ), hexan-3-one; (\blacktriangle), 3-methylpentan-2-one; (\triangleleft), 4-methylpentan-2-one; (\triangleright), 2-methylpentan-3-one; (\blacktriangle), 3,3-dimethylbutan-2-one.

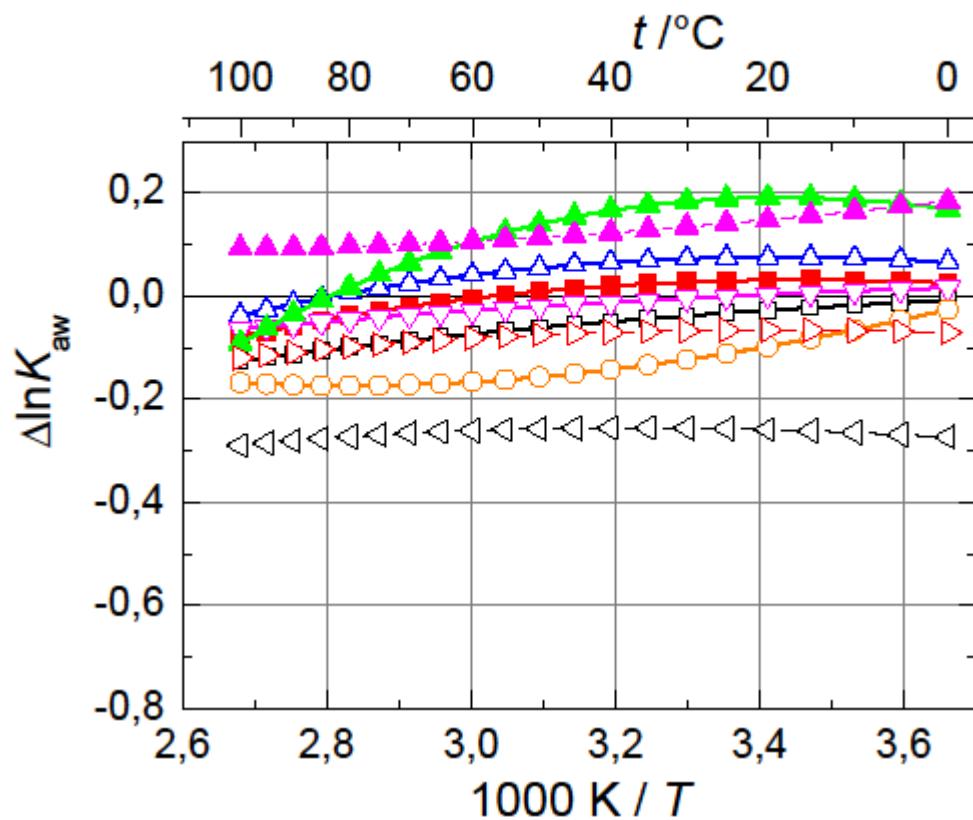


Figure S7. Deviation $\Delta \ln K_{aw} = \ln K_{aw}(\text{predicted}) - \ln K_{aw}(\text{recommended})$ as a function of temperature for the Plyasunov second-order group contribution method: (\square), pentan-2-one; (\blacksquare), pentan-3-one; (\triangle), 3-methylbutan-2-one; (∇), hexan-2-one; (\circ), hexan-3-one; (\blacktriangle), 3-methylpentan-2-one; (\blacktriangleleft), 4-methylpentan-2-one; (\blacktriangleright), 2-methylpentan-3-one; (\blacktriangleup), 3,3-dimethylbutan-2-one.

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