

Supporting information

Effects of Cu precursor type on the catalytic activity of Cu/ZrO₂ towards methanol synthesis *via* CO₂ hydrogenation

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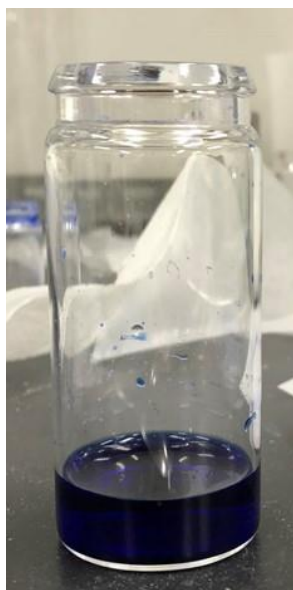


Figure S1 Photograph of copper ammine complex solution.

Section S1 Validation of our experimental condition for N₂O titration

In our previous work, the experimental condition of N₂O titration for Cu-based catalysts were examined using a series of Cu/SiO₂ catalysts ¹.

Prior to the examination, H₂ chemisorption for the catalysts was investigated at 25 °C *via* experiments and calculation. We confirmed that H₂ molecules adsorb on the surface of Cu⁰ nanoparticles. The maximum H₂ uptake was 0.46 H₂ molecules per Cu surface atoms. The value (0.46) was slightly higher than the stoichiometry of H₂ to Cu (Cu + 0.5 H₂ = Cu-H).

When the N₂O titration was carried out at 90 °C, the amount of decomposed N₂O was almost the same to the H₂ uptake. The experiments clarified that the stoichiometry of N₂O to Cu was 0.5 mol_{N₂O} mol_{Cu}⁻¹. The stoichiometry (0.5 mol_{N₂O} mol_{Cu}⁻¹) is also expected from the equation of N₂O titration (Cu + 0.5 N₂O = Cu₂O + 0.5 N₂). X-ray absorption spectroscopy measurements showed that the N₂O-treated Cu/SiO₂ catalysts possessed Cu-O scattering path with the distance = 1.82 Å which was similar to that of Cu₂O (1.85 Å) and different from that of CuO (1.96 Å). In consequence, the N₂O titration at 90 °C oxidizes the exposed Cu⁰ surface to Cu⁺, not the Cu⁰ bulk.

Here, we explained the detection way of N₂ and N₂O not using any column. **Figure S2** shows the typical N₂O titration sequence. A thermal conductivity detector was used to measure the gas composition of N₂ and N₂O in a He stream (a carrier gas). In the figure, twenty peaks are observed. The peak size of N₂ must be smaller than that of N₂O due to the thermal conductivity difference: thermal conductivities of N₂, N₂O, and He (a carrier gas) at STP are 0.026, 0.017, and 0.149 W mK⁻¹, respectively ². For the first four peaks, their area was *ca.* 55000 count sec and their height was *ca.* 4700 count. The peaks are attributed to N₂ decomposed from N₂O. For the last six peaks, their area was *ca.* 65000 count sec and their height was *ca.* 5500 count. The peaks are attributed to N₂O which was not decomposed on the Cu-based catalysts. In addition, the other peaks are attributed to the mixture gas of N₂ and N₂O. Our previous work ¹ also used this detection way and came up with the conclusion described in the previous paragraph.

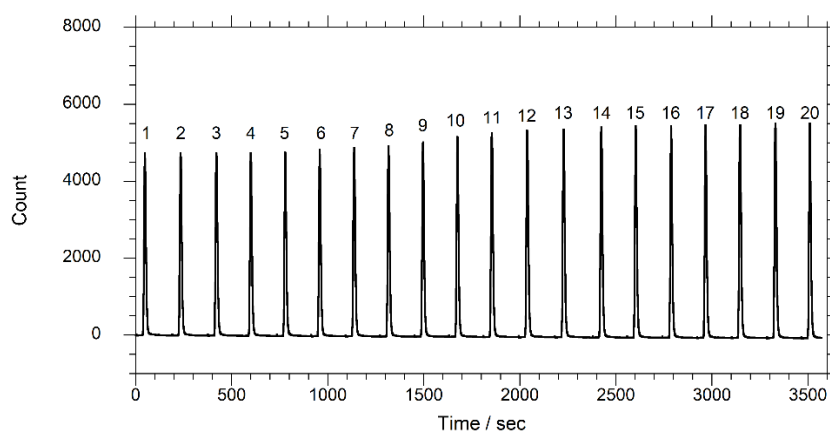


Figure S2 N₂O titration sequence for **NIT-500** at 90 °C. Carrier gas: He.

Table S1 Height and area of peaks in **Figure S1** and N₂/N₂O composition.

No.	Peak height	Peak area	Composition calculated from peak areas / %	
	/ count	/ count sec	N ₂	N ₂ O
1	4728	54940	100	0
2	4723	54978	100	0
3	4726	54895	100	0
4	4726	54865	100	0
5	4762	56449	86	14
6	4811	57603	74	26
7	4870	57857	71	29
8	4943	57976	70	30
9	5031	59682	53	47
10	5155	62483	25	75
11	5258	63604	14	86
12	5326	63683	13	87
13	5371	62656	23	77
14	5404	64792	2	98
15	5436	65002	0	100
16	5452	65221	0	100
17	5474	65352	0	100
18	5485	65821	0	100
19	5495	65156	0	100
20	5504	66061	0	100

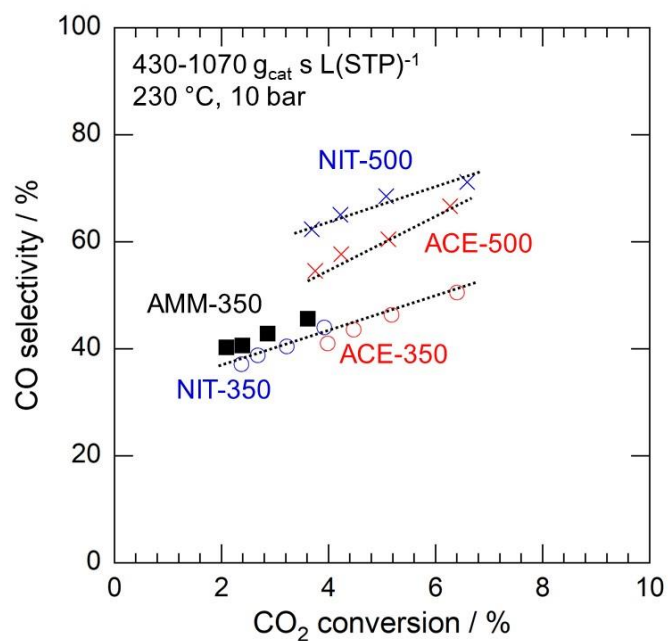


Figure S3 CO selectivity at different CO₂ conversions for **NIT-*T*** and **ACE-*T*** samples.

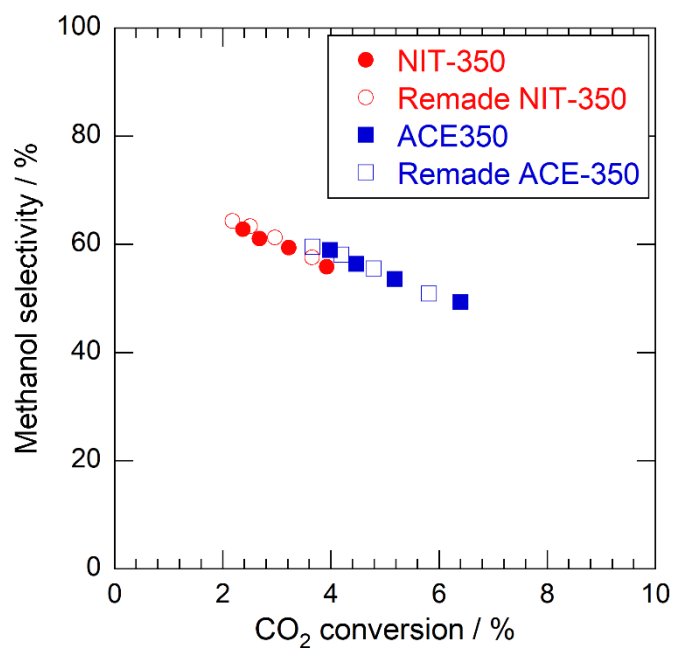


Figure S4 Methanol selectivity at different CO₂ conversion for **NIT-350**, remade **NIT-350**, **ACE-350**, and remade **ACE-350**.

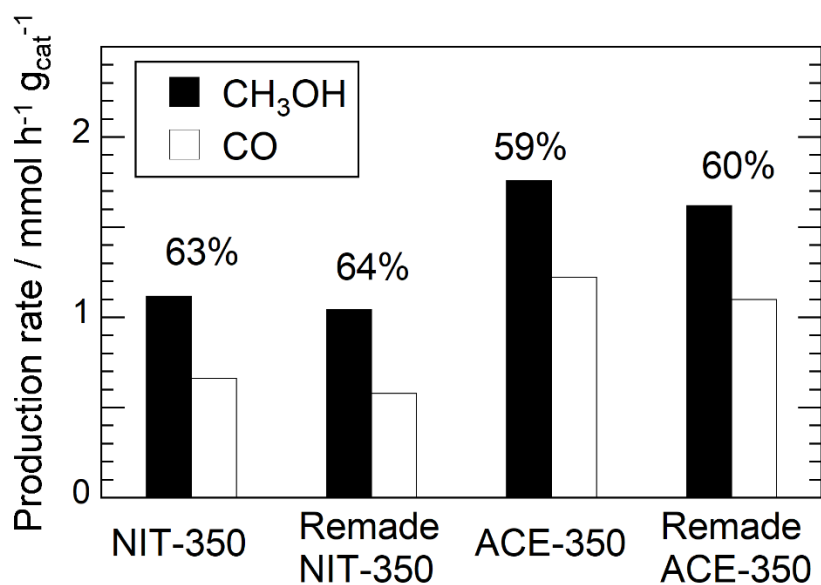


Figure S5 Methanol and CO production rates for **NIT-350**, remade **NIT-350**, **ACE-350**, and remade **ACE-350** when the contact time was 430 g_{cat} s L(STP)⁻¹. The values above the bars indicate their selectivity towards methanol.

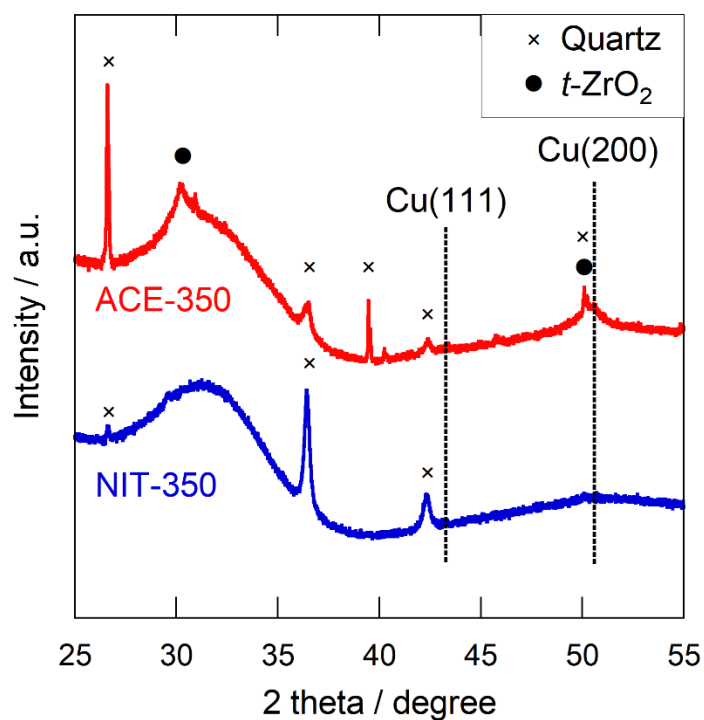


Figure S6 PXRD patterns for spent **ACE-350** and **NIT-350**. Although the quartz sand was removed as much as possible from the spent catalysts, it remained a little and was detected by PXRD.

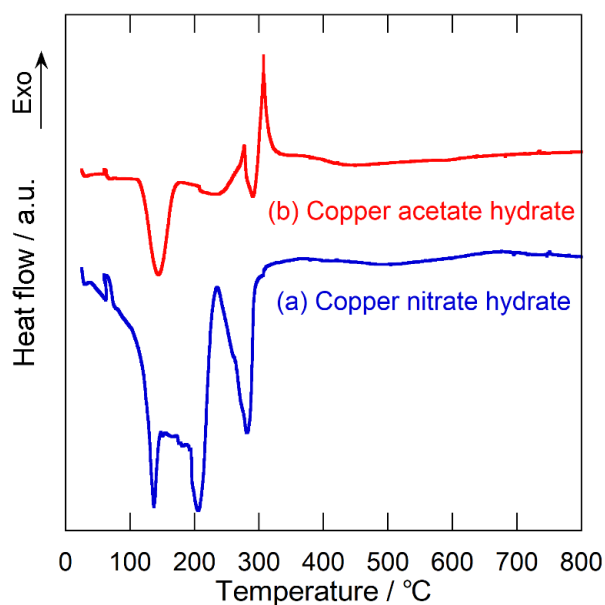


Figure S7 DTA curves for (a) copper nitrate hydrate and (b) copper acetate hydrate. Heating rate: $10\text{ }^{\circ}\text{C min}^{-1}$.

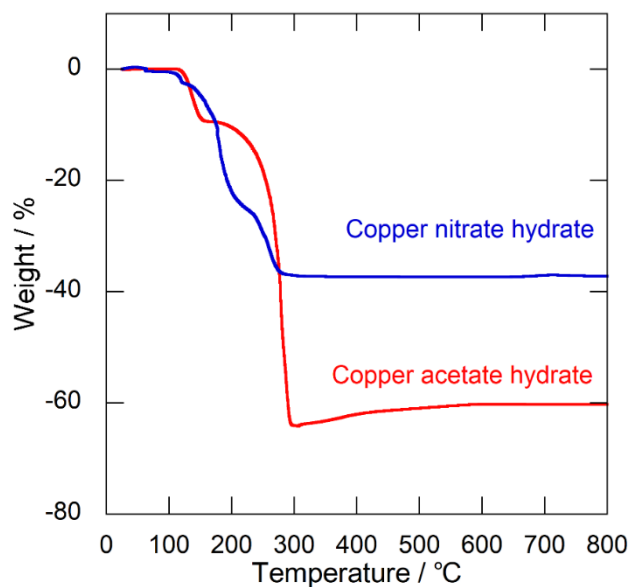


Figure S8 TG curves of copper nitrate hydrate and copper acetate hydrate. For copper acetate hydrate, the sample gains weight with increasing calcination temperature starting from 300 °C. Heating rate: $10\text{ }^{\circ}\text{C min}^{-1}$.

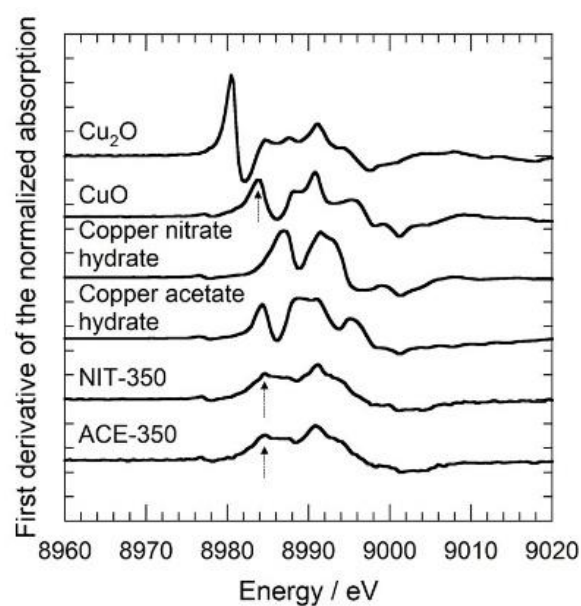


Figure S9 First derivative XANES spectra of **NIT-350**, **ACE-350**, Cu_2O , CuO , copper nitrate hydrate, and copper acetate hydrate. These spectra were obtained at room temperature. The spectra of CuO , **NIT-350**, and **ACE-350** possessed a peak at 8984 eV corresponding to the $1s \rightarrow 4p\pi$ transition.

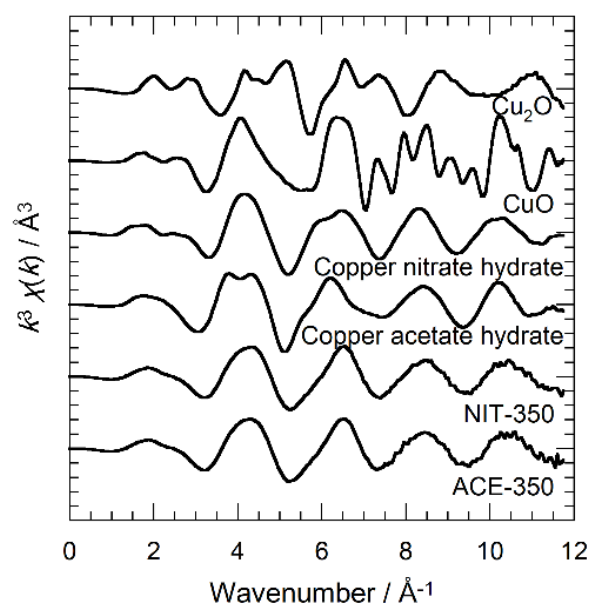


Figure S10 k^3 -weighted EXAFS oscillations of **NIT-350**, **ACE-350**, Cu_2O , CuO , copper nitrate hydrate, and copper acetate hydrate measured at room temperature near the Cu K-edge.

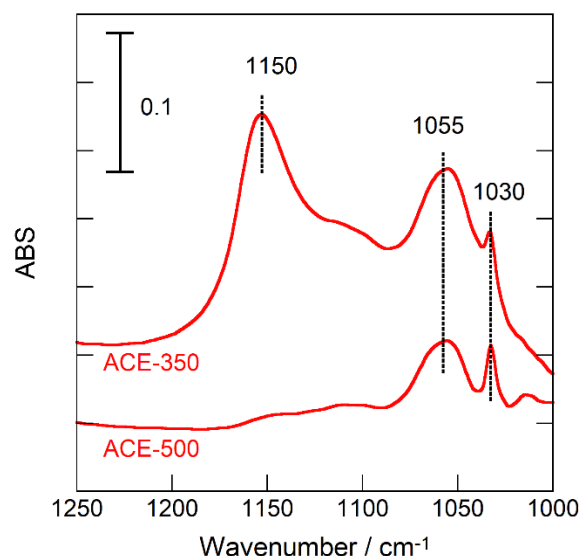


Figure S11 FTIR spectra of methoxy species on ACE-350 and ACE-500.

Methanol vapor sorption on **ACE-350** and **ACE-500** was examined by *in-situ* Fourier transform infrared spectroscopy (*in-situ* FTIR) measurements. The windows of the FTIR cell was high purity CaF_2 . The cell was put in a JASCO FT/IR 4600 instrument with a mercury-cadmium-telluride (MCT) detector. The catalyst powder was mixed with KBr (Wako). The weight ratio of the catalyst to KBr was 0.2. The obtained mixture (*ca.* $9 \text{ mg}_{\text{cat}} \text{ cm}^{-2}$) were pressed into a thin self-supporting disk and set in the cell, heated at 330°C for 30 min under vacuum, and cooled down to 205°C under vacuum. Then, background spectra were collected at 205°C . The samples were exposed to methanol vapor (10 kPa) for 5 min at 205°C . Afterward, the methanol vapor was evacuated for 5 min at 205°C . Typically, 20 scans were collected for 1 spectrum, and the results were presented as absorbance spectra.

In **Figure S11**, three peaks are observed at 1150, 1055, and 1030 cm^{-1} . According to the reports³⁻⁴, the peak at 1150 cm^{-1} is attributed to on-top methoxy species on Zr^{4+} . The peaks at 1055 cm^{-1} and 1030 cm^{-1} are related to doubly bridging methoxy species on Zr^{4+} . On **ACE-500**, doubly bridging methoxy species were only observed, indicating that most of the surface methoxy species was strongly bounded on ZrO_2 . On **ACE-350**, on the other hand, one-top and doubly bridging methoxy species are detected by FTIR. Assuming that a peak area is proportional to the population of the corresponding species, the on-top methoxy species is greater than the doubly bridging methoxy species. Therefore, methoxy species on **ACE-350** adsorbed more weakly on ZrO_2 than that on **ACE-500**.

References

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