## Supporting Information

## Facile Design of Highly Effective CuCe<sub>x</sub>Co<sub>1-x</sub>O<sub>y</sub> Catalysts with Diverse Surface/Interface Structures towards NO Reduction by CO at Low Temperatures

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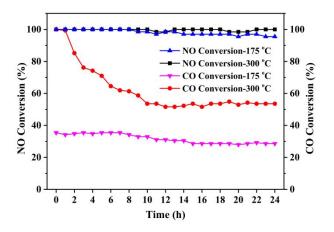
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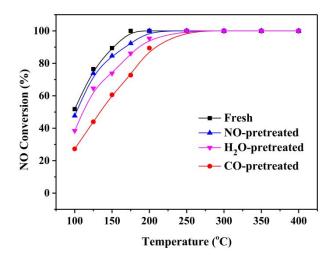
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**Figure S1.** The stability test of  $CuCe_{0.2}Co_{0.8}O_y$  catalyst at 175 °C and 300 °C for 24 h. Reaction condition: 1000ppm NO, 2000ppm CO, He balance, GHSV = 50,000 h<sup>-1</sup>.



**Figure S2.** NO conversion of  $CuCe_{0.2}Co_{0.8}O_y$  catalyst pretreated under 5000 ppm CO, 5000 ppm NO and 10 % H<sub>2</sub>O/He steam at 200 °C. Reaction condition: 1000ppm NO, 2000ppm CO, He balance, GHSV = 50,000 h<sup>-1</sup>.

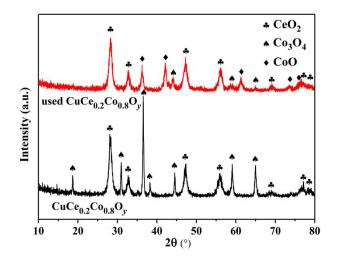
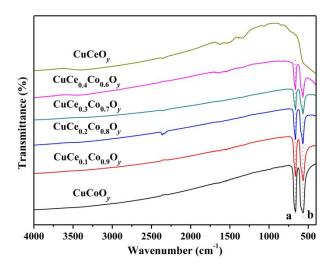
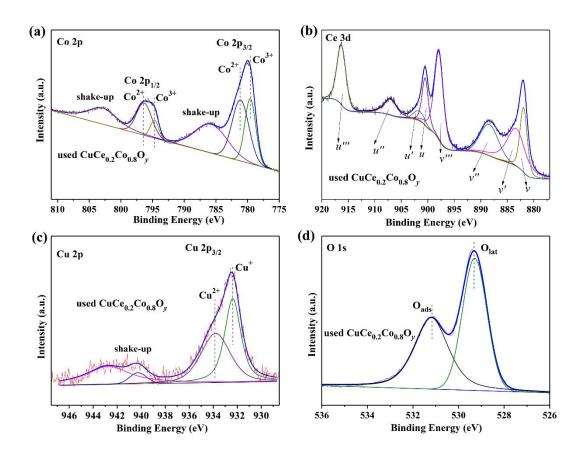


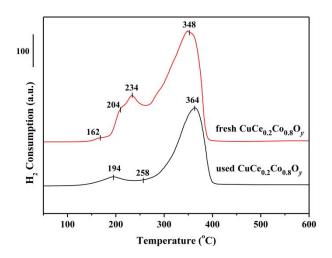
Figure S3. XRD patterns of fresh and used  $CuCe_{0.2}Co_{0.8}O_y$  catalysts.



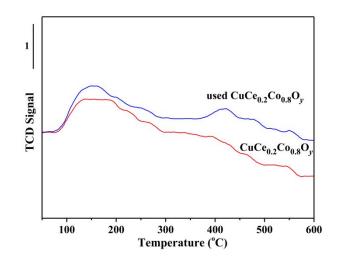
**Figure S4.** FT-IR spectra of  $CuCe_xCo_{1-x}O_y$  catalysts.



**Figure S5.** XPS profiles of (a) Co 2p, (b) Ce 3d, (c) Ce 3d and (d) O 1s of used  $CuCe_xCo_{1-x}O_y$  catalysts.



**Figure S6.** H<sub>2</sub>-TPR profiles of fresh and used  $CuCe_{0.2}Co_{0.8}O_y$  catalyst.



**Figure S7.** CO-TPD profile of fresh and used  $CuCe_{0.2}Co_{0.8}O_y$  catalyst.

Catalysts	Reaction condition	NO conversion	Reference
$CuCe_{0.2}Co_{0.8}O_y$	1000 ppm NO, 2000 ppm CO, He balance, $GHSV = 50,000 \text{ h}^{-1}$	175 °C, 100 %	This work
Fe-Co/ASC	1000 ppm NO, 2000 ppm CO, N <sub>2</sub> balance, GHSV = $6000 \text{ h}^{-1}$	175 °C, 70 %	1
Cu/MCM-41	250 ppm NO, 750 ppmCO, Flow rate = 80 mL/min	350 °C, 23 %	2
4% Cu/Fe-Ce	800 ppm NO, 1600 ppm CO, N <sub>2</sub> balance, GHSV = 30,000 h <sup>-1</sup>	175 °C, 100 %	3
Cu-Ce/CNTs	250 ppm NO, 5000 ppm CO, He balance, GHSV = 12,600 h <sup>-1</sup>	175 °C, 70 %	4
Al(Cu+Co+Ce)	1200 ppm NO, 1200 ppm CO, GHSV = 26,000 h <sup>-1</sup>	175 °C, 65 %	5
CuO/Ce <sub>0.2</sub> Ti <sub>0.8</sub> O <sub>2</sub>	6.0% NO, 6.0% CO, He balance, GHSV = $5000 \text{ h}^{-1}$	175 °C, 45 %	6
Cu/CeO <sub>2</sub>	5% NO, 10% CO, He balance, GHSV = 36,000 h <sup>-1</sup>	175 °C, 83 %	7
CuO-CoO <sub>x</sub> / $\gamma$ -Al <sub>2</sub> O <sub>3</sub>	2.5% NO, 5% CO, He balance, GHSV = 12,000 mL $\Box$ g <sup>-1</sup> $\Box$ h <sup>-1</sup>	175 °C, 30 %	8
Cu-Fe/CNTs	5% NO, 10 % CO, He balance, GHSV = $60,000 \text{ h}^{-1}$	175 °C, 55 %	9
CuO-MnO <sub>x</sub> /TiO <sub>2</sub>	5% NO, 10% CO, He balance, GHSV = 12,000 h <sup>-1</sup>	200 °C, 13 %	10

**Table S1.** Comparison of NO conversion for NO reduction by CO over different catalysts.

## References

(1) Wang, L.; Cheng, X.; Wang, Z.; Ma, C.; Qin, Y., Investigation on Fe-Co binary metal oxides supported on activated semi-coke for NO reduction by CO. *Appl. Catal., B* **2017,** 201, 636.

(2) Patel, A.; Shukla, P.; Rufford, T. E.; Rudolph, V.; Zhu, Z., Selective catalytic reduction of NO with CO using different metal-oxides incorporated in MCM-41. *Chem. Eng. J.* **2014**, 255, 437.

(3) Cheng, X.; Zhang, X.; Su, D.; Wang, Z.; Chang, J.; Ma, C., NO reduction by CO over copper catalyst supported on mixed CeO<sub>2</sub> and Fe<sub>2</sub>O<sub>3</sub>: Catalyst design and activity test. *Appl. Catal.*, *B* **2018**, 239, 485.

(4) Gholami, Z.; Luo, G., Low-Temperature Selective Catalytic Reduction of NO by CO in the Presence of O<sub>2</sub> over Cu:Ce Catalysts Supported by Multiwalled Carbon Nanotubes. *Ind. Eng. Chem. Res.* **2018**, 57, 8871.

(5) Spassova, I.; Velichkova, N.; Nihtianova, D.; Khristova, M., Influence of Ce addition on the catalytic behavior of alumina-supported Cu-Co catalysts in NO reduction with CO. *J. Colloid Interface Sci.* **2011**, 354, 777.

(6) Jiang, X.; Huang, W.; Li, H.; Zheng, X., Catalytic Properties of  $CuO/Ce_{0.2}Ti_{0.8}O_2$  and  $CuO/Ce_{0.5}Ti_{0.5}O_2$  in the NO + CO Reaction. *Energy Fuels* **2010**, 24, 261.

(7) Yao, X. J.; Gao, F.; Yu, Q.; Qi, L.; Tang, C. J.; Dong, L.; Chen, Y., NO reduction by CO over CuO-CeO<sub>2</sub> catalysts: effect of preparation methods. *Catal. Sci. Technol.* **2013**, 3, 1355.

(8) Zhang, L.; Yao, X.; Lu, Y.; Sun, C.; Tang, C.; Gao, F.; Dong, L., Effect of precursors on the structure and activity of CuO-CoO<sub>x</sub>/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalysts for NO reduction by CO. *J. Colloid Interface Sci.* **2018**, 509, 334.

(9) Dasireddy, V. D. B. C.; Likozar, B., Selective catalytic reduction of NO<sub>x</sub> by CO over bimetallic transition metals supported by multi-walled carbon nanotubes (MWCNT). *Chem. Eng. J.* **2017**, 326, 886.

(10) Sun, C.; Tang, Y.; Gao, F.; Sun, J.; Ma, K.; Tang, C.; Dong, L., Effects of different manganese precursors as promoters on catalytic performance of CuO-MnO<sub>x</sub>/TiO<sub>2</sub> catalysts for NO removal by CO. *Phys. Chem. Chem. Phys.* **2015**, 17, 15996.