

Supporting Information

Evolution of Pd Species for the Conversion of Methane under Operation Conditions

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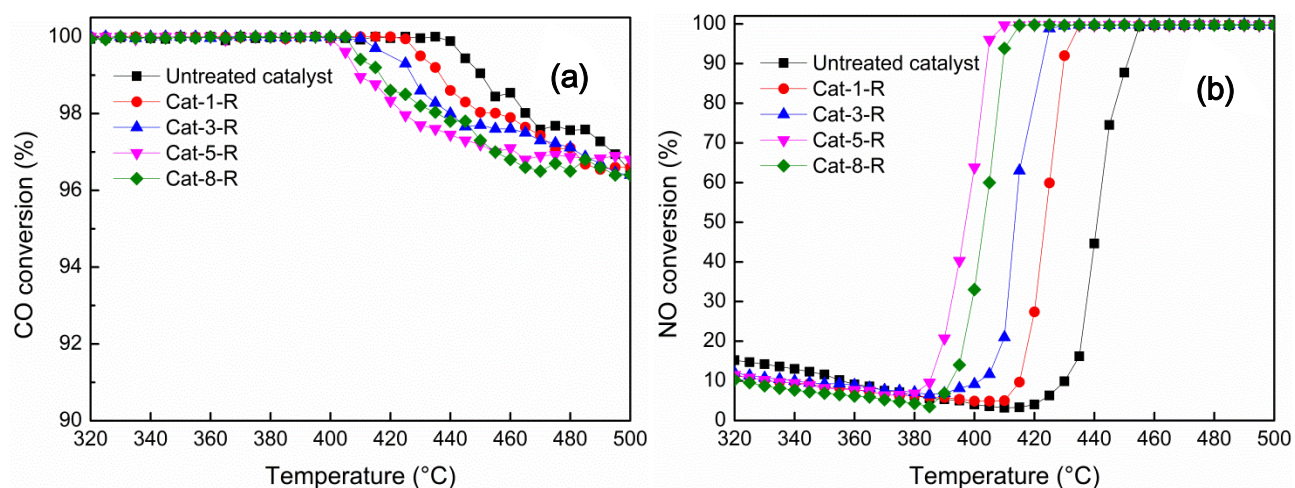


Figure S1. (a) CO and (b) NO light-off curves as temperature was raised from 300 to 500 °C in simulated stoichiometric NGVs exhaust gas for the Pd model catalyst (50 g/ft³) after pretreated in reaction gas. Conditions: 1000 ppm CH₄ + 5000 ppm CO + 930 ppm NO + 4035 ppm O₂ + 10vol. %CO₂ + 10vol. %H₂O balanced with N₂ (lambda=1); Gas hourly space velocity (GHSV) = 50,400 h⁻¹.

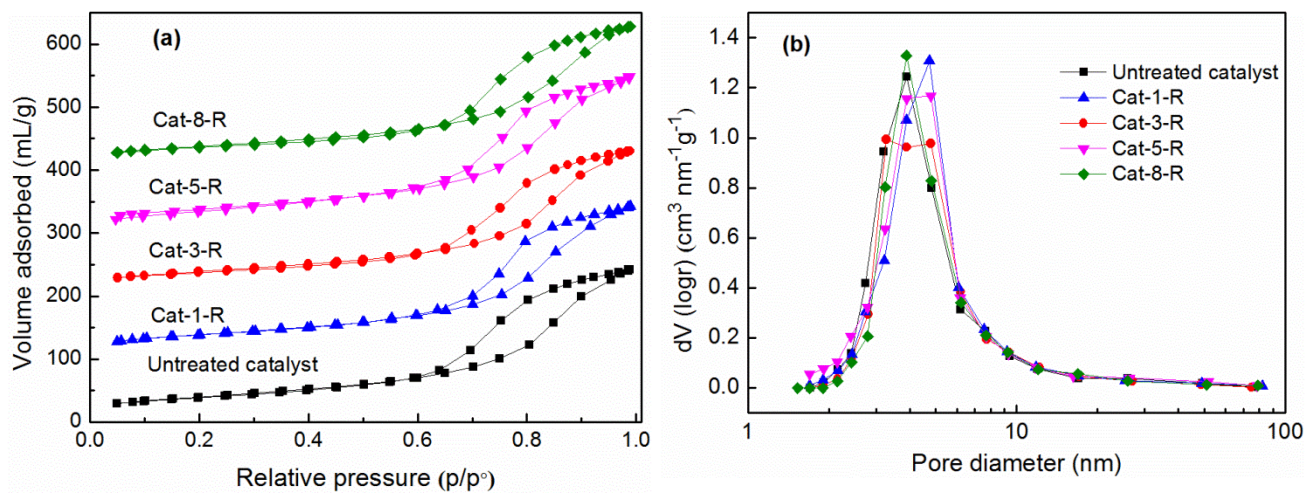


Figure S2. (a) Nitrogen adsorption-desorption isotherms and (b) Barrett-Joyner-Halenda

pore size distribution of the Pd model catalysts after pretreatment in reaction gas.

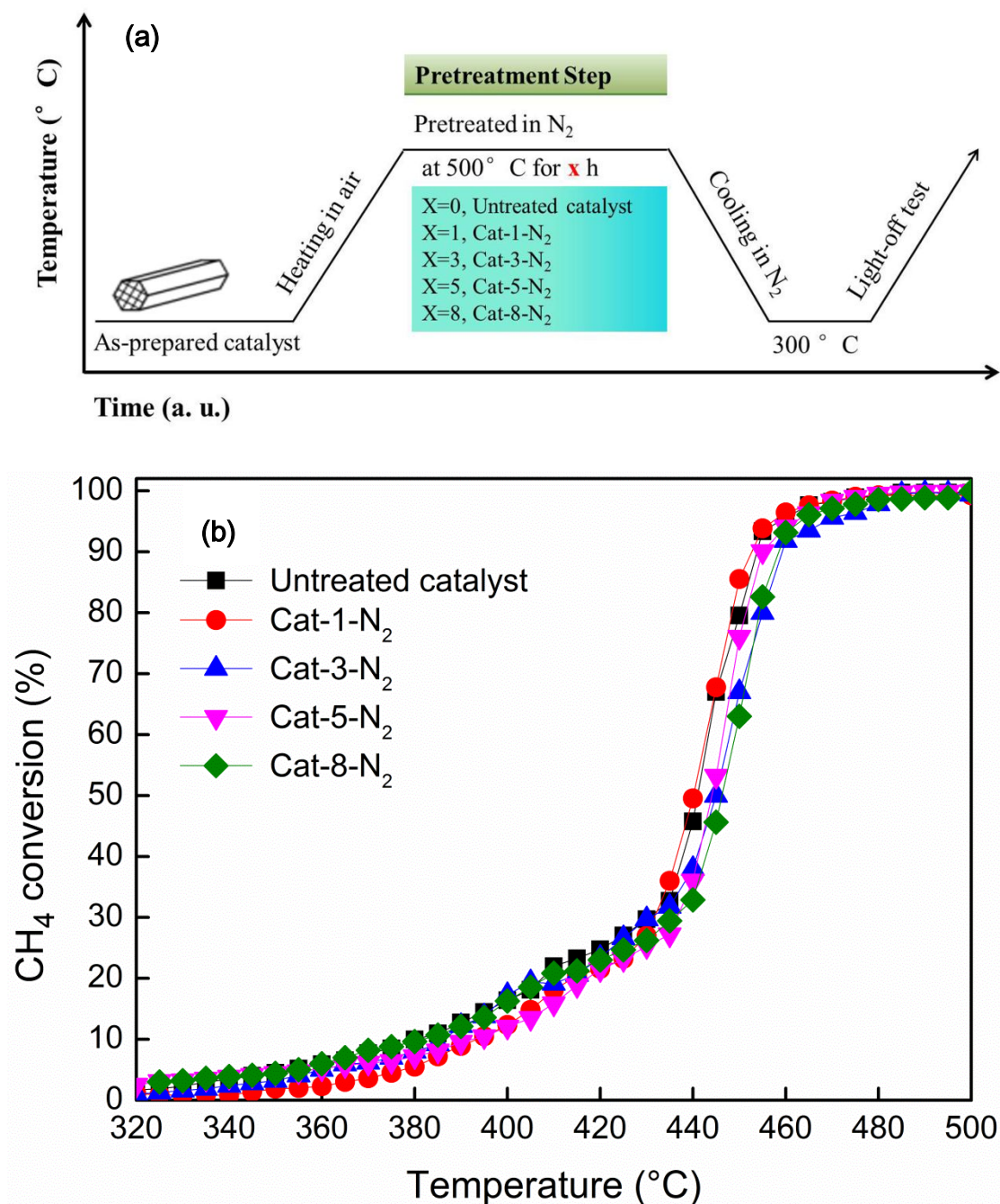


Figure S3. (a) Description of the pretreatment procedures under flowing N_2 ; (b) CH_4

light-off test for Pd model catalyst (50 g/ft^3) after the above pretreatment.

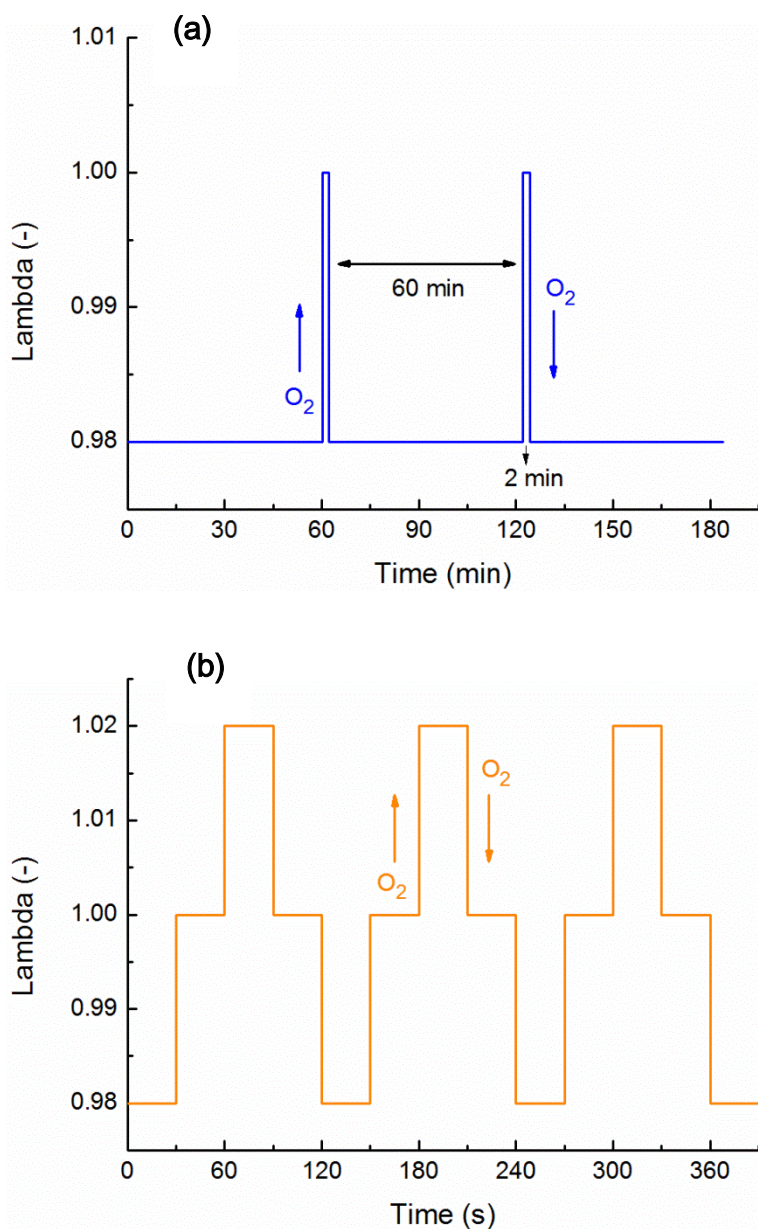


Figure S4. (a) Periodic pulse experiments were conducted by performing every 2 min long stoichiometric pulses ($\lambda=1.00$) per 60 min on a stationary rich reaction gas mixture ($\lambda=0.98$); (b) Lambda oscillating operating tests: lambda oscillation value from 0.98 to 1.02 at constant cycle period of 120 s.

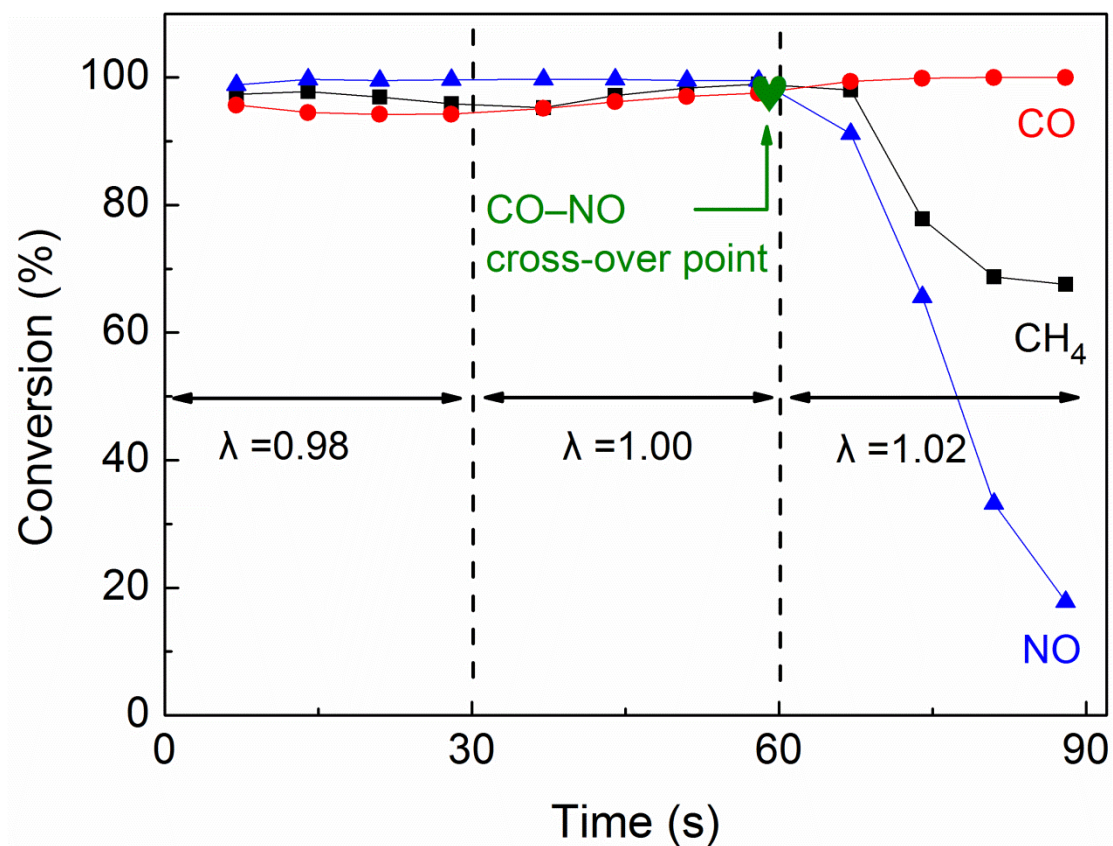


Figure S5. The changes in the pollutants conversion with lambda over the pretreated catalyst ($T_{\text{oven}} = 450\text{ }^{\circ}\text{C}$). The time shown in the Figureure is corresponding to that in Figure. 11. The green heart-shaped point indicates the CO-NO crossover point, also indicated by a green arrow.

Table S1. Texture properties of the Pd model catalysts after pretreatment in reaction gas.

Samples	BET area (m ² /g)	Pore volume (mL/g)	Mean pore radii (nm)
Untreated catalyst	142.8	0.37	5.3
Cat-1-R	138.7	0.37	5.4
Cat-3-R	139.1	0.36	5.1
Cat-5-R	137.6	0.38	5.6
Cat-8-R	134.9	0.35	5.2