

## Supporting Information

### **Fine tuning the diffusion length in hierarchical ZSM-5 to maximize the yield of propylene in catalytic cracking of hydrocarbons**

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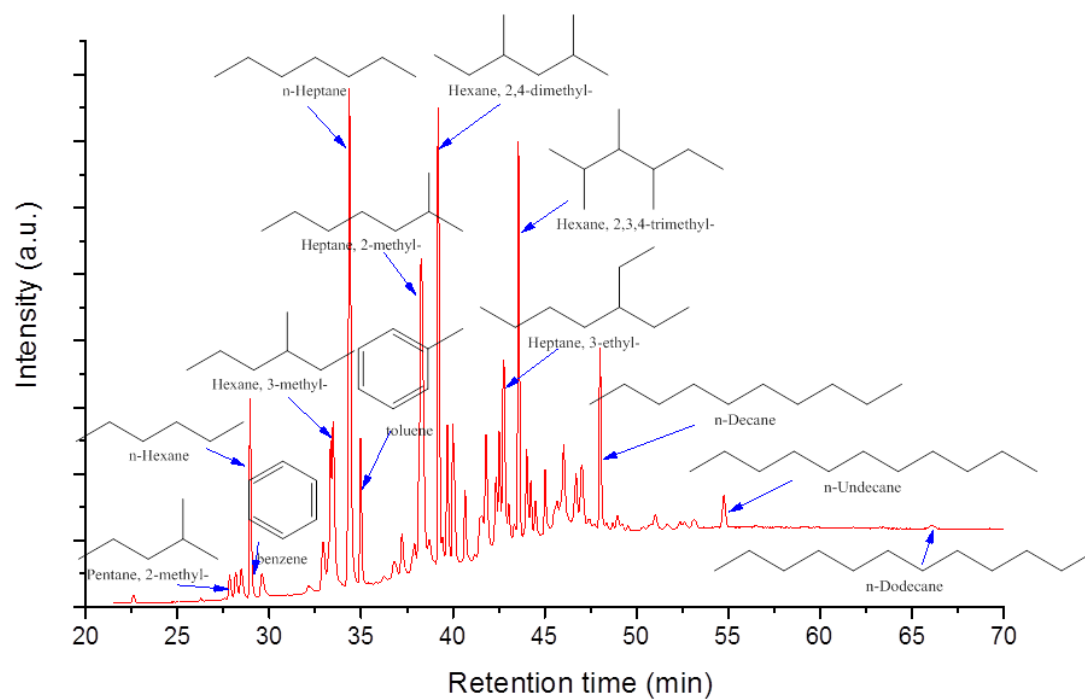


Fig. S1. Analysis of Full Range Naphtha by GC/MS. Conditions: HP-PLOTQ column, Carrier gas: Helium, column flow: 7.24 ml/min. Temperature Program: 60 °C hold for 5 min, ramp 50 to 260 at 5 °C /min, 260 °C hold for 40min.

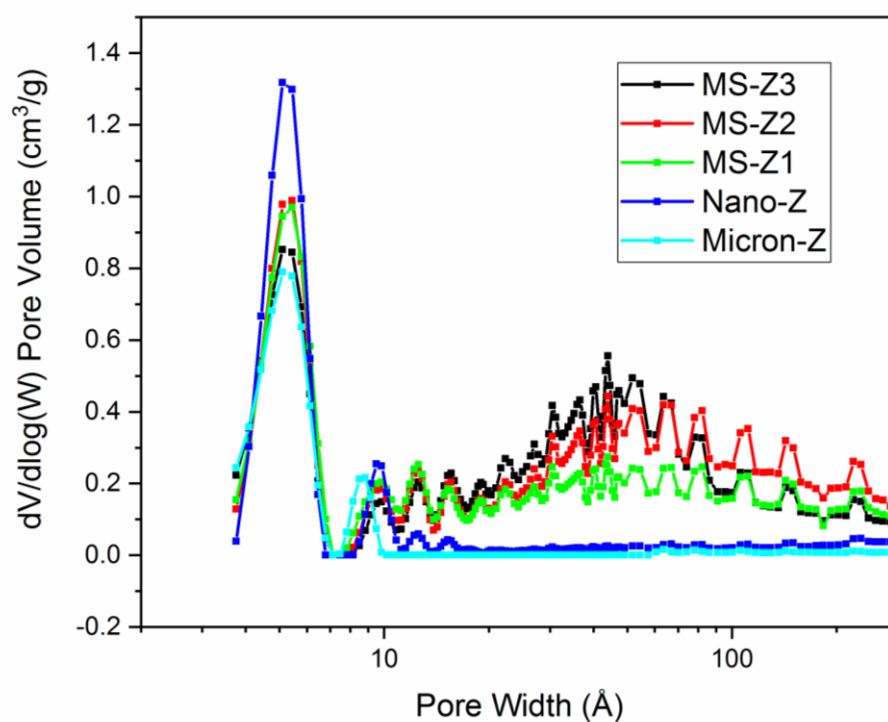


Fig. S2. Pore size distributions of the catalysts studied.

Table S1 Conversion of cumene and 1,3,5-Triisopropylbenzene (TIPB) over MS-Z3, MS-Z2, MS-Z1, Nano-Z and Micron-Z catalysts at 400 °C, TOS=10 min.

| Conversion (wt %) | Catalysts |       |       |        |          |
|-------------------|-----------|-------|-------|--------|----------|
|                   | MS-Z3     | MS-Z2 | MS-Z1 | Nano-Z | Micron-Z |
| Cumene            | 45.5      | 44.6  | 39.8  | 29.8   | 17.2     |
| TIPB              | 36.1      | 35.8  | 20.5  | 7.4    | 1.9      |

Table S2 Selectivity (wt%) of products from catalytic cracking of n-decane over different catalysts at iso-conversion (71~75wt%) at 550 °C, TOS=5min.

| Products                                                                               | Catalysts |       |       |        |          |
|----------------------------------------------------------------------------------------|-----------|-------|-------|--------|----------|
|                                                                                        | MS-Z3     | MS-Z2 | MS-Z1 | Nano-Z | Micron-Z |
| WHSV ( $\text{g}_{\text{Feed}} \cdot \text{g}_{\text{Cat}}^{-1} \cdot \text{h}^{-1}$ ) | 36        | 36    | 54    | 108    | 108      |
| Conversion (wt %)                                                                      | 71.0      | 74.0  | 70.9  | 73.2   | 75.0     |
| Selectivity (wt %)                                                                     |           |       |       |        |          |
| Methane                                                                                | 0.9       | 0.8   | 0.7   | 0.6    | 0.8      |
| Ethylene                                                                               | 9.6       | 10    | 9.5   | 7.4    | 6.7      |
| Ethane                                                                                 | 3.8       | 3.7   | 3.2   | 2.6    | 3.0      |
| Propylene                                                                              | 24.7      | 24.1  | 22.6  | 17.6   | 14.6     |
| Propane                                                                                | 14.4      | 16.1  | 16.2  | 19.4   | 22.3     |
| Butenes                                                                                | 17.5      | 15.7  | 16.3  | 16.0   | 14.2     |
| Butane                                                                                 | 7.3       | 7.6   | 8.6   | 11.2   | 11.9     |
| Benzene                                                                                | 3.9       | 3.4   | 3.4   | 2.9    | 2.1      |
| Toluene                                                                                | 0.5       | 0.7   | 0.6   | 0.7    | 1.3      |
| Xylenes                                                                                | 1.9       | 2.6   | 2.5   | 3.1    | 5.6      |
| Others                                                                                 | 13.0      | 13.2  | 12.0  | 13.6   | 11.8     |
| Coke                                                                                   | 2.4       | 2.1   | 4.4   | 4.7    | 5.6      |

Table S3 Properties of Arabian Light.

| Property                             | Value  |
|--------------------------------------|--------|
| Density (g/cm <sup>3</sup> ) (15 °C) | 0.8658 |
| Sulfur (wt%)                         | 1.9    |
| Nitrogen (ppm)                       | 660    |
| Vanadium (ppm)                       | 13     |
| Nickel (ppm)                         | 5      |
| Residue (wt%)                        | 4.0    |
| Simulated Distillation (°C)          |        |
| Initial boiling point                | 34     |
| 50%                                  | 363    |
| End boiling point                    | 773    |

Table S4 Cracking of Arabian Light over different catalysts at 600 °C, TOS=5min.

| Products                        | Catalysts   |             |             |            |            |
|---------------------------------|-------------|-------------|-------------|------------|------------|
|                                 | MS-Z3       | MS-Z2       | MS-Z1       | Nano-Z     | Micron-Z   |
| Yield (wt %)                    |             |             |             |            |            |
| Methane                         | 3.3         | 3.9         | 3.2         | 3.3        | 3.8        |
| Ethylene                        | 11.5        | 10.5        | 9.8         | 9.7        | 6.7        |
| Ethane                          | 4.4         | 4.0         | 4.2         | 4.3        | 4.3        |
| <b>Propylene</b>                | <b>15.0</b> | <b>13.9</b> | <b>11.4</b> | <b>9.8</b> | <b>5.7</b> |
| Propane                         | 5.9         | 5.6         | 5.4         | 5.6        | 4.5        |
| Butenes                         | 5.9         | 5.9         | 4.6         | 3.8        | 2.1        |
| Butanes                         | 1.8         | 1.8         | 1.6         | 1.4        | 0.8        |
| Light olefins                   | 32.4        | 30.2        | 25.7        | 23.3       | 14.5       |
| Total gas                       | 47.8        | 45.5        | 40.1        | 37.8       | 27.9       |
| Selectivity in gas phase (wt %) |             |             |             |            |            |
| Ethylene                        | 24.1        | 23.1        | 24.4        | 25.8       | 23.9       |
| Propylene                       | 31.3        | 30.5        | 28.7        | 25.8       | 20.6       |