Supporting Information for

Rational Design of High-Performance Continuous-Flow Microreactors Based on Gold Nanoclusters and Graphene for Catalysis

Yanbiao Liu^{a,c,d*}, Xiang Liu^a, Shengnan Yang^a, Fang Li^{a,c}, Chensi Shen^{a,c}, Manhong Huang^{a,c}, Junjing Li^d, Ricca Rahman Nasaruddin^b, Jianping Xie^{b*}

^a Textile Pollution Controlling Engineering Center of Ministry of Environmental Protection, College of Environmental Science and Engineering, Donghua University,
2999 North Renmin Road, Shanghai 201620, P. R. China. E-mail: yanbiaoliu@dhu.edu.cn; Fax: +86 21 6779 2522; Tel: +86 21 6779 8752.

^b Department of Chemical and Biomolecular Engineering, National University of Singapore, 4 Engineering Drive 4, 117585 Singapore, E-mail: <u>chexiej@nus.edu.sg</u>; Fax:
+65 6516 1936; Tel: +65 6516 1067.

^c Shanghai Institute of Pollution Control and Ecological Security, 1239 Siping Road, Shanghai 200092, P. R. China.

^d State Key Laboratory of Separation Membranes and Membrane Processes, Tianjin Polytechnic University, 399 Binshuixi Avenue, Tianjin 300387, P. R. China.

Supporting Information: 1 table and 14 figures.

Real water sample	CODcr	pН	Conductivity	TDS
tap water	<25 mg/L	7.2	569.3 s/cm	287.4mg/L
surface water	84 mg/L	8.2	676.5	337.1 mg/L
			s/cm	
alkali-decrement wastewater	37600 mg/L	13.6	90.36 ms/cm	45.0 g/L
(diluted by 1000 times before use)				

 Table S1. Characteristics of three real water samples.

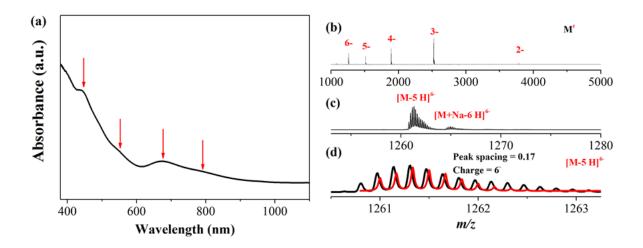


Figure S1. (a) UV-vis absorption spectra and (b-d) ESI mass spectra of the assynthesized Au₂₅(MHA)₁₈ clusters. M in (b-d) denotes Au₂₅(MHA)₁₈ and the red line in (d) is the simulated isotope pattern of $[Au_{25}(MHA)_{18} - 5H]^{6-}$.

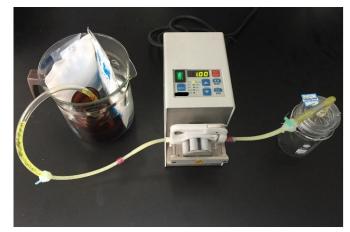


Figure S2. Experimental setup for the continuous flow catalytic reaction.

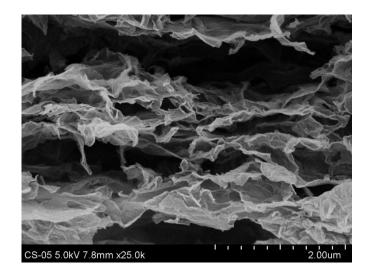


Figure S3. FESEM image of cross-sectional analysis of the AuNC/4h-rGO catalytic membranes at high magnification, indicating the presence of nanochannels that are permeable to fluid.

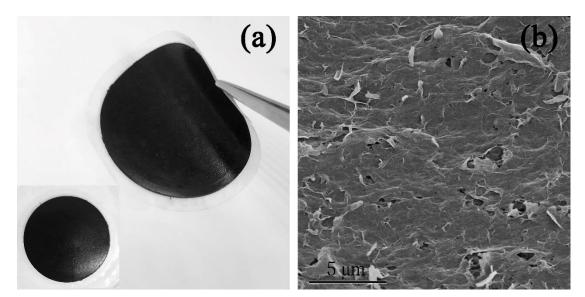


Figure S4. Photograph (a), FESEM image (b) of the AuNC/rGO membrane.

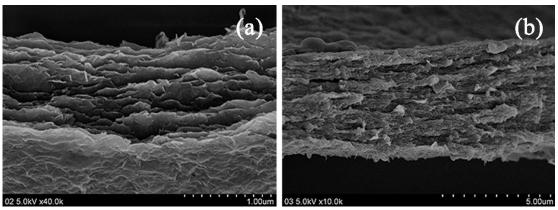


Figure S5. FESEM images for cross sectional analysis of the as-fabricated AuNC/4h-

rGO hybrid catalytic membrane: 5 mg rGO (left) and 10 mg rGO (right).

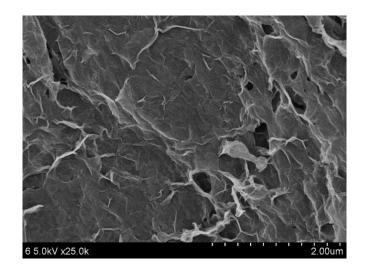


Figure S6. FESEM image of a typical rGO membrane.

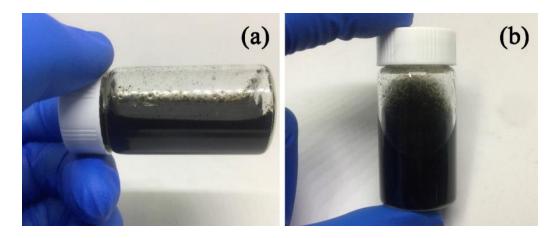


Figure S7 (a) Digital picture of a 10h-rGO in DI-H₂O after 2 h continuous ultrasonication; (b) Digital picture of a 20h-rGO in AuNC solution after 2 h continuous ultrasonication.

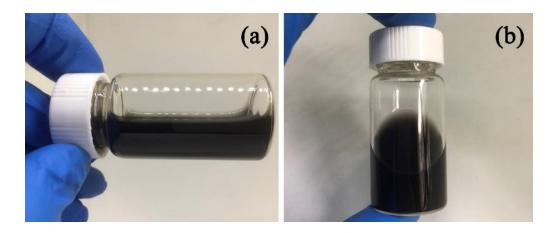


Figure S8. Digital picture of a 4h-rGO in AuNC solution after 20 min ultrasonication

treatment.

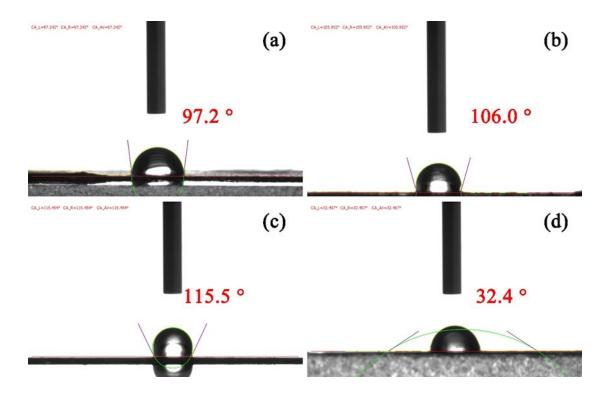


Figure S9. Measurement of static contact angle of a water drop on rGO membrane surface with 4 h (a), 10 h (b), and 20 h (c) hydrothermal treatment. (d) The profile of a water drops on the AuNC/4h-rGO membrane (with 10 mol Au loading).

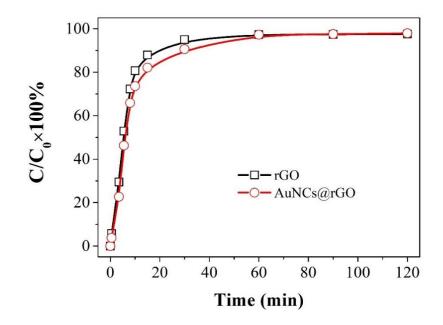


Figure S10. Breakthrough curves of rGO membrane and AuNC/4h-rGO membrane of

4-NP only.

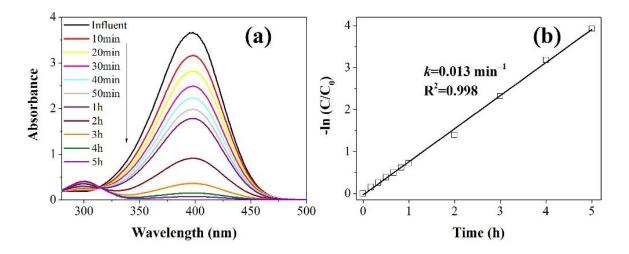


Figure S11. (a) Time-dependent UV-vis adsorption spectra and (b) The reaction kinetics for the conversion of 4-NP in a batch reactor using AuNC/4h-rGO catalytic membrane.

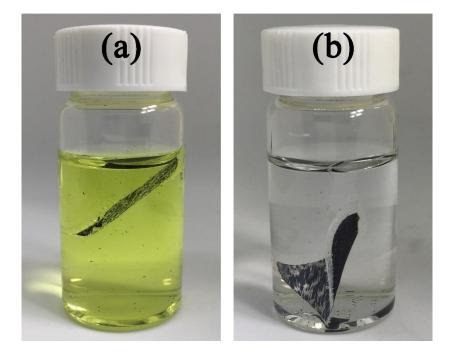


Figure S12. Digital photos of the batch reactor (a, at the beginning; b, after 5 h reaction) towards the conversion of 4-nitrophenol using the AuNC/4h-rGO hybrid membrane.

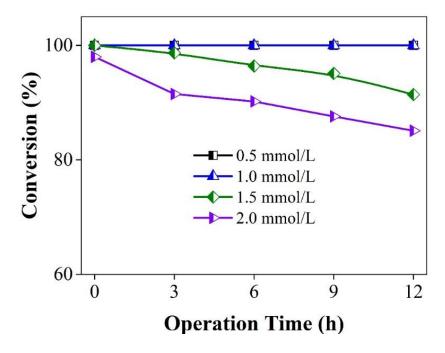


Figure S13. The effect of operation time and 4-NP concentration on the catalytic performance of an AuNC/4h-rGO membrane.

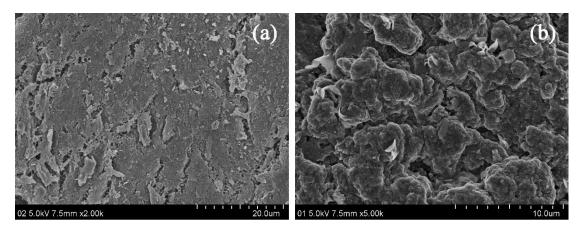


Figure S14. FESEM images of the AuNC/4h-rGO catalytic membrane after 12 h continuous operation (at different magnifications).