

Supporting Information Paragraph

Hydrotreating performance of FCC diesel and Dibenzothiophene over NiMo supported zirconium modified Al-TUD-1 catalysts

Bo Wang[†], Chengkun Xiao[†], Pengfei Li, Zhenshan Zhao, Chunming Xu, Zhen Zhao, Qian Meng, Jianmei Li, Aijun Duan*, Zhentao Chen*

¹State Key Laboratory of Heavy Oil Processing, China University of Petroleum, Beijing, 102249, P. R. China

[[†]] These authors contributed equally to this work

*Corresponding author: duanaijun@cup.edu.cn; czt@cup.edu.cn

Figure & Table Captions

Figure S1. Wide-angle XRD pattern of AT-x and γ -Al₂O₃ material.

Figure S2. (A) the nitrogen adsorption-desorption isotherms and (B) pore diameter distribution of Al-TUD-1 series materials.

Figure S3. TEM image of AT (A) and ZrAT-25 (B).

Figure S4. Wide-angle XRD patterns of NiMo/ZrAT-x and NiMo/ZrO₂ catalysts.

Figure S5. N₂ isotherm curves (A) and pore size distributions (B) of NiMo/ZrAT-x catalysts.

Figure S6. EDX characterizations of (A) NiMo/ZrAT-25 and (B) NiMo/AT catalysts.

Figure S7. Zr3d XPS spectra of (A) NiMo/ZrAT-5, (B) NiMo/ZrAT-10, (C) NiMo/ZrAT-25, (D) NiMo/ZrAT-50, (E) NiMo/ZrAT-100, (F) NiMo/ZrAT-25 sulfided catalysts.

Figure S8. The pyridine IR spectra of (a) NiMo/AT, (b) NiMo/ZrAT-100, (c) NiMo/ZrAT-50, (d) NiMo/ZrAT-25, (e) NiMo/ZrAT-10, and (f) NiMo/ZrAT-5 after degassing at (A) 473 K and (B) 623 K.

Figure S9. The phase equilibrium image of decalin under the reaction conditions.

Figure S10. HDS results of NiMo/ZrAT-5 and NiMo/Al₂O₃ catalysts at different WHSVs (613 K, 6 MPa, 200 ml/ml).

Figure S11. The product distribution in the HDS of DBT over NiMo/ZrAT-100 at different WHSVs (573 K, 6 MPa, 200 ml/ml).

Figure S12. The product distribution in the HDS of DBT over NiMo/ZrAT-100 at different temperatures (100 h⁻¹, 6 MPa, 200 ml/ml).

Figure S13. The product distributions in the HDS of DBT over different catalysts at about 50 % of the total DBT conversion..

Figure S14. N₂ isotherm curves (A) and pore size distributions (B) of the used NiMo/ZrAT-x catalysts.

Figure S15. Time on stream over NiMo/ZrAT-100 and NiMo/AT catalysts (573 K, 6 MPa, 200 ml/ml).

Figure S16. HDS efficiencies of NiMo/ZrAT-100 obtained at 6-run operations (20 h⁻¹, 573 K, 6 MPa, 200 ml/ml)

Table S1. Textural properties of Al-TUD-1 series materials with different heating times.

Table S2. Textural properties of the NiMo/ZrAT-x catalysts.

Table S3. XPS fitting results of Mo 3d spectra of the sulfided catalysts.

Table S4. XPS fitting results of Ni 2p spectra of the sulfided catalysts.

Table S5. Average length and average layer number of MoS₂ crystallites.

Table S6. The amounts of Brönsted and Lewis acid determined by pyridine-FT-IR of the different catalysts.

Table S7. The typical property of diesel feedstock.

Table S8. Textual properties of NiMo/ γ -Al₂O₃ catalyst.

Table S9. Acid properties of NiMo/ γ -Al₂O₃ catalyst.

Table S10. HDS activities of NiMo/ZrAT-x series catalysts.

Table S11. Textural properties of the used NiMo/ZrAT-x catalysts.

S1. XRD of AT-x material with different thermal treatment times

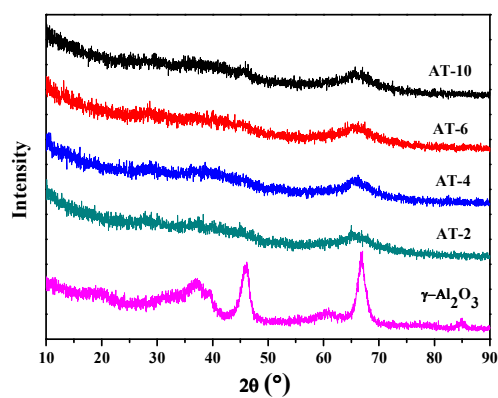


Figure S1. Wide-angle XRD pattern of AT-x and $\gamma\text{-Al}_2\text{O}_3$ material

S2. BET characterization of AT-x material with different thermal treatment times

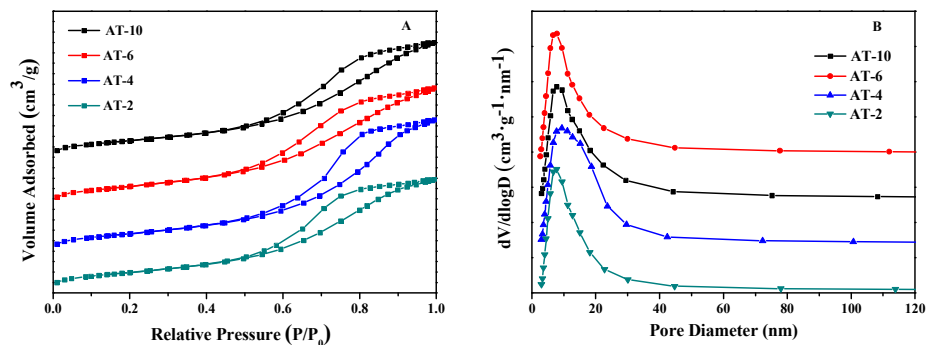


Figure S2. (A) the nitrogen adsorption-desorption isotherms and (B) pore diameter distribution of Al-TUD-1 series materials

Table S1. Textural properties of Al-TUD-1 series materials with different heating times

Materials	S_{BET} (m ² g ⁻¹)	V_{BJH} (cm ³ g ⁻¹)	Pore diameter (nm)
AT-10h	381	0.82	7.4
AT-6h	403	0.82	8.2
AT-4h	409	0.86	9.6
AT-2h	396	0.76	7.2

S3. TEM characterization of ZrAT-x materials

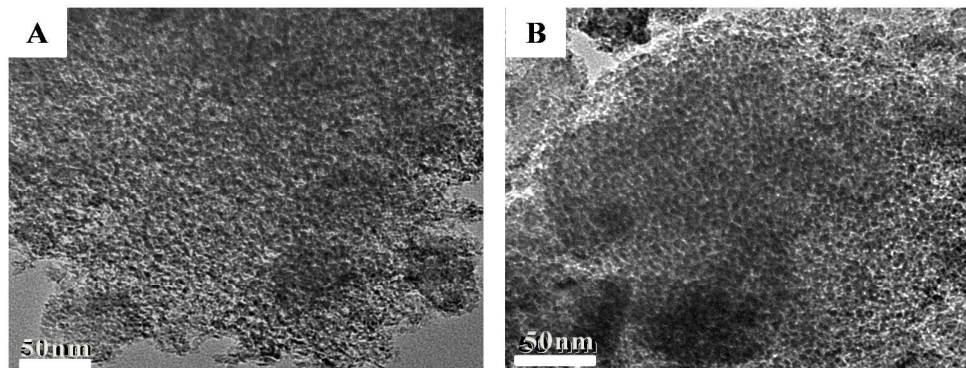


Figure S3. TEM image of AT (A) and ZrAT-25 (B)

S4. Wide-angle XRD characterization of NiMo/ZrAT-x catalysts

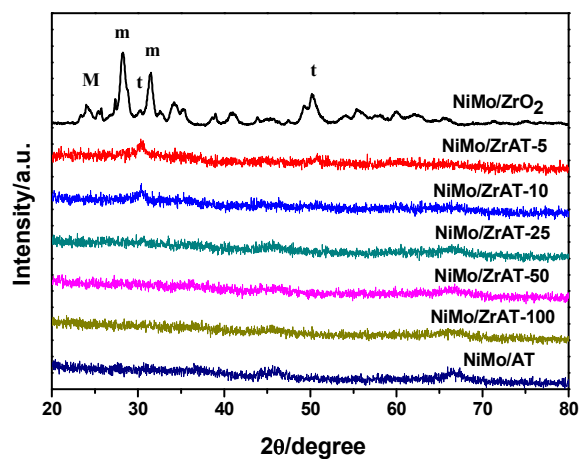


Figure S4. Wide-angle XRD patterns of NiMo/ZrAT-x and NiMo/ZrO₂ catalysts

S5. BET characterization of NiMo/ZrAT-x catalysts

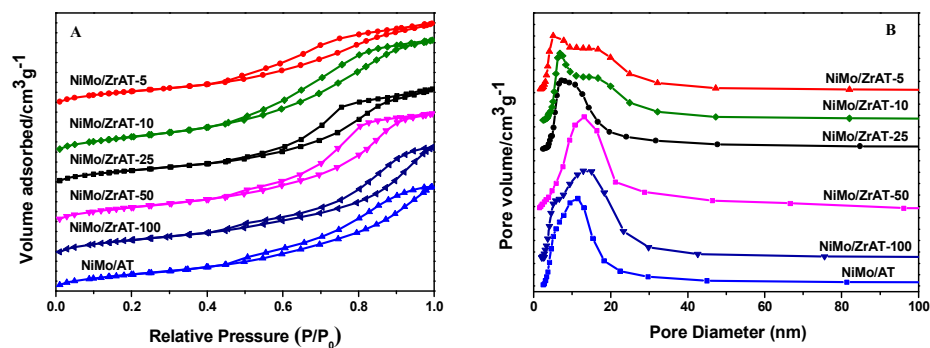


Figure S5. N₂ isotherm curves (A) and pore size distributions (B) of NiMo/ZrAT-x catalysts

Table S2. Textural properties of the NiMo/ZrAT-x catalysts

Materials	Weight percentage of ZrO ₂ (%)	Al/Zr	S _{BET} (m ² g ⁻¹)	V _{BJH} (cm ³ g ⁻¹)	Pore diameter (nm)
NiMo/ZrAT-5	32.6	5	221	0.29	8.5
NiMo/ZrAT-10	18.5	10	237	0.33	9.5
NiMo/ZrAT-25	8.8	25	252	0.38	12.8
NiMo/ZrAT-50	4.6	50	264	0.40	14.5
NiMo/ZrAT-100	2.4	100	268	0.41	15.9
NiMo/AT	0	∞	266	0.47	13.4

S6. SEM-EDS

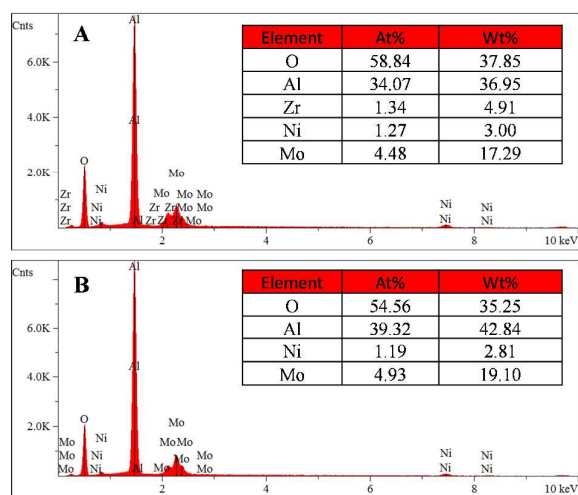


Figure S6. EDX characterizations of (A) NiMo/ZrAT-25 and (B) NiMo/AT catalysts

S7. XPS

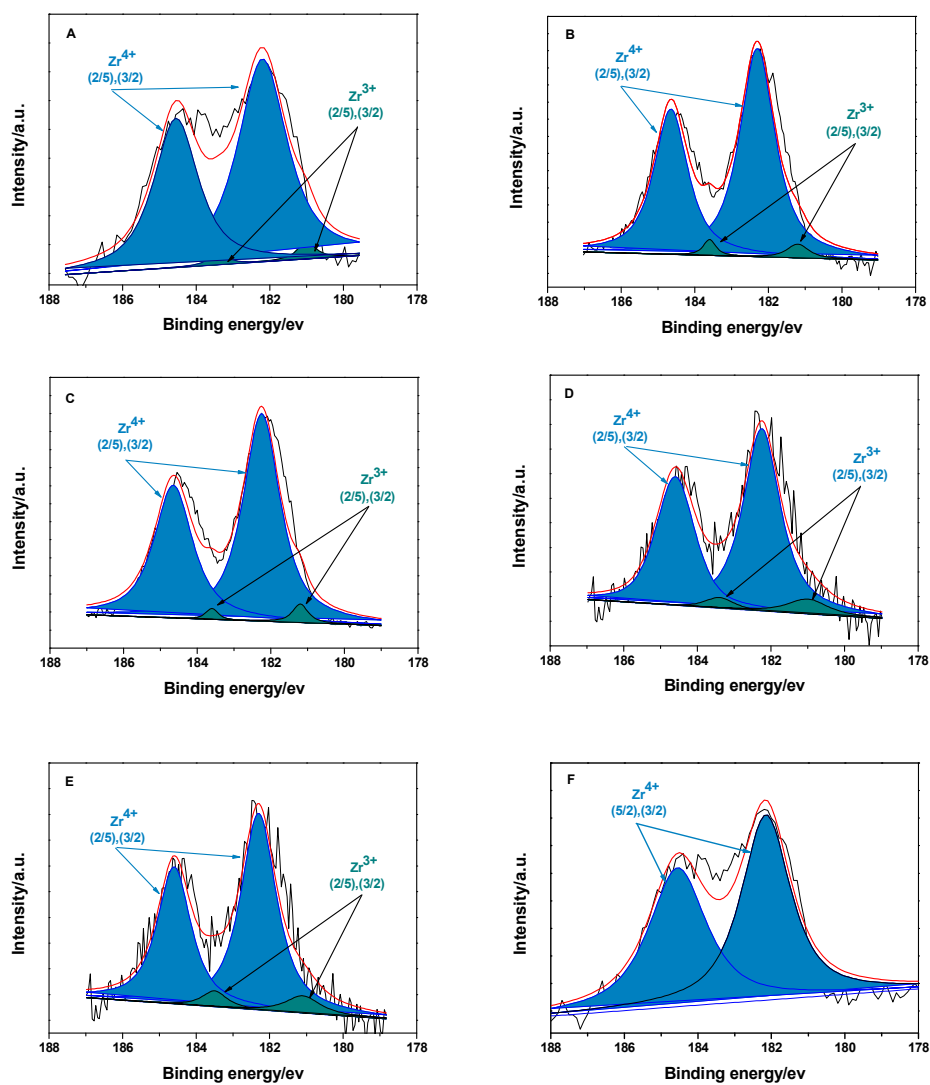


Figure S7. Zr3d XPS spectra of (A) NiMo/ZrAT-5, (B) NiMo/ZrAT-10, (C) NiMo/ZrAT-25, (D) NiMo/ZrAT-50, (E) NiMo/ZrAT-100, (F) NiMo/ZrAT-25 sulfided catalysts

Table S3. XPS fitting results of Mo 3d spectra of the sulfided catalysts

Catalysts	Mo ⁴⁺		Mo ⁵⁺		Mo ⁶⁺		Mo _{sulfidity} ^[a]
	ar.%	ar.%	ar.%	ar.%	ar.%	ar.%	
	(228.6 ev)	(231.7 ev)	(230.1 ev)	(233.2 ev)	(232.5 ev)	(235.6 ev)	
NiMo/ZrAT-100	34.5	23.0	6.8	4.5	18.8	12.5	57.5
NiMo/ZrAT-50	32.6	21.7	5.9	4.0	21.4	14.4	54.3
NiMo/ZrAT-25	31.9	21.3	11.1	7.4	17.1	11.4	53.2
NiMo/ZrAT-10	28.5	19.0	7.1	4.7	24.4	16.3	47.5
NiMo/ZrAT-5	26.5	17.7	2.9	1.9	30.6	20.4	44.2
NiMo/AT	15.3	10.2	18.6	12.4	26.1	17.4	25.5

^[a] $S_{Mo} = Mo^{4+} / Mo_{total}$

Table S4. XPS fitting results of Ni 2p spectra of the sulfided catalysts

Catalysts	Wt% _{ZrO2}	NiMoS ar.%	NiS ar.%	NiO ar.%	Ni _{sulfidity} ^[a]
NiMo/ZrAT-100	2.4	58.8	11.1	30.1	69.9
NiMo/ZrAT-50	4.6	53.7	12.1	34.2	65.8
NiMo/ZrAT-25	8.8	49.7	14.1	36.2	63.8
NiMo/ZrAT-10	19.5	39.8	14.3	45.9	54.1
NiMo/ZrAT-5	32.6	39.3	12.8	47.9	52.1
NiMo/AT	0	36.8	13.4	49.8	50.2

^[a] $Ni_{sulfidity} = (NiMoS + NiS_x) / Ni_{total}$

S8. HRTEM

Table S5. Average length and average layer number of MoS₂ crystallites

Catalyst	L_{av} (nm)	N_{av}	f_{Mo}
NiMo/AT	3.39	2.26	0.30
NiMo/ZrAT-100	3.11	2.50	0.35
NiMo/ZrAT-50	3.18	2.65	0.34
NiMo/ZrAT-25	3.22	2.67	0.33
NiMo/ZrAT-10	3.29	2.89	0.30
NiMo/ZrAT-5	3.35	3.02	0.28

S9. Py-FTIR

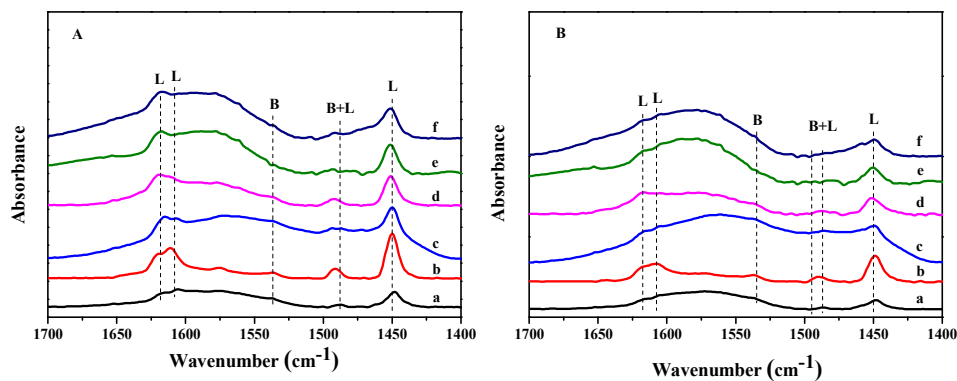


Figure S8. The pyridine IR spectra of (a) NiMo/AT, (b) NiMo/ZrAT-100, (c) NiMo/ZrAT-50, (d) NiMo/ZrAT-25, (e) NiMo/ZrAT-10, and (f) NiMo/ZrAT-5 after degassing at (A) 473 K and (B) 623 K

Table S6. The amounts of Brønsted and Lewis acid determined by pyridine-FT-IR of the different catalysts

Catalysts	473 K				623 K			
	Acid sites (μmol g ⁻¹)				Acid sites (μmol g ⁻¹)			
	B	L	L+B	B/L	B	L	L+B	B/L
NiMo/ZrAT-5	2.43	41.57	44.00	0.058	1.00	17.90	18.90	0.056
NiMo/ZrAT-10	2.80	42.86	45.66	0.065	1.10	18.31	19.41	0.060
NiMo/ZrAT-25	3.30	44.80	48.10	0.074	1.20	18.91	20.11	0.063
NiMo/ZrAT-50	3.41	47.20	50.61	0.072	1.41	22.11	23.52	0.064
NiMo/ZrAT-100	4.00	55.47	59.47	0.072	2.02	23.38	25.40	0.086
NiMo/AT	0.88	24.86	25.74	0.035	0.55	7.91	8.46	0.069

S10. Hydrotreating performance of FCC diesel

Table S7. The typical property of diesel feedstock

Properties	Data
Density @ 293K, kg·cm ⁻³	0.87
N, µg·ml ⁻¹	640.3
S, µg·ml ⁻¹	1013
cetane number	37.7
Hydrocarbon type	
Saturated hydrocarbon (v%)	39.3
Arene (v%)	49.0
Olefin (v%)	11.7
Engler Distillation (K)	
IBP	417
5%	450
10%	464
30%	488
50%	513
70%	545
90%	583
95%	598
FBP	599

Note: IBP & FBP are the abbreviations of initial boiling point final boiling poi

Table S8. Textual properties of NiMo/ γ -Al₂O₃ catalyst

Catalyst	S _{BET} (m ² g ⁻¹)	V _{BJH} (cm ³ g ⁻¹)	Pore diameter (nm)
NiMo/ γ -Al ₂ O ₃	167	0.30	8.3
NiMo/Zr-SBA-15	447	0.72	9.6

Table S9. Acid properties of NiMo/ γ -Al₂O₃ catalyst

Catalysts	473 K			623 K		
	Acid sites (μmol g ⁻¹)			Acid sites (μmol g ⁻¹)		
	B	L	L+B	B	L	L+B
NiMo/ γ -Al ₂ O ₃	0	80	80	0	26	26

Table S10. HDS activities of NiMo/ZrAT-x series catalysts

Catalysts ^[1]	ZrO ₂ , wt%	Sulfur content (mg•L ⁻¹)	HDS (%)	Nitrogen content (mg•L ⁻¹)	HDN (%)
NiMo/ZrAT-5	32.6	24.9	97.5	26.7	95.8
NiMo/ZrAT-10	19.5	22.4	97.8	20.8	96.7
NiMo/ZrAT-25	8.8	16.8	98.3	15.5	97.6
NiMo/ZrAT-50	4.6	11.9	98.8	10.7	98.3
NiMo/ZrAT-100	2.4	8.6	99.1	8.5	98.7
NiMo/AT	-	38.2	96.2	37.8	94.1
NiMo/ γ -Al ₂ O ₃	-	57.0	94.4	41.7	93.5

^[1] Catalyst = 81 wt% supports + 15.5 wt% MoO₃ + 3.5 wt% NiO

S11. HDS results of DBT

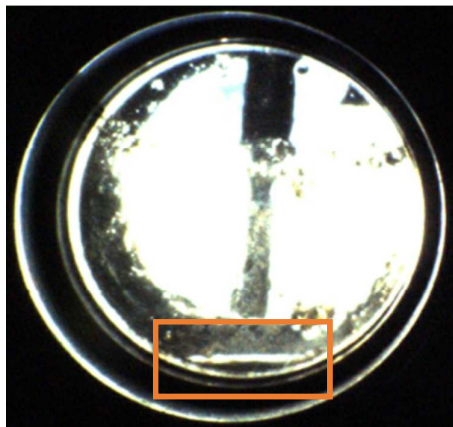


Figure S9. The phase equilibrium image of decalin under the reaction conditions

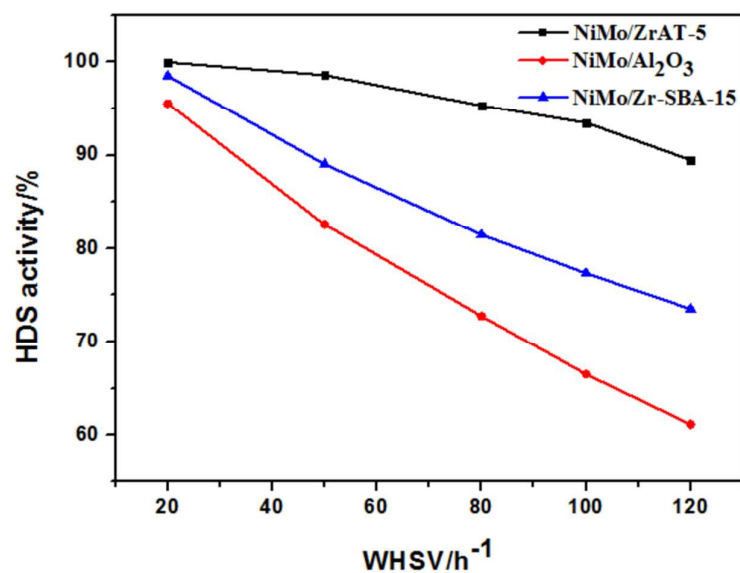


Figure S10. HDS results of NiMo/ZrAT-5 and NiMo/Al₂O₃ catalysts at different WHSVs (613 K, 6 MPa, 200 ml/ml)

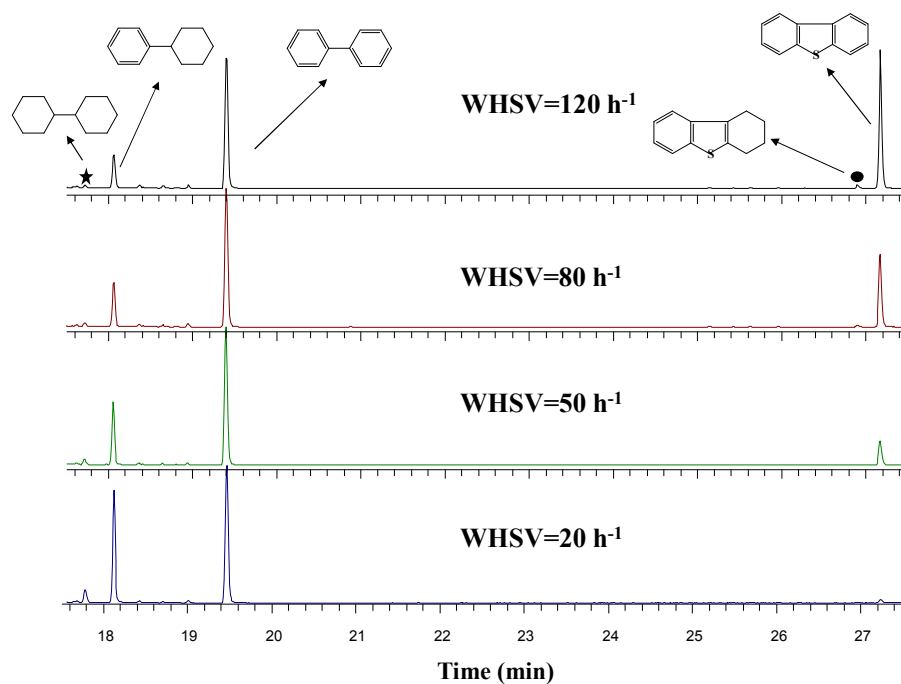


Figure S11. The product distribution in the HDS of DBT over NiMo/ZrAT-100 at different WHSVs (573 K, 6 MPa, 200 ml/ml)

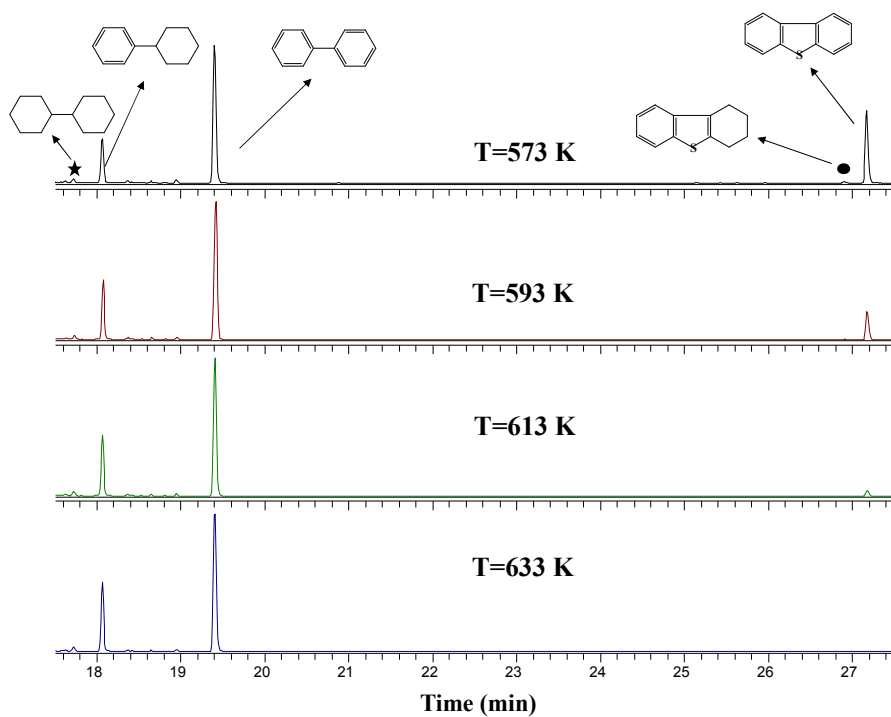


Figure S12. The product distribution in the HDS of DBT over NiMo/ZrAT-100 at different temperatures (100 h⁻¹, 6 MPa, 200 ml/ml)

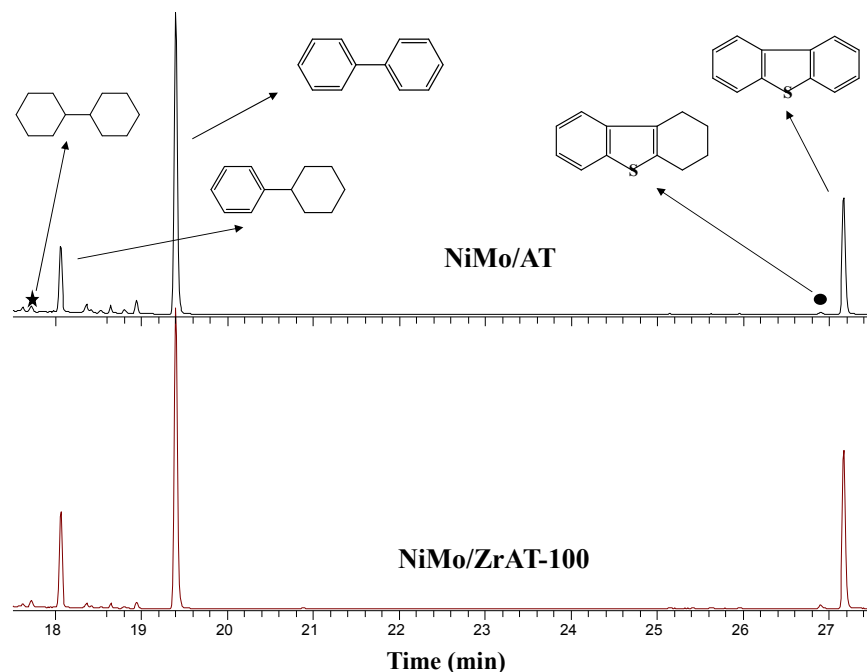


Figure S13. The product distributions in the HDS of DBT over different catalysts at about 50 % of the total DBT conversion.

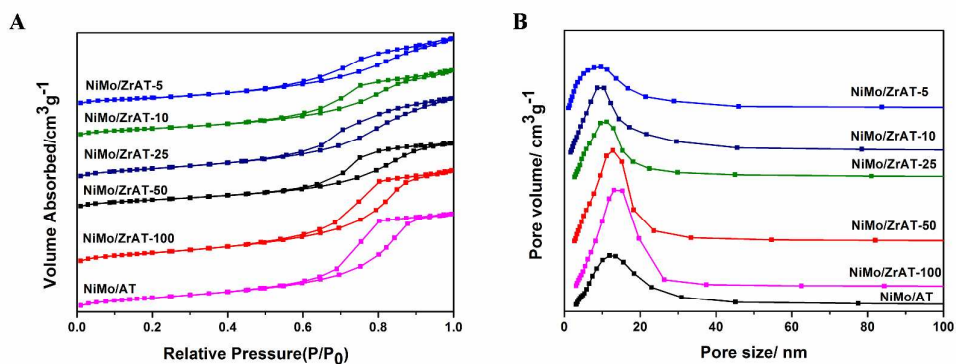


Figure S14. N₂ isotherm curves (A) and pore size distributions (B) of the used NiMo/ZrAT-x catalysts

Table S11. Textural properties of the used NiMo/ZrAT-x catalysts

Materials	Weight percentage of ZrO ₂ (%)	Al/Zr	S _{BET} (m ² g ⁻¹)	V _{BJH} (cm ³ g ⁻¹)	Pore diameter (nm)
NiMo/ZrAT-5	32.6	5	197	0.25	8.2
NiMo/ZrAT-10	18.5	10	208	0.29	9.4
NiMo/ZrAT-25	8.8	25	223	0.33	11.6
NiMo/ZrAT-50	4.6	50	239	0.37	13.8
NiMo/ZrAT-100	2.4	100	243	0.39	15.2

NiMo/AT	0	∞	238	0.43	12.5
---------	---	----------	-----	------	------

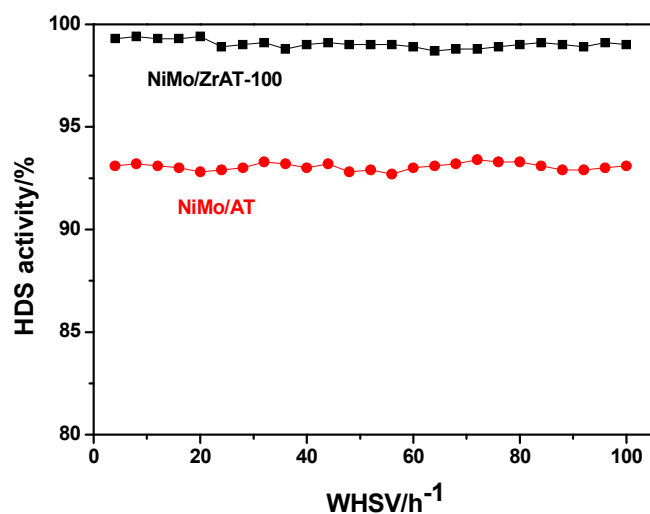


Figure S15. Time on stream over NiMo/ZrAT-100 and NiMo/AT catalysts (573 K, 6 MPa, 200

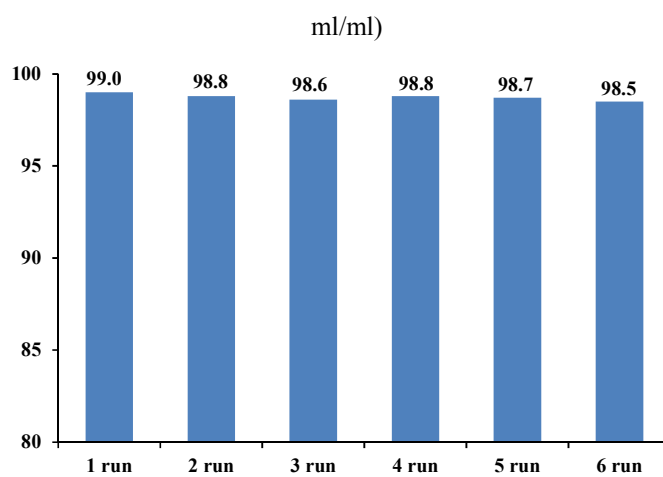


Figure S16. HDS efficiencies of NiMo/ZrAT-100 obtained at 6-run operations (20 h⁻¹, 573 K, 6 MPa, 200 ml/ml)