

SUPPORTING INFORMATION FOR

Dissociation Constants of Perchloric and Sulfuric Acids in Aqueous Solution

Alexander V. Levanov,* Oksana Ya. Isaikina, Ulkar D. Gurbanova,
Valeriy V. Lunin

Department of Chemistry, M.V. Lomonosov Moscow State University, Leninskiye
Gory 1, building 3, 119991 Moscow (Russia)

* Corresponding Author.

E-mail address: levanov@kge.msu.ru;

Fax: (+7) 495-939-4575; Phone: (+7) 495-939-3685

The Supporting Information contains:

**Brief Description of the Methods for Evaluation of Apparent Dissociation
Constants and Limiting Activity Coefficients from Reference Data, the Input
Data and Results of the Calculations**

Method No.1. The Henry's law constant K_H is computed with the expression

$$K_H = \exp\left(-\frac{1}{RT} (\Delta_f G^\circ_{298}(A^-,aq) - \Delta_f G^\circ_{298}(HA,gas))\right), \quad (19)$$

where $\Delta_f G^\circ_{298}(A^-,aq)$ and $\Delta_f G^\circ_{298}(HA,gas)$ are standard Gibbs energies of formation of A^- ions in aqueous solution and HA molecules in the gas phase at 298.15 K. Hereafter, the equation numbers in the Supporting Information are the same as in the text of the article.

The apparent dissociation constant is calculated by the formula

$$K'_a \equiv K_H \times p^*_{HA} / 55.51, \quad (17)$$

where p^*_{HA} is the saturated vapor pressure (or fugacity) of pure liquid acid HA.

Table S1. The input data and results of calculation of the apparent dissociation constants at 298.15 K using Method No.1.

HA	$\Delta_f G^\circ_{298}(HA,gas)$, kJ/mol	$\Delta_f G^\circ_{298}(A^-,aq)$, kJ/mol	K_H , mol ² kg ⁻² bar ⁻¹	p^* , bar	K'_a , mol kg ⁻¹
HClO ₄	91.37 ¹	-3.397 ¹	4.01×10^{16}	0.0471 ^{2,3}	3.40×10^{13}
HClO ₄	85.14 ⁴	-8.52 ⁵	2.57×10^{16}	0.0471 ^{2,3}	2.18×10^{13}
H ₂ SO ₄	-662.91 ¹	-756.97 ¹	3.01×10^{16}	1.88×10^{-8} ⁶	1.02×10^7
H ₂ SO ₄	-653.37 ⁷	-755.91 ⁵	9.25×10^{17}	7.58×10^{-8} ⁸	1.26×10^9

Method No.2. The apparent dissociation constant is calculated by the formula

$$K'_a = \frac{1}{55.51} \exp\left(-\frac{1}{RT} (\Delta_f G^\circ_{298}(A^-,aq) - \Delta_f G^*(HA,liq))\right). \quad (25)$$

where $\Delta_f G^\circ_{298}(A^-,aq)$ and $\Delta_f G^*(HA,liq)$ are standard Gibbs energies of formation of A^- ions in aqueous solution and pure liquid acid HA at 298.15 K.

Table S2. The input data and results of calculation of the apparent dissociation constants at 298.15 K using Method No.2.

HA	$\Delta_f G^*(HA,liq)$, kJ/mol	$\Delta_f G^\circ_{298}(A^-,aq)$, kJ/mol	K'_a , mol kg ⁻¹
HClO ₄	83.972 ¹	-3.397 ¹	3.65×10^{13}
H ₂ SO ₄	-690.29 ¹	-756.97 ¹	8.66×10^9
H ₂ SO ₄	-690 ⁵	-755.91 ⁵	6.34×10^9

Method No.3. The limiting activity coefficient is calculated by the formula

$$f_X^\infty = \frac{55.51}{H_X p^*_X}, \quad (26)$$

where H_X is the Henry's law constant of substance X, and p^*_X is the saturated vapor pressure (or fugacity) of pure substance X.

Table S3. The values of Henry's law constants ($\text{mol kg}^{-1} \text{bar}^{-1}$) for CO_2 , SO_2 , HCOOH , CH_3COOH , $\text{C}_2\text{H}_5\text{COOH}$, CF_3COOH , together with the literature references, taken from review of Sander (2015)¹⁰ and used for the calculation of the limiting activity coefficients by Method No.3.

CO_2		HCOOH
3.3×10^{-2}	Sander et al. (2011)	8800 Sander et al (2011)
3.3×10^{-2}	Sander et al. (2006)	8800 Sander et al (2006)
3.3×10^{-2}	Fernández-Prini et al. (2003)	6700 Staudinger and Roberts (2001)
3.4×10^{-2}	Carroll et al. (1991)	8800 Johnson et al (1996)
3.4×10^{-2}	Crovetto (1991)	5400 Khan et al (1995)
3.4×10^{-2}	Yoo et al. (1986)	5400 Khan and Brimblecombe (1992)
3.4×10^{-2}	Edwards et al. (1978)	1500 Hwang et al (1992)
3.3×10^{-2}	Wilhelm et al. (1977)	3700 Jacob (1986)
3.4×10^{-2}	Weiss (1974)	5500 Keene and Galloway (1986)
3.6×10^{-2}	Zheng et al. (1997)	7500 Johnson (1990)
3.5×10^{-2}	Bohr (1899)	5900 Gaffney and Senum (1984)
3.4×10^{-2}	Chen et al. (1979)	5100 Johnson et al (1996)
3.1×10^{-2}	Chameides (1984)	5100 Keene et al (1995)
3.5×10^{-2}	Scharlin (1996)	5300 Keene et al (1995)
3.4×10^{-2}	Perry and Chilton (1973)	3700 Lelieveld and Crutzen (1991)
3.4×10^{-2}	Lelieveld and Crutzen (1991)	3500 Pandis and Seinfeld (1989)
3.4×10^{-2}	Pandis and Seinfeld (1989)	CH_3COOH
4.5×10^{-2}	Yaws (1999)	4000 Sander et al. (2011)
3.3×10^{-2}	Dean (1992)	4000 Sander et al. (2006)
4.5×10^{-2}	Yaws and Yang (1992)	4600 Staudinger and Roberts (2001)
3.4×10^{-2}	Seinfeld (1986)	1400 von Hartungen et al. (2004)
3.3×10^{-2}	Hoffmann and Jacob (1984)	4000 Johnson et al. (1996)
SO_2		5400 Khan et al. (1995)
1.3	Sander et al. (2011)	5400 Khan and Brimblecombe (1992)
1.3	Sander et al. (2006)	9200 Servant et al. (1991)
1.2	Yoo et al. (1986)	910 Hwang et al. (1992)
1.2	Maahs (1982)	8700 Jacob et al. (1989)
1.2	Edwards et al. (1978)	8700 Keene and Galloway (1986)
1.4	Wilhelm et al. (1977)	970 Goldstein (1982)
1.2	Johnstone and Leppla (1934)	9900 Gaffney and Senum (1984)
1.1	Terraglio and Manganelli (1967)	5100 Johnson et al. (1996)
1.2	Chameides (1984)	5200 Keene et al. (1995)
1.3	Young (1983)	8500 Keene et al. (1995)
1.2	Pandis and Seinfeld (1989)	$\text{C}_2\text{H}_5\text{COOH}$
CF_3COOH		1500 von Hartungen et al. (2004)
8900	Sander et al. (2011)	5600 Khan et al. (1995)
5700	Kutsuna and Horia (2008)	5500 Khan and Brimblecombe (1992)
8800	Bowden et al. (1996)	6100 Servant et al. (1991)
		2200 Butler and Ramchandani (1935)

Table S4. The input data and results of calculation of the limiting activity coefficients at 298.15 K using Method No.3.

X	H_X , mol kg ⁻¹ bar ⁻¹	p^*_X , bar	f_X^∞	$\lg f_X^\infty$
CO ₂	0.031 - 0.045 ¹⁰	44.3 ⁸	27.8 - 40.4	1.44 - 1.61
SO ₂	1.1 - 1.4 ¹⁰	3.98 ¹¹	9.97 - 12.7	1.00 - 1.10
HCOOH	1500 - 8800 ¹⁰	0.0567 ⁸	0.111 - 0.652	-0.954 - -0.186
CH ₃ COOH	910 - 9900 ¹⁰	0.0208 ⁸	0.270 - 2.94	-0.569 - 0.468
C ₂ H ₅ COOH	1500 - 6100 ¹⁰	5.38×10^{-3} ¹¹	1.69 - 6.88	0.228 - 0.837
CF ₃ COOH	5700 - 8900 ¹⁰	0.144 ¹¹	0.0432 - 0.0674	-1.36 - -1.17

Method No.4. The Henry's law constant H_X is computed with the expression

$$H_X = \exp\left(-\frac{1}{RT} (\Delta_f G^\circ_{298}(X, \text{aq}) - \Delta_f G^\circ_{298}(X, \text{g}))\right), \quad (27)$$

where $\Delta_f G^\circ_{298}(X, \text{aq})$ and $\Delta_f G^\circ_{298}(X, \text{g})$ are standard Gibbs energies of formation of substance X in aqueous solution and in the gas phase at 298.15 K.

The limiting activity coefficient is calculated by the formula

$$f_X^\infty = \frac{55.51}{H_X p^*_X}, \quad (26)$$

where p^*_X is the saturated vapor pressure (or fugacity) of pure substance X.

Table S5. The input data and results of calculation of the limiting activity coefficients at 298.15 K using Method No.4.

X	$\Delta_f G^\circ_{298}(X, \text{gas})$, kJ/mol	$\Delta_f G^\circ_{298}(X, \text{aq})$, kJ/mol	H_X , mol kg ⁻¹ bar ⁻¹	p^*_X , bar	f_X^∞	$\lg f_X^\infty$
CO ₂	-394.379 ¹	-386.02 ¹	3.43×10^{-2}	44.3 ⁸	36.5	1.56
CO ₂	-394.359 ⁵	-385.98 ⁵	3.40×10^{-2}	44.3 ⁸	36.8	1.57
SO ₂	-300.194 ⁵	-300.676 ⁵	1.21	3.98 ¹¹	11.5	1.06
HF	-272.809 ¹	-296.185 ¹	1.25×10^4	1.20 ⁸	3.73×10^{-3}	-2.43
HF	-273.2 ⁵	-296.82 ⁵	1.37×10^4	1.20 ⁸	3.38×10^{-3}	-2.47
HCOOH	-351.389 ¹	-372.961 ¹	6.02×10^3	0.0567 ⁸	0.163	-0.789
CH ₃ COOH	-373.61 ¹	-396.517 ¹	1.03×10^4	0.0208 ⁸	0.259	-0.586
CH ₃ COOH	-374 ⁵	-396.46 ⁵	8.61×10^3	0.0208 ⁸	0.310	-0.508
HNO ₃	-74.847 ¹	-102.845 ^{12, 13}	8.04×10^4	0.0752 ⁸	9.19×10^{-3}	-2.04
HNO ₃	-74.72 ⁵	-102.299 ^{12, 14}	6.79×10^4	0.0752 ⁸	0.0109	-1.96

Method No.5. The limiting activity coefficient is calculated by the formula

$$f_X^\infty = 55.51 \times \exp\left(-\frac{1}{RT} (\Delta_f G^*(X, \text{liq}) - \Delta_f G^\theta(X, \text{aq}))\right). \quad (29)$$

where $\Delta_f G^\theta_{298}(A^-, \text{aq})$ and $\Delta_f G^*(HA, \text{liq})$ are standard Gibbs energies of formation of A^- ions in aqueous solution and pure liquid acid HA at 298.15 K.

Table S6. The input data and results of calculation of the limiting activity coefficients at 298.15 K using Method No.5.

X	$\Delta_f G^*(X, \text{liq})$, kJ/mol	$\Delta_f G^\theta(X, \text{aq})$, kJ/mol	f_X^∞	$\lg f_X^\infty$
HCOOH	-362.2^1	-372.961^1	0.723	-0.141
HCOOH	-361.35^5	-372.3^5	0.670	-0.174
CH ₃ COOH	-389.358^1	-396.517^1	3.09	0.490
CH ₃ COOH	-389.9^5	-396.46^5	3.94	0.595
H ₃ PO ₄	-1119.107^1	-1136.54^1	0.0490	-1.31
H ₃ PO ₄	-1119.1^5	-1142.54^5	4.34×10^{-3}	-2.36
HNO ₃	-80.843^1	$-102.845^{12, 13}$	7.76×10^{-3}	-2.11
HNO ₃	-80.71^5	$-102.299^{12, 14}$	9.17×10^{-3}	-2.04

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