

Supporting Information

Selective Electrochemical Production of Formate from Carbon Dioxide with Bismuth-Based Catalysts in an Aqueous Electrolyte

*Chan Woo Lee,^{†,§} Jung Sug Hong,[†] Ki Dong Yang,[†] Kyoungsuk Jin,[†] Jun Ho Lee,[†] Hyo-Yong Ahn,[†]
Hongmin Seo,[†] Nark-Eon Sung,[‡] and Ki Tae Nam^{*,†}*

*[†]Department of Materials Science and Engineering, Seoul National University, Seoul 151-744,
Korea*

*[‡]Pohang Accelerator Laboratory, Pohang University of Science and Technology, Pohang, 37673,
Republic of Korea*

*[§]Clean Energy Research Center, Korea Institute of Science and Technology (KIST), 5 Hwarang-ro
14-gil, Seongbuk-gu, Seoul 02792, Republic of Korea*

**Correspondence to: nkitae@snu.ac.kr*

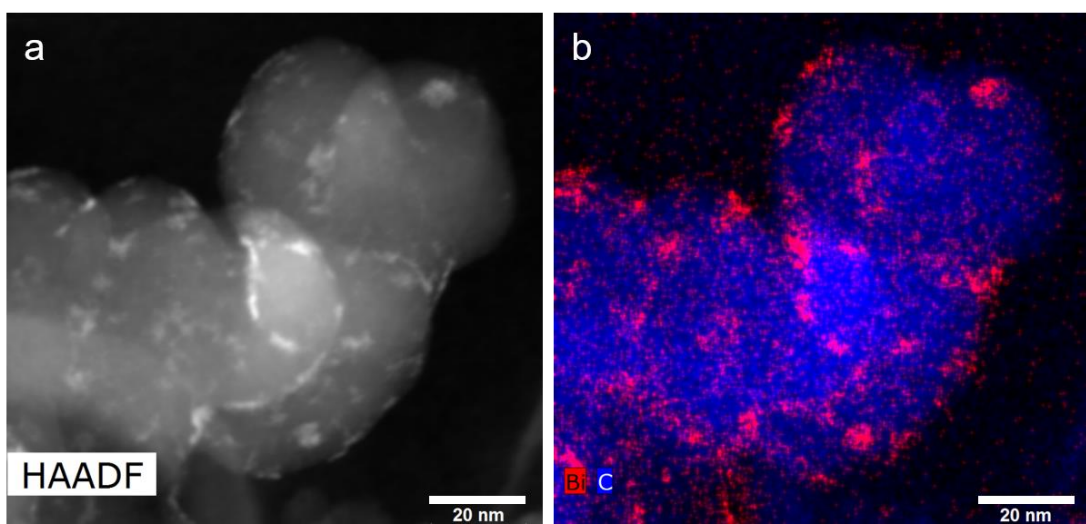


Figure S1. (a) STEM image and (b) EDS elemental mapping of the synthesized BiO_x/C .

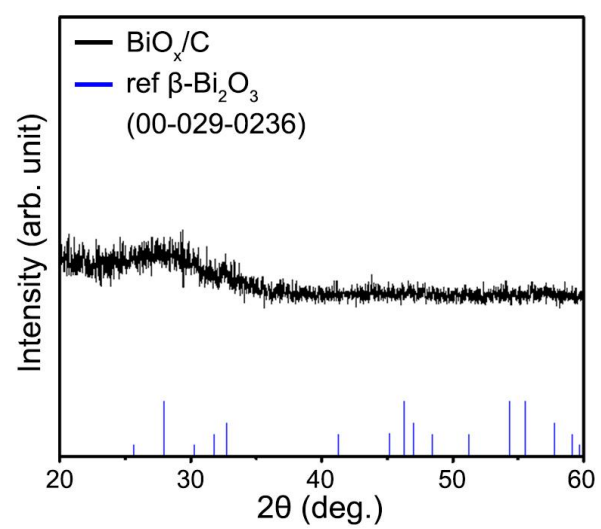


Figure S2. The XRD patterns of the synthesized BiO_x/C.

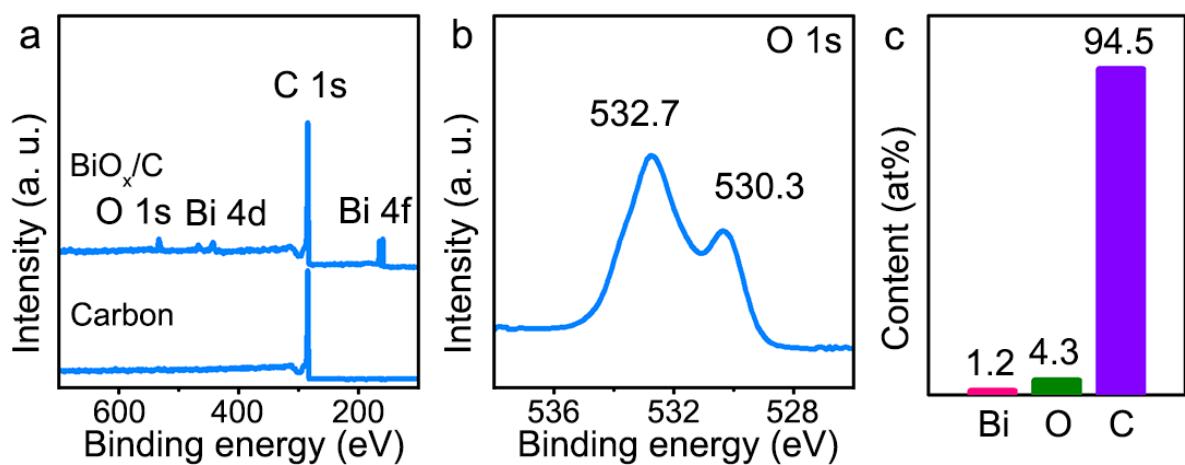


Figure S3. (a) Survey XPS and (b) O 1s spectra of the BiO_x/C. (c) Atomic percentages of Bi, O, and C measured by XPS.

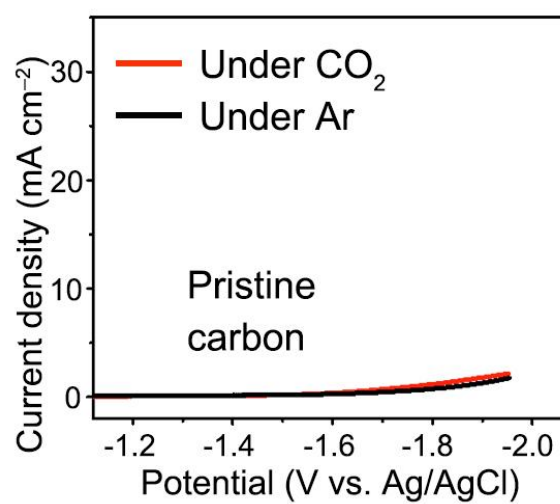


Figure S4. Cathodic linear sweep voltammetric scans of carbon black on glassy carbon plate electrode at 50 mV s⁻¹ in 0.5 M NaHCO₃/0.5 M NaClO₄ under CO₂ and Ar.

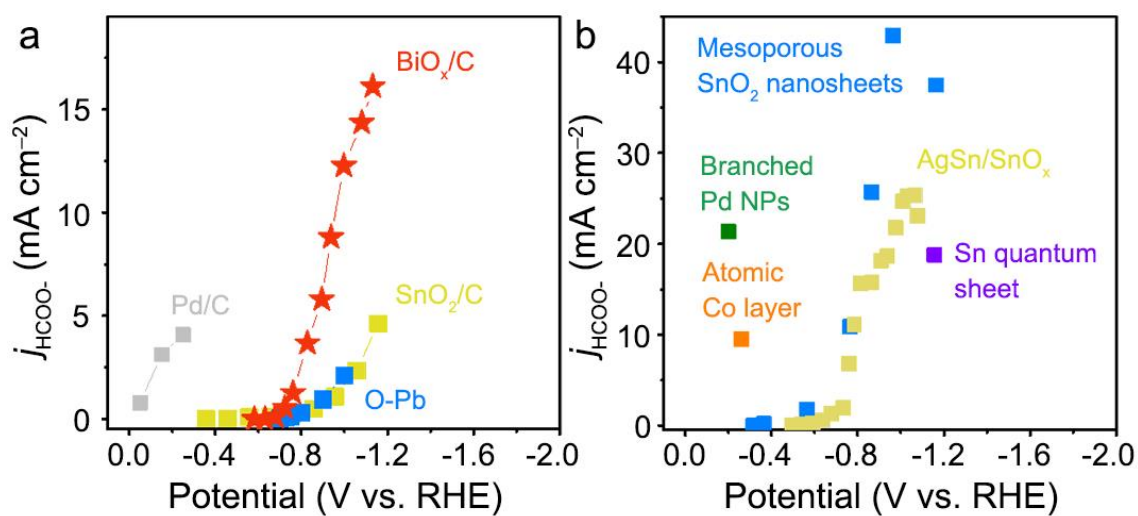


Figure S5. Comparison with reported HCOO^- catalysts. Data of the reported catalysts were extracted or collected from the previous literatures. The Figure S5(a) includes Pd/C, SnO₂/C and PbO₂ particle film for the comparison. The Figure S5(b) includes the current state of the art catalysts for HCOO^- production.

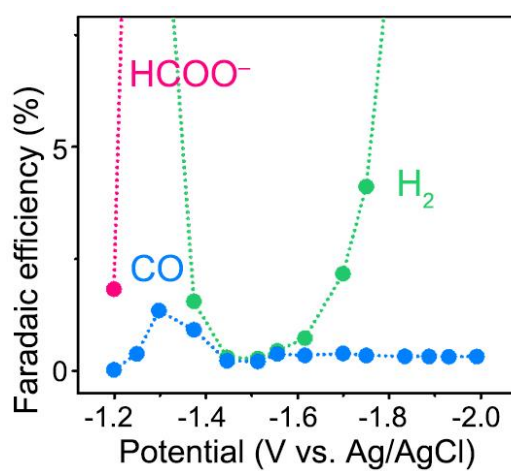


Figure S6. An enlarged view of potential dependence of faradaic efficiencies for HCOO⁻, H₂ and CO production.

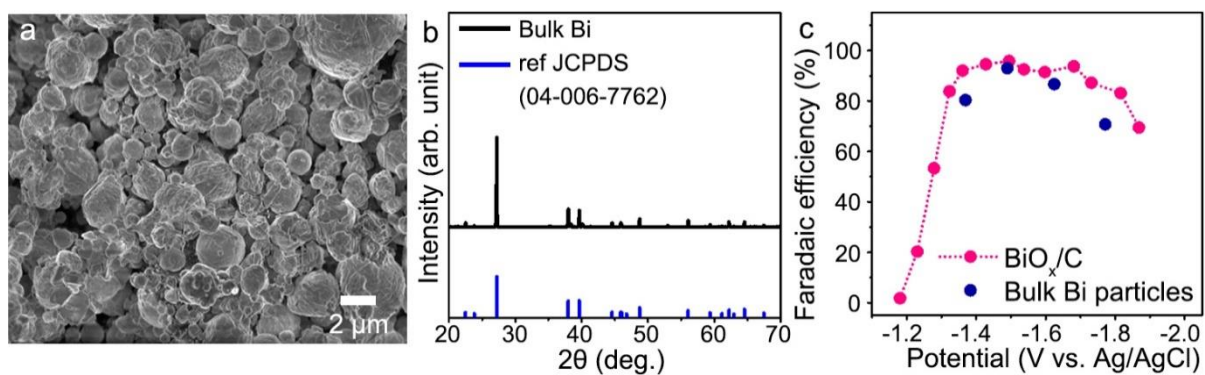


Figure S7. (a) Typical FESEM images and (b) XRD patterns of bulk Bi particles. (c) The faradaic efficiency of bulk Bi particles for HCOO^- at various potentials.

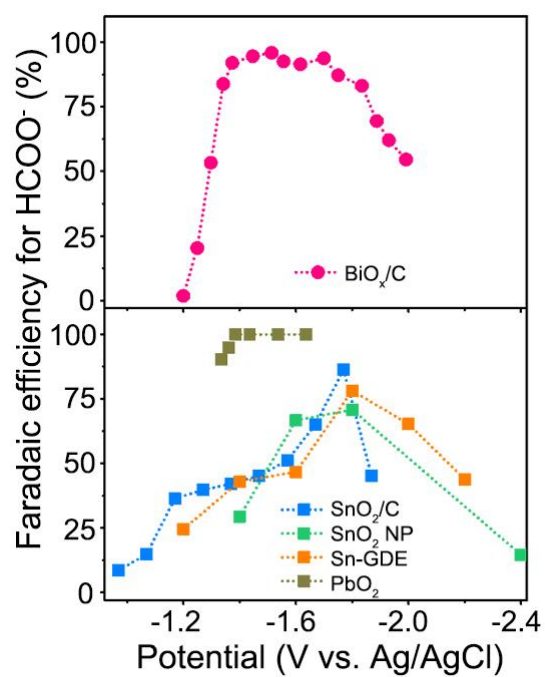


Figure S8. Potential dependence of faradaic efficiency for HCOO^- and comparison with SnO_2/C , SnO_2 NP, Sn-GDE and PbO_2 . Data were extracted or collected from the previous literatures.

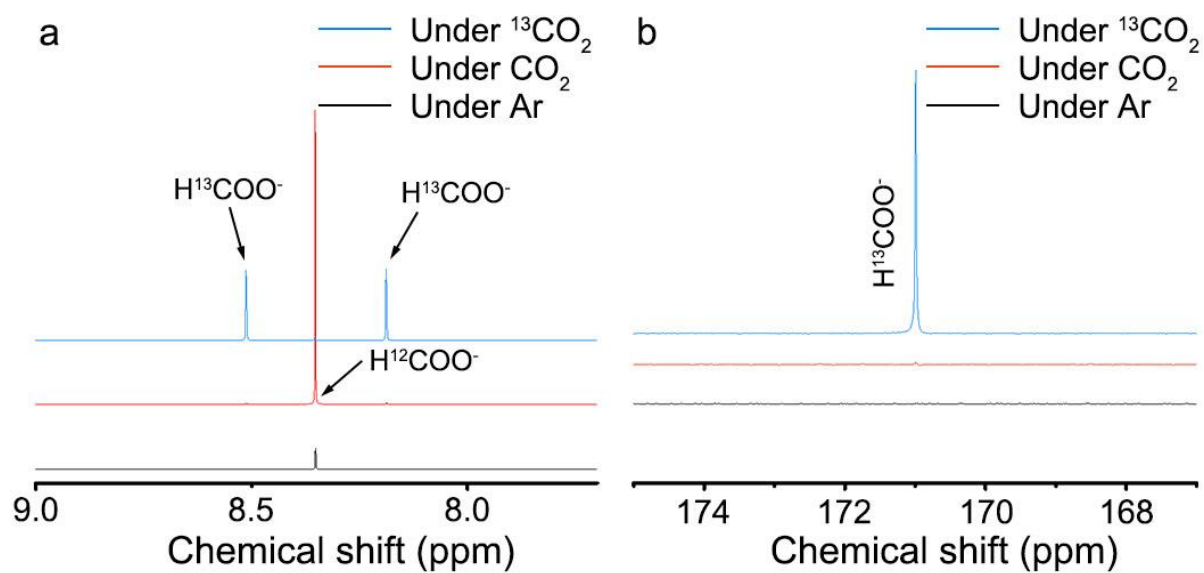


Figure S9. (a) ^1H NMR and (b) ^{13}C NMR spectra of the resultant solutions after bulk electrolysis at -1.51 V vs. Ag/AgCl under CO_2 , Ar and $^{13}\text{CO}_2$ flow.

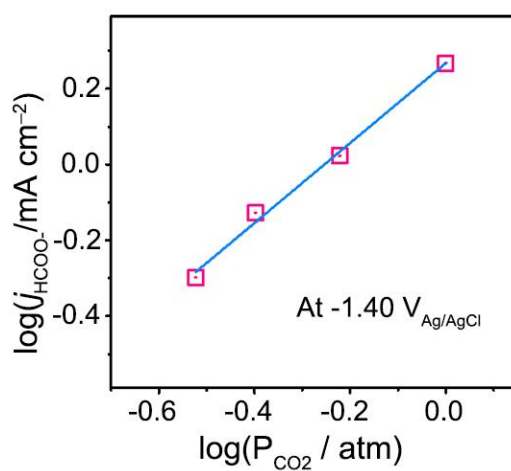


Figure S10. Plot of the partial current density for HCOO^- as a function of the CO_2 partial pressure at the fixed potential. The CO_2 partial pressure was controlled by changing the ratio of the CO_2 and Ar flows (20 cc min^{-1} in total).

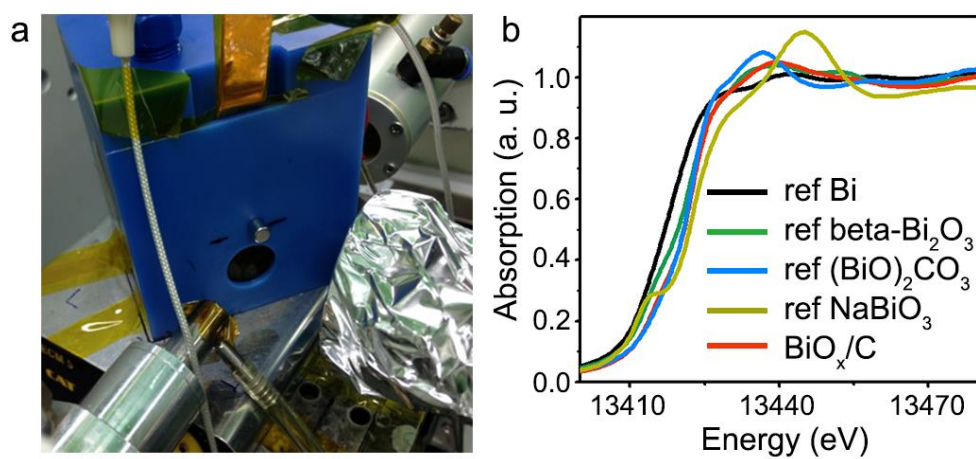


Figure S11. (a) A picture of in situ XANES cell. (b) Normalized Bi L₃-edge XANES spectra of reference Bi, β -Bi₂O₃, Bi₂O₂CO₃, NaBiO₃ and BiO_x/C.

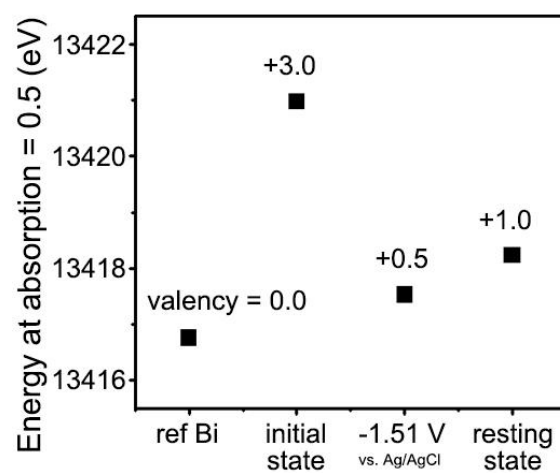


Figure S12. Average Bi valencies of Bi metal and BiO_x/C at the initial state, -1.51 V vs. Ag/AgCl and resting state.

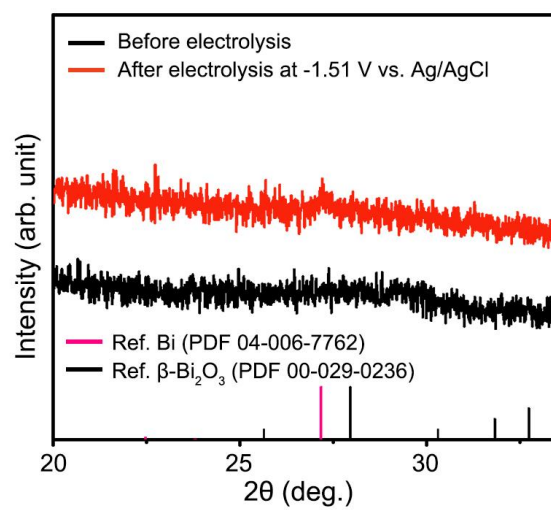


Figure S13. XRD patterns of BiO_x/C before and after electrolysis at -1.51 V vs. Ag/AgCl . Bar graphs at the bottom represent the referenced XRD patterns of Bi metal (pink) and $\beta\text{-Bi}_2\text{O}_3$ (black).

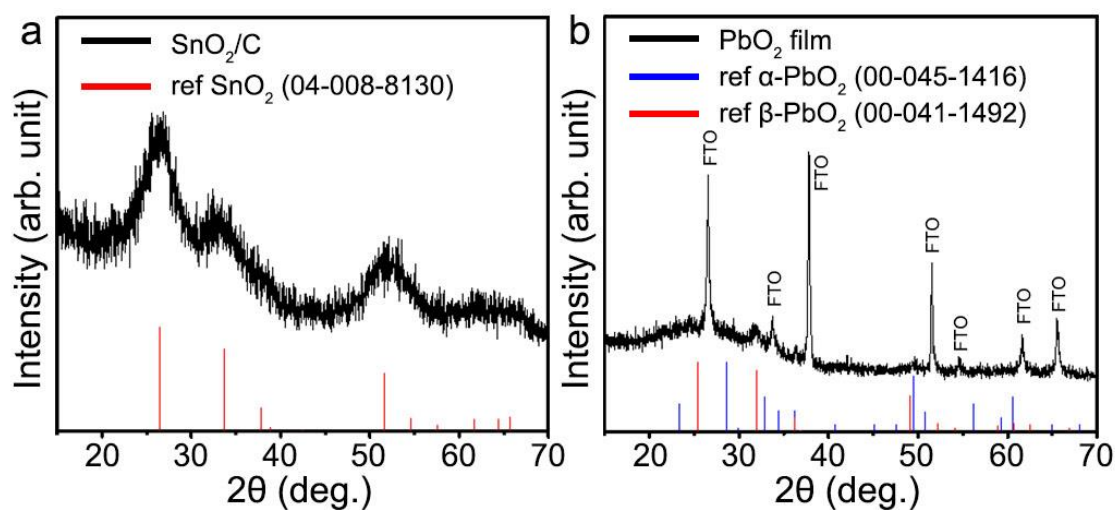


Figure S14. XRD patterns of (a) SnO₂/C powder and (b) PbO₂ film which were synthesized using the experimental methods reported from previous literatures. For XRD analysis, the PbO₂ film was electrodeposited on FTO glass. Bar graphs at the bottom represent the referenced XRD patterns of SnO₂, α-PbO₂ and β-PbO₂.

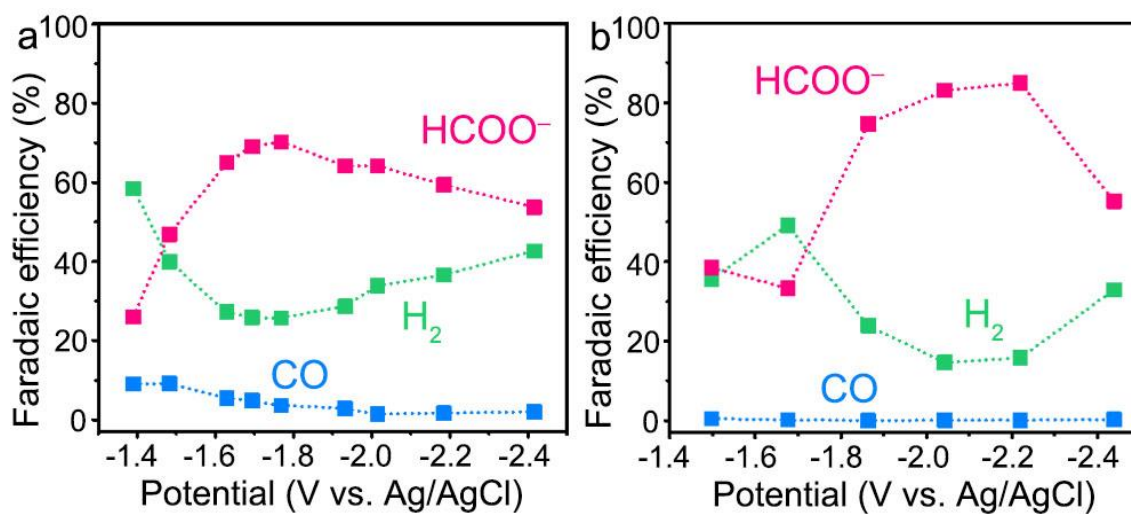


Figure S15. Potential dependence of Faradaic efficiencies for HCOO^- , H_2 , and CO production in CO_2 -saturated $0.1 \text{ M NaHCO}_3/0.9 \text{ M NaClO}_4$ on (a) SnO_2/C and (b) PbO_2 film electrodes. The SnO_2/C was dispersed in ethanol with Nafion and drop-coated on a glassy carbon plate. The PbO_2 film was directly electrodeposited on a glassy carbon plate electrode.

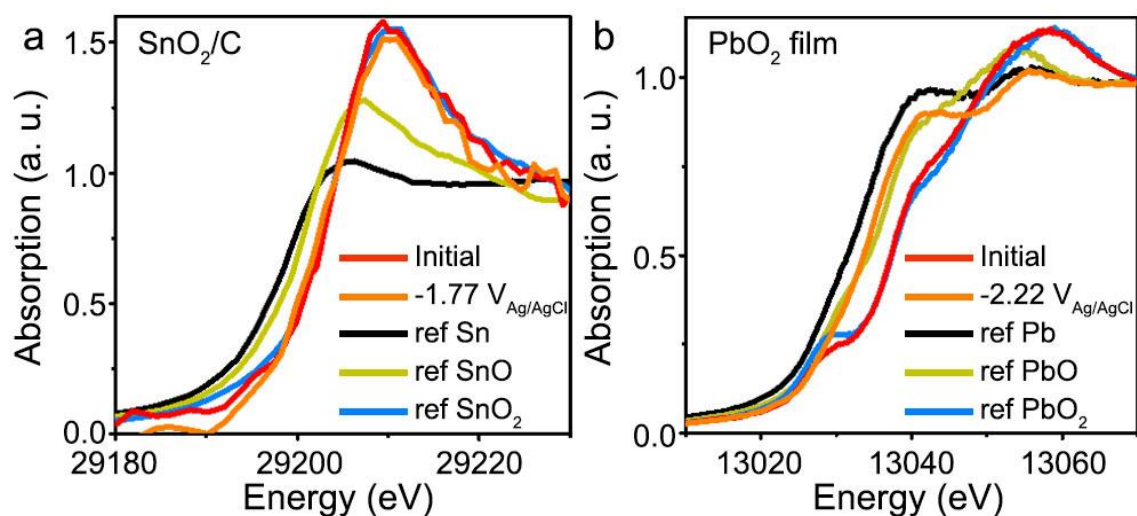


Figure S16. (a) Normalized Sn K-edge XANES spectra of ref Sn, ref SnO, ref SnO_2 , and SnO_2/C at the initial state and -1.77 V vs. Ag/AgCl . (b) Normalized Pb L3-edge XANES spectra of ref Pb, ref PbO, ref PbO_2 , and PbO_2 film at the initial state and -2.22 V vs. Ag/AgCl . The electrolysis was conducted at the potentials achieving a maximum faradaic efficiency for HCOO^- .

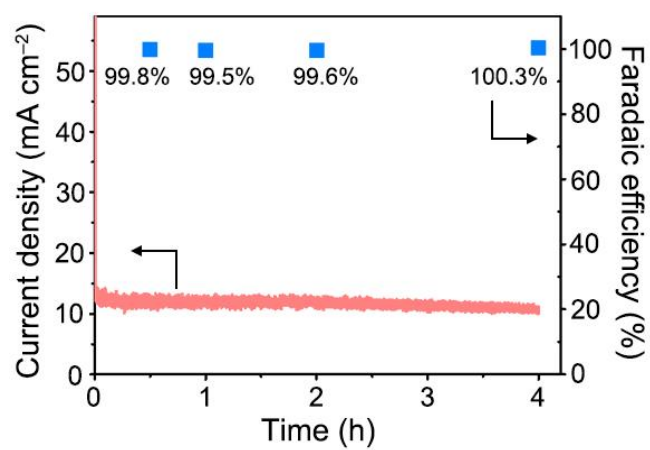


Figure S17. Total current densities and Faradaic efficiencies for HCOO^- as a function of time at -1.65 V vs. Ag/AgCl in 0.5 M NaCl.

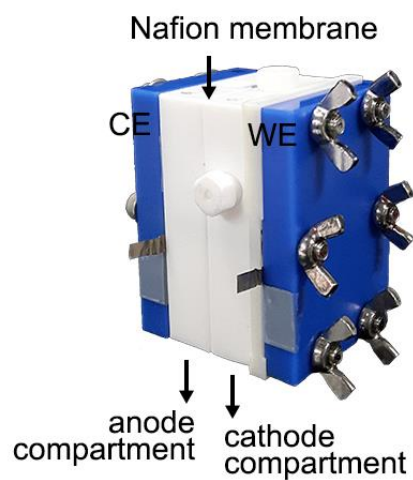


Figure S18. A picture of CO₂ reduction cell used in this study. The cell consists of cathode and anode compartments with a piece of Nafion membrane. The working and counter electrodes are inserted between white and blue plates. The separator is inserted between two compartments.